

# TECHNICAL NOTE

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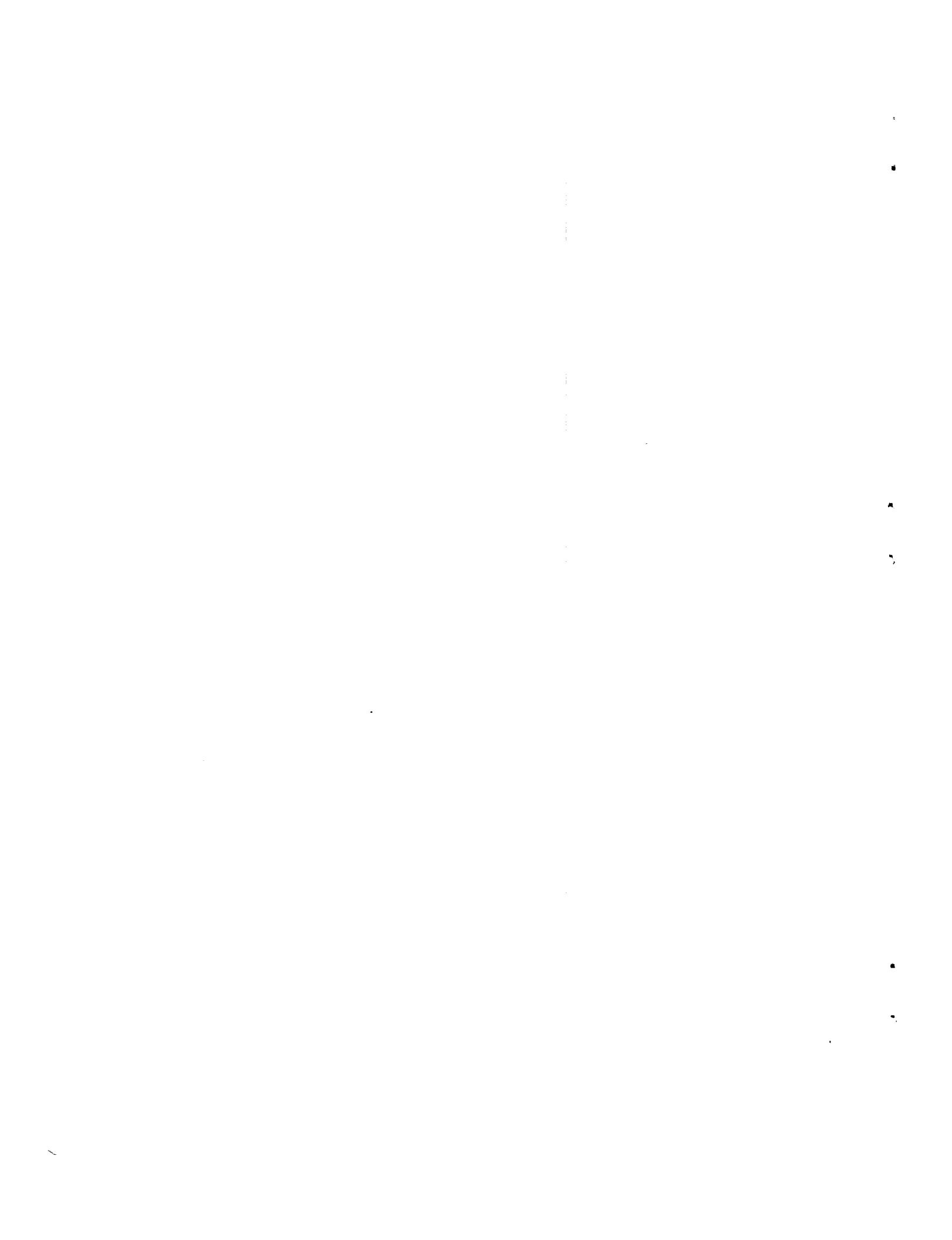
A GENERAL METHOD FOR AUTOMATIC COMPUTATION OF  
EQUILIBRIUM COMPOSITIONS AND THEORETICAL  
ROCKET PERFORMANCE OF PROPELLANTS

By Sanford Gordon, Frank J. Zeleznik, and Vearl N. Huff

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Figure 2, page 138: The second term of  $\Delta \ln T$  for "Enthalpy" should be  $\sum (H_T^0)_i q_i p_i$ .

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Figure 3, page 139: The terms in the column headings should be (a change in mathematical sign)

$-\left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P$ ,  $-\left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P$ ,  $-\left(\frac{\partial \ln p_X}{\partial \ln T}\right)_P$ ,  $-\left(\frac{\partial n_M}{\partial \ln T}\right)_P$ ,  $-\left(\frac{\partial n_N}{\partial \ln T}\right)_P$ , and  $+\left(\frac{\partial \ln A}{\partial \ln T}\right)_P$ .

Page 71, cards 464, 470, 471, and 474: TEMPO and 9059 should be TEM 1 and 9049, respectively.



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NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

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A GENERAL METHOD FOR AUTOMATIC COMPUTATION OF EQUILIBRIUM COMPOSITIONS

AND THEORETICAL ROCKET PERFORMANCE OF PROPELLANTS

By Sanford Gordon, Frank J. Zeleznik, and Vearl N. Huff

SUMMARY

A general computer program for chemical equilibrium and rocket performance calculations was written for the IBM 650 computer with 2000 words of drum storage, 60 words of high-speed core storage, indexing registers, and floating point attachments. The program is capable of carrying out combustion and isentropic expansion calculations on a chemical system that may include as many as 10 different chemical elements, 30 reaction products, and 25 pressure ratios. In addition to the equilibrium composition, temperature, and pressure, the program calculates specific impulse, specific impulse in vacuum, characteristic velocity, thrust coefficient, area ratio, molecular weight, Mach number, specific heat, isentropic exponent, enthalpy, entropy, and several thermodynamic first derivatives.

INTRODUCTION

Almost the entire work involved in the calculation of theoretical performance of propellants is in the determination of the equilibrium composition and temperature of the reaction products. The difficulty in determining equilibrium compositions, especially where many reaction products are involved, is due to the fact that the necessary equations for their solution are not simultaneously linear; and hence, in general, a direct solution is not feasible.

In recent years, a number of articles have appeared in the literature dealing with equilibrium calculations for complex mixtures that describe various systematic iterative techniques for obtaining equilibrium compositions (e.g., refs. 1 to 22). With the increasing availability of high-speed digital computers, a number of programs have been prepared to solve for equilibrium compositions automatically (e.g., refs. 13, 16, and 19 to 22).

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The present report presents a completely general method programmed for the IBM 650 data processing system with 2000 words of drum storage, 60 words of high-speed core storage, index registers, floating decimal-point attachment, and alphabetic device. This program can handle any chemical system within certain limitations set by the storage capacity of the IBM 650. The program is based essentially on the method described in reference 9; however, some modifications have been made. The program was prepared during 1957 and has been in operation since January 1958.

## EQUATIONS DEFINING ADIABATIC COMBUSTION AND ISENTROPIC EXPANSION

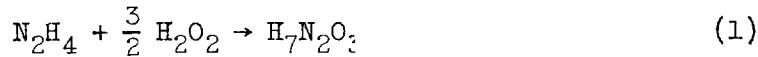
The computer program described in this report is primarily concerned with the calculation of theoretical rocket performance of chemical propellants. This calculation is simple and straightforward once the temperature and composition of the reaction products are known at combustion and exit points in the nozzle. The temperature and composition following a process such as adiabatic combustion at constant pressure or isentropic expansion to an assigned pressure can be determined from an appropriate combination of equations describing the conservation of atomic species, chemical equilibrium, Dalton's law of partial pressures, and the conservation of enthalpy or entropy. Since these equations do not constitute a set of linear equations, they must usually be solved by some iterative technique.

### Combustion at Constant Pressure

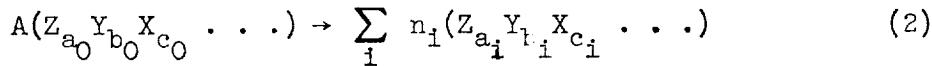
For given initial conditions, the temperature and composition following a combustion process are to be found. The substances entering into the reaction may be represented by an equivalent formula

$$Z_{a_0} Y_{b_0} X_{c_0} \dots$$

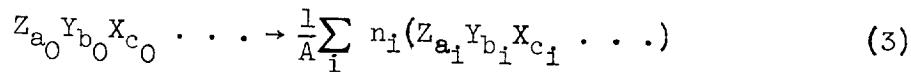
where  $a_0, b_0, c_0, \dots$  are proportional to the total number of gram atoms of the elements Z, Y, X, ... in the reaction mixture. (A complete list of symbols is given in appendix A.) For example,



The reaction at equilibrium may be written as



or



where  $A$  is the number of formula weights of the equivalent reactant, and  $n_i$  is the number of moles of the  $i^{\text{th}}$  molecule or atom.

With this representation of the reaction, the equations involving mass conservation, chemical equilibria, pressure, and enthalpy may be written as follows.

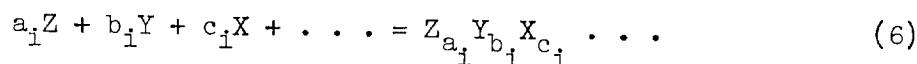
Conservation of mass. - Equations defining the relative amounts of each element in the reaction products may be written as follows:

$$\left. \begin{aligned} a &= \frac{1}{A} \sum_i a_i n_i \\ b &= \frac{1}{A} \sum_i b_i n_i \\ c &= \frac{1}{A} \sum_i c_i n_i \\ \dots &= \dots \end{aligned} \right\} \quad (4)$$

where  $a, b, c, \dots$  are the number of gram atoms of substance  $Z, Y, X, \dots$  per equivalent formula required to form the reaction products. For the reaction of equation (3), conservation of mass is defined by the following relations:

$$\left. \begin{aligned} a &= a_0 \\ b &= b_0 \\ c &= c_0 \\ \dots &= \dots \end{aligned} \right\} \quad (5)$$

Chemical-equilibrium equations. - For convenience in handling the equations, each reaction product can be considered as being formed from the gaseous atoms as follows:



The change in free energy across reaction (6),  $(\Delta F)_i$ , in terms of activities  $\alpha$  is given by the relation

$$(\Delta F)_i = (\Delta F^\circ)_i + RT(\ln \alpha_i - a_i \ln \alpha_Z - b_i \ln \alpha_Y - c_i \ln \alpha_X - \dots) \quad (7)$$

where  $(\Delta F^\circ)_i$  is the standard-state free-energy change across the reaction.

For gaseous reaction products, the standard state, or the state of unit activity, is usually taken to be the ideal gas at 1-atmosphere pressure. This choice of standard state makes the activity and the fugacity numerically equal. If, furthermore, all the gaseous reaction products are assumed to behave ideally, then the fugacity and partial pressure are identical. In this case, dividing by  $RT$  and using the symbol  $\delta$  for  $\Delta F/RT$ , equation (7) may be written as

$$\delta_i = \left( \frac{\Delta F^\circ}{RT} \right)_i + \ln p_i - (a_i \ln p_Z + b_i \ln p_Y + c_i \ln p_X + \dots) \quad (8)$$

The criterion for equilibrium for a reaction at constant temperature and pressure is that  $\Delta F$  (or  $\delta_i$ ) be equal to zero; that is,

$$\left( \frac{\Delta F^\circ}{RT} \right)_i + \ln p_i - (a_i \ln p_Z + b_i \ln p_Y + c_i \ln p_X + \dots) = 0 \quad (9)$$

In this report, a condensed phase is assumed to be a pure solid or liquid, excluding the possibility of solid or liquid solutions. The activity for a condensed phase is conventionally taken to be unity for the pure solid or liquid at 1-atmosphere pressure. At moderate pressures the activity of the condensed phase is essentially the same as in the standard state, and hence the equilibrium relation for the formation of the condensed product  $Z_{a_N} Y_{b_N} X_{c_N} \dots$  from the gaseous atoms may be written as

$$\delta_N = \left( \frac{\Delta F^\circ}{RT} \right)_N - (a_N \ln p_Z + b_N \ln p_Y + c_N \ln p_X + \dots) \quad (10)$$

Similar expressions may be written for other condensed products,  $Z_{a_M} Y_{b_M} X_{c_M} \dots$ , and so forth. At equilibrium conditions  $\delta_N, \delta_M, \dots$  are equal to zero; that is,

$$\left. \begin{aligned} \left( \frac{\Delta F^\circ}{RT} \right)_N - (a_N \ln p_Z + b_N \ln p_Y + c_N \ln p_X + \dots) &= 0 \\ \dots &= 0 \end{aligned} \right\} \quad (11)$$

Dalton's law of partial pressures. - The static pressure of the system is the sum of the partial pressures of the gaseous products:

$$P = \sum_i p_i \quad (12)$$

If a process has an assigned pressure  $P_0$ , then

$$P = P_0 \quad (13)$$

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In this report, it is assumed that the gases at combustion conditions have zero velocity; and hence, in the combustion chamber, static pressure is equal to the total pressure.

Conservation of enthalpy. - Adiabatic combustion is a constant-enthalpy process; and hence, if chemical energy is included in the enthalpy of each substance, the enthalpy of the products of reactions must equal the enthalpy of the reactants.

Since only differences in enthalpy are involved, an arbitrary base may be adopted for assigning absolute values to the enthalpy of various substances. The molar enthalpy of a substance is defined as

$$(H_T^{\circ})_i = \int_0^T (C_P^{\circ})_i dT + (H_0^{\circ})_i \quad (14)$$

where  $(C_P^{\circ})_i$  is the molar specific heat at constant pressure, and  $(H_0^{\circ})_i$  is the assigned reference enthalpy at  $0^{\circ}$  K of the  $i^{\text{th}}$  substance.

If the enthalpy of the reactants per formula weight of the equivalent formula  $Z_{a_0} Y_{b_0} X_{c_0} \dots$  is  $H_0$ , then

$$H_0 = \sum_i n_{f_i} (H_T^{\circ})_{f_i} + \sum_i n_{x_i} (H_T^{\circ})_{x_i} \quad (15)$$

where  $n_{f_i}$  and  $n_{x_i}$  are the moles of the  $i^{\text{th}}$  fuel and  $i^{\text{th}}$  oxidant corresponding to equivalent formula  $Z_{a_0} Y_{b_0} X_{c_0} \dots$ , and  $(H_T^{\circ})_{f_i}$  and  $(H_T^{\circ})_{x_i}$  are the molar enthalpies of the  $i^{\text{th}}$  fuel and  $i^{\text{th}}$  oxidant, respectively.

The enthalpy of the combustion products per equivalent formula of reactants may be written as

$$H = \frac{1}{A} \sum_i (H_T^0)_i n_i \quad (16)$$

If the  $H_T^0$  values for all substances are consistently assigned (taking into account heats of reaction and transition), then for adiabatic combustion,

$$H = H_0 \quad (17)$$

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### Isentropic Expansion to Assigned Pressure

The temperature and composition following an isentropic expansion of the combustion gases to an assigned pressure may be determined by equations for (1) conservation of atomic species, (2) chemical equilibrium, (3) the law of partial pressures, and (4) the conservation of entropy. The first three types of equations ((5), (9), (11), and (13)) have been discussed in the previous section and again apply. The fourth type is discussed herein.

The entropy of the reaction products per formula weight of the equivalent reactant is given by

$$S = \frac{1}{A} \sum_i (S_T)_i n_i \quad (18)$$

where

$$(S_T)_i = \begin{cases} (S_T^0)_i - R \ln p_i & \text{for gases} \\ (S_T^0)_i & \text{for condensed phases} \end{cases} \quad (19)$$

and  $(S_T^0)_i$  is the absolute molar entropy of the  $i^{th}$  product at temperature  $T$  in the standard state.

For an isentropic expansion following a combustion process, the entropy at any point in the expansion  $S_e$  must be equal to the value of entropy at combustion conditions  $S_c$ . If  $S_e$  is considered to be an assigned value  $S_0$ , then

$$S_e = S_c = S_0 \quad (20)$$

Summary of Equations for Adiabatic Combustion  
and Isentropic Expansion

Equations (5), (9), (11), and (13), together with equation (17) for adiabatic combustion or equation (20) for isentropic expansion, are sufficient to solve the problem of equilibrium calculations completely. However, these equations involve both the moles  $n_i$  and the partial pressures  $p_i$ . The equations can be expressed in the same variables by letting  $A$  be that number of formula weights of equivalent reactant such that, for ideal gases,

$$p_i = n_i \quad (21)$$

This is the same as saying that the reaction takes place in a volume  $V$  numerically equal to  $RT$ . Each condensed phase is considered to occupy a negligible volume with respect to the volume occupied by the gases, even when finely divided and suspended in the gas. Condensed phases are further discussed in the subsequent section on "Condensation phenomena."

ITERATION TECHNIQUE

The two sets of equations ((5), (9), (11), (13), and (17), and (5), (9), (11), (13), and (20)) are sets of nonlinear equations, and therefore it is usually not feasible to find a direct solution. The Newton-Raphson method for solving nonlinear equations (ref. 23) is well suited to this type of calculation. In this method the finite-difference approximation to the total differential serves as a basis for the iteration procedure. This method will be illustrated by a simple example.

Let  $Q_1$  and  $Q_2$  be two nonlinear functions of  $x$  and  $y$ :

$$\left. \begin{array}{l} Q_1 = Q_1(x, y) = 0 \\ Q_2 = Q_2(x, y) = 0 \end{array} \right\} \quad (22)$$

and let their simultaneous solution be  $\bar{x}, \bar{y}$ . For any other values of  $x$  and  $y$ , say  $x_i, y_i$ ,

$$\left. \begin{array}{l} Q_1(x_i, y_i) \neq Q_1(\bar{x}, \bar{y}) \\ Q_2(x_i, y_i) \neq Q_2(\bar{x}, \bar{y}) \end{array} \right\} \quad (23)$$

or

$$\left. \begin{array}{l} \Delta Q_1 = Q_1(\bar{x}, \bar{y}) - Q_1(x_i, y_i) \\ \Delta Q_2 = Q_2(\bar{x}, \bar{y}) - Q_2(x_i, y_i) \end{array} \right\} \quad (24)$$

The total differentials of (22) are

$$\left. \begin{aligned} dQ_1 &= \frac{\partial Q_1}{\partial x} dx + \frac{\partial Q_1}{\partial y} dy \\ dQ_2 &= \frac{\partial Q_2}{\partial x} dx + \frac{\partial Q_2}{\partial y} dy \end{aligned} \right\} \quad (25)$$

In finite-difference form, these become

$$\left. \begin{aligned} \Delta Q_1 &= \left( \frac{\partial Q_1}{\partial x} \right) \Delta x + \left( \frac{\partial Q_1}{\partial y} \right) \Delta y \\ \Delta Q_2 &= \left( \frac{\partial Q_2}{\partial x} \right) \Delta x + \left( \frac{\partial Q_2}{\partial y} \right) \Delta y \end{aligned} \right\} \quad (26)$$

If the difference terms  $\Delta Q_1$  and  $\Delta Q_2$  and the analytic expressions for the partial derivatives are evaluated numerically at the point  $x_i, y_i$ , the correction variables  $\Delta x$  and  $\Delta y$  can be solved for simply, since equation (26) is a simultaneous linear set of equations in the correction variables.

Because equation (26) is not exact,

$$\left. \begin{aligned} x_{i+1} &= x_i + \Delta x \neq \bar{x} \\ y_{i+1} &= y_i + \Delta y \neq \bar{y} \end{aligned} \right\} \quad (27)$$

but rather  $x_{i+1}$  and  $y_{i+1}$  will in general be a closer approximation to  $\bar{x}$  and  $\bar{y}$  than are  $x_i$  and  $y_i$ . The process of solving for corrections  $\Delta x$  and  $\Delta y$  is repeated until  $\Delta x$  and  $\Delta y$  (or  $\Delta Q_1$  and  $\Delta Q_2$ ) are sufficiently small.

#### Linear Correction Equations

Equations. - The finite-difference form of the total differential of equations (5), (9), (11), (13), (17), and (20) in terms of logarithmic correction variables is

$$\left. \begin{aligned}
 A \Delta a &= A(a_0 - a) = \sum_i a_i n_i \Delta \ln n_i - \sum_i a_i n_i \Delta \ln A \\
 A \Delta b &= A(b_0 - b) = \sum_i b_i n_i \Delta \ln n_i - \sum_i b_i n_i \Delta \ln A \\
 A \Delta c &= A(c_0 - c) = \sum_i c_i n_i \Delta \ln n_i - \sum_i c_i n_i \Delta \ln A \\
 \dots &= \dots = \dots
 \end{aligned} \right\} \quad (28)$$

$$-\delta_i = \Delta \ln p_i - (a_i \Delta \ln p_Z + b_i \Delta \ln p_Y + c_i \Delta \ln p_X + \dots) - q_i \Delta \ln T \quad (29)$$

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$$\left. \begin{aligned}
 -\delta_N &= -(a_N \Delta \ln p_Z + b_N \Delta \ln p_Y + c_N \Delta \ln p_X + \dots) - q_N \Delta \ln T \\
 \dots &= \dots
 \end{aligned} \right\} \quad (30)$$

where  $q = \frac{\Delta H_T^O}{RT} = \frac{\partial \left( -\frac{\Delta F_T^O}{RT} \right)}{\partial \ln T}$ ;

$$\Delta P = (P_0 - P) = \sum_i p_i \Delta \ln p_i \quad (31)$$

$$\begin{aligned}
 A \Delta H &= A(H_0 - H) = \sum_i (H_T^O)_i n_i \Delta \ln n_i - \sum_i (H_T^O)_i n_i \Delta \ln A \\
 &\quad + T \sum_i (C_P^O)_i n_i \Delta \ln T
 \end{aligned} \quad (32)$$

$$\begin{aligned}
 A \Delta S &= A(S_0 - S) = \sum_i (S_T)_i n_i \Delta \ln n_i - \sum_i (S_T)_i n_i \Delta \ln A \\
 &\quad + \sum_i (C_P^O)_i n_i \Delta \ln T
 \end{aligned} \quad (33)$$

where

$$(S_T)_i \begin{cases} = (S_T^0)_i - R(1 + \ln p_i) = (S_T)_i - R & \text{for gases} \\ = (S_T^0)_i & \text{for condensed phases} \end{cases} \quad (34)$$

The values for  $\Delta a$ ,  $\Delta b$ ,  $\Delta c$ , . . . ,  $(-\delta_i)$ ,  $(-\delta_N)$ , . . . ,  $\Delta P$ ,  $\Delta H$ , and  $\Delta S$  serve to indicate the error still left in the system of equations with the estimates  $n_i$ ,  $A$ , and  $T$ .

Relation between  $\delta_i$  and  $q_i$ . - For purposes of machine computation, it was found more convenient to write equations (8) and (10) in a different form. The relation

$$\left(\frac{\Delta F_T^0}{RT}\right)_i = \left(\frac{\Delta H_T^0}{RT}\right)_i - \left(\frac{\Delta S_T^0}{R}\right)_i = q_i - \left(\frac{\Delta S_T^0}{R}\right)_i \quad (35)$$

is used to eliminate  $(\Delta F_T^0/RT)_i$  in equations (8) and (10), which become

$$\delta_i = q_i - \left[ \left(\frac{S_T^0}{R}\right)_i - \ln p_i \right] + a_i \left[ \left(\frac{S_T^0}{R}\right)_Z - \ln p_Z \right] + b_i \left[ \left(\frac{S_T^0}{R}\right)_Y - \ln p_Y \right] + c_i \left[ \left(\frac{S_T^0}{R}\right)_X - \ln p_X \right] + \dots \quad (36)$$

$$\delta_N = q_N - \left[ \left(\frac{S_T^0}{R}\right)_N \right] + a_N \left[ \left(\frac{S_T^0}{R}\right)_Z - \ln p_Z \right] + b_N \left[ \left(\frac{S_T^0}{R}\right)_Y - \ln p_Y \right] + c_N \left[ \left(\frac{S_T^0}{R}\right)_X - \ln p_X \right] + \dots \quad (37)$$

#### Matrix Representation of Correction Equations

Matrix. - The augmented matrix for the combustion problem (eqs. (28) to (32)) is given in figure 1. The augmented matrix for the expansion problem is identical to that for combustion, except that equation (32) is replaced by equation (33), as indicated in the footnote in fig-ure 1. A direct elimination of the correction variables pertaining to the gaseous molecules gives a new matrix whose order is equal to the sum of the different chemical elements and condensed phases plus 2. This reduced matrix is presented as figure 2, where the correction variables for the condensed phases are linear rather than logarithmic to permit a greater symmetry in the coefficient matrix.

In figure 2 and elsewhere in this report, the symbol  $p_i$  is used in summations that include only gaseous reaction products, whereas the symbol  $n_i$  is used in summations that include condensed as well as gaseous reaction products.

Condensation phenomena. - In this report, a molecular species which appears in a condensed phase is considered to be independent of the same species in the gaseous phase. The vapor pressure is assigned completely to the gas phase, and a zero vapor pressure is assigned to the condensed phase. Two separate equilibrium equations (eqs. (8) and (10)) are written for this species, one for the gaseous phase and one for the condensed. The vapor-condensed-phase equilibrium is implicit in these two equations.

The present program is capable of considering several situations when the chemical system is such that condensed reaction products are possible. In the first situation, a condensed product is assumed to be present. After the equilibrium compositions have been determined, the assumption is checked. If correct, the program continues; if incorrect (a negative value for the amount of the condensed product), the program automatically restarts the calculations with this condensed phase excluded. In a second situation, a condensed phase is assumed to be not present. After equilibrium compositions have been determined, if the assumption is correct the program continues. If the assumption is incorrect (the partial pressure of the condensable gas exceeds the vapor pressure), the program automatically restarts the calculations with the condensed phase included.

The criterion for condensation is easily obtained from the equilibrium constant. Thus, for the reaction

$$(Z_{a_1} Y_{b_1} X_{c_1} \dots)_g = (Z_{a_N} Y_{b_N} X_{c_N} \dots)_c \quad (38)$$

where  $a_i = a_N$ ,  $b_i = b_N$ ,  $c_i = c_N \dots$ , the equilibrium constant is

$$K = \frac{K_N}{K_i} = \frac{1}{p_{vap}} = e^{-\left[ \frac{(F_T^0)_c - (F_T^0)_g}{RT} \right]} \quad (39)$$

Condensation occurs when

$$p_i \geq p_{vap} = \frac{1}{K}$$

or

$$p_i K \geq 1$$

which can be written as

$$\frac{(F_T^{\circ})_c - (F_T^{\circ})_g}{RT} - \ln p_i \leq 0 \quad (40)$$

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## THERMODYNAMIC FIRST PARTIAL DERIVATIVES

From the many thermodynamic first partial derivatives, it is possible arbitrarily to select three independent derivatives and then to express all the other possible thermodynamic first partial derivatives in terms of these three. The three thermodynamic derivatives selected for calculation in this report are  $(\partial H/\partial T)_P$ ,  $(\partial \ln M/\partial \ln T)_P$ , and  $(\partial \ln M/\partial \ln P)_T$ , where  $M$  is the molecular weight of the reaction products as defined in equation (45).

## Heat Capacity at Constant Pressure

The enthalpy of the products of reaction per equivalent formula of reactant is given by (16). Since the heat capacity per equivalent formula of reactant is  $(\partial H/\partial T)_P$ , then the heat capacity of the reaction products per mole of reaction product is

$$\frac{A}{n} \left( \frac{\partial H}{\partial T} \right)_P = C_P^{\circ} \quad (41)$$

where

$$n = \sum_i n_i$$

Differentiation of equation (16) gives an expression for  $(\partial H/\partial T)_P$  that may be used to obtain  $C_P^{\circ}$  in equation (41):

$$\begin{aligned} \left( \frac{\partial H}{\partial T} \right)_P = \frac{1}{AT} & \left[ \sum_i (H_T^{\circ})_i p_i \left( \frac{\partial \ln p_i}{\partial \ln T} \right)_P + (H_T^{\circ})_N \left( \frac{\partial n_N}{\partial \ln T} \right)_P + (H_T^{\circ})_M \left( \frac{\partial n_M}{\partial \ln T} \right)_P + \right. \\ & \left. \dots + T \sum_i (C_P^{\circ})_i r_i - \sum_i (H_T^{\circ})_i n_i \left( \frac{\partial \ln A}{\partial \ln T} \right)_P \right] \quad (42) \end{aligned}$$

Equation (42) may be written in another form that was found more convenient with the calculation method of this report. Differentiation of (9) gives the identity

$$\left( \frac{\partial \ln p_i}{\partial \ln T} \right)_P = a_i \left( \frac{\partial \ln p_Z}{\partial \ln T} \right)_P + b_i \left( \frac{\partial \ln p_Y}{\partial \ln T} \right)_P + \dots + q_i \quad (43)$$

Combining equations (41), (42), and (43) gives the following expression for  $C_P^o$ :

$$C_P^o = \frac{1}{nT} \left[ \sum_i (H_T^o)_i a_i p_i \left( \frac{\partial \ln p_Z}{\partial \ln T} \right)_P + \sum_i (H_T^o)_i b_i p_i \left( \frac{\partial \ln p_Y}{\partial \ln T} \right)_P + \dots + (H_T^o)_N \left( \frac{\partial n_N}{\partial \ln T} \right)_P + (H_T^o)_M \left( \frac{\partial n_M}{\partial \ln T} \right)_P + \dots - \sum_i (H_T^o)_i n_i \left( \frac{\partial \ln A}{\partial \ln T} \right)_P + T \sum_i (C_P^o)_i n_i + (H_T^o)_i q_i p_i \right] \quad (44)$$

A comparison of equation (44) with the last row in figure 2 shows that the coefficients of the derivatives are the elements of the enthalpy row. The solution of the partials  $(\partial \ln p_Z / \partial \ln T)_P$ ,  $(\partial \ln p_Y / \partial \ln T)_P$ ,  $\dots$ , is discussed in the section on "Derivative Matrices."

#### Molecular-Weight Derivatives

Each condensed phase is considered to occupy a negligible volume with respect to the volume occupied by the gases, even when finely divided and suspended in the gas. An average molecular weight is then defined to be the weight of the reaction products divided by the number of moles of gaseous products:

$$\bar{M} = \frac{\sum_i n_i M_i}{\sum_i p_i} = \frac{A M_r}{P} \quad (45)$$

where  $M_r$  is the formula weight of the equivalent formula of equation (3). When only gaseous products are formed in the reaction, this definition is identical to the usual definition of an average molecular weight. With the definition of equation (45), the molecular weight is suitable for use in the ideal gas law even when solids are present:

$$\left. \begin{aligned} P &= \frac{\rho R T}{M} \\ \text{or} \\ P_v &= \frac{R T}{M} \end{aligned} \right\} \quad (46)$$

The density  $\rho$  or specific volume  $v$  in equation (46) is the average value of the mixture of gases and condensed phases. Taking logarithms of equation (45),

$$\ln \mathcal{M} = \ln A + \ln \mathcal{M}_r - \ln P \quad (47)$$

Differentiation of equation (47) with respect to  $\ln T$  at constant  $P$  gives

$$\left( \frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P = \left( \frac{\partial \ln A}{\partial \ln T} \right)_P \quad (48)$$

Differentiation of equation (47) with respect to  $\ln P$  at constant  $T$  gives

$$\left( \frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \left( \frac{\partial \ln A}{\partial \ln P} \right)_T - 1 \quad (49)$$

Differentiation of equation (12) with respect to  $\ln A$  at constant  $T$  gives

$$\left( \frac{\partial \ln P}{\partial \ln A} \right)_T = \frac{1}{\left( \frac{\partial \ln A}{\partial \ln P} \right)_T} = \frac{1}{P} \sum_i p_i \left( \frac{\partial \ln p_i}{\partial \ln A} \right)_T \quad (50)$$

which may be used in equation (49) to give

$$\left( \frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \left[ \frac{P}{\sum_i p_i \left( \frac{\partial \ln p_i}{\partial \ln A} \right)_T} - 1 \right] \quad (51)$$

Differentiation of equation (9) gives

$$\left( \frac{\partial \ln p_i}{\partial \ln A} \right)_T = a_i \left( \frac{\partial \ln p_Z}{\partial \ln A} \right)_T = b_i \left( \frac{\partial \ln p_Y}{\partial \ln A} \right)_T + \dots \quad (52)$$

Equations (51) and (52) may be combined to give

$$\left( \frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T = \left[ \frac{P}{\sum_i a_i p_i \left( \frac{\partial \ln p_Z}{\partial \ln A} \right)_T + \sum_i b_i p_i \left( \frac{\partial \ln p_Y}{\partial \ln A} \right)_T + \dots} - 1 \right] \quad (53)$$

Comparison of equation (53) and the pressure row in figure 2 shows that the coefficients of the derivatives in equation (53) are the elements of the pressure row.

Other First Partial Derivatives ( $\gamma$  and  $C_V^o$ )

Bridgman (ref. 24) presents a convenient scheme for expressing all first partial derivatives in terms of three first partial derivatives, one of which is the same as selected in this report,  $(\partial H/\partial T)_P = C_P^o$ , and two of which are different,  $(\partial v/\partial T)_P$  and  $(\partial v/\partial P)_T$ . In order to make use of the tables of reference 24,  $(\partial v/\partial T)_P$  and  $(\partial v/\partial P)_T$  can be obtained from the derivatives given in this report by means of the following equations, which have been derived from the equation of state for ideal gases with variable molecular weight (eq. (46)):

$$\left(\frac{\partial v}{\partial T}\right)_P = \frac{v}{T} \left[ 1 - \left( \frac{\partial \ln \mu}{\partial \ln T} \right)_P \right] \quad (54)$$

$$\left(\frac{\partial v}{\partial P}\right)_T = - \frac{v}{P} \left[ 1 + \left( \frac{\partial \ln \mu}{\partial \ln P} \right)_T \right] \quad (55)$$

With the aid of the tables in reference 24 and equations (46), (54), and (55), other first partial derivatives can be expressed in terms of  $C_P^o$ ,  $(\partial \ln \mu / \partial \ln T)_P$ , and  $(\partial \ln \mu / \partial \ln P)_T$ . As examples, expressions are derived for the isentropic exponent  $\gamma$ , which is used to calculate velocity of sound, and specific heat at constant volume  $C_V^o$ .

By definition,

$$\gamma = \left( \frac{\partial \ln P}{\partial \ln \rho} \right)_S = - \left( \frac{\partial \ln P}{\partial \ln v} \right)_S = - \frac{v}{P} \left( \frac{\partial P}{\partial v} \right)_S \quad (56)$$

From Bridgman's tables (ref. 24),

$$\left( \frac{\partial P}{\partial v} \right)_S = \frac{C_P^o \mu}{\left( \frac{C_P^o}{\mu} \right) \left( \frac{\partial v}{\partial P} \right)_T + T \left( \frac{\partial v}{\partial T} \right)_P} \quad (57)$$

Substituting equations (46), (54), (55), and (57) into equation (56) yields

$$\gamma = \frac{C_P^o / R}{\frac{C_P^o}{R} \left[ 1 + \left( \frac{\partial \ln \mu}{\partial \ln P} \right)_T \right] - \left[ 1 - \left( \frac{\partial \ln \mu}{\partial \ln T} \right)_P \right]^2} \quad (58)$$

For nonreacting gases ("frozen" composition),  $\mathcal{M}$  is a constant, and equation (58) reduces to

$$\gamma = \frac{C_P^O/R}{\frac{C_P^O}{R} - 1} \quad (59)$$

By definition and from Bridgman's tables (ref. 24),

$$\frac{C_V^O}{\mathcal{M}} = \frac{1}{\mathcal{M}} \left( \frac{\partial E}{\partial T} \right)_V = \frac{\left( \frac{C_P^O}{\mathcal{M}} \right) \left( \frac{\partial V}{\partial P} \right)_T + T \left( \frac{\partial V}{\partial T} \right)_P^2}{\left( \frac{\partial V}{\partial P} \right)_T} \quad (60)$$

Substituting equations (46), (54), and (55) into equation (60) gives

$$C_V^O = C_P^O - R \frac{\left[ 1 - \left( \frac{\partial \ln \mathcal{M}}{\partial \ln T} \right)_P \right]^2}{\left[ 1 + \left( \frac{\partial \ln \mathcal{M}}{\partial \ln P} \right)_T \right]} \quad (61)$$

For nonreacting gases,  $\mathcal{M}$  is constant, and equation (61) reduces to

$$C_V^O = C_P^O - R \quad (62)$$

#### Derivative Matrices:

The evaluation of the three independent thermodynamic first partial derivatives is possible if the quantities  $(\partial \ln p_Z / \partial \ln T)_P$ ,  $(\partial \ln p_Y / \partial \ln T)_P \dots (\partial n_N / \partial \ln T)_P \dots (\partial \ln A / \partial \ln T)_P$  and  $(\partial \ln p_Z / \partial \ln A)_T$ ,  $(\partial \ln p_Y / \partial \ln A)_T \dots$  are known. These quantities may be calculated for equilibrium conditions by the solution of a set of simultaneous equations involving the preceding derivatives. The necessary equations for the temperature derivatives may be obtained from equations (5), (9), (11), and (13). Differentiation of these equations with respect to  $\ln T$  at constant  $P$  gives

$$\left. \begin{aligned} \sum_i a_i p_i \left( \frac{\partial \ln p_i}{\partial \ln T} \right)_P + a_N \left( \frac{\partial n_N}{\partial \ln T} \right)_P + \dots + \sum_i a_i n_i \left( \frac{\partial \ln A}{\partial \ln T} \right)_P &= 0 \\ \sum_i b_i p_i \left( \frac{\partial \ln p_i}{\partial \ln T} \right)_P + b_N \left( \frac{\partial n_N}{\partial \ln T} \right)_P + \dots + \sum_i b_i n_i \left( \frac{\partial \ln A}{\partial \ln T} \right)_P &= 0 \\ \dots &= 0 \end{aligned} \right\} \quad (63)$$

$$\left( \frac{\partial \ln p_i}{\partial \ln T} \right)_P - \left[ a_i \left( \frac{\partial \ln p_Z}{\partial \ln T} \right)_P + b_i \left( \frac{\partial \ln p_Y}{\partial \ln T} \right)_P + \dots \right] - q_i = 0 \quad (64)$$

$$\left. \begin{aligned} a_N \left( \frac{\partial \ln p_Z}{\partial \ln T} \right)_P + b_N \left( \frac{\partial \ln p_Y}{\partial \ln T} \right)_P + \dots + q_N &= 0 \\ \dots &= 0 \end{aligned} \right\} \quad (65)$$

$$\sum_i p_i \left( \frac{\partial \ln p_i}{\partial \ln T} \right)_P = 0 \quad (66)$$

If equation (64) is used to eliminate  $(\partial \ln p_i / \partial \ln T)_P$  from equations (63) and (66), then the resulting augmented matrix is identical to the matrix of figure 2 with the last row and column deleted, as shown in figure 3.

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The derivatives with respect to  $\ln A$  at constant  $T$  are obtained in a similar fashion. Differentiation of equations (5), (9), and (11) yields:

$$\left. \begin{aligned} \sum_i a_i p_i \left( \frac{\partial \ln p_i}{\partial \ln A} \right)_T + a_N \left( \frac{\partial n_N}{\partial \ln A} \right)_T + \dots - \sum_i a_i n_i &= 0 \\ \sum_i b_i p_i \left( \frac{\partial \ln p_i}{\partial \ln A} \right)_T + b_N \left( \frac{\partial n_N}{\partial \ln A} \right)_T + \dots - \sum_i b_i n_i &= 0 \\ \dots &= 0 \end{aligned} \right\} \quad (67)$$

$$\left( \frac{\partial \ln p_i}{\partial \ln A} \right)_T - \left[ a_i \left( \frac{\partial \ln p_Z}{\partial \ln A} \right)_T + b_i \left( \frac{\partial \ln p_Y}{\partial \ln A} \right)_T + \dots \right] = 0 \quad (68)$$

$$\left. \begin{aligned} a_N \left( \frac{\partial \ln p_Z}{\partial \ln A} \right)_T + b_N \left( \frac{\partial \ln p_Y}{\partial \ln A} \right)_T + \dots &= 0 \\ \dots &= 0 \end{aligned} \right\} \quad (69)$$

If equation (68) is used to eliminate  $(\partial \ln p_i / \partial \ln A)_T$  from equation (67), then the resulting augmented matrix is identical to the matrix of figure 2 with the last two rows and columns deleted, as shown in figure 4.

## ROCKET PERFORMANCE PARAMETERS

## Calculation

The evaluation of rocket performance parameters for a propellant is simple once the temperature and composition are known at combustion and exit points of a nozzle. The following formulas used in computing the various performance parameters were derived from the one-dimensional forms of continuity, energy, and momentum equations and the following assumptions: zero velocity in the combustion chamber, perfect gas law, complete combustion, homogeneous mixing, adiabatic combustion, and isentropic expansion. (The units used were  $h = \text{cal/g}$ ,  $T = {}^\circ\text{K}$ ,  $P = \text{lb force/sq in.}$ ,  $A = \text{sq in.}$ ,  $w = \text{lb mass/sec}$ , and  $g_c = 32.174 (\text{lb mass/lb force})(\text{ft/sec}^2)$ .)

Specific impulse with ambient and exit pressures equal,  $(\text{lb force})(\text{sec})/\text{lb mass}$ :

$$I = 294.98 \sqrt{\frac{h_c - h}{1000}} \quad (70)$$

Specific impulse in vacuum (ambient pressure zero),  $(\text{lb force})(\text{sec})/\text{lb mass}$ :

$$I_{\text{vac}} = I + P \left( \frac{A}{w} \right) \quad (71)$$

Nozzle area per unit mass-flow rate,  $(\text{sq in.})(\text{sec})/\text{lb}$ :

$$\frac{A}{w} = \frac{86.4554 T}{PMI} \quad (72)$$

Characteristic velocity,  $\text{ft/sec}$ :

$$c^* = g_c P_c \frac{A_t}{w} = 32.174 P_c \frac{A_t}{w} \quad (73)$$

Coefficient of thrust:

$$C_F = \frac{g_c I}{c^*} = 32.174 \frac{I}{c^*} \quad (74)$$

Mach number:

$$M = \frac{U}{a} = \frac{I}{\sqrt{\frac{86.4554 rT}{M}}} \quad (75)$$

### Effect of Chamber Pressure on Performance Parameters

For a given pressure ratio  $P_c/P$ , the logarithms of the performance parameters given in equations (70) to (74) are very nearly linear in the logarithm of the combustion-chamber pressure  $P_c$ . Thus, if any one of the performance parameters is denoted by  $\lambda$ , then, to a good approximation,

$$\left( \frac{\partial \ln \lambda}{\partial \ln P_c} \right)_{P_c/P} = \pi_\lambda \approx \frac{\ln \lambda_2 - \ln \lambda_1}{\ln(P_c)_2 - \ln(P_c)_1} \quad (76)$$

or

$$\frac{\lambda_2}{\lambda_1} \approx \left[ \frac{(P_c)_2}{(P_c)_1} \right]^{\pi_\lambda} \quad (77)$$

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Analytical expressions are readily obtained for the partial derivatives  $\pi_\lambda$  by the method indicated in reference 25. Using this technique it is possible to derive the following identities:

$$\pi_I = \frac{RT}{I^2} \left[ \frac{1}{M_c} - \frac{1}{M} \right] \quad (78)$$

$$\pi_{A/w} = - \left\{ \frac{R}{C_P^o} \frac{M_c}{M} \left[ 1 - \left( \frac{\partial \ln M}{\partial \ln T} \right)_P \right] + \frac{1}{\gamma} + \pi_I \right\} \quad (79)$$

$$\pi_\epsilon = \pi_{A/w} - (\pi_{A/w})_t \quad (80)$$

$$\pi_{c*} = 1 + (\pi_{A/w})_t \quad (81)$$

$$\pi_T = \frac{R}{C_P^o} \left[ 1 - \left( \frac{\partial \ln M}{\partial \ln T} \right)_P \right] - \frac{R}{C_P^o \left( \frac{M_c}{M} \right)} \quad (82)$$

$$\pi_{C_F} = \pi_I - \pi_{c*} \quad (83)$$

$$\pi_{I_{vac}} = \frac{I(\pi_I) + (I_{vac} - I)(\pi_\epsilon + \pi_{c*})}{I_{vac}} \quad (84)$$

## ITERATION TO AN ASSIGNED MACH NUMBER

It may sometimes be desired to calculate conditions following an isentropic expansion to an assigned Mach number rather than to an assigned pressure. For example, one might wish to find the conditions at the throat of a nozzle where the Mach number is 1. The procedure used in this report for calculating conditions at an assigned Mach number is as follows:

(1) An estimate of pressure corresponding to the assigned Mach number is made.

(2) After equilibrium composition and temperature have been obtained in a manner identical to isentropic expansion to assigned pressure, the Mach number is then calculated.

(3) The error between the desired Mach number and the calculated Mach number is used to obtain a new estimate for pressure.

(4) Steps (2) and (3) are repeated until the desired degree of accuracy is obtained.

The correction to the assumed pressure ratio can be obtained by using a parameter  $h^*$ , defined as

$$h^* = h + \frac{M_0^2}{2} \frac{\gamma R T}{\infty} \quad (85)$$

where  $h$ ,  $\gamma$ ,  $T$ , and  $\infty$  are values corresponding to the assumed pressure, and  $M_0$  is the assigned Mach number. When the correct pressure (or pressure ratio) is used,  $h^*$  will equal the initial enthalpy of the propellants  $h_c$ . The estimate for the pressure ratio is corrected on the basis of the difference between  $h^*$  and  $h_c$ . Since  $h^*$  is a function of  $P$ ,

$$\Delta h^* = \left( \frac{\partial h^*}{\partial \ln P} \right)_S \Delta \ln P \quad (86)$$

where

$$\Delta h^* = h_c - h_k^*$$

and

$$\Delta \ln P = \frac{P_{k+1} - P_k}{P_k}$$

with the subscript  $k$  referring to the  $k^{\text{th}}$  estimate. Equation (86) then gives

$$\frac{P_c}{P_{k+1}} = \frac{P_c/P_k}{1 + \left[ \frac{h_c - h_k^*}{\left( \frac{\partial h^*}{\partial \ln P} \right)_s} \right]} \quad (87)$$

The  $(k+1)^{\text{th}}$  estimate can be obtained from the  $k^{\text{th}}$  estimate for the pressure ratio by means of equation (87), provided that  $\left( \frac{\partial h^*}{\partial \ln P} \right)_s$  can be evaluated. Since  $\gamma$  is essentially constant for a small change in pressure ratio, then from equation (85),

$$\left( \frac{\partial h^*}{\partial \ln P} \right)_s \approx P \left\{ \left( \frac{\partial h}{\partial P} \right)_s + \frac{\gamma M_0^2}{2} \left[ \frac{\partial (T/\mu)}{\partial P} \right]_s \right\} \quad (88)$$

From equation (46) for an ideal gas,

$$\left[ \frac{\partial (T/\mu)}{\partial P} \right]_s = \frac{1}{R\rho} \left[ 1 - \left( \frac{\partial \ln \rho}{\partial \ln P} \right)_s \right] = \frac{1}{R\rho} \left( \frac{\gamma - 1}{\gamma} \right) \quad (89)$$

Using the thermodynamic relation  $(\partial h/\partial P)_s = 1/\rho$  and equation (89) in equation (88) yields

$$\left( \frac{\partial h^*}{\partial \ln P} \right)_s \approx \frac{RT}{\mu} \left[ 1 + \frac{M_0^2}{2} (\gamma - 1) \right] \quad (90)$$

In particular, at the throat  $M_0 = 1$  and equation (90) becomes

$$\left( \frac{\partial h^*}{\partial \ln P} \right)_s \approx \frac{RT}{2\mu} (\gamma + 1) \quad (91)$$

#### COMPUTER PROGRAM

A computer program for performing the calculations previously discussed has been made for an IBM 650 Magnetic Drum Data-Processing Machine with 2000 words of drum storage, 60 words of high-speed core storage, indexing registers, floating point attachments, and an alphabetic device. When additional attachments such as tapes and RAMAC are available, the program may be modified to make use of these attachments. A wiring diagram for the IBM type 533 Read-Punch Unit is given in appendix I. In the description of the program, a familiarity with the symbolic coding for the IBM 650 computer (SOAP II) is assumed, as described in IBM Form 32-7646-1, "Soap Programmer's Reference Manual." References to storage

locations will be made with symbolic addresses given in upper case and enclosed by quotes. For the absolute equivalents of the symbolic addresses, the program listing given in appendixes F, G, and H can be consulted.

Because of computer storage limitations, it was necessary to divide the program into two sections, (1) The "Vector and Propellant Program," which prepares most of the input data and requires an alphabetic device on the IBM 650, and (2) The "Main Calculating Program," which solves for the equilibrium compositions and temperatures and the performance parameters. The Main Calculating Program may be used without using the Vector and Propellant Program if the necessary input data are prepared manually. The primary use of the Vector and Propellant Program is to simplify the preparation of input data and to minimize the possibility of errors. However, since the use of the Vector and Propellant Program is optional, the Main Calculating Program will be described first.

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## MAIN CALCULATING PROGRAM

### General Description

Figure 5 gives a schematic outline of the Main Calculating Program. Individual portions of the program will be discussed in more detail in later sections. A SOAP listing of the Main Program is given in appendix F, and operating instructions are given in appendix C.

The program as written is capable of performing thermodynamic equilibrium calculations for both combustion and isentropic expansion conditions for a chemical system that may include as many as 10 different chemical elements (if no condensed phases appear as reaction products). When condensed phases are present as reaction products, then the sum of the different chemical elements and different condensed phases must not exceed 10. This restriction implies that the size of the reduced augmented matrix (fig. 2) is limited to 12x13. It should be emphasized that this restriction is imposed solely by machine storage limitations.

The program will handle as many as 30 reaction products and 25 pressure ratios including the combustion chamber and the throat. The restriction on the number of products and pressure ratios is also the result of storage limitations. The program calculates the equilibrium composition, temperature, pressure, enthalpy, and entropy of the reaction products, and the following performance parameters: specific impulse, specific impulse in vacuum, thrust coefficient, characteristic velocity, area ratio, specific heat, isentropic exponent  $\gamma$ , and Mach number. The program also calculates the derivatives  $\left(\frac{\partial \ln \pi}{\partial \ln P}\right)_P$ ,  $\left(\frac{\partial \ln \pi}{\partial \ln P}\right)_T$ , and the chamber-pressure derivatives  $\pi_I$ ,  $\pi_e$ ,  $\pi_T$ , and  $\pi_c^*$ .

Normally the program calculates combustion conditions ( $P_c/P = 1$ ), then throat conditions, and finally other exit conditions corresponding to assigned pressure ratios. The program is easily modified to operate for assigned temperatures and pressures or to work a series of constant-enthalpy calculations at various pressures. The necessary changes in the program are given in the section "Program Modifications."

The following input data are required by the Main Calculating Program for the solution of equilibrium compositions and temperature following an adiabatic combustion process:

- (1) The reaction products to be considered
- (2) Gram atoms of elements in 1 gram of fuel and 1 gram of oxidant
- (3) Enthalpies of fuel and oxidant per gram of fuel and oxidant
- (4) Oxidant to fuel weight ratio O/F (or percent fuel or equivalence ratio  $r$ )
- (5) Thermodynamic data for products considered
- (6) Chamber pressure
- (7) Initial estimate of temperature, composition, and number of formula weights A. (A set of estimates is already provided by the program and therefore need not be supplied unless a better set is desired.)

Reaction products (the composition vector). - The composition of any product of reaction in terms of the elements may be represented as a chemical vector whose components are determined by the chemical formula for the reaction product. Thus, the molecule  $Z_{a_i} Y_{b_i} X_{c_i} \dots$  may be associated with the vector

$$C = \{a_i, b_i, c_i \dots\}$$

The number of components associated with each composition vector is known once it is decided how many chemical elements are to be considered in any particular problem. For example, if hydrogen and oxygen were the only two elements appearing, then any reaction product could be specified with two components. If hydrogen, oxygen, and nitrogen were the elements under consideration, then each reaction product would have three components. This is illustrated in the following table for four possible products of reaction involving hydrogen, oxygen, and nitrogen:

Product	Component		
	H	N	O
N	0	1	0
OH	1	0	1
H <sub>2</sub> O	2	0	1
NO	0	1	1

A considerable portion of the matrix of figure 2 may be constructed in a reasonably systematic manner with the aid of the composition vector. This is described in the section "Vector multiplication routine."

Packed chemical vector. - The total number of components of all the chemical vectors is directly related to the size of the chemical system and to the number of possible reaction products. Thus, for a 10-element system in which 30 different products of reaction are to be considered, a total of 300 components requiring 300 storage locations would have to be specified. Since these numbers would be placed in the storage area of a computer with limited storage capacity, the storage area available for programming would be seriously reduced. It has been found that with a few suitable restrictions all the components of a vector may be packed into one 10-digit word, and thus only 30 storages would be required for 30 products. The following restrictions have been set forth:

- (1) All the chemical vector components that are not specified are assumed to be zero.
- (2) No reaction product may be formed from more than five different chemical elements; that is, the chemical vector may have no more than five nonzero components.
- (3) Each subscript in the chemical formula for the reaction product must be less than 10; that is, no vector component may be greater than 9.

The packed chemical vector may now be generated from the chemical formula of a reaction product in the following manner:

- (1) Each element in the chemical system is assigned a number equal to one less than its column assignment in the reduced augmented matrix (fig. 2). This number is used to specify the component.
- (2) The magnitude of any component is equal to the subscript associated with the chemical element in the chemical formula for the reaction product under consideration.
- (3) The packed vector consists of five pairs of numbers. In each pair of numbers (where both numbers are not zero) the number designating the component precedes the number that gives the magnitude of the component.

(4) The nonzero vector components and their associated magnitudes are arranged in the packed vector in the order of their appearance in the chemical formula of the reaction product, the entire packed vector being shifted as far to the right as possible.

(5) The sign of the packed composition vector is positive for a gaseous reaction product and negative for a condensed-phase reaction product.

An example of how components might be designated in an H-N-O system is as follows:

Element	H	N	O
Column of matrix in fig. 2	1	2	3
Number designat- ing component (column number - 1)	0	1	2

The assignment of numbers designating the elements is completely arbitrary. However, once an assignment has been made for some problem, then all product vectors must be consistent with this assignment.

Examples of packed vectors for four reaction products using the numbers designating components given in the previous table are as follows:

Reaction product	Packed vector
N	00 00 00 00 11+
OH	00 00 00 21 01+
H <sub>2</sub> O	00 00 00 02 21+
NO	00 00 00 11 21+

To read the preceding packed vectors, proceed as follows:

- (1) Pair the digits into groups of two.
- (2) The first digit of a pair designates the atom.
- (3) The second digit of the pair tells how many of these atoms there are.

(4) The sign is + for gas and - for condensed phases.

For example, the H<sub>2</sub>O packed vector may be interpreted as follows:

00	00	00	02	21	+
Ignored because both digits of each pair are zero					
Number designating element hydrogen					
Magnitude (number of hydrogen atoms)					
Number designating element oxygen					
Magnitude (number of oxygen atoms)					
Gaseous product					

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Calculation of gram atoms of elements in fuel and oxidant or in reactant. - To specify a reactant, the relative proportion of the elements in the reactant is all that is required. That is, the absolute magnitude of the elements  $a_0, b_0, c_0, \dots$  in the equivalent reactant  $Z_{a_0} Y_{b_0} X_{c_0} \dots$  is immaterial if their ratios remain constant. In the IBM 650 program the number of gram atoms of each element in a reactant is calculated to be that number which gives an equivalent formula with a formula weight  $M_r$  of 1.

For example, the equivalent formula in equation (1) ( $H_7N_2O_3$ ) has a molecular weight of 83.072. In the IBM 650 program the equivalent formula would be  $H(7/83.072) N(2/83.072) O(3/83.072)$  or  $H_0.08426 N_0.02408 O_0.03611$  ( $M_r = 1$ ).

The method selected in this report for the calculation of the gram atoms of element per gram of reactant was based on the assumption that performance data for a particular reactant would be desired for a number of oxidant-fuel ratios. For this reason, the input to the Main Calculating Program consists of the number of gram atoms of each element per gram of fuel and the number of gram atoms of each element per gram of oxidant. The number of gram atoms of each element per gram of reactant can then be calculated from these quantities as soon as the oxidant-fuel ratio (or % fuel or equivalence ratio  $r$ ) is specified as shown in the following discussion.

The fuels are considered to be those materials undergoing oxidation primarily and the oxidants those materials undergoing reduction primarily. Let 1 gram of equivalent fuel be  $Z_{a_f} Y_{b_f} X_{c_f} \dots$  and 1 gram of equivalent oxidant be  $Z_{a_x} Y_{b_x} X_{c_x} \dots$  where  $a_f, b_f, c_f \dots$  and  $a_x, b_x, c_x \dots$  are the number of gram atoms of elements  $Z, Y, X \dots$  in 1 gram of equivalent fuel and 1 gram of equivalent oxidant, respectively. If  $W_x$  is the weight of the oxidant and  $W_f$  the weight of

the fuel ( $O/F = W_x/W_f$ ), then the number of gram atoms of each element in 1 gram of equivalent reactant  $Z_{a_0} Y_{b_0} X_{c_0} \dots$  is

$$\left. \begin{aligned} a_0 &= \frac{W_x a_x + W_f a_f}{W_x + W_f} = \frac{(O/F)a_x + a_f}{(O/F) + 1} \\ b_0 &= \frac{W_x b_x + W_f b_f}{W_x + W_f} = \frac{(O/F)b_x + b_f}{(O/F) + 1} \\ \dots &= \dots = \dots \end{aligned} \right\} \quad (92)$$

Equation (92) may be illustrated by considering the example of equation (1):



The formulas per gram of equivalent fuel and oxidant are

$$\left. \begin{aligned} N(2/32.048) H(4/32.048) &= N_{0.062406390} H_{0.12481278} \\ H(2/34.016) O(2/34.016) &= H_{0.058795860} O_{0.058795860} \end{aligned} \right\} \quad (93)$$

(Eight significant figures are kept in this example, since the IBM 650 floating point attachment keeps eight significant figures.) For equation (1),

$$O/F = \frac{1.5(34.016)}{32.048} = 1.5921118 \quad (94)$$

and therefore

$$\left. \begin{aligned} (H) a_0 &= \frac{1.5921118(0.058795860) + 0.12481278}{1.5921118 + 1} = 0.084264252 \\ (N) b_0 &= \frac{1.5921118(0) + 0.062406390}{1.5921118 + 1} = 0.024075501 \\ (O) c_0 &= \frac{1.5921118(0.058795860) + 0}{1.5921118 + 1} = 0.036113250 \end{aligned} \right\} \quad (95)$$

Calculation of enthalpy of fuel and oxidant or of propellant. - Let  $h_f$  and  $h_x$  be the enthalpy per gram of equivalent fuel and per gram of equivalent oxidant, respectively. Then the enthalpy per gram of equivalent reactant  $Z_{a_0} Y_{b_0} X_{c_0} \dots$  is

$$h_O = h_O = \frac{(O/F)h_x + h_f}{(O/F) + 1} \quad (96)$$

Equation (96) may be illustrated by again considering the reaction of equation (1). Using values similar to those on page 19 of reference 9 and the O/F value from equation (94),

$$\left. \begin{aligned} h_{N_2H_4} &= h_f = \frac{154,702.97}{32.048} = 4827.2269 \text{ cal/g} \\ h_{H_2O_2} &= h_x = \frac{28,681.626}{34.016} = 843.18043 \text{ cal/g} \end{aligned} \right\} \quad (97)$$

$$h_O = \frac{1.5921118 (843.18043) + 4827.2269}{1.5921118 + 1} = 2380.1691 \text{ cal/g} \quad (98)$$

Optional specification of O/F. - In addition to the oxidant to fuel weight ratio O/F, two other quantities may be used to give the relative amounts of oxidant and fuel. One of these is the weight percent of fuel in the propellant %F and the other is the equivalence ratio r.

(1) %F: The relation between O/F and %F is given by

$$\%F = \frac{100}{(O/F) + 1} \quad (99)$$

(2) Equivalence ratio r: The equivalence ratio is defined in terms of arbitrary, permanently assigned oxidation states for each element in a compound. This practice produces no difficulty so long as all the elements have the assigned oxidation state in all their compounds (e.g., H = +1, Na = +1, F = -1). Some elements have various oxidation states; for example, sulfur, which has the oxidation numbers -2, +4, +6 in the compounds H<sub>2</sub>S, SO<sub>2</sub>, and H<sub>2</sub>SO<sub>4</sub>, respectively. In cases such as this the assigned oxidation states are taken to be those considered as occurring commonly in products. For this reason it is possible that some components of the propellant combination may show a net positive or negative oxidation state, contrary to the usual practice of having the sum of the oxidation numbers of a compound add up to zero.

Let V<sub>Z</sub><sup>+</sup>, V<sub>Y</sub><sup>+</sup>, V<sub>X</sub><sup>+</sup> . . . be the positive oxidation states and V<sub>Z</sub><sup>-</sup>, V<sub>Y</sub><sup>-</sup>, V<sub>X</sub><sup>-</sup> . . . be the negative oxidation states of the elements Z, Y, X . . . in the reactant. Let V<sub>x</sub><sup>+</sup> and V<sub>x</sub><sup>-</sup> be the total positive oxidation state and total negative oxidation state, respectively, per gram of equivalent oxidant, and let V<sub>f</sub><sup>+</sup> and V<sub>f</sub><sup>-</sup> be the total positive and negative oxidation states, respectively, per gram of equivalent fuel. Then,

$$\left. \begin{array}{l} V_x^+ = \left[ a_x V_z^+ + b_x V_y^+ + c_x V_x^+ + \dots \right] \\ V_x^- = \left[ a_x V_z^- + b_x V_y^- + c_x V_x^- + \dots \right] \\ V_f^+ = \left[ a_f V_z^+ + b_f V_y^+ + c_f V_x^+ + \dots \right] \\ V_f^- = \left[ a_f V_z^- + b_f V_y^- + c_f V_x^- + \dots \right] \end{array} \right\} \quad (100)$$

The total positive oxidation state  $V^+$  and total negative oxidation state  $V^-$  per gram of propellant are

$$\left. \begin{array}{l} V^+ = \frac{(O/F)V_x^+ + V_f^+}{(O/F) + 1} \\ V^- = \frac{(O/F)V_x^- + V_f^-}{(O/F) + 1} \end{array} \right\} \quad (101)$$

The equivalence ratio may now be defined as

$$r \equiv \left| \frac{V^-}{V^+} \right| = \left| \frac{V_f^- + (O/F)V_x^-}{V_f^+ + (O/F)V_x^+} \right| \quad (102)$$

This definition of  $r$  gives  $r = 1$  for stoichiometric conditions,  $r > 1$  for oxidant-rich conditions, and  $r < 1$  for fuel-rich conditions. For those who prefer to consider  $r > 1$  for fuel-rich conditions and  $r < 1$  for oxidant-rich conditions, the reciprocal of  $r$  in equation (102) may be taken as the definition of equivalence ratio, provided that the computing program be correspondingly modified.

The reaction of equation (1) may be again taken to illustrate equations (100) and (102). Let  $a, b, c$  refer to H, N, O, respectively. Then, from equation (100),

$$\left. \begin{array}{l} H_2O_2 \left\{ \begin{array}{l} V_x^+ = [2(1) + (0)(0) + 2(0)]/34.016 = 0.058795860 \\ V_x^- = [2(0) + (0)(0) + 2(-2)]/34.016 = -0.11759172 \end{array} \right. \\ N_2H_4 \left\{ \begin{array}{l} V_f^+ = [4(1) + 2(0) + 0(0)]/32.048 = 0.12481278 \\ V_f^- = [4(0) + 2(0) + 0(0)]/32.048 = 0 \end{array} \right. \end{array} \right\} \quad (103)$$

From equation (102), and using the  $O/F = 1.5921118$  of equation (94),

$$r = \frac{(1.5921118)(-0.11759172) + 0}{(1.5921118)(0.058795860) + 0.12481278} = 0.85714286 \quad (104)$$

For any problem it is sufficient to specify any one of the three quantities  $O/F$ ,  $\%F$ , or  $r$ , since any two may be expressed in terms of the third. (See eqs. (99) and (102), e.g.)

Thermodynamic data. - Since the computer program solves for temperature simultaneously with composition, it was found convenient to represent the thermodynamic data for each product as a function of temperature as follows:

$$C_P^0/R = A + BT + CT^2 + DT^3 \quad (105)$$

$$H_T^0/RT = A + \frac{BT}{2} + \frac{CT^2}{3} + \frac{DT^3}{4} + \frac{ET}{T} \quad (106)$$

$$S_T^0/R = A \ln T + BT + \frac{CT^2}{2} + \frac{DT^3}{3} + F \quad (107)$$

where  $T$  is in degrees Kelvin. The function  $H_T^0/RT$  must include  $H_0^0/RT$ , where  $H_0^0$  is the reference enthalpy at  $0^\circ K$  (see eq. (14)).

In order to minimize the errors resulting from a functional representation of the thermodynamic data, the six coefficients  $A$ ,  $B$ ,  $C$ ,  $D$ ,  $E$ , and  $F$  for each product were obtained from a simultaneous least-squares fit of the thermodynamic functions  $C_P^0/R$ ,  $H_T^0/RT$ , and  $S_T^0/R$  for several selected temperature intervals with continuity from one interval to the next. Coefficients for several substances in the C, H, O, N, F, and Cl chemical system are given in table I.

### Calculating Routines

The Main Calculating Program consists of ten major routines and several auxiliary routines with suitable connecting links. These routines are described in the following sections.

Packed vector loading routine. - The flow chart for the packed vector loading routine is given in figure 6. This short program permits direct loading of the packed vectors from the Vector and Propellant Program. The packed vectors are in the form of load hub cards on which the second word gives the permanent code number associated with the reaction product, and the fourth word gives the packed vector for the same product. The permanent code and the packed vector are loaded into sequential locations in

the P region; that is, the code and packed vector from the first card are placed into "P0001" and "P0002," respectively; the code and vector from the next card are placed into "P0003" and "P0004," and so forth.

When the program encounters a condensed phase, it examines the contents of the word "OASIS" to determine whether or not this product is to be considered in the first iteration. Thereafter, the decision to use or not to use a condensed phase is made internally. All positions of "OASIS" must be either zero or one, a zero indicating use and one indicating nonuse of a condensed phase. Each position of "OASIS" corresponds to a different condensed phase; thus position 1 (right-most position) is associated with the first condensed phase encountered, position 2 with the second, and so forth. For example, if "OASIS" contained

00 0000 1101 +

the program would not initially consider the first, third, and fourth condensed phases encountered. Should only two condensed-phase packed vectors be present, the program will ignore all positions beyond the first two. If the operator does not specify the contents of "OASIS," the program puts ones in all positions, thus initially considering only the gas phase.

The packed vector loading routine requires a transfer card to precede the first packed vector. The transfer card is a load hub card on which the first word is

NOP 0000 V0001 + (or numerical equivalent, 000000 1599+)

The last packed vector must be followed by another load hub card on which the first word is

00 0000 0000+

The packed vectors themselves must be arranged so that all the gaseous atoms enter storage before any gaseous molecules or condensed phases. If this condition is not met, a programmed stop will halt the loading. (The vectors for gaseous atoms may be loaded in any order followed by the remainder of the vectors in any order. However, the thermal data coefficients must be loaded in the same order as the vectors.) As each gaseous atom and each condensed-phase vector considered by "OASIS" is placed into storage, it is counted so that the two constants "ATOM1" and "SYS," used to specify the size of the reduced augmented matrix, may be obtained. Both of these are fixed point numbers in the low-order positions. "ATOM1" gives the number of different elements in the chemical system, and "SYS" gives the number of elements plus the condensed phases currently being considered. During the course of loading packed vectors, any load card with word 2 blank or zero will be bypassed.

Input data routine. - The flow chart for the input data routine is given in figure 7. The routine converts the input data as specified by the operator into suitable form for use in the computer. Thus, using equations (99) and (102), it calculates any two of the quantities  $O/F$ ,  $r$ , and  $\%F$  from the one which is supplied by the operator. The numbers  $a_0$ ,  $b_0$ ,  $c_0$ , . . .  $h_0$  are calculated from  $a_f$ ,  $a_x$ ,  $b_f$ ,  $b_x$ , . . .  $h_x$ ,  $h_f$  using equations (92) and (96). Also, the combustion-chamber pressure in pounds per square inch absolute is converted to atmospheres.

The input data for this routine and, hence, for the general program consist of the following:

- (1) A 4-digit identification number for the problem (case no.) is loaded into "FO039" as

0000 Case no. 00+

- (2) The chamber pressure  $P_c$  in pounds per square inch absolute is loaded into "FO000."

- (3) The numbers  $a_x$ ,  $b_x$ , . . .  $j_x$ ;  $h_x$ ,  $V_x^+$ , and  $V_x^-$  are loaded into locations 0537, 0538, . . . ; 0547, 0548, and 0549, respectively, and the numbers  $a_f$ ,  $b_f$ , . . .  $j_f$ ;  $h_f$ ,  $V_f^+$ , and  $V_f^-$  are loaded into locations 0587, 0588, . . . ; 0597, 0598, and 0599, respectively. If the Vector and Propellant Program is used, these numbers will be prepared automatically.

- (4) Any one of the three quantities  $O/F$ ,  $r$ , and  $\%F$  is loaded into "O/F," "EQRAT," or "PCT F," respectively, while the other two are loaded as zero.

- (5) A schedule of up to 25 pressure ratios is loaded into the region R(1075-1099).

A set of estimates for  $\ln p_i$ ,  $n_N$ ,  $\ln T$ , and  $\ln A$  is already provided by the program and need not be supplied unless one wishes to use a better set of estimates. Convergence usually occurs without good estimates.

The output from this routine is seven Bell format cards (see discussion in section on "Auxiliary routines" and also appendix B). The first Bell card contains the following six words:  $r$ ,  $O/F$ ,  $\%F$ ,  $P_c$  (atm),  $h_0$  (cal/g), and the identification number for the problem. The identification number is a composite of the equivalence ratio, the case number, and the chamber pressure in pounds per square inch absolute. The input data  $a_f$ ,  $b_f$ , . . .  $j_f$ ;  $h_f$ ,  $V_f^+$ ,  $V_f^-$ ,  $a_x$ ,  $b_x$ , . . .  $j_x$ ;  $h_x$ ,  $V_x^+$ , and  $V_x^-$  are punched out on the next six Bell cards. A console-controlled punch can be used to obtain the calculated numbers  $a_0$ ,  $b_0$  . . . ( $h_0/R$ ).

Load thermal data routine. - The thermodynamic data for each reaction product are represented by six coefficients A, B, C, D, E, and F, which were discussed in the section on "Thermodynamic data." The routine requires the coefficients to be on a load hub card in columns 21 through 80 (the last six words). The first word on the card is actually the first instruction in the routine following the read command for a basic load card and is

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The second word is the identification for the card, being a composite of the permanent code for the molecule and the low temperature (divided by 10) and high temperature (divided by 10) of the interval for which the coefficients were obtained. Thus, if the code for the molecule is 0121 and the temperature range is from 2600° to 3200° K, word 2 would be

Code	T <sub>low</sub>	T <sub>high</sub>
0121	260	320

With this scheme no molecule may have a code greater than four digits in length or a temperature interval higher than 9990° K.

The information from a thermodynamic coefficient card appears on the drum in a block of ten consecutive storages in the T region. The first word of the block contains the permanent code for the molecule in the instruction address position. For the previous example this would be

00 0000 0121

The following six storage positions contain the thermal coefficients. The eighth word is reserved for the composition estimate  $\ln p_i$  or  $n_N$ , while the last two words of the block are reserved for  $q_i$  and  $-\delta_i$ . Since the sequential blocks of ten storages are assigned to reaction products on the basis of their order of appearance, within any temperature interval the order of the thermal data cards must match the order of the packed vectors. If this is not so, a programmed stop will halt the loading of the thermal coefficients.

Each set of basic load cards corresponding to some temperature interval must be followed by a Bell format card that is filled with zeros except for words 1 (columns 11 to 21) and 2 (columns 22 to 32). Word 1 is the floating point number for the low temperature, and word 2 is the floating point number for the high temperature of the interval covered by the preceding cards.

The flow chart for the load thermal data routine is given in figure 8.

Unpacking routine and thermal routine. - The purpose of the unpacking and thermal routines is to construct a "row vector." This row vector is a set of consecutive core storage locations representing a convenient arrangement of quantities that will eventually be used to construct the elements of the reduced augmented matrix. The row vector and its contents are as follows:

Symbolic location	Absolute location	Contents
RV000	9004	$(H_T^O/R)_i$ During expansion, zero during combustion
RV001	9005	$a_i$
RV002	9006	$b_i$
RV003	9007	$c_i$
RV004	9008	$d_i$
RV005	9009	$e_i$
RV006	9010	$f_i$
RV007	9011	$g_i$
RV008	9012	$h_i$
RV009	9013	$i_i$
RV010	9014	$j_i$
RV011	9015	1 For gas, 0 for condensed
RV012	9016	$q_i$
RV013	9017	$\delta_i$
RV014	9018	$(H_T^O/R)_i$ For combustion, $(S'/R)_i$ for expansion

Storage space has been provided for ten subscripts or ten components of the composition vector. If the chemical system being used does not require ten components, then the first component appears in the location "RV011" minus "SYS" and is followed by the remaining components. The locations from "RV001" to "RV010" minus "SYS" inclusive remain zero. The unpacking routine fills in the locations "RV001" through "RV011" inclusive, the thermal routine completing the remaining quantities. The flow chart for the unpacking routine is given in Figure 9, while the thermal routine is given in figure 10.

Vector multiplication routine. - The vector multiplication routine calculates the elements of the reduced augmented matrix by multiplication of vectors. The gaseous-product contributions to the matrix elements of the mass-balance equations in figure 2 are generated by the following operation:

$$\begin{bmatrix} a_i p_i \\ b_i p_i \\ \dots \\ \dots \\ j_i p_i \end{bmatrix} \quad \begin{bmatrix} a_i, b_i, \dots, j_i, l, q_i, \delta_i \end{bmatrix} \quad (108)$$

Only those terms that are on or to the right of the principal diagonal are filled in. The gaseous-product contributions to the pressure-row elements are obtained from

$$p_i \begin{bmatrix} a_i, b_i, \dots, j_i, 0, q_i, \delta_i \end{bmatrix} \quad (109)$$

The gaseous-product contributions to the enthalpy-row elements are obtained from

$$\frac{p_i (H_T^O)}{R} \begin{bmatrix} a_i, b_i, \dots, j_i, l, q_i, \delta_i \end{bmatrix} \quad (110)$$

An entropy row is used in place of the enthalpy row during expansion, and the gaseous-product contributions to the entropy-row elements are given by

$$\frac{p_i S'_i}{R} \begin{bmatrix} a_i, b_i, \dots, j_i, l, q_i, \delta_i \end{bmatrix} \quad (111)$$

The condensed products each contribute a row to the reduced augmented matrix, which, for  $Z_{a_N} Y_{b_N} X_{c_N} \dots$ , is

$$\begin{bmatrix} a_N, b_N, \dots, j_N, 0, q_N, \delta_N \end{bmatrix} \quad (112)$$

and, in addition, the contribution of this condensed product to the column  $(-\Delta \ln A)$  is

$$\begin{bmatrix} a_N^{n_N} \\ b_N^{n_N} \\ \dots \\ \dots \\ j_N^{n_N} \\ 0 \\ (H_T^O)_{N^{n_N}} \end{bmatrix} \quad (113)$$

The flow chart for this routine is given in figure 11.

Matrix completion routine. - This routine completes the matrix by calculating and adding to the appropriate matrix elements the quantities  $A \Delta a$ ,  $A \Delta b$ , . . .  $\Delta P$ ,  $A \Delta h$ ,  $\sum_i (C_P^0)_{in_i} / R$  or  $T \sum_i (C_P^0)_{in_i} / R$ , and reflecting the symmetric portions of the matrix about the diagonal. During expansion,  $\sum_i (S_T)_{in_i} / R$  replaces the term in the entropy row and

$-\Delta \ln A$  column. When this has been completed, the routine examines all the error terms, requiring them to be smaller than some preassigned value before the iteration process is halted. After convergence is complete, the program checks to make sure that the thermal data for the correct temperature interval were used and examines the partial pressures of the condensable materials to ascertain whether or not condensed-phase products should have been considered. The flow chart for this routine is given in figure 12.

Matrix solution routine. - The correction variables for the gaseous atoms and condensed phases are obtained from the reduced augmented matrix (fig. 2) by the matrix solution routine presented in figure 13. The corrections to the gaseous molecules are obtained from the correction equations for the gaseous atoms using equation (29). When the iteration process has converged to the equilibrium values, this same routine is used to solve the two sets of equations discussed in the section on "Derivative Matrices."

The solution routine carries out a Gauss reduction on the linear set; that is, it eliminates the first variable from all equations following the first equation, the second variable from all equations following the second equation, and so on. The solution routine assumes that the equations appear in consecutive bands of storage, the  $n^{th}$  equation in band one, the  $(n - 1)^{th}$  equation in band two, and so forth. Thus, the energy equation appears in band one and the pressure equation in band two. Within each band the coefficients of the variables are placed in consecutive storage locations with the constant term appearing in the last storage location of the band.

The number of equations to be solved must appear as an integer in the low-order positions of the upper accumulator when entering the routine. For the correction equations, this is specified by the constant "SYS + 2." The results of the solution appear in the first band with the first variable appearing in location 0049-"(SYS + 1)" as shown in the following table:

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Storage location	Variable
0049 - "(SYS + 1)"	$\Delta \ln n_Z$
0049 - "(SYS)"	$\Delta \ln n_Y$
0049 - "(SYS - 1)"	$\Delta \ln n_X$
-----	-----
-----	-----
0046	$\Delta n_M$
0047	$\Delta n_N$
0048	$-\Delta \ln A$
0049	$\Delta \ln T$

Two entries to the routine are provided. The first is at location "SOLVE," and the second is at location "BACK." The first entry is used when the Gauss reduction must be performed, while the second is used when the reduction has already been accomplished and only the back solution is needed.

The solution routine can run into difficulty in several situations while carrying out the Gauss reduction. The first happens when the machine attempts to perform a floating multiplication of two numbers that are so small that the resulting product would be less than  $10^{-51}$ , and an underflow occurs. This has been taken care of for several operations by using branch on overflow commands and replacing the result of the multiplication by a zero if underflow occurs.

A second difficulty occurs when the coefficient matrix of figure 2 is singular or nearly singular; that is, its determinant is zero or very nearly so. In this case, because of the way in which the reduction is performed, the machine attempts division by zero. This problem arises when the system is such that within the precision of the calculations only one reaction product exists, as may occur for stoichiometric conditions at low temperatures. For example, in the chemical system hydrogen and oxygen at low temperatures and stoichiometric conditions, gaseous water is the only reaction product of any significance. This type of difficulty may be handled by changing the relative amounts of oxidant and fuel slightly from stoichiometric conditions (perhaps 1 to 10 parts per million) and repeating the calculation.

A third, and perhaps the most difficult, situation occurs when the coefficient matrix is poorly conditioned. For example, if the coefficient of the  $k^{th}$  variable in the  $k^{th}$  equation is small relative to the coefficients of the  $(k+1)^{th}$ ,  $(k+2)^{th}$ , . . . variables in the same equation, and if the  $k^{th}$  equation is then used to eliminate the  $k^{th}$

variable from the  $(k + 1)^{\text{th}}$ ,  $(k + 2)^{\text{th}}$ , . . . equations at an early stage of the calculations, then large rounding errors may occur. This situation occurs more often when condensed phases are present in the calculation than when only gaseous products are considered. In particular, if one chemical element appears almost exclusively in the condensed phase, the matrix element for this chemical element, which appears on the diagonal, will be very small. Should the row containing this small element be used to eliminate its variable at an early stage of the solution, then large rounding errors may occur, causing the solution vector obtained to bear little resemblance to the true solution vector.

To take care of this situation, a modified pivot method has been incorporated into the solution routine. This feature may be used at the operator's discretion, since it is console-controlled. An 8 in position one of the console (right-most position) causes pivoting. Prior to each elimination, the program examines the remaining equations and selects the best one for eliminating the next variable. The program selects the best equation to be that equation in which the coefficients differ by the smallest amount after division by the coefficient of the variable to be eliminated.

For the usual problems involving only gaseous products and those for which graphite is the only condensed phase, adequate solutions can be obtained without use of the modified pivoting routine. If no difficulty is expected, it is recommended that the pivot feature not be used, since each iteration will require more time.

Correction routine and performance-parameter routine. - The correction routine (fig. 14) applies the corrections to the estimates during the course of iteration. Once the iteration procedure has converged to a solution, the performance-parameter routine (fig. 15) calculates the performance parameters.

Auxiliary routines. - During the course of calculations it is necessary to use subroutines for exponentiation, taking square roots, and for punching the results of the calculations on Bell format cards. The subroutines that have been incorporated into the program for this purpose were taken from a collection of closed subroutines in reference 26. The three subroutines have been assembled in the locations 1833 to 1999, and a listing is given in appendix F. The arrangement of the words in and the punch band by the punching subroutine, just prior to punching, and the corresponding card columns in which they are to appear are given in appendix B.

Because of the iterative nature of the calculation, it is at times desirable to have information on the progress of the calculations. This has been provided in the form of four console-controlled punches that

may be used individually or in any combination to give intermediate answers during the iterative process. However, because of storage limitations it was necessary to consider these intermediate answer-punching routines as expendable. For this reason they were assembled in the lower portions of the P and T regions and hence can only be used at the expense of a number of reaction products. The output of the punches is on Bell format cards. The punches are as follows:

(1) Console position 2: To be used only when there are 28 or less reaction products. An 8 in position 2 of the console causes punching, in order, of  $(1 - P/P_0)$ ,  $(1 - h/h_0)$ , or  $(1 - s/s_0)$  depending upon whether it is a combustion or expansion process,  $(1 - a/a_0)$ ,  $(1 - b/b_0)$ , . . . . These are followed by the code and  $-\delta_i$  for each reaction product.

(2) Console position 3: To be used only when there are 26 or less reaction products. An 8 in position 3 of the console causes punching of P, T, and A, followed by the code and  $n_i$  for each reaction product.

(3) Console position 4: To be used only when there are 26 or less reaction products. An 8 in position 4 of the console causes punching of the entire reduced matrix, one equation at a time.

(4) Console sign: To be used only when there are 28 or less reaction products. A minus sign on the console causes punching of the solution to the reduced augmented matrix.

#### Convergence

Because of the complexity and variability of the problem, no exact analysis can be made of the rate of convergence of the iteration. It is possible, however, to obtain useful information on the rate of convergence by studying a few representative chemical systems. A function E is defined that will be used to indicate the error left in the system by the current estimates:

$$E = \left(1 - \frac{P}{P_0}\right)^2 + \left(1 - \frac{h}{h_0}\right)^2 + \left(1 - \frac{a}{a_0}\right)^2 + \dots + \sum \delta_i^2 \quad (114)$$

where the summation includes all reaction products. The first group of terms will be called the mass balance errors, and the last group will be referred to as the equilibrium errors. Using identical initial estimates in all cases - namely,  $p_i = 1$  atm,  $n_N = 1 \times 10^{-11}$  mole,  $T = 3800^\circ$  K, and  $A = 148.4$  formula weights - it was possible to construct the curves given in figures 16 to 18.

From figure 16 it is seen that  $\ln\sqrt{E}$  decreases linearly in the initial stages of the calculation, the slope increasing quite rapidly once  $E$  has been reduced to approximately 1. In other words, as convergence is approached, the rate of convergence increases. The erratic behavior of the curves for small  $E$  is due to loss of significance when convergence is essentially complete. Although the total error of the system is exponentially reduced in a rather systematic fashion, no such trend has been observed in the mass balance or equilibrium errors taken separately.

For the three cases shown in figure 16, 10 to 18 iterations were required to reduce the error to an acceptable limit when starting with poor estimates. The number of iterations may be even higher in some cases, in particular, if the temperature interval for the thermodynamic data that was selected on the basis of the initial estimate for the temperature is not the correct interval, or if there are any additions to or subtractions from the list of reaction products when the program checks for condensation of condensable materials.

The number of iterations can usually be significantly reduced if the correct assumption on the existence or nonexistence of condensed phases is made and if a good estimate for the reaction temperature and composition is available. A large number of iterations is unusual for pressure ratios other than the first, because the program uses the answers from the preceding calculation as estimates for the following point. These are generally good estimates, and therefore fewer iterations are required. This is illustrated in figure 17, where  $\ln\sqrt{E}$  is plotted as a function of the iteration number. The data in figure 17 were obtained for the reaction of equation (1) using the same initial estimates as for figure 16. As shown by figure 17, convergence to combustion and throat conditions each required 11 iterations, while the following three exit points needed only 8, 6, and 5 iterations, respectively. The performance results of this example are given in table IV.

For the problem shown in figure 17, it was assumed that the iteration procedure had converged to a solution when each of the mass balance errors, such as  $(1 - a/a_0)$ , had a magnitude less than  $5 \times 10^{-7}$  and each of the equilibrium errors  $\delta_i$  had a magnitude less than  $5 \times 10^{-6}$ :

$$\left. \begin{array}{l} \left| 1 - \frac{P}{P_0} \right| \\ \left| 1 - \frac{h}{h_0} \right| \\ \left| 1 - \frac{a}{a_0} \right| \\ \dots \end{array} \right\} < 5 \times 10^{-7}; \quad |\delta_i| < 5 \times 10^{-6}$$

These convergence criteria result in more accuracy than may be desired in some cases. For the example in figure 17, relaxing the convergence criteria by a factor of 10 permitted the total number of iterations to be reduced from 41 to 34 while still retaining five or more figures of accuracy in the final result.

When a poor set of estimates is made for the variables, the first iteration usually overcorrects the estimates and results in an increase in the value of  $E$ , as may be seen from figure 16. A solution to this problem is to restrict the size of the applied corrections. This technique is often used in iterative calculations; however, an increased number of iterations is generally required to converge. One procedure is to multiply each correction by some constant factor less than 1 (see ref. 19, e.g.). With such a technique it is often possible to induce convergence in what would normally be a divergent case, although an increased number of iterations is required. An alternative procedure has been developed that not only prevents overcorrection and produces convergence in all divergent cases that have occurred so far in this laboratory, but also often decreases the number of iterations required to reach convergence. In this procedure, the magnitude of each component of the solution vector of figure 2 must be less than a specified maximum value. If one or more components are larger than this specified maximum, the largest component is reduced to the specified maximum, and all the other components, including all  $\Delta \ln p_i$ , are reduced proportionally.

Figure 18 shows the effect of various maximum magnitudes imposed on the solution vector. Restricting the magnitudes of the components to 5 results in the fewest number of iterations for this case. In other cases a maximum component magnitude of 3 appeared to be best, particularly in systems with fewer chemical elements and reaction products.

The restriction of magnitude of the solution vector is given as an optional program and is discussed in the next section.

#### Program Modifications

The standard program is considered to be the program that first calculates combustion conditions for assigned enthalpy and pressure and then throat and other exit conditions assuming equilibrium composition of the reaction products during isentropic expansion. However, several modifications to the standard program are available.

The limitations to be discussed apply only to the particular assembly given in appendix F. If the program were assembled in some other fashion, then these limitations would no longer apply.

Assigned enthalpy for series of pressures. - The first modification permits the calculation of an assigned enthalpy problem for a series of pressures. This is accomplished by changing one instruction of the program and can be done at no sacrifice in the number of permitted reaction products.

Restriction on magnitude of solution vector. - A second modification places a size restriction on the maximum magnitude of the solution vector of the matrix of figure 2. If any component is larger than this maximum value, then all the corrections, including  $\Delta \ln p_i$ , are multiplied a number less than 1 so that the maximum component of the solution vector of figure 2 becomes equal to the maximum permitted value. This program modification may be used only if no more than 26 reaction products are being considered. In addition, only the intermediate punches controlled by console position 2 and sign may be used.

Assigned temperature and pressure. - The third program modification permits calculations for an assigned temperature and pressure. This is done at a sacrifice of five reaction products; however, the intermediate punches controlled by console position 2 and sign may be used in addition to the program change that controls the size of the solution vector. The modified program for calculations at assigned temperature and pressure is not very efficient, since the program performs many unnecessary calculations. However, a more efficient program for this type of calculation can be made with more extensive modifications. The modified pivoting routine may not be used for assigned temperature and pressure calculations. To perform calculations at an assigned temperature for a series of pressures, the program modifications for an assigned enthalpy and a series of pressures must also be included.

#### Calculations for Assumption of Frozen

#### Composition During Expansion

Rocket performance parameters are generally calculated either with the assumption of complete chemical equilibrium among the combustion products during the expansion process (equilibrium expansion) or with composition remaining fixed at combustion-chamber composition during the expansion process (frozen composition). The method for calculating performance for the first assumption has been described in the previous sections. Performance calculations for the second assumption are the same with respect to determining combustion conditions; however, determination of exit conditions, which is described in the next section, is far simpler, since the composition of reaction products is already known.

Equations for frozen-composition isentropic expansion to assigned pressure. - Since composition during expansion is fixed as the combustion-chamber composition, the following relations are obtained:

$$\frac{(p_i)_c}{(p_i)_e} = \frac{(n_i)_c}{(n_i)_e} = \frac{A_c}{A_e} = \frac{P_c}{P_e} \quad (115)$$

Substituting equation (115) into equations (18), (19), and (20) and rearranging terms give, as the condition for frozen isentropic expansion,

$$\sum_i (n_i)_c (S_T^o)_i_e + RP_c \ln \frac{P_c}{P_e} = \left[ \sum_i n_i (S_T^o)_i \right]_c \quad (116)$$

Equation (116) can be written in a form analogous to equation (20) if the following definitions are used:

$$S_e^f = \sum_i (n_i)_c (S_T^o)_i_e + RP_c \ln \frac{P_c}{P_e} \quad (117)$$

$$S_c^f = \left[ \sum_i n_i (S_T^o)_i \right]_c \quad (118)$$

for then,

$$S_e^f = S_c^f \quad (119)$$

For an assigned exit pressure, equation (117) is a function of temperature only. For any guess of exit temperature  $T$ , equation (119) will not be satisfied identically, and hence an iteration scheme again is employed to converge to correct temperature. The total differential of equation (119) in finite-difference form is

$$\Delta S^f = (S_c^f - S_e^f) = \sum_i (n_i)_c (c_P^o)_i \Delta \ln T \quad (120)$$

or

$$\Delta \ln T = \frac{\Delta S^f}{\sum_i (n_i)_c (c_P^o)_i} \quad (121)$$

Equation (121) may be used to obtain new values of  $T$  until the value of  $\Delta S^f$  is less than some assigned small value.

After convergence has been reached, the calculation of the rocket performance parameters is similar to that described for equilibrium composition during expansion.

Description of program. - Because of storage limitations, the program for the calculation of rocket performance assuming frozen composition during expansion could not be incorporated as part of the standard program for equilibrium-composition calculations. Equilibrium composition in the combustion chamber is first calculated with the standard deck. The program for frozen-composition calculations is then read into storage and calculations for frozen composition are begun. Operating instructions for this program are given in appendix D, a flow diagram in figure 19, and a SOAP listing in appendix G.

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#### VECTOR AND PROPELLANT PROGRAM

The Vector and Propellant Program was prepared in order to have a simple and almost automatic method of preparing the packed vectors and the quantities (henceforth referred to as packed propellants)  $a_f$ ,  $b_f$ ,  $c_f$ ,  $\dots$ ,  $a_x$ ,  $b_x$ ,  $c_x$ ,  $\dots$ ,  $v_f^+$ ,  $v_f^-$ ,  $v_x^+$ ,  $v_x^-$ ,  $h_f$ , and  $h_x$ . The output of this program serves as part of the input data for the Main Calculating Program (see input data routine). The storage locations for the packed propellants are  $a_x$ ,  $b_x$ ,  $c_x$ ,  $\dots$ , 537 to 546;  $h_x$ ,  $v_x^+$ ,  $v_x^-$ , 547, 548, 549;  $a_f$ ,  $b_f$ ,  $c_f$ ,  $\dots$ , 587 to 596;  $h_f$ ,  $v_f^+$ ,  $v_f^-$ , 597, 598, 599.

The flow diagrams for this program are given in figures 20 to 25 and are discussed in the section on "Calculating Routines." Operating instructions are given in appendix E, and a SOAP listing is given in appendix H. Included in the SOAP listing are two punch subroutines taken from reference 26. The format of the output of these two routines (Bell and Random) is given in appendix B. Also given in appendix B is the output format of the packed vectors.

There are ten types of input cards to the Vector and Propellant Program. The type of card is indicated by a symbol of two or three alphabetic or numerical characters appearing in columns 48, 49, and 50 of the IBM card. The data (if any) corresponding to the type of card follow in columns 51 through 72 of the card. The ten types and their functions are listed in the following table and will be discussed more fully in the following sections:

Symbol for type of input	Function	Comment
ATM	Specifies an alphabetic chemical vector for the gaseous atom; e.g., H, AL, or CL	No subscripts permitted for chemical symbol
BOP	Begins program by clearing and initializing	
END	Begins calculations (end of input data)	Begins calculation of $a_f$ , $a_x$ , $b_f$ , $b_x$ , etc.
EFn	Specifies enthalpy of $n^{\text{th}}$ fuel in cal/g-mol	$0 \leq n \leq 9^*$
EXn	Specifies enthalpy of $n^{\text{th}}$ oxidant in cal/g-mol	$0 \leq n \leq 9^*$
Fn	Specifies $n^{\text{th}}$ fuel	$0 \leq n \leq 9^*$
MOL	Specifies all reaction products that are not atoms; e.g., H1F1, N1H3, H1CLL	All subscripts must be given explicitly
PFn	Gives the weight percent or weight fraction of $n^{\text{th}}$ fuel in combined fuel	Weight percent or weight fraction in floating point $0 \leq n \leq 9^*$
PXn	Gives weight percent or weight fraction of $n^{\text{th}}$ oxidant in combined oxidant	Weight percent or weight fraction in floating point $0 \leq n \leq 9^*$
Xn	Specifies $n^{\text{th}}$ oxidant	$0 \leq n \leq 9^*$

\* $n = 1$  through 9 specifies fuel or oxidant 1 through 9, but  $n = 0$  specifies the tenth fuel or oxidant.

Only two types of cards in the preceding table are general for every problem. These are BOP and END.

## Transfer Cards

BOP - Initialize card. - The BOP card serves to initialize the program, preparing it to process a new collection of vector and propellant cards. BOP precedes all other input cards:

Input		Output
Card column		
3	+ Sign (12 punch)	
48-50	BOP	No output

END - Start calculations. - The END card follows at the end of all other input cards and serves as a transfer card to begin calculation of the packed propellants:

Input		Output
Card column		
3	+ Sign (12 punch)	
48-50	END	No output

## Input for Packed Vectors

The preparation of the packed vectors requires only two types of input cards, ATM and MOL. These two types specify the products of reaction to be considered. For bookkeeping purposes each product of reaction is given a permanent 4-digit numerical code. This permanent code also appears on the thermodynamic data cards for the same product and serves as a check during calculations in the Main Calculating Program.

ATM - Atom cards. - The ATM cards are used to specify which chemical elements will be considered in the equilibrium calculations. They are to be used only for the gaseous atoms. The reduced matrix column assignments are based on the order of appearance of the ATM cards. ATM cards must precede all the other type cards with the exception of BOP cards. The output of an ATM card is a packed vector for the gaseous atom:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	17-20	4-Digit code for gaseous element (same as 44-47 of input)
44-47	4-Digit permanent code for gaseous element	31-40	Packed chemical vector
48-50	ATM	41-80	Input reproduced
51-52	Chemical symbol for element, e.g., AL, CL, H (no numerical subscripts)		
53-80	Blank		

MOL - Molecule cards. - The MOL cards are used for the composition vectors of all reaction products that are not gaseous atoms. Thus, condensed elements such as graphite would be on MOL cards. The output of a MOL card is a packed vector for the corresponding product:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	17-20	4-Digit code for reaction product
42	Sign (- for condensed phase, + or blank for gaseous phase)	31-40	Packed chemical vector
44-47	4-Digit permanent code for reaction product	41-80	Input reproduced
48-50	MOL		
51-65	Chemical symbol for reaction product. All subscripts must be explicitly given; e.g., $\text{CH}_4$ is CLH4 $\text{H}_2\text{O}$ is H2O1 $\text{Al}_2\text{O}_3$ is AL2O3 (O is an alphabetic character)		
66-80	Blank		

### Input for Packed Propellants

A number of propellants consist of more than one fuel or one oxidant. The Vector and Propellant Program can accommodate a propellant consisting of a mixture of up to 10 fuels and up to 10 oxidants. Each fuel and each oxidant in the propellant is characterized by three cards. For the fuel, the three cards are Fn, PFn, and EFn; and for the oxidant, Xn, PXn, and EXn.

Fn - Fuel cards. - The Fn cards are used to specify the chemical formula of the  $n^{\text{th}}$  fuel, where  $n$  is any one of the integers 1, 2, 3, 4, 5, 6, 7, 8, 9, 0 (0 is used for the tenth fuel). The subscripts for elements on the fuel cards may either be integers less than 9 digits in length or floating point numbers. Either one or both forms may be used in the same Fn card. Should the chemical formula for the  $n^{\text{th}}$  fuel be too long to fit on one card (more than 22 columns) it may be continued on the next card providing that (1) the same Fn symbol is used, and (2) on the next card providing that (1) the same Fn symbol is used, and (2) the complete numerical subscript for an element is on the same card as the alphabetic symbol for the element:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	0-80	Input reproduced
43-47	Anything - never used in program		
48-49	Fn where $n = 1,2,3,4,5,6,7,8,9,0$		
50	Blank		
51-72	Chemical formula for the fuel		

Three examples are given to illustrate Fn cards:

Fuel	Columns 48-49	Columns 51-72
$\text{N}_2\text{H}_4$	F1	N2H4
$\text{C}_8\text{H}_{18}$	F1	C8H18 (or C8H1800000052)
Mixture of $\text{NH}_3$ and $\text{H}_2$	F1 F2	N1H3 H2

Xn - Oxidant cards. - The Xn cards are identical to the fuel cards except that these cards are used for the  $n^{\text{th}}$  oxidant, and Fn in card columns 48 and 49 is replaced by Xn. Two examples are given to illustrate Xn cards:

Oxidant	Columns 48-49	*Columns 51-72
H <sub>2</sub> O <sub>2</sub>	X1	H2 <sup>O</sup> 2
HN <sub>1.0529061</sub> O <sub>3.0344255</sub> (Red fuming nitric acid)	X1 X1	HN1052906151 O3034425551

\*<sup>O</sup> is an alphabetic character.

PFn - Percent fuel cards. - The percent fuel card PFn gives the weight percent of the  $n^{\text{th}}$  fuel in the fuel mixture. The percent or weight fractions must be expressed as floating point numbers. There must be a PFn card corresponding to each Fn card:

Input		Output	
Card column		Card column	
3	+ Sign (12 punch)	0-80	Input reproduced
48-50	PFn ( $n = 1,2,3,4,5,6,7,8,9,0$ )		
51-60	Weight percent of $n^{\text{th}}$ fuel in fuel mixture (a floating point number)		

Two examples are given to illustrate PFn cards:

	Columns 48-50	Columns 51-60
One fuel only	PF1	1000000053
Mixture of fuels (20 percent fuel 1, 80 percent fuel 2 by weight)	PF1 PF2	2000000052 8000000052

PXn - Percent oxidant cards. - The PXn cards are identical to the PFn cards except that they refer to the  $n^{\text{th}}$  oxidant.

EFn - Fuel enthalpy cards. - The EF<sub>n</sub> card format is identical to that of PF<sub>n</sub> and PX<sub>n</sub>, except that instead of weight percentages this type of card gives the enthalpy of the  $n^{\text{th}}$  fuel in calories per formula weight as a floating point number. An example is given to illustrate an EF<sub>n</sub> card:

	Columns 48-50	Columns 51-72
Enthalpy of N <sub>2</sub> H <sub>4</sub> (l) at 298.16° K (see eq. (97))	EFL	1547029756

EXn - Oxidant enthalpy cards. - The EX<sub>n</sub> cards are the same as the EF<sub>n</sub> card except that they refer to oxidant rather than fuel.

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#### Calculating Routines

Flow charts and tables. - Figure 20 gives a general flow chart for the Vector and Propellant Program and includes the BOP routine. Flow charts for the other routines are given in figures 21 to 25.

For the calculation of the packed propellants, the program requires a table of atomic weights and assigned oxidation states. The atomic weight table for 101 elements is located in the M region, while the corresponding table for the oxidation states is in the V region. The atomic weight table is complete, while oxidation-state assignments have been made only for several elements. Additions or alterations to the tables of atomic weights and oxidation states may be made as needed.

Formulas for propellants containing several fuels or several oxidants. - The program can prepare "packed propellant cards" for propellants containing as many as 10 fuels and 10 oxidants. The combination of all fuels is referred to as the equivalent fuel, while the combination of all oxidants is referred to as the equivalent oxidant. The necessary equations are given as follows:

According to the definitions given in previous sections,  $Z_{a_f} Y_{b_f} X_{c_f} \dots$  and  $Z_{a_x} Y_{b_x} X_{c_x} \dots$  refer to 1 gram of equivalent fuel and 1 gram of equivalent oxidant having enthalpies  $h_f$  and  $h_x$ , respectively, where  $a_f, b_f, c_f \dots$  and  $a_x, b_x, c_x \dots$  are the number of gram atoms of elements Z, Y, X, . . . in the gram of equivalent fuel and the gram of equivalent oxidant, respectively. Let the  $i^{\text{th}}$  oxidant have the formula  $Z_{a_{x_i}} Y_{b_{x_i}} X_{c_{x_i}} \dots$ , its mass  $w_{x_i}$ , and its

enthalpy  $(H_T^O)_{x_i}$ , while the  $i^{th}$  fuel has the formula  $Z_{a_{f_i}} Y_{b_{f_i}} X_{c_{f_i}} \dots$ , its mass  $W_{f_i}$ , and its enthalpy  $(H_T^O)_{f_i}$ . The total weight of oxidant is  $W_x$  and the total weight of fuel is  $W_f$ :

$$\left. \begin{aligned} W_f &= \sum_i W_{f_i} \\ W_x &= \sum_i W_{x_i} \end{aligned} \right\} \quad (122)$$

Therefore, the oxidant-to-fuel weight ratio is

$$\frac{O}{F} = \frac{W_x}{W_f} \quad (123)$$

The gram atoms of elements per gram of equivalent oxidant or fuel are

$$\left. \begin{aligned} a_x &= \frac{1}{W_x} \sum_i \frac{a_{x_i} W_{x_i}}{\mathcal{M}_{x_i}}, \quad b_x = \frac{1}{W_x} \sum_i \frac{b_{x_i} W_{x_i}}{\mathcal{M}_{x_i}}, \dots \\ a_f &= \frac{1}{W_f} \sum_i \frac{a_{f_i} W_{f_i}}{\mathcal{M}_{f_i}}, \quad b_f = \frac{1}{W_f} \sum_i \frac{b_{f_i} W_{f_i}}{\mathcal{M}_{f_i}}, \dots \end{aligned} \right\} \quad (124)$$

and the enthalpies are

$$\left. \begin{aligned} h_x &= \frac{1}{W_x} \sum_i \frac{(H_T^O)_{x_i} W_{x_i}}{\mathcal{M}_{x_i}} \\ h_f &= \frac{1}{W_f} \sum_i \frac{(H_T^O)_{f_i} W_{f_i}}{\mathcal{M}_{f_i}} \end{aligned} \right\} \quad (125)$$

Equation (124) may be used in equations (92) and (100) to obtain  $a_0$ ,  $b_0$ ,  $c_0$ ,  $\dots$  and  $V_x^+$ ,  $V_x^-$ ,  $V_f^+$ , and  $V_f^-$ , while equation (125) may be used in equation (96) to obtain  $h_0$ .

## Example

The propellant  $N_2H_4 + \frac{3}{2} H_2O_2$  has been used in this report for purposes of illustration (see eqs. (1), (93), (94), (95), (97), and (98)). This same problem will be used to illustrate the input and output of the Vector and Propellant Program and the Main Calculating Program.

The products considered, which are all gaseous, are H, N, O,  $H_2$ ,  $H_2O$ ,  $N_2$ , NO,  $O_2$ , and OH. The values of enthalpy for the propellants are similar to those on page 19 of reference 9:

$$(H_{298.16}^{\circ})_{N_2H_4(l)} = 154,702.97 \text{ cal/mol}$$

$$(H_{298.16}^{\circ})_{H_2O_2(l)} = 28,681.626 \text{ cal/mol}$$

The input and output of the Vector and Propellant Deck and the Main Operating Deck are given in tables II to V.

Lewis Research Center  
 National Aeronautics and Space Administration  
 Cleveland, Ohio, July 2, 1959

## APPENDIX A

## SYMBOLS

A	number of formula weights of equivalent reactant; also, cross-sectional area of a nozzle, sq in.
a	velocity of sound, $\sqrt{\left(\frac{\partial P}{\partial \rho}\right)_s}$ , ft/sec
a,b,c, . . .	number of gram atoms of the elements Z,Y,X, . . .
C <sub>F</sub>	thrust coefficient
C <sub>P</sub> <sup>o</sup>	molar heat capacity at constant pressure, cal/(mole)(°K)
C <sub>V</sub> <sup>o</sup>	heat capacity at constant volume, cal/(mole)(°K)
c*	characteristic velocity, ft/sec
E	internal energy per unit mass, cal/mole; also error function defined by eq. (114)
F	free energy per mole of formula weight of material, cal/mole
%F	weight or mass percent fuel
g <sub>c</sub>	gravitational conversion factor, 32.174 (lb mass/lb force)(ft/sec <sup>2</sup> )
H	sum of sensible enthalpy and chemical energy per mole or formula weight of material, cal/mole
h	sum of sensible enthalpy and chemical energy per unit mass of material, cal/g
h*	iteration parameter defined by eq. (85)
I	specific impulse with ambient and exit pressures equal, (lb force)(sec)/(lb mass)
I <sub>vac</sub>	specific impulse in vacuum (ambient pressure equal to zero), (lb force)(sec)/(lb mass)

K	thermodynamic equilibrium constant
M	Mach number
$\mathcal{M}$	molecular weight, formula weight or atomic weight
N	number
n	number of moles or formula weights of material
O/F	oxidant-to-fuel weight or mass ratio
P	static pressure (sum of partial pressures), consistent units
p	partial pressure, consistent units
$p_{vap}$	equilibrium vapor pressure of gas
Q	any function
q	symbol for $\frac{\partial(-\Delta F_T^{\circ}/RT)}{\partial \ln T} = \Delta H_T^{\circ}/RT$
R	universal gas constant, consistent units
r	equivalence ratio defined by eq. (102)
S	entropy per mole or formula weight of material
s	entropy per unit mass of material, cal/(g)(°K)
T	temperature, °K
U	velocity
V	oxidation state or volume
v	volume per unit mass
W	mass
w	mass-flow rate, (lb mass)/sec; also, weight or mass fraction
x,y	independent variables
Z,Y,X, . . .	symbols for the chemical elements

$\alpha$	activity of a material
$\gamma$	isentropic exponent, $(\partial \ln P / \partial \ln \rho)_s$
$\delta$	error in equilibrium equation, $\Delta F / RT$
$\epsilon$	area ratio
$\pi$	with a subscript, a chamber-pressure exponent defined by eq. (76)
$\rho$	mass density, consistent units

## Subscripts:

$c$	combustion chamber or condensed phase
$e$	exit points of a nozzle
$f_i$	$i^{\text{th}}$ fuel
$g$	gaseous phase
$i$	$i^{\text{th}}$ product of reaction, $i^{\text{th}}$ function, $i^{\text{th}}$ variable
$M, N$	$M^{\text{th}}, N^{\text{th}}, \dots$ condensed reaction products
$P$	constant pressure
$r$	equivalent reactant
$s$	constant entropy
$T$	at temperature $T$ ; also, constant temperature
$t$	throat of a nozzle
$V$	constant volume
$x_i$	$i^{\text{th}}$ oxidant
$Z, Y, X, \dots$	refers to chemical elements
$0$	an assigned value, equivalent reactant, or absolute zero of temperature

## Superscripts:

f	frozen composition during expansion
o	thermodynamic standard state
+	positive oxidation state
-	negative oxidation state

## APPENDIX B

## CARD FORMATS

Following are word arrangements for Bell, Random, and SOAP II output cards:

Word arrangement for Bell card:

Punch band	Card column
Word 1	11-21 (sign in 11)
Word 2	22-32 (sign in 22)
Word 3	33-43 (sign in 33)
Word 4	44-54 (sign in 44)
Word 5	55-65 (sign in 55)
Word 6	66-76 (sign in 66)
Word 7 (positions 8-5)	6-9 (location of word 1)
Word 8 (positions 8-5)	5, 77-79 (prob. no.)
Word 9 (position 5)	10 (word count)
Word 10 (positions 9-5)	80 (tab. space control) 1-4 (card number)

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## Word arrangement for Random card:

Punch band	Card column
Word 1	5-15 (sign in 15)
Word 2	20-30 (sign in 30)
Word 3	35-45 (sign in 45)
Word 4	50-60 (sign in 60)
Word 5	65-75 (sign in 75)
Word 6 (positions 8-5)	1-4 (location of word 1)
Word 7 (positions 8-5)	16-19 (location of word 2)
Word 8 (positions 8-5)	31-34 (location of word 3)
Word 9 (positions 8-5)	46-49 (location of word 4)
Word 10 (positions 8-5)	61-64 (location of word 5)
	76-80 (not used)

Word arrangement for SOAP II output (packed vectors):

Punch band	Card column	Comments
Word 9	1-10 (sign in 10), emitted 11-20 (sign in 20) 21-30 (sign in 30), emitted	Not used in program Columns 17-20 are product code Not used in program
Word 7	31-40 (sign in 40)	Packed vectors
Word 8 (position 1)	41	Reproduce input
Sign of word 7	42	
Word 1 (positions 5 to 1)	43-47	
Word 4 (positions 5 to 3)	48-50	
Word 1 (positions 5 to 1)	51-55	
Word 4 (position 2)	56	
Word 3 (positions 5 to 1)	57-61	
Word 4 (position 1)	62	
Word 5 (positions 5 to 1)	63-67	
Word 6 (positions 5 to 1)	68-72	

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## APPENDIX C

## OPERATING INSTRUCTIONS FOR MAIN CALCULATING PROGRAM

Normally the computer program will not be loaded as one instruction per card, SOAP cards, but will be subjected to some shrinking procedure that will permit loading of five or six instructions per card. (See appendix B for formats of Bell and Random cards.) Assuming this to be the case and also assuming that all input data which must be loaded are in the same card format, the following operating instructions apply for the Main Calculating Program:

## (1) Set console:

- (a) Storage entry switches (70 1951 9/8 9/8 9/8±):
  - An 8 in position 1 - pivoting during solution
  - An 8 in position 2 - punching of current errors
  - An 8 in position 3 - punching of current values for variables
  - An 8 in position 4 - punching of reduced augmented matrix
  - Minus sign - punching of solution vector for reduced augmented matrix

When the program has been loaded, the 9 in the position 7 of the console may be changed to an 8 if the operator does not wish the program to check for condensation.

- (b) Set programmed switch to STOP.
- (c) Set half-cycle switch to RUN.
- (d) Set control switch to RUN.
- (e) Set display switch to PROGRAM REGISTER.
- (f) Set overflow switch to SENSE.
- (g) Set error switch to STOP.

## (2) Place cards in the read feed so that they will be read in the following order:

- (a) Loading routine for program
- (b) Computer program
  - Equilibrium program
  - Rocket package excerpt

## (c) Input data to be loaded:

Case card  
 r card: O/F, %F, or r (any one of the three may be used)  
 Chamber-pressure card in lb/sq in. abs  
 Pressure-ratio schedule, as many as 25 pressure ratios  
 Atoms cards ( $a_f, b_f, c_f, \dots j_f;$   
 $h_f, V_f^+, V_f^-, a_x, b_x, c_x, \dots j_x; h_x, V_x^+, V_x^-$ )

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## (d) Packed vectors

## (e) Thermodynamic data as coefficients

Items (a), (b), and (c) are loaded by a loading routine, while (d) and (e) are read into storage by program read commands.

(3) Ready the punch feed with blank cards.

(4) Press computer reset key.

(5) Press program start key.

To aid in detecting errors, programmed stops have been incorporated into the program. The following list gives the card number of the instruction, in the SOAP listing, which produced the stop; the contents of the program register at the time of the stop; and the significance of the stop:

Card number	Instruction	Significance
198	HLT 0000 7766	Thermal data out of order
229	HLT 0000 7777	Elements plus condensed phases greater than 10
325	HLT 0000 8855	Trying to process a molecule or condensed phase before all atoms done
378	HLT 0000 8866	Picked up wrong thermal data for the product
635	NZU XXXX 8877	Trying to process too many condensed phases
1702	HLT 0000 9955	Overflow occurred during construction of matrix
1740	HLT 0000 9966	Overflow occurred in back solution
1827	HLT 0000 9988	Some molecules ahead of some atoms
1570	NZU XXXX 9999	End of program

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## APPENDIX D

## OPERATING INSTRUCTIONS FOR FROZEN COMPOSITION

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To carry out frozen-composition calculations it is necessary first to perform an equilibrium-combustion calculation. Thus, the initial operating instructions are identical to those of the Main Calculating Program (appendix C), with the exception that an additional instruction is included (with the input data (2)(c)) that causes the program to stop when combustion calculations are complete. The instruction loads into storage location "FROZ" (1362) and is HLT 9999 9999 (01 9999 9999).

The following instructions apply after combustion calculations are complete:

(1) Run out any cards remaining in the read hopper.

(2) Place cards in the read feed hopper so that they will be read in the following order:

- (a) Loading routine for program
- (b) Frozen-composition program
- (c) A transfer card to start program at "START"
- (d) Thermodynamic data as coefficients

(3) Press computer reset key.

(4) Press program start key.

## APPENDIX E

## OPERATING INSTRUCTIONS FOR VECTOR AND PROPELLANT PROGRAM

The following operating instructions are for the Vector and Propellant Program, which may be used to prepare input data for the Main Calculating Program:

(1) Prepare the appropriate alphabetic ATM and MOL cards. There must be one ATM card for each chemical element and one MOL card for each other product of reaction.

(2) Prepare Fn, PFn, and EFn cards for each fuel, and Xn, Px<sub>n</sub>, and EX<sub>n</sub> cards for each oxidant in the equivalent reactant.

## (3) Set console:

(a) Storage entry switches (70 1951 19 9/8 8 $\pm$ ); an 8 in position 2 - punching of fuels, oxidants, and percents and enthalpies of fuels and oxidants.

(b) Set programmed switch to STOP.

(c) Set half-cycle switch to RUN.

(d) Set control switch to RUN.

(e) Set display switch to PROGRAM REGISTER.

(f) Set overflow switch to STOP.

(g) Set error switch to STOP.

(4) Place cards in read feed so that they will be read in the following order:

(a) Loading routine for program

(b) Vector and Propellant Program

(c) Input data to be read:

BOP card (if desired)

ATM cards

MOL cards

Fn, PFn, EFn, Xn, PXn, EXn in any order

END card

(5) Ready punch feed with blank cards.

(6) Press computer reset key.

(7) Press program start key.

As an aid in the detection of errors, the following programmed stops have been included in the program:

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Card number	Instruction	Significance
337	HLT 9999 1111	Wrong symbol in ATM program
342	HLT 9999 2222	Wrong symbol in BOP program
351	HLT 9999 3333	Wrong symbol in EFn program
364	HLT 9999 4444	Wrong symbol in END program
378	HLT 9999 5555	Wrong symbol in EXn program
388	HLT 9999 6666	Wrong symbol in Fn program
395	HLT 9999 7777	Wrong symbol in MOL program
404	HLT 9999 8888	Wrong symbol in PFn program
414	HLT 9999 9999	Wrong symbol in PXn program
424	HLT 9999 0000	Wrong symbol in Xn program
460	HLT 2222 8888	Trying to process ATM card after MOL, Fn, or Xn cards
466	HLT 3333 7777	Symbol for atom has more than two letters
491	HLT 4444 6666	More than 10 atoms processed
500	HLT 5555 5555	Trying to process more condensed phases than are permitted
506	HLT 6666 4444	Formula for reaction product has more than 15 letters and digits
509	HLT 7777 3333	No chemical formula on MOL card
551	HLT 8888 2222	An element on a MOL card that did not appear on an ATM card
616	HLT 9988 9988	More than 10 ATM cards
665	HLT 4321 4321	Column equivalent for element not in table
680	HLT 2233 4455	Subscript for element greater than 10 digits
684	HLT 5544 3322	Subscript for element is 9 digits
713	HLT 8888 1111	Enthalpy or percent greater than 10 digits
784	HLT 1111 1111	Sum of percents not close enough to 100

APPENDIX F  
MAIN OPERATING PROGRAM (CHEMICAL EQUILIBRIUM)

## CHEMICAL EQUILIBRIUM PROGRAM

```

1 1          PROTECT ROCKET PACKAGE EXCERPT
2 1          BY LOADING AVAILABILITY TABLE
3 1
4 1
5 1
6      SYN FROZ    1362
7      SYN CHEK    0499
8      SYN PROR    1954
9      SYN EXP_E   1850
10     SYN SORT    1900
11     SYN PUNCH   1950
12     SYN CARDN   1852
13     SYN LINK    1855
14     SYN TEMP1   1048      LOW TEMP
15     SYN TEMP2   1049      HIGH TEMP
16     REG A0961   0980      ATOM DATA
17     REG B1247   1249      TWO 3 FOU
18     REG C9050   9050
19     REG D0001   0001
20     PLA 0001   0001
21     ALR 0037   0049
22     ALR 0087   0099
23     BLR 0137   0149
24     BLR 0187   0199
25     BLR 0237   0249
26     BLR 0287   0299
27     BLR 0337   0349
28     BLR 0387   0399
29     BLR 0437   0449
30     BLR 0487   0499
31     PLR 0537   0549
32     BLR 0587   0599
33     REG F1110   1149
34     REG G0001   0015
35     REG H0987   0999      EXTRA H E
36     REG I1001   1005
37     REG J1006   1012
38     REG K1013   1019
39     REG M9000   9000
40     REG N9015   9015      PROD DATA
41     REG P1599   1659
42     REG Q1020   1027
43     REG R1075   1099      PRES RATIO
44     REG T0660   0959      HEAT DATA
45     REG U0050   0058
46     REG Y0059   0065
47     REG Z1340   1349      PRESS ROV
48     EQU PCP    F0001
49     EQU TEE    F0002
50     EQU P     F0003
51     EQU H     F0004
52     EQU I     F0005
53     EQU M     F0006
54     EQU CF    F0007
55     EQU FPSIL  F0008
56     EQU MACH   F0009
57     EQU I_VAC  F0010
58     EQU CP    F0011
59     EQU GAMMA F0012
60     EQU LMPT   F0013
61     EQU LMTP   F0014
62     EQU S     F0015
63     EQU NI    F0016
64     EQU NT    F0017
65     EQU NEPS   F0018
66     EQU NCSTR  F0019
67     EQU CSTAR  F0020
68     EQU AW    F0021
69     EQU NAW   F0022
70     EQU HSTR   F0023
71     EQU AAY   F0024
72     EQU HC    F0025
73     EQU RECMC  F0026
74     EQU NAKT   F0027
75     EQU AKT   F0028
76     EQU HSTR?  F0029
77     EQU P1    F0030
78     EQU CONS1  F0031
79     EQU CONS2  F0032
80     EQU CONS3  F0033
81     EQU CONS4  F0034
82     EQU CONS5  F0035
83     EQU S2    F0036
84     EQU R     F0037
85     EQU GC    F0038
86     EQU IDENT F0039

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```

87      EQU ONE    F0040
88      EQU LNAAY  C0001
89      EQU LNT    C0002
90      EQU SO/R   C0003
91      EQU HO/R   C0004
92      EQU AOMOL  S0005
93      EQU BOMOL  G0006
94      EQU COMOL  G0007
95      EQU DOMOL  G0008
96      EQU EOMOL  G0009
97      EQU FOMOL  G0010
98      EQU GOMOL  G0011
99      EQU HOMOL  G0012
100     EQU IOMOL  G0013
101     EQU JOMOL  G0014
102     EQU P0    G0015
103     EQU CODE   9000
104     EQU SIR    9001
105     EQU ATOM2  9002
106     EQU T     9003
107     EQU RV000  9004
108     EQU RV001  9005
109     EQU RV002  9006
110     EQU RV003  9007      ROW VECTOR
111     EQU RV004  9008      EXTENDS
112     EQU RV005  9009      FROM 9005
113     EQU RV006  9010      TO 9018
114     EQU RV007  9011
115     EQU RV008  9012
116     EQU RV009  9013
117     EQU RV010  9014
118     EQU RV011  9015
119     EQU RV012  9016
120     EQU RV013  9017
121     EQU RV014  9018
122     EQU NI    9019
123     EQU A     9021
124     EQU B     9022
125     EQU C     9023
126     EQU D     9024
127     EQU E     9025
128     EQU F     9026
129     EQU LN NI 9027
130     EQU IA    9011
131     EQU 1B    9012
132     EQU 1C    9013
133     EQU 1D    9014
134     EQU 1E    9015
135     EQU 1F    9016
136     EQU LNNI  9017
137     EQU TWO   9028
138     EQU THREE 9029
139     EQU FOUR  9030
140     EQU CPR   9031
141     EQU S CPR 9032
142     EQU HRT   9033
143     EQU S HRT 9034
144     EQU SR    9035
145     EQU S SR   9036
146     EQU MINFX 9045
147     EQU MINCO  9046
148     EQU MAXCO 9047
149     EQU VARRL  9048
150     EQU TEM 1  9049
151     EQU TEMPO  9059
152     EQU MOVE1  9058
153     EQU MOVE2  9059
154     EQU BASIC  9050
155     EQU INDXA  THREE
156     EQU INDXC  FOUR
157     EQU S1    C0001
158     EQU ELMIN C0001
159     EQU NOROW C0000
160     SYN PDR   1193
161     SYN PC    F0000
162 1-
163 1
164 BEGIN RAU LNT      SET TO 0000 60 0002 0107
165 STL COMEX      COMBUSTION 0107 20 0111 0114
166 STD PCPCT      FIRST PC 0114 24 0017 0020
167 LDD EXP E      OVER P 0020 69 0023 1850
168 STU T          T FROM LNT 0023 21 9003 0031
169 LDD TDATA     PCP 1 0031 69 0034 0637
170 1
171 1      IF COMEX IS ZERO WE ARE DOING
172 1      COMBUSTION OTHERWISE EXPANSION
173 1      COMEX EQUALS MINUS UNITY FOR
174 1      THROAT AND PLUS UNITY FOR
175 1      EXPANSION
176 1
177 1

```

```

178 1      READ THERMAL DATA ROUTINE FOR
179 1      GENERAL ROCKET PERFORMANCE
180 1      CALCULATION
181 TDATA RAA 0000          0034 80 0000 0640
182 RAC 0000 TD001          064C 88 0000 0646
183 TD001 RCD BASIC BELL   READ CARD 064E 70 9050 1046
184 BASIC RAL 9051 RDB     ARE WE  9050 65 9051 1193
185 RDB   SLT 0004          GOING TO 1193 35 0004 0103
186       STU 9051           STORE IN 0103 21 9051 0161
187       RAU P0001 A        COPRECT 016 60 3599 0153
188       SLT 0001           PLACE   0153 35 0001 0109
189       SRT 0001           0109 30 0001 0115
190       SUP 9051           0115 11 9051 0073
191       NZU TD005          0073 44 0027 0028
192       LDD T0008 C        YES STORE 0028 69 6667 0070
193       STD 9058           THERMAL 0070 24 9058 0026
194       SET 9051           DATA    0026 27 9051 0081
195       SBB T0001 C        0081 28 6660 0113
196       AXA 0002           011 50 0002 0019
197       AXC 0010 TD001    001 58 0010 0646
198 TD005 HLT 0000 7766    WAS THE 104 60 9051 0203
199 BELL  RAU 9051           DATA JUST 0203 33 9003 0033
200       FSB T             READ IN 0033 46 0034 1037
201       BMI TDATA          FOR THE 1037 60 9003 0645
202       RAU T             CORRECT 0645 33 9050 0025
203       FSB 9050           INTERVAL 0025 46 0034 0029
204       BMI TDATA          0029 27 9050 0084
205       SET 9050           0084 28 1048 0101
206       SBB TEMP1 UNPAK

207 1
208 1      UNPACKING ROUTINE FOR GENERAL
209 1      ROCKET PERFORMANCE CALCULATION
210 1
211 1      ATOM1 IS THE NUMBER OF THE
212 1      ELEMENTS IN THE SYSTEM AND IS
213 1      IN THE I ADDRESS POSITION
214 1
215 1      SYS IS THE SUM OF ELEMENTS
216 1      AND CONDENSED PHASES IN THE
217 1      I ADDRESS POSITION AND MUST
218 1      BE LESS THAN OR EQUAL TO TEN
219 1
220 1      SYSTM IS GENERATED FROM SYS
221 1      BY SHIFTING TO THE D ADDRESS
222 1      POSITION
223 1
224 1
225 UNPAK  RAU UNITY          IS SYS  0101 60 0104 0159
226       SLT 0001           GREATER 0159 35 0001 0165
227       SUP SYS            THAN TEN 0145 11 0018 0123
228       BMI    UP000          0113 46 0076 0077
229       HLT 0000 7777        GENERATE 00'6 01 0000 7777
230 UP000  RAU SYS            00'7 60 0018 0173
231       SLT 0004           I ADDRESS 01'3 35 0004 0083
232 1      CONSTANTS
233       STU SYSTM          SYS+1 AND 00'3 21 0638 0641
234       RAL SYS            SYS+2 AND 06'1 65 0018 0223
235       ALO UNITY          ATM-1 ALSO 02'3 15 0104 0209
236       AUP 8001            D ADDRESS 02'9 10 8001 0067
237       AUP 8002            CONSTANT 00'7 10 8002 0075
238       STL SYS+1          SYSTM FROM 00'5 20 0079 0032
239       STU SYS+2          SYS AND  0012 21 0036 0639
240       RAU ATOM1          ATOM1   06'9 60 0642 0647
241       SUP UNITY          06'4 11 0104 0259
242       STU ATM-1          02'9 21 0164 0117
243       STU S CPR           CLEAR THE 0117 20 9032 0024
244       STD S HRT           SUMMATION 00'4 24 9034 0030
245       STD S SR            STORAGES 00'0 24 9036 0086
246       STD P               00'6 24 1112 0215
247       RAL STORE          SET STORE 0215 65 0068 0273
248       SLO SYSTM          ORDER FOR 0273 16 0638 0643
249       LDD UP033           SUBSCRIPT 06'4 69 1196 0649
250       SDA UP033           06'9 22 1196 1199
251       LDD TH024           SET DATA  1199 69 0102 0105
252       SDA TH024           ADDRESS OF 0105 22 0102 0155
253       LDD TH035           TH024 AND 0155 69 0108 0211
254       SDA TH035           TH035   0211 22 0108 0261
255       RAU SYS             SET SOLIDS 0251 60 0018 0323
256       SUP ATOM1          COUNTER  0323 11 0642 1047
257       STU COUNT           1047 21 0152 0205
258       STD SOLID           0205 24 0158 0311
259       SLT 0004             SET     0311 35 0004 0021
260       RSL 8003             DATA   0021 66 8003 0129
261       ALO STORE           ADDRESS OF 0129 15 0068 0373
262       LDD VM007           VM007 AND 0173 69 0126 0179
263       SDA VM007           VM048 TO 0179 22 0126 0229
264       LDD VM048           RV011R 0229 69 0082 0035
265       SDA VM048           LESS SOLID 0035 22 0082 0085
266       RAU LNT              GET T FROM 0085 60 0002 0157
267       LDD UP001 EXP E     LNT    0'57 69 0110 1850

```

268	UP001	STU T		0110	21	9003	0167
269		LDD ATOM1	SET ATOM	0167	39	0642	1045
270		STD ATOM?	COUNTER	1045	24	9002	0151
271	1	INDEX ACCUMULATOR C WILL BE					
272	1	USED FOR PICKING UP THE					
273	1	THERMAL DATA IN THE FUTURE					
274	1						
275	1						
276		RAC 0000		0151	88	0000	0207
277		RAA 001?		0207	80	0012	0163
278		RAU WIPE1 8003	CLFAR THF	0163	60	0016	8003
279	8003	STL 9007 A UP003	LAST 13	8003	20	9207	0078
280	UP003	NZA UP005 UP007	POSITIONS	0078	40	0131	0132
281	UP005	SXA 0001 8003	OF FIRST	0131	51	0001	8003
282	UP007	RAB 0011 UP009	12 BANDS	0132	82	0011	1038
283	UP009	SET 9007	FOR MATRIX	1038	27	9007	1043
284		STS 0037 A		1043	29	2037	1040
285		NZR	UP012	1040	42	1243	0644
286		SXB 0001		1243	53	0001	1299
287		AXA 0050 UP009		1299	50	0050	1038
288	UP012	SFT 9007	CLEAR THF	0644	27	9007	1299
289		STR H0001	H PEGION	1399	29	0987	1190
290		RAA 0000 UP013		1190	80	0000	1246
291	UP013	RAB 0013	CLEAR 14	1246	82	0013	0202
292		RAU WIPE2 8003	CORF LOCA	0202	60	0255	8003
293	8003	STL RV001 R UP015	FOR ROW	8003	20	9405	0066
294	UP015	NZB UP017 UP019	VECTOR	0066	42	0069	0120
295	UP017	SXB 0001 8003		0069	53	0001	8003
296	1						
297	1	INDEX ACCUMULATOR A WILL BE					
298	1	USED FOR PICKING UP THE					
299	1	CURRENT PRODUCT CODE IN FUTURE					
300	1						
301	1	DATA ADDRESS OF UP033 HAS REFN					
302	1	SFT TO RV011R MINUS SYSTM AT					
303	1	START OF UNPAK ROUTINE					
304	1						
305	UP019	RAL P0001 A	STORE PROD	0120	65	3599	0259
306		NZE MATRX	CODE IF	0253	45	0106	0257
307		SLT 0001	HERE IF NO	0106	35	0001	0213
308		NZU UP021	GO CLEAN	0213	44	0217	0118
309		SRT 0001	UP MATRIX	0118	30	0001	0125
310		STL CODE UP024		0125	20	9000	0182
311	UP021	SRT 0001	PASS UP	0217	30	0001	0223
312		STU T0008 C	SOLID AND	0423	21	6667	0170
313		STD T0010 C	SET NI AND	0170	24	6669	0022
314		AXA 0002	DELTAI TO	0022	50	0002	0128
315		AXC 0010 UP019	ZERO	0128	58	0010	0120
316	UP024	RAU P0002 A	GAS OR	0182	60	3600	0305
317		STL CHECK	CONDENSED	0305	20	0309	0112
318		HMI UP037	SET ONE OR	0112	46	0265	0116
319		PSU 8003 UP029	LEAVE ZERO	0765	61	8003	0473
320	UP029	SRT 0002 UP030	IN RV011	0473	30	0002	0279
321	UP030	SUP 8003		0279	11	8003	1197
322		STD TEMPO		1187	24	9059	1283
323		AUP ATOM2	CHECK ATOM	1293	10	9002	0201
324		NZU UP031		0201	44	0355	0156
325		HLT 0000 8855		0355	01	0000	8855
326	UP031	SLT 0001		0156	35	0001	0263
327		ALO 51	FLOAT AND	0263	15	0165	0071
328		RAB 8003 UP033	STORE THE	0071	82	8003	1196
329	UP033	STL RV011 B	SUBSCRIPT	1196	20	9415	0154
330		RAU TEMPO	GET NEXT	0154	60	9059	0361
331		NZU UP029	SUBSCRIPT	0361	44	0473	0216
332		AXA 0002 THERM		0216	50	0002	0072
333	1						
334	1	PREPARE FOR NEXT PRODUCT THEN					
335	1	GO TO THE THERMAL ROUTINE					
336	1						
337	UP037	LDD ONE	SET ONE IN	0116	69	1149	0252
338		STD RV011	RV011	0252	24	9015	0208
339		SRT 0002	IS IT ONE	0208	30	0002	0315
340		NZU UP020	ELEMENT	0315	44	0279	0220
341		STL TEMPO	YES IT WAS	0220	20	9059	0178
342		SLT 0001	IS IT AN	0178	35	0001	0135
343		RAU 8002	ATOM	0135	60	8002	1393
344		SUP UNE		1393	11	1296	0251
345		NZU UP038	IT WAS A	0251	44	0405	0206
346		RAL TEMPO UP030	MOLECULE	0405	65	9059	0279
347	UP038	PAU ATOM2	IT WAS AN	0206	30	9002	0313
348		SUP INITY	ATOM	0313	11	0104	0359
349		STD CHECK		0359	24	0309	0162
350		STU ATOM2		0162	21	9002	0119
351		RAL TEMPO		0119	65	9059	0127
352		STU TEMPO UP031		0127	21	9059	0156
353	1						
354	1	CONSTANTS FOR UNPACKING					
355	STORE	GO RV011 R 0000		0068	00	9415	0000
356	WIPE1	STL 9007 A UP003		0016	20	9207	0078
357	WIPE2	STL RV001 R UP015		0255	20	9405	0066
358	ONE	10 0000 0051		1149	10	0000	0051

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350   UNITY    00 0000  0001      0104  00 0000 0001
360   51       00 0000  0051      0156  00 0000 0051
361   UNF      10 0000  0000      1296  10 0000 0000
362 1
363 1
364 1      THERMAL ROUTINE FOR GENERAL
365 1      ROCKET PERFORMANCE CALCULATION
366 1
367 1      THE DATA ADDRESSES OF TH024
368 1      AND TH035 SHOULD BE SET TO
369 1      RVO11B MINUS SYSTEM AT START OF
370 1      UNPACKING ROUTINE
371 1
372   THERM   SET 9020      PICK UP   0072  27 9020 0177
373   LRR T0001 C      THERMAL   0177  08 6660 0363
374 1
375   RAU 9020      IS THIS   0353  60 9020 0121
376   SUP CODE      THE RIGHT  0171  11 9000 0329
377   NZU TH003      DATA     0329  44 0133 0134
378   HLT 0000  8866      0133  01 0000 8866
379   TH003   RAU P0000 A      0134  30 3598 0303
380   RMI      TH007      0303  46 0256 0307
381 1
382 1      IF DEALING WITH CONDENSED
383 1      PRODUCT SET LN NI TO ZERO
384 1
385   RAU LN NI      LN NI IS   0216  60 9027 0413
386   STL LN NI      REALLY NI  043  20 9027 0270
387   STU NI      TH009      0210  21 9019 0227
388   TH007   RAU LN NI      GET NI    0317  60 9027 0365
389   LDD      EXP E      FROM LN NI  0315  69 0168 1850
390   STU NI      TH009      0118  21 9019 0227
391   TH009   SET TWO      TWO 3 FOUR  0217  27 9028 0232
392   LDR R0001      ON CORE   0232  09 1247 0100
393   RAU D      CALCULATE  0100  60 9024 0357
394   FMP T      CPR      0357  39 9003 0160
395   FAD C      0130  32 9024 1039
396   FMP T      1019  39 9003 1042
397   FAD B      102  32 9022 0171
398   FMP T      011  39 9003 0074
399   FAD A      004  32 9021 0353
400 1
401 1      S CPR S HRT S SR MUST BE
402 1      CLEARED AT MATRIX CLEARING
403 1
404   STU CPR      033  21 9031 0411
405   FMP NI      SUM CPRXNI  041  39 9019 0214
406   FAD S CPR      IN CORE   024  32 9032 1443
407   STU S CPR      1443  21 9032 0301
408   RAU D      CALCULATE  0311  60 9024 0409
409   FDV FOUR      HRT      0409  34 9030 0212
410   FMP T      0212  39 9003 0415
411   STU TEMPO      045  21 9059 0523
412   RAU C      053  60 9023 0181
413   FDV THREE      0111  34 9029 0184
414   FAD TEMPO      0114  32 9059 0463
415   FMP T      0413  39 9003 0266
416   STU TEMPO      0216  21 9059 0573
417   RAU B      053  60 9022 0231
418   FDV TWO      0211  34 9028 0234
419   FAD TEMPO      0214  32 9059 0513
420   FMP T      053  39 9003 0316
421   STU TEMPO      0316  21 9059 0623
422   RAU F      0613  60 9025 0281
423   FDV T      0211  34 9003 0284
424   FAD TEMPO      0214  32 9059 0563
425   FAD A      0513  32 9021 1493
426   STU HRT      1443  21 9033 0351
427   FMP NI      SUM HRTXNI  0311  39 9019 0204
428   FAD S HRT      IN CORE   0214  32 9032 0183
429   STU S HRT      0113  21 9034 1041
430   RAU D      CALCULATE  1041  60 9024 1449
431   FDV THREE      SR      1449  34 9029 0302
432   FMP T      0302  39 9003 0455
433   STU TEMPO      0415  21 9059 0613
434   RAU C      0613  60 9023 0221
435   FDV TWO      0221  34 9024 0124
436   FAD TEMPO      0114  32 9059 0403
437   FMP T      0403  39 9003 0306
438   FAD B      0306  32 9022 0185
439   FMP T      0115  39 9003 1188
440   STU TEMPO      1118  21 9054 1195
441   RAU A      1155  60 9021 0453
442   FMP LNT      0453  39 0002 0352
443   FAD TEMPO      0352  32 9059 0331
444   FAD F      0311  32 9026 0461
445   FSP LN NI      SR MINUS  0461  33 9027 1191
446   STU SR      LN PI    1151  21 9035 1499
447   FMP NI      SUM SR    1459  39 9019 0402
448   FAD S SR      LESS LN PI  0402  32 9036 0381
449   STU S SR      X NI CORE  0381  21 9036 1189
450   RAU CHECK      IS IT ATOM  1189  60 0309 1063

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451 NZU TH023  
 452 1  
 453 1 REGION A IS PERMANENT STORAGE  
 454 1 OF ATOM GAS THERMAL PROPERTIES  
 455 1  
 456 RAU HRT  
 457 STU A0001 F PERMANENT 0267 60 9033 0175  
 458 PAL SR STORAGE OF 0175 21 4961 0264  
 459 STL A0011 R HRT AND SR 0264 65 9035 0271  
 460 STU T0009 C LESS LN PI 0271 20 4971 0174  
 461 STD T0010 C TH044 OF GASEOUS 0174 21 6668 0321  
 462 TH023 RAU ATM-1 ATOMS 0321 24 6669 0122  
 463 RAB 8003 SET MULT 0218 60 0164 0169  
 464 STL TEMPO FREQUENCY 0169 82 8003 0228  
 465 SET 9050 FOR RI 0228 20 9059 0136  
 466 LRB A0001 TH024 0136 27 9050 1241  
 467 TH024 RAU RV011 P 1241 08 0961 0102  
 468 NZU TH027 0102 60 9415 0459  
 469 FMP 9050 R 0459 44 1163 0314  
 470 FAD TEMPO 1163 39 9450 0366  
 471 STU TEMPO TH027 0366 32 9059 1245  
 472 TH027 NZB TH031 1245 21 9059 0314  
 473 SXB 0001 TH024 0314 42 0317 0268  
 474 TH031 RSU TEMPO 0317 53 0001 0102  
 475 FAD HRT 0266 61 9059 0225  
 476 STU RV012 OI IN 9016 0225 32 9033 0505  
 477 STD TEM 1 AND TEM 1 0505 21 9016 1213  
 478 STD T0009 C AND T REGN 1213 24 9049 0219  
 479 RAU ATM-1 SET MULT 0219 24 6668 0371  
 480 RAB 8003 FREQUENCY 0371 60 0164 0269  
 481 SET 9050 0269 82 8003 0278  
 482 LRB A0011 TH035 0278 27 9050 0233  
 483 TH035 RAU RV011 B 0233 08 0971 0108  
 484 NZU TH039 0108 60 9415 0465  
 485 FMP 9050 B 0465 44 0319 0320  
 486 FAD TEM 1 0319 39 9450 0172  
 487 STU TEM 1 TH039 0172 32 9049 0401  
 488 TH039 NZB TH043 0401 21 9049 0320  
 489 SXB 0001 TH035 0320 42 1073 0224  
 490 TH043 RAU TEM 1 1073 53 0001 0108  
 491 FSR SR DELTA I IN 0224 60 9049 0431  
 492 STU RV013 9017 0431 33 9035 0511  
 493 RSU 8003 STORE NEG 0511 21 9017 0369  
 494 STU T0010 C TH044 DELTA I IN 0369 61 8003 0277  
 495 TH044 AXC 0010 T REGION 0277 21 6669 0122  
 496 RAU HRT H OVER R 0122 58 0010 0328  
 497 FMP T IN HR 0328 60 9033 0235  
 498 STU HR 0235 39 9003 1238  
 499 RAU P0000 A 1238 21 1192 1295  
 500 BMI TH045 1295 60 3598 0503  
 501 RAU SR S PRIMED 0403 46 0356 0407  
 502 FSB ONE OVER R 0407 60 9035 0515  
 503 TH045 RAU SP TH050 0515 33 1149 0275  
 504 TH050 STU SIR TH051 IN SIR 0356 60 9035 0275  
 505 TH051 RAU COMEX 0275 21 9001 0283  
 506 NZU EXPAN COMB 0283 60 0111 0565  
 507 COMB RAU HR 0565 44 0419 0370  
 508 STL RV000 TH047 0370 60 1192 1197  
 509 EXPAN RAU SIR 1197 20 9004 0254  
 510 LDD HR 0419 60 9001 0327  
 511 STD RV000 TH047 0327 69 1192 1395  
 512 TH047 STU RV014 MULT 1395 24 9004 0254  
 513 1  
 514 1 CONSTANTS FOR THERMAL ROUTINE  
 515 ONE 10 0000 0051 1149 10 0000 0051  
 516 UNITY 00 0000 0001 0104 00 0000 0001  
 517 B0001 20 0000 0051 TWO 1247 20 0000 0051  
 518 B0002 30 0000 0051 THREE 1248 30 0000 0051  
 519 B0003 40 0000 0051 FOUR 1249 40 0000 0051  
 520 1  
 521 1  
 522 1 VECTOR MULTIPLICATION ROUTINE  
 523 1 FOR GENERAL ROCKET PERFORMANCE  
 524 1 CALCULATION  
 525 1  
 526 1 WHEN THERE ARE N EQUATIONS THE  
 527 1 NTH APPEARS IN RAND 1 AND THE  
 528 1 1ST APPEARS IN RAND N  
 529 1  
 530 1 IN THIS ROUTINE INDEX A WILL  
 531 1 TRACK THE CURRENT EQUATION B  
 532 1 WILL TRACK THE CURRENT  
 533 1 SUBSCRIPT C WILL TRACK THE  
 534 1 NUMBER OF MULTIPLICATIONS  
 535 1  
 536 1 THE SOLIDS COUNTER SHOULD BE  
 537 1 SET TO ITS MAXIMUM VALUE PRIOR  
 538 1 TO CLEARING MATRIX LOCATIONS  
 539 1

540 1 THE DATA ADDRESSES OF VM007  
 541 1 AND VM048 SHOULD BE SET TO  
 542 1 RV011B MINUS SOLID AT THE  
 543 1 START OF THE UNPACKING ROUTINE  
 544 1  
 545 1  
 546 MULT LDD 8005 VM001 STORE INDX 0561 69 8005 0367  
 547 VM001 STD INDXA A AND C 0367 24 9029 1173  
 548 LDD 8007 FOR THE 1173 69 8007 0379  
 549 STD INDXC TIME BEING 0379 24 9030 0285  
 550 RAU P0000 A IS PRODUCT 0285 60 3598 0553  
 551 BMI VM042 CONDENSED 0553 46 0406 0457  
 552 1 GASEOUS PRODUCT PROCESSING  
 553 1  
 554 1  
 555 RAU SYS+1 SET INDXA 0457 60 0079 0333  
 556 MPY 50 TO SYS+1 0333 19 0186 0456  
 557 RAA 8002 TIMES 50 0456 80 8002 0615  
 558 RSU ATOM1 SET INDEXB 0615 61 0642 1297  
 559 RAB 8003 VM002 TO ATOM 1297 82 8003 0506  
 560 1 NEGATIVED  
 561 VM002 RAC 8003 SET INDEXC 0506 88 8003 0364  
 562 LDD SOLID TO INDEXB 0364 69 0158 0611  
 563 SXC 8001 LESS SOLID 0611 59 8001 0417  
 564 SXC 0002 VM007 LESS TWO 0417 59 0002 0126  
 565 VM007 RAU RV011 B IS IT ZERO 0126 60 9415 0383  
 566 NZU VM023 SUBSCRIPT 0383 44 1237 1288  
 567 FMP NI SUBSCRIPT 1237 39 9019 1240  
 568 STU TEMPO TIMES NI 1240 21 9059 1397  
 569 SET 9037 BRING IN 1397 27 9037 0452  
 570 LDB 0037 A VM013 EQUATION 0452 09 2037 1290  
 571 VM013 RAU RV013 C 1290 60 9617 1447  
 572 NZU VM017 1447 44 0451 0502  
 573 FMP TEMPO PERFORM A 0451 39 9059 0304  
 574 FAD 9049 C MULTIPLY 0304 32 9649 0433  
 575 STU 9049 C VM017 AND ADD 0433 21 9649 0502  
 576 VM017 NZC VM021 ANY MORE 0502 48 0555 0556  
 577 AXC 0001 VM013 TO MULTPLY 0555 58 0001 1290  
 578 VM021 SET 9037 0556 27 9037 1061  
 579 STB 0037 A VM023 1C61 29 2037 1288  
 580 VM023 AXB 0001 ANY MORE 1288 52 0001 1044  
 581 NZB VM027 EQUATIONS 1044 42 1497 0648  
 582 RAA 8006 1497 60 8006 0605  
 583 SXA 0050 VM002 0605 51 0050 0506  
 584 VM027 RAA 0000 COMPLETE 0648 80 0000 0354  
 585 RAB 0001 BOTH THE 0354 82 0001 0210  
 586 RAU RV014 VM101 ENTROPY 0210 60 9018 0467  
 587 VM101 NZU VM104 AND THE 0467 44 0421 0222  
 588 FMP NI ENTHALPY 0421 39 9019 0274  
 589 STU TEMPO DURING THE 0274 21 9059 0481  
 590 RAU SYS+2 EXPANSION 0481 60 0036 1291  
 591 RSC 8003 SET INDXC 1291 89 8003 0150  
 592 SET 9037 0150 27 9037 0655  
 593 LDB 0037 A VM028 0655 09 2037 1390  
 594 VM028 RAU RV013 C DO THE 1390 60 9617 1547  
 595 NZU VM031 LAST 1547 44 0501 0552  
 596 FMP TEMPO EQUATION 0501 39 9059 0404  
 597 FAD 9049 C WHICH IS 0404 32 9649 0483  
 598 STU 9049 C VM031 ENTHALPY 0483 21 9649 0552  
 599 VM031 NZC VM035 OR ENTROPY 0552 48 1055 0606  
 600 AXC 0001 VM028 1055 58 0001 1390  
 601 VM035 SET 9037 0606 27 9037 1161  
 602 STB 0037 A VM104 1161 29 2037 0222  
 603 VM104 NZB VM036 DURING 0222 42 0325 0176  
 604 SXB 0001 EXPANSION 0325 53 0001 0531  
 605 RAA 0950 ENTHALPY 0531 80 0950 1287  
 606 RAU RV000 VM101 EQUATION 1287 60 9004 0467  
 607 1 IS IN 095  
 608 1 BAND  
 609 1 ALSO FILL  
 610 1  
 611 VM036 RAU SYS+2 IN THE 0176 60 0036 1391  
 612 STL RV011 PRESSURE 1391 20 9015 1198  
 613 RSC 8003 EQUATION 1198 89 8003 0656  
 614 SET 9037 0656 27 9037 1211  
 615 LDB 0087 VM037 1211 09 0087 1440  
 616 VM037 RAU RV013 C 1440 60 9617 1597  
 617 NZU VM039 1597 44 0551 0602  
 618 FMP NI 0551 39 9019 0454  
 619 FAD 9049 C 0454 32 9649 0533  
 620 STU 9049 C VM039 0533 21 9649 0602  
 621 VM039 NZC VM041 0602 48 1105 1056  
 622 AXC 0001 VM037 1105 58 0001 1440  
 623 VM041 SET 9037 1056 27 9037 1261  
 624 STB 0087 1261 29 0087 1490  
 625 RAU NI SUM PI 1490 60 9019 1697  
 626 FAD P 1697 32 1112 1239  
 627 STU P VM061 1239 21 1112 1065  
 628 1

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629 1 CONDENSED PRODUCT PROCESSING  
 630 1  
 631 1 COUNT IS NUMBER OF UNPROCESSED  
 632 1 CONDENSED PRODUCTS  
 633 1  
 634 VM042 RAU COUNT 0406 60 0152 0507  
 635 NZU 8877 0507 44 1311 8877  
 636 1  
 637 1 ARE WE TRYING TO PROCESS TOO  
 638 1 MANY CONDENSED PHASES  
 639 1  
 640 RSR 8003 SET THE 1311 83 8003 0420  
 641 ALO 8003 INDICES TO 0420 15 8003 0377  
 642 SUP UNITY STORE 0377 11 0104 0509  
 643 ALO 8001 CONDENSED 0509 15 8001 0517  
 644 STU COUNT PHASE 0517 21 0152 1155  
 645 RAU 8002 EQUATION 1155 60 8002 1263  
 646 MPY 50 AND ITS 1263 19 0186 1106  
 647 RAA 8002 ENTHALPY 1106 80 8002 1165  
 648 1 OR ENTROPY  
 649 SET RV001 STORE THE 1165 27 9005 0470  
 650 STB 0037 A EQUATION 0470 29 2037 1540  
 651 RAU RV014 STORE THE 1540 60 9018 1747  
 652 STU 0047 P ENTHALPY 1747 21 4047 0200  
 653 1 OR ENTROPY  
 654 FMP NI COMPLETE 0200 39 9019 0603  
 655 FAD 0047 ENTHALPY 0603 32 0047 1223  
 656 STU 0047 ROW 1223 21 0047 0250  
 657 RAU COMEX 0250 60 0111 1215  
 658 NZU VM111 1215 44 0469 0520  
 659 RAU RV000 0469 60 9004 0427  
 660 STU H0011 R 0427 21 4997 0300  
 661 FMP NI 0300 39 9019 0653  
 662 FAD H0011 0653 32 0997 1273  
 663 STU H0011 VM111 1273 21 0997 0520  
 664 VM111 RAU SYS+1 COMPLETE 0520 60 0079 0583  
 665 MPY 50 THE COLUMN 0583 19 0186 1156  
 666 RAA 8002 FOR AAY 1156 80 8002 1265  
 667 RAU ATOM1 1265 60 0642 1797  
 668 RSB 8003 VM048 1797 83 8003 0082  
 669 VM048 RAU RV011 B 0082 60 9415 1289  
 670 NZU VM051 1289 44 1543 1194  
 671 FMP NI 1543 39 9019 1396  
 672 FAD 0047 A 1396 32 2047 1323  
 673 STU 0047 A VM051 1323 21 2047 1194  
 674 VM051 AXR 0001 1194 52 0001 0350  
 675 NZR VM061 0350 42 1053 1065  
 676 SXA 0050 VM048 1053 51 0050 0082  
 677 VM061 RAA INDXA GO TO NEXT 1065 60 9029 1373  
 678 RAC INDXC UP013 PRODUCT 1373 88 9030 1246  
 679 1  
 680 1 CONSTANTS FOR VECTOR MULTIPLY  
 681 1 ROUTINE  
 682 50 00 0000 0050 0186 00 0000 0050  
 683 1  
 684 1  
 685 1 MATRIX CLEAN UP ROUTINE FOR  
 686 1 GENERAL ROCKET PERFORMANCE  
 687 1 CALCULATION  
 688 1  
 689 MATRX RAU LNAAY GET AAY 0257 60 0001 1205  
 690 LDD MC003 EXP E FROM 1205 69 0258 1850  
 691 MC003 STU AAY LNAAY 0258 21 1133 0236  
 692 LDD ATM-1 SET INDXB 0236 69 0164 0567  
 693 RAB 8001 TO ATM-1 0567 82 8001 1423  
 694 RAU SOLID 1423 60 0158 1313  
 695 AUP UNITY SET INDXA 1313 10 0104 0559  
 696 AUP 8001 TO SOLID 0559 10 8001 0617  
 697 MPY 50 PLUS TWO 0617 19 0186 1206  
 698 RAA 8002 MC007 TIMES 50 1206 80 8002 1315  
 699 1  
 700 MC007 RAU AMOL R MC009 ADD MASS 1315 60 4005 0609  
 701 MC009 FMP AAY BALANCE 0609 39 1133 0653  
 702 STU TEMPO AND 0633 21 9059 1441  
 703 FSA 0047 A ENTHALPY 1441 33 2047 1473  
 704 FAD 0049 A OR ENTROPY 1473 32 2049 0375  
 705 STU 0049 A DELTAS TO 0375 21 2049 0652  
 706 1 MATRIX  
 707 RAU TEMPO STORE 0652 60 9059 0659  
 708 FSA 0047 A ERRORS 0659 33 2047 1523  
 709 FDV TEMPO 1523 34 9059 0226  
 710 STU RV002 R 0226 21 9406 0983  
 711 RMA MC031 0983 43 0286 1337  
 712 NZR MC015 MC017 1337 42 1590 1491  
 713 MC015 SXB 0001 1590 53 0001 1446  
 714 AXA 0050 MC007 1446 50 0050 1315  
 715 MC017 RAA 0000 1491 80 0000 1298  
 716 RSB 0001 1298 63 0001 0504  
 717 RAU COMEX 0504 60 0111 1365  
 718 NZU MC019 MC021 1365 44 0519 0570  
 719 MC019 LDD S SR PLACE S/R 0519 69 9036 0425  
 720 STD 0047 TN ENTRONY 0425 24 0047 0400

			ROW AND COLUMN A	0400	60 0003 0609
721		RAU SO/R	MC009	0570	60 0004 0609
722	1	RAU HO/R	MC009	0286	60 0015 0569
723	MC021	RAU PO		0569	33 1112 1339
724	MC031	FSR P		DELTA TO	1339 21 9059 1398
725		STU TEMPO		MATRIX	1598 32 0099 0475
726		FAD 0099		C475	21 0099 1052
727		STU 0099		STORE	1052 60 9059 1059
728		RAU TEMPO		ERROR	1059 34 0015 1415
729		FDV PO			1415 21 9004 1573
730		STU RV000	MC103		
731		RAU COMEX		COMPLETE	1573 60 0111 1465
732	MC103	NZU MC109	MC105	ENTROPY	1465 44 0619 0620
733		RAU S CPR		AND THE	1620 60 9032 0477
734	MC105	FMP T		ENTHALPY	1477 39 9003 0080
735		FAD 0048		EQUATIONS	1080 32 0048 0525
736		STU 0048			0525 21 0048 0601
737		SFT 9037			1601 27 9037 1256
738		LDR 0037			1256 09 0037 1690
739		SFT 9037			1690 27 9037 1445
740		STU H0001	MC115		1445 29 0987 1740
741		RAU S CPR			0619 60 9032 0527
742	MC109	FAD 0048			0527 32 0048 0575
743		STU 0048			0575 21 0048 0651
744		RAU S CPR			0651 60 9032 1159
745		FMP T			1159 39 9003 0262
746		FAD 0998			0262 32 0998 0625
747		STU 0998	MC115		0625 21 0998 1740
748					
749	1			DURING COMPLETION OF SYMMETRIC	
750	1			PORTIONS OF MATRIX FOR GAS	
751	1			PHASE INDEXA WILL TRACK THE	
752	1			EQUATION BEING USED INDEXB	
753	1			WILL TRACK THE DIAGONAL	
754	1			POSITION AND INDEXC WILL TRACK	
755	1			THE CURRENT MOVE OPERATION	
756	1				
757	1			THE PHASE TEST WORD CHECK IS	
758	1			ZERO FOR GAS REFLECTION AND	
759	1			UNITY FOR SOLID REFLECTION	
760	1				
761	1				
762	MC115	RSU SOLID		1740 61 0158 1363	
763		SLT 0004		SET CHECK	1363 35 0004 1673
764		STL CHECK		TO GAS	1673 20 0309 0312
765		AUP LDD			0312 10 1515 1069
766		STU MOVE1		GENERATE	1069 21 9058 0577
767		RSU SYSTM		MOVE1 AND	0577 61 0638 1593
768		AUP STD		MOVE2	1593 10 1496 1051
769		STU MOVE2		ORDERS	1051 21 9059 1209
770		RAU ATM-1		SET INDXB	1209 60 0164 1169
771		NZU MC151		TO ATM-1	1169 44 1723 0324
772		RSR 8003	MC117	NEGATIVE	1723 83 8003 0282
773	MC117	LDD 8006		SET INDXC	0282 69 8006 1338
774		RAC 8001		TO INDXB	1338 88 8001 1244
775		RSU 8001		INDEXA IS	1244 61 8001 1101
776		AUP SOLID		SOLID PLUS	1101 10 0158 1413
777		AUP UNITY		TWO MINUS	1413 10 0104 1259
778		AUP 8001		INDXB ALL	1259 10 8001 1067
779		MPY 50		TIMES 50	1067 19 0186 1306
780		RAA 8002			1306 80 8002 1565
781		LDD 8005		GAS	1565 69 8005 0471
782		STD INDXA	MC123		0471 24 9029 0627
783	MC121	LDD 8005		CONDENSED	0450 69 8005 1356
784		STD INDXA			1356 24 9029 0362
785		RSU 8006			0362 61 8006 1219
786		AUP UNITY			1219 10 0104 1309
787		MPY 50			1309 19 0186 1406
788		RAA 8002	MC123		1406 80 8002 0627
789	MC123	SET 9037			0627 27 9037 0332
790		LDR 0037 A			0332 09 2037 1790
791		RAA INDXA			1790 80 9029 1448
792		RAU MOVE1			1448 60 9058 1255
793		ALO MOVE2	8003	REFLECT	1255 15 9059 8003
794	8003	LDD 9046 C	8002	ONE	8003 69 9646 8002
795	8002	STD 0047 A	MC133	EQUATION	8002 24 2047 0500
796	MC133	NZC MC135	MC139	AT A TIME	0500 48 1103 0554
797	MC135	AXC 0001			1103 58 0001 1359
798		SXA 0050	8003		1359 51 0050 8003
799	MC139	AXB 0001			0554 52 0001 0260
800		NZB MC151			0260 42 1463 0324
801		ALO UNO			1463 15 0416 0521
802		STL MOVE2	MC143		0521 20 9059 0378
803	MC143	RAU CHECK		GAS OR	0378 60 0309 1513
804		NZU MC160	MC117		1513 44 1167 0282
805	MC151	RAU SOLID		ANY SOLIDS	0324 60 0158 1563
806		NZU MC153	MC041	IN SYSTEM	1563 44 1217 0318
807	MC153	RAU CHECK			1217 60 0309 1663
808		NZU MC041	MC159		1663 44 0318 0368
809	MC159	ALO UNITY		SET CHECK	0368 15 0104 1409
810		STL CHECK		TO SOLID	1409 20 0309 0412
811		RSU SOLID		GENERATE	0412 61 0158 1713
812		SLT 0004			1713 35 0004 1773

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813      STM TEMPO          MOVE1 AND   1773  21 9059 0581
814      AUP LDP          MOVE2 FOR   0581  10 1514 1269
815      STM MOVE1          CONDENSED  1269  21 9059 1177
816      RAU TEMPO          PHASEF    1177  60 9059 0335
817      AUP STD          0335  10 1494 1151
818      STM MOVE2          1151  21 9059 1459
819      RAU SOLID          INDEXP IS  1459  60 0159 1763
820      RSR 8003 MC160      NFG SOLID  1763  83 8003 1167
821      LDD ATY-1          INDEXC IS  1167  69 0164 1267
822      RSC 8001          ATM-1     1267  89 8001 1823
823      !                   NEGATIVEN
824      RAU SYS+1          INDEXA IS  1823  60 0079 1033
825      MPY 50              SYS+1    1033  19 0186 1456
826      RAA 8002 MC121      TIMES 50   1456  10 8002 0450
827      !
828      !                   AT THIS POINT DECIDE IF
829      !                   ITERATION WILL BE NEEDED
830      !                   BY TESTING ON EXPONENT EACH
831      !                   DELTA MUST BE LESS THAN
832      !                   SOME SPECIFIED VALUE
833      !
834      MC041  PAR 0052 MC042      EXP TEST   0318  82 0052 0374
835      !
836      MC042  RAU ATOM1          CONTINUED  0374  60 0642 1498
837      AUP UNITY          UNTIL THE 1498  10 0104 1509
838      RAC 8003 MC043      EXPONENT  1509  88 8003 0418
839      MC043  RAU RV000 C      OF DELTAS  0418  60 9604 1175
840      FAD 8006          IS FIGHT   1175  32 8006 1305
841      NZU MC053          LESS THAN 1305  44 1559 0310
842      NZC               THAT GIVEN 0310  48 1813 0414
843      SXC 0001 MC043      BY WORD   1813  59 0001 0418
844      MC049  PAR 0054 MC050      IN INDEXP 0414  82 0054 1070
845      MC050  RAA 0000          1070  80 0000 0276
846      RAC 0000 MC051          0276  88 0000 0382
847      MC051  RAU P0001 A      0382  60 3599 1153
848      NZU               MC052          1153  44 0557 0308
849      RAU T0010 C          DEL SUB I  0557  60 6669 0424
850      AXA 0002          0424  50 0002 0130
851      AXC 0010          0130  58 0010 0336
852      FAD 8006          0336  32 8006 1665
853      NZU MC053 MC051      1665  44 1559 0382
854      MC052  RAU TESTX          CONVERGED 0308  60 1361 1715
855      NZU MC054          IF ERROR  1715  44 1319 1170
856      LDD UNITY          LESS THAN 1170  69 0104 0607
857      STD TESTX          EXPON 45  0607  24 1361 0464
858      PAR 0053 MC050      ONCE OR   0464  82 0053 1070
859      !
860      !
861      !
862      !                   WHEN CONVERGED GO TO MC054
863      !
864      MC054  LDD T          SAVE TEMP  1319  69 9003 1225
865      STD TEE          ON DRUM   1225  24 1111 0514
866      SET 9050          WAS THE   0514  27 9050 1369
867      LPP TEMP1          ITERATION 1369  08 1048 1201
868      RAU 9051          DONE WITH 1201  60 9051 1709
869      FSP T             THE RIGHT 1709  33 9003 1389
870      PMI MC058          THERMAL  1389  46 1242 1694
871      RAU T             DATA    1693  60 9003 1251
872      FSP 9050          1251  33 9050 0631
873      PMI MC058          0631  46 1242 0385
874      !
875      !                   ROUTINE TO CHECK ON TRANSITION
876      !                   FROM GAS TO CONDENSED PHASE
877      !
878      !                   IF POSITION 7 ON THE CONSOLE
879      !                   IS AN FIGHT CONDENSING
880      !                   PROGRAM IS PASSED BY
881      !
882      !                   THE PROGRAM ASSUMES THAT BOTH
883      !                   GAS AND CONDENSED VECTOR ARE
884      !                   IN STORAGE
885      !
886      LDD 8000          0385  69 8000 1541
887      R07 DONE          1541  97 1294 1546
888      STL SW1          INITIALIZE 1546  20 1301 0604
889      RAA 0000          SWITCH SW1  0604  80 0000 0360
890      RAC 0000 MC201      0360  88 0000 0466
891      MC201  RAU P0001 A      ANY MORE  0466  60 3599 1203
892      NZU               MC230      PRODUCTS  1203  44 0657 0358
893      RAU P0002 A      YES IS IT  0657  60 3600 1355
894      PMI               MC227      GASEOUS  1355  46 0404 1759
895      RAU P0001 A      NO     0408  65 3599 1259
896      SET 0001          WAS THE   1252  35 0001 1809
897      NZU MC205          SOLID USED 1809  44 0564 0614
898      RAU T0008 C      YES IS NI  0614  65 6667 0571
899      PMI               MC227      NEGATIVE 0571  46 0474 1759
900      RAU UNITY          YES IGNORE 0474  60 0104 0410
901      SRT 0001          THIS SOLID 0410  30 0001 1317
902      ALD P0001 A      NEXT TIME 1317  15 3599 1303
903      STL P0001 A      1303  20 3599 1102
904      PMI UNITY MC219          1102  61 0104 0460

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905	MC205	RAB 0000		NO LOCATE	1564	82 0000 1220
906		RAU P0002 A MC207		THE GAS	1220	60 3600 1405
907	MC207	AUP 00002 R		PHASE	1405	10 5600 1455
908		NZU MC211		VECTOR	1455	44 0510 0560
909		SUP 8001			1510	11 8001 1367
910		AXR 0002 MC207			1367	52 0002 1405
911	MC211	RAU 8006		FOUND IT	1560	60 8006 1417
912		MPY FUNF			1417	19 1270 1591
913		PAR 8002			1591	82 8002 1549
914	1					
915	1		INDEX C LOCATES SOLID AND			
916	1		INDEX B THE GAS PHASE DATA			
917	1					
918		LDD 8007		STORE	1549	69 8007 1505
919		STD INDXC		INDEX C	1505	24 9030 1411
920		LDD TEE		GET T TWO	1411	69 1111 1064
921		STD T		AND THREE	1064	24 9003 1320
922		SET TWO		FOR CORE	1320	27 9028 1275
923		LBR P0001			1275	08 1247 0550
924		LDD MC215 F/RT			0550	69 1353 1506
925	F/RT	STD LTK		CALCULATES	1506	24 1855 0458
926		SET 9010		F/RT FOR	0458	27 9010 1164
927		LBR T0001 C		SOLID AND	1164	08 6660 1214
928		RAU 1F		GAS	1214	60 9015 0621
929		FDV T			0621	34 9003 0524
930		STU TEM1			0524	21 0428 0981
931		RAU 1D			0981	60 9014 1439
932		FDV TWO			1439	34 9029 1292
933		FMD T			1292	39 9003 1495
934		FAD 1C			1495	32 9013 1325
935		FDV THREE			1325	34 9029 0478
936		FMD T			0478	39 9003 1031
937		FAD 1B			1031	32 9012 1461
938		FDV TWO			1461	34 9028 1264
939		FMD T			1264	39 9003 1467
940		FAD 1F			1467	32 9016 1548
941		FSR TEM1			1548	33 0428 1555
942		STU TEM 1			1555	21 9049 1314
943		RAU ONE			1314	60 1149 1403
944		FSR LNT			1403	33 0002 0429
945		FMD 1A			0429	39 9011 0432
946		FSR TEM 1 LINK			0432	33 9049 1855
947	MC216	STU TEMPO		STORE F/RT	1253	21 9059 1511
948		LDD 8006			1511	69 8006 1517
949		PAC 8001			1517	88 8001 0574
950		LDD MC217 F/RT			0574	69 1227 1506
951	MC217	RSU 8003		CHECK FOR	1227	61 8003 0435
952		FAD TEMPO		CONDENSING	0435	32 9059 1765
953		FSR LNNI			1765	33 9017 1545
954		PMI MC225			1545	46 1598 1699
955		RAU P0001 A		IT SHOULD	1598	60 4599 1453
956		SLT 0001		HAVE BEEN	1453	35 0001 0610
957		SPT 0001		CONDENSED	0610	30 0001 1567
958		STU P0001 A		FIX IT	1567	21 4599 1152
959		RAU UNITY MC219			1152	60 0104 0460
960	MC219	AND SYS			0460	10 0018 0624
961		STU SYS			0624	21 0018 1071
962		LDD UNITY		SET SWITCH	1071	69 0104 1057
963		STD SW1 MC225			1057	24 1301 1699
964	MC225	PAC INDXC MC227		ADVANCE TO	1699	88 9030 1759
965	MC227	AXA 0002		THE NEXT	1759	50 0002 1815
966		AXC 0010 MC201		PRODUCT	1815	58 0010 0466
967	MC220	CTL TESTX			0358	20 1361 1264
968		RAU SW1			1364	60 1301 1705
969		NZU UNPAK DONE		ANY WRONG	1705	44 0101 1294
970	DONE	LDD S SR		PRODUCTS	1794	49 9036 0600
971		STD S		SUMMATIONS	0600	24 1124 1277
972		LDD S HPT		OF S/P AND	1277	69 9034 1183
973		STD H		H/RT ON	1183	24 1113 0516
974		LDD ATY-1		DRUM	1184	INDXA IS 0516 49 0164 1667
975		PAC 8001		ATM-1 NEG	1667	89 8001 1074
976		LDD SYS#2		INDXA IS	1074	69 0036 1489
977		RSF 8001		SYS#2 NEG	1489	81 8001 1595
978		SET 9059 C		STORE	1595	27 9659 0650
979		LBR 8009 A		PRESSURE	0650	08 2059 1202
980		SET 9059 C		ROW IN	1202	27 9659 1107
981		SRP Z0010 C MC057		7 REGION	1107	28 7349 1252
982	MC058	STL TESTX MC059			1242	20 1361 1414
983	1					
984	1		TEST CONSOLE FOR PUNCHING			
985	1		INTERMEDIATE ANSWERS			
986	1					
987	MC053	LDD ITERA TEST1			1559	69 0462 0566
988	MC057	LDD DERIV TEST1			1252	69 1755 0566
989	MC059	LDD MC060 TEST1			1414	69 1717 0566
990	MC060	LDD TEE TEST1			1717	69 1111 1464
991		STD T	TDATA		1464	24 9003 0034
992	TEST1	STD LTK1			0566	24 1412 0272
993		LDD 8000			0772	69 8000 0528
994		AND DELS NEXT1		TEMPORARY	0528	92 1181 1233
995	NEXT1	LDD 8000		PUNCHES	1233	69 8000 1539
996		AND VARIA NEXT2		FOR	1539	93 1392 1394

Line Number	Statement	Program	Program	Line Number	Statement	Program	Program
997	NEXT? LDD 8000	PROGRAM	1394	69	R000 1000		
998	R04 MATRIX LINK1	CHECKING	1000	94	1502 1419		
999 1							
1000 1	CONSTANTS FOR MATRIX						
1001 1	CLEAN UP ROUTINE						
1002 1	LDD 9045 C 8002		1515	69	9646 R002		
1003 1	STD 0007 A MC132		1496	24	2047 0500		
1004 1	IND 00 0001 0000		0416	00	0001 0000		
1005 1	FUNE 00 0000 0005		1270	00	0000 0005		
1006 1							
1007 1							
1008 1	ROUTINE FOR CALCULATING THE						
1009 1	CORRECTIONS TO THE CURRENT						
1010 1	COMPOSITIONS AAY AND THE						
1011 1	TEMPERATURE						
1012 1							
1013 1	ITERA PAU SYS+2 NEW00	SOLVE FOR	0462	60	0036 1691		
1014 1	NEW00 LDD NEW01 SOLVE	CORRECTIONS	1691	69	1444 1698		
1015 1	NEW01 LDD SYS+2	LOAD	1444	69	0016 1589		
1016 1	RSR 8001	VARIABLES	1589	83	8001 1695		
1017 1	SET M0001	IN	1495	27	9000 1050		
1018 1	LDR 00050 R NEW02	M-REGION	1050	09	4050 1553		
1019 1							
1020 1	INDEXA WILL TRACK THE PRODUCT						
1021 1	CORE AND INDEXC WILL TRACK						
1022 1	THE LN NI						
1023 1							
1024 1	NEW02 PSA 0002		1553	81	0002 0960		
1025 1	PSC 0010		0960	89	0010 0616		
1026 1	LDD SOLID		0616	69	0158 1561		
1027 1	STD COUNT NEW03		1561	24	0152 1805		
1028 1							
1029 1	NEW03 LDD ATOM1		1805	69	0642 1745		
1030 1	PAB 0010	CLEAR 11	1745	82	0010 1951		
1031 1	PAU WIPE9 8003	CORE	1351	60	0654 8003		
1032 1	8003 STL N0001 R NEW04	LOCATIONS	8003	20	9415 1066		
1033 1	NEW04 NZB NEW06	FOR ROW	1066	42	1469 1370		
1034 1	SXP 0001 8003	VECTOR	1469	53	0001 8003		
1035 1	WIPE9 STL N0001 R NEW04		0654	20	9415 1066		
1036 1							
1037 1	NEW06 AXA 0002		1370	50	0002 0326		
1038 1	AXC 0010		0326	58	0010 0482		
1039 1	PAL P0001 A	DO WE HAVE	0682	65	3599 1703		
1040 1	NZB NEW07 NEW18	A PRODUCT	1703	45	1556 1157		
1041 1	NEW07 SLT 0001	YES USE	1556	35	0001 1514		
1042 1	NZB NEW08 NEW08	OR BYPASS	1514	44	1370 0468		
1043 1							
1044 1	NEW08 PAU P0002 A	TEST FOR	0468	60	3600 1706		
1045 1	PMI NEW20 NEW10	CONDENSED	1706	46	1060 1160		
1046 1							
1047 1	NEW10 SRT 0002	GET THF	1160	30	0002 1767		
1048 1	SUP 8003	MOLECULE	1767	11	8003 1375		
1049 1	STD TEMPO	SURSCRIPTS	1775	24	9059 1231		
1050 1	SLT 0001	AND LOCATE	1231	35	0001 1387		
1051 1	ALO 51	POSITION	1387	15	0166 1171		
1052 1	PAB 8003	TO STORE	1171	82	8003 0180		
1053 1	STL N0001 R	STORE	0180	20	9415 1388		
1054 1	PAU TEMPO	SURSCRIPTS	1388	60	9059 1795		
1055 1	NZB NEW10	IN CORE	1795	44	1160 1100		
1056 1	LDD SYS+2	LOAD	1100	69	0036 1689		
1057 1	PAB 8001	O1 AND	1689	82	8001 1596		
1058 1	SFT N0000 R	DELTAI	1596	27	9414 1401		
1059 1	LDR T0009 C NEW15	ON CORE	1401	09	6668 1221		
1060 1							
1061 1	NEW15 SET C0001	ROUTINE	1221	27	9050 0376		
1062 1	LPR 00001 C0001	FOR	0376	08	1020 9050		
1063 1	SXR 0001 C0002	DEL LN PI	1020	53	0001 9051		
1064 1	00002 PAU M0001 R C0003		1021	60	9400 9052		
1065 1	00003 FMP 00001 R C0004		1022	39	9415 9053		
1066 1	00004 FAD N0002 R C0005		1023	32	9416 9054		
1067 1	00005 STU N0001 R C0006		1024	21	9415 9055		
1068 1	00006 NZB C0001 C0007		1025	42	9050 9056		
1069 1	00007 FAD T0008 C C0008		1026	32	6667 9057		
1070 1	00008 STU T0008 C NEW03	NEW LN NI	1027	21	6667 1805		
1071 1		FOR GAS					
1072 1	NEW20 LDD COUNT	NEW NI	1060	69	0152 1756		
1073 1	RSR 8001 NEW21	FOR	1756	83	8001 0512		
1074 1	PAU D0048 R NEW22	CONDENSED	0512	60	4048 1753		
1075 1	NEW22 FAD T0008 C		1753	32	6667 1743		
1076 1	STU T0008 C		1743	21	6667 1420		
1077 1	PAU COUNT	DECRAESE	1420	60	0152 1207		
1078 1	SUP UNITY	COUNT	1207	11	0104 1210		
1079 1	STU COUNT NEW06	FOR SOLIDS	1210	21	0152 1370		
1080 1							
1081 1	NEW18 PAU D0049 NEW19	NEW LNT	1157	60	0049 1803		
1082 1	FAU LNT		1803	32	0002 0479		
1083 1	STU LNT NEW60		0479	21	0002 1806		
1084 1	PSU D0048 NEW61	NEW LNA	1806	61	0048 1104		
1085 1	FAU LNAAY		1104	32	0001 1327		
1086 1	STU LNAAY		1327	21	0001 1154		
1087 1	PAU 8000	PUNCH THE	1154	60	8000 1661		
1088 1	PSU DELX UMPAK	CORRECTION	1661	46	1564 0101		
1089 1							

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1090 1           START NEW ITERATION AT UNPAK
1091 1
1092 1
1093 1           PERFORMANCE PARAMETER ROUTINE
1094 1
1095 1           WHEN ITERATION IS COMPLETED
1096 1           ENTER AT DERIV
1097 1
1098  DERIV  RAU SYS+2  D1      SOLVE FOR  1755  60 0036 1741
1099  D1      LDD 2LESS  REDUC  DLNP1/   1741  69 1494 1748
1100  2LESS  RAU SYS+1          DLNT AT   1494  60 0079 1283
1101  LDD CP 1  SOLVE    CONSTANT P  1281  69 0386 1698
1102  CP 1  LDD SYS+1          LOAD     0386  69 0079 0532
1103  RSA 8001          PARTIALS  0532  81 8001 1438
1104  RAR 8001          DLNP1/   1438  82 8001 1544
1105  SET MC0001          DLNT AT   1544  27 9000 1749
1106  LDR D00050 A  CONSTANT P  1749  09 2050 1204
1107 1
1108 1
1109  SET MC0001          ENTHALPY  1204  27 9015 1260
1110  LDR MC0012 A CP 2  ROW MOVED  1260  09 2998 1451
1111 1
1112 1
1113  CP 2  SXP 0001          CALCULATE 1451  53 0001 1257
1114  PSU MC0001 R  SPECIFIC  1257  61 9400 1166
1115  EMP MC0001 R  HEAT TIMES 1166  39 9415 1519
1116  FAD MC0002 R  MOLECULAR 1519  32 9416 1799
1117  STU MC0001 R  WEIGHT    1799  21 9415 1307
1118  NZR CP 2          DIVIDED   1307  42 1451 1711
1119  FDV P             BY R     1711  34 1112 0562
1120  FDV TEE            0562  34 1111 1761
1121  STU CPMR            1761  21 1216 1569
1122  RAU D0049          STORE    1569  60 0049 1254
1123  STU LMTP            DLNM/DLNT 1254  21 1123 0426
1124  LDD 8000            AT CONST P 0426  69 8000 0582
1125  RDI CP 3            CHANGES   0582  91 0485 1437
1126  LDD NOOP            MADE     0485  69 1488 1791
1127  STD MC041          UNPAK    1791  24 0318 0101
1128  ONCE  LDD NORM          BY      1150  69 1304 1357
1129  STD MC041          EQUATION 1357  24 0318 1271
1130  RAU SYS+2          SHIFTING 1271  60 0036 1442
1131  LDD               REDUC   1442  69 1696 1748
1132  RAU SYS+1          1696  60 0079 1333
1133  LDD               REDUC   1333  69 0436 1748
1134  RAU SYS             0436  60 0018 1174
1135  LDD DLMP1  SOLVE   1174  69 1377 1698
1136  NOOP  NOP 0000  ONCE  1488  00 0000 1150
1137  NORM  PAR 0052  MC042  1304  82 0052 0374
1138  CP 3  RAU SYS+1          1437  60 0079 1383
1139  LDD 2LESS  REDUC   1383  69 0486 1748
1140 1
1141  2LESS  RAU SYS          0486  60 0018 1224
1142  LDD DLMP1  BACK    1224  69 1377 0230
1143 1
1144 1
1145 1           CONSTANTS FOR USE IN PARAMETER
1146 1           CALCULATIONS
1147 1
1148  CONS1  14  6960  0652  PSI/ATM  1140  14  6960  0652
1149  CONS2  86  4554  0052          1141  86  4554  0052
1150  CONS3  10  0000  0054          1142  10  0000  0054
1151  CONS4  29  4980  0053          1143  29  4980  0053
1152  CONS5  57  0000  0050          1144  57  0000  0050
1153  52  00  0000  0052          1145  00  0000  0052
1154  R   19  8718  0051  CAL/MOL K  1146  19  8718  0051
1155  GC  32  1740  0052  GRAVITY  1147  32  1740  0052
1156  ONE  10  0000  0051          1149  10  0000  0051
1157 1
1158 1           SET CORE LOCATIONS EQUIVALENT
1159 1           TO PARAMETERS AND CONSTANTS
1160 1           OF THE F REGION
1161 1
1162  EQU PCP  M0001  9000
1163  EQU TEE  M0002
1164  EQU P   M0003
1165  EQU H   M0004
1166  EQU I   M0005
1167  EQU M   M0006
1168  EQU CF  M0007
1169  EQU FPSIL M0008
1170  EQU MACH M0009
1171  EQU I VAC M0010
1172  EQU CP  M0011
1173  EQU GAMMA M0012
1174  EQU LMPT M0013
1175  EQU LMTP M0014
1176  EQU S   M0015
1177  EQU NI  M0016
1178  EQU NT  M0017
1179  EQU NEPS M0018
1180  EQU NCSTR M0019

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1181      EQU CSTAR    M0020
1182      EQU AW       M0021
1183      EQU NAW      M0022
1184      EQU HSTR     M0023
1185      EQU AAY      M0024
1186      EQU HC       M0025
1187      EQU RECMC   M0026
1188      EQU NAWT     M0027
1189      EQU AWT      M0028
1190      EQU HSTR2   M0029
1191      EQU P1       M0030
1192      EQU CONS1   M0031
1193      EQU CONS2   M0032
1194      EQU CONS3   M0033
1195      EQU CONS4   M0034
1196      EQU CONS5   M0035
1197      EQU S2       M0036
1198      EQU R        M0037
1199      EQU GC       M0038
1200      EQU IDENT   M0039
1201      EQU ONE     M0040      9039
1202 1
1203 1      CALCULATE THE PARTIAL DERIV
1204 1      OF THE LOG OF MOLEC WEIGHT
1205 1      WITH RESPECT TO THE LOG OF
1206 1      PRESSURE AT CONSTANT TEMPUR
1207 1
1208  DLMPPT  SET M0001          1377  27 9000 0632
1209  LDB F0001          0632  09 1110 1664
1210  LDD SYS           LOAD   1664  69 0018 1321
1211  RSA 8001          DLNPT/DLNA 1321  81 8001 1427
1212  SET M0041          IN CORE 1427  27 9040 0982
1213  LDR D0050 A          0982  09 2050 1354
1214  LDD ATM-1          1354  69 0164 1817
1215  RSA 8001           1817  81 8001 1274
1216  RAB 8001           1274  82 8001 0280
1217  SET M0051          0280  27 9050 0535
1218  LDR Z0010 A LMPT1  BRING AAY  0535  09 3349 1302
1219  LMPT1  RAU M0041 B  COLUMN   1302  60 9440 1310
1220  FMP M0051 R  TO CORE  1310  39 9450 1714
1221  FAD LMPT          1714  32 9012 1793
1222  STU LMPT          1793  21 9012 1501
1223  NZR               LMPT2   1501  42 1404 1407
1224  SXB 0001          LMPT1   1404  53 0001 1302
1225  LMPT2  RAU P       1407  60 9002 1266
1226  FDV LMPT          1266  34 9012 1669
1227  FSB ONE           1669  33 9039 1200
1228  STU LMPT          1200  21 9012 1457
1229 1
1230 1      CALCULATE SEVERAL OTHER
1231 1      PARAMETERS
1232 1
1233  RAU AAY           CALCULATE 1457  60 9023 1316
1234  FDV P              MOLECULAR 1316  34 9002 1719
1235  STU M              WEIGHT    1719  21 9005 1477
1236 1
1237  RAU CPMR          SPECIFIC  1477  60 1216 1371
1238  FMP R              HEAT     1371  39 9036 1324
1239  FDV M              CAL/G    1324  34 9005 1527
1240  STU CP              1527  21 9010 0585
1241 1
1242  RAU ONE            GAMMA    0585  60 9039 1594
1243  FSR LMPT          EQUALS   1594  33 9013 1374
1244  FMP 8003          PARTIAL OF 1374  39 8003 1577
1245  STU TEMPO          LN PRESSUR 1577  21 9059 0635
1246  RAU ONE            WITH RESP  0635  60 9039 1694
1247  FAD LMPT          TO      1694  32 9012 1424
1248  FMP CPMR          LN DENSITY 1424  39 1216 1366
1249  FSR TFMPO          AT CONSTNT 1366  33 9059 1746
1250  STU TEMPO          ENTROPY   1746  21 9059 1454
1251  RAU CPMR          1454  60 1216 1421
1252  FDV TEMPO          1421  34 9059 1474
1253  STU GAMMA          1474  21 9011 1281
1254 1
1255  RAU H              CALCULATE 1281  60 9003 1739
1256  FDV AAY            ENTHALPY  1739  34 9023 1492
1257  FMP TEE             CAL/G    1492  39 9001 1796
1258  FMP R              1796  39 9036 1250
1259  STU H              1250  21 9003 1507
1260 1
1261  RAU S              CALCULATE 1507  60 9014 1416
1262  FDV AAY            ENTHALPY  1416  34 9023 1769
1263  STU TFMPO          1769  21 9059 1677
1264  FMP R              1677  39 9036 0330
1265  STU S              0330  21 9014 1487
1266 1
1267 1      TEST IF COMBUSTION THROAT OR
1268 1      EXIT
1269 1
1270  RAU COMFX          1487  60 0111 1466
1271  NZU TORFX          1466  44 1819 1470
1272 1

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1273	RAU ONE		STORE	1470	60	9039	1727	
1274	FDV M	1/MC		1727	34	9005	0380	
1275	STU RFM/C			1380	21	9025	1537	
1276 1			CALCULATE	1537	39	9036	1542	
1277	FMP R	N SUB T		1542	34	9010	1798	
1278	FDV CP			1798	39	9013	1551	
1279	FMP LMTP			1551	61	8003	1360	
1280	RSU 8003			1360	21	9016	0518	
1281	STU NT							
1282 1			SAVE HC	0518	69	9003	1524	
1283	LDD H			1524	24	9024	0430	
1284	STD HC			0430	69	9059	0536	
1285	LDD TEMPO							
1286	STD SO/R		SAVE SO/R	0536	24	0003	1557	
1287	PSU UNITY	FIX H	SET COMEX	1557	61	0104	1410	
1288	STU COMEX	H FIX	FOR THROAT	1410	21	0111	1764	
1289	STL CSTAR	PNCN	CLEAR CSTR	1764	20	9019	0322	
1290 1								
1291 1			TEST IF THROAT OR EXIT IS REFING PROCESSED					
1292 1								
1293 1								
1294 1								
1295	TORFX	BMI THROT	EXIT		1819	46	0372	1574
1296	EXIT	LDD RFMAN	SEVRL		1574	69	1777	0480
1297 1								
1298 1								
1299	EQU TWO	80001						
1300 1								
1301	THROT	RAU TEE		CALCULATE	0372	60	9001	0529
1302		FDV M		HSTR AS	0529	34	9005	1032
1303		FMP R		H PLUS	1032	39	9036	0985
1304		FDV TWO		VELOCITY	0985	34	1247	1300
1305		STU RT/2M		OF SOUND	1300	21	1504	1707
1306		FMD GAMMA		SQUARED	1707	39	9011	1460
1307		FAD H		OVER TWO	1460	32	9003	1789
1308		STU HSTR			1789	21	9027	1350
1309		FDV HC		THROAT IS	1350	34	9024	1554
1310		FSR FINS		GOOD WHEN	1554	33	1757	1433
1311		NZIJ	CSTR1	HSTR EQUAL	1433	44	1587	1538
1312 1			HC					
1313		RAU GAMMA		THROAT NOT	1587	60	9011	1400
1314		FAD ONF		DONE YET	1400	32	9039	0579
1315		FMP RT/2M			0579	39	1504	1704
1316		STU TEMPO		CALCULATE	1704	21	9059	1811
1317		RAU HC		THE NEXT	1811	60	9024	1520
1318		FSR HSTR		PRESSURE	1520	33	9022	1450
1319		FDV TEMPO		ESTIMATE	1450	34	9059	1754
1320		FAD ONE		FOR THROAT	1754	32	9039	1483
1321		FMP P			1483	39	9002	0586
1322		STU PC			0586	21	0015	0568
1323		RAU PC			0568	60	1109	1814
1324		STL TESTX			1814	20	1361	1516
1325		FDV PC			1516	34	0015	1566
1326		STU R0002			1566	21	1076	0629
1327		STU F0001	UNPAK	STOR PC/PT	0629	21	1110	0101
1328 1								
1329 1			START REITERATING WITH THE NEW THROAT PRESSURE ESTIMATE					
1330 1								
1331 1			CONSTANT FOR TESTING THROAT					
1332 1			FOR CONVERGENCE					
1333 1								
1334	FINS	00 1000	0053	THROT TEST	1757	00 1000	0053	
1335								
1336 1								
1337 1								
1338	CSTR1	LDD CSTR2	SEVRL		1538	69	1592	0480
1339 1								
1340	CSTR2	STU NAWT		CALCULATE	1592	21	9026	1500
1341		FAD ONE		C STAR	1500	32	9039	1029
1342		STU NCSTR		EXPONENT	1029	21	9018	1687
1343 1								
1344		RAU AW		STORF	1687	60	9020	1550
1345		STD AMT		THROAT AWK	1550	24	9027	1807
1346 1								
1347	FMP PC				1807	39	1109	1510
1348	FWD GC			CALCULATE	1510	39	9037	1666
1349	FWD CONS1			CSTAR	1666	39	9030	1570
1350	STU CSTAR				1570	21	9019	1827
1351 1								
1352	LDD UNITY			SET COMEX	1827	.69	0104	0508
1353	STD COMEX	REMAN		FOR EXIT	0508	24	0111	1777
1354 1								
1355 1								
1356 1								
1357 1								
1358 1								
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1365	SEVRL	STD LINK1		CALCULATE	0480	24	1419	0422
1366		PAU HC		SPECIFIC	0422	60	9024	1179
1367		FSR H		IMPULSF	1179	33	9003	1560
1368		FDV CONS3			1560	34	9032	1716
1369		LDD IMPUL	SQRT		1716	69	1670	1900
1370	INPUT	FMP CONS4			1670	39	9033	1674
1371		STU T			1674	21	9004	1331
1372	1							
1373		RSU ONE		CALCULATE	1331	61	9039	1692
1374		FDV M		SPECIFIC	1692	34	9005	1700
1375		FAD RECMC		IMPULSE	1700	32	9025	1229
1376		FMP TEE		EXPONENT	1229	39	9001	1182
1377		FMP CONS2			1182	39	9031	1035
1378		FDV I			1035	34	9004	1588
1379		FDV I			1488	34	9004	1742
1380		STU NI			1742	21	9015	1750
1381	1							
1382		PAU TEE		CALCULATE	1750	60	9001	0558
1383		FDV AAY		AREA PER	0558	34	9023	0612
1384		FDV I		UNIT FLOW	0612	34	9004	1766
1385		FMP CONS2		RATE	1766	39	9031	1720
1386		FDV CONS1			1720	34	9030	1724
1387		STU AW			1724	21	9020	1381
1388	1							
1389		PAU R		CALCULATE	1381	60	9036	1792
1390		FDV CP		R OVER	1792	34	9010	1800
1391		FMP RECMC		CP TIMES	1800	39	9025	1804
1392		STU RCPMC		MC	1804	21	0608	1062
1393	1							
1394		PAU ONE		CALCULATE	1062	60	9039	1770
1395		FDV GAMMA		AREA PER	1770	34	9011	1774
1396		STU TEMPO		UNIT FLOW	1774	21	9059	1431
1397		PAU LMTP		RATE	1431	60	9013	1744
1398		FSR ONE		EXPONENT	1744	33	9039	1824
1399		FMP RCPMC			1824	39	0608	0658
1400		FSB TEMPO			0658	33	9059	1737
1401		FSR NI			1737	33	9015	0618
1402		STU NAW	LINK1		0618	21	9021	1419
1403	1							
1404	1							
1405	1			CALCULATE THOSE PERFORMANCE				
1406	1			PARAMETERS WHICH HAVE NOT YET				
1407	1			BEEN CALCULATED				
1408	1							
1409	1							
1410	REMAN	RAU I		CALCULATE	1777	60	9004	1185
1411		FMP GC		THRUST	1185	39	9037	1688
1412		FDV CSTAR		COEFFICIENT	1688	34	9019	1794
1413		STU CF		C SUB F	1794	21	9006	1701
1414	1							
1415		RAU AW		CALCULATE	1701	60	9020	1660
1416		FDV AWT		AREA RATIO	1660	34	9027	1816
1417		STU EPSIL			1816	21	9007	1425
1418	1							
1419		RAU AW		CALCULATE	1425	60	9020	1533
1420		FMP P		SPEC IMPLS	1533	39	9002	0636
1421		FMP CONS1		ASSUMING	0636	39	9030	1751
1422		FAD I		AMBIENT	1751	32	9004	1481
1423		STU I VAC		PRESS ZERO	1481	21	9009	1801
1424	1							
1425		RAU GAMMA		CALCULATE	1801	60	9011	1710
1426		FMP TEE		MACH	1710	39	9001	1068
1427		FMP CONS2		NUMBER	1068	39	9031	1471
1428		FDV M			1471	34	9005	1475
1429		LDD MACH1	SQRT		1475	69	0578	1900
1430	MACH1	STU TEMPO			0578	21	9059	1235
1431		RAU I			1235	60	9004	1352
1432		FDV TEMPO			1352	34	9059	1058
1433		STU MACH			1058	21	9008	1168
1434	1							
1435		RAU ONE		CALCULATE	1168	60	9039	1525
1436		FSB LMTP		TEMPERATUR	1525	33	9013	1108
1437		FDV CPMR		EXPONENT	1108	34	1216	1218
1438		FSB RCPMC		N SUB T	1218	33	0608	1285
1439		STU NT			1285	21	9016	1402
1440	1							
1441		RAU NAW		CALCULATE	1402	60	9021	1760
1442		FSR NAWT		AREA RATIO	1760	33	9026	1452
1443		STU NEPS	PNCH	EXPONENT	1452	21	9017	0322
1444	1							
1445	1							
1446	1			ROUTINE FOR PUNCHING ROCKET				
1447	1			PERFORMANCE PARAMETERS AND				
1448	1			COMPOSITION OF COMBUSTION				
1449	1			PRODUCTS				
1450	1							
1451	PNCH	RAU 8003		SET CARD	0322	60	8003	1279
1452		STL CARON		NUMBR ZERO	1279	20	1852	1158
1453		SET M0001			1158	27	9000	1268
1454		STB F0001			1268	29	1110	1318
1455		RSA 0005		PUNCHES 2	1318	81	0005	1575
1456		RAB 0004		PERFORMANC	1575	82	0004	1531

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1457	LDD IDENT		PARAMETERS	531	69 9038 1787
1458	STD M0011	PNCH1	ON 4 CARDS	787	24 9010 1502
1459 1					
1460	PNCH1	NZA EXP 0001	COMP1	502	42 1208 1258
1461		AXA 0005		208	53 0001 1368
1462		SET M0005		368	50 0005 1675
1463		LPP F001 A		575	27 9005 0530
1464		NZA SPEC		530	08 3110 1418
1465		RAL SPEC1	PNCH2	418	40 1521 0472
1466		RAL SPEC1	PUNCH	1472	65 1725 1329
1467	PNCH2	LDD PNCH1		1329	69 1502 1950
1468 1					
1469	SPEC	RAL SPEC2	PNCH2	1521	65 1775 1329
1470	COMP1	RAU 0000		1258	80 0000 1468
1471		RAL 0000	COMP2	1468	82 0000 1825
1472 1					
1473	COMP2	RSC 0005		CLEAR	1825 89 0005 1581
1474		RAU P003	COMP3	POSITIONS	1581 60 8003 1552
1475	COMP3	STL M0011 C		FOR	1552 20 9610 1810
1476		AXC 0001		PRODUCTS	1810 58 0001 1518
1477		RMC COMP3		AND CODES	1518 49 1552 0522
1478 1					
1479		RSC 0004	COMP4	DO WE HAVE	1522 89 0004 0628
1480	COMP4	RAU P0001 A		A PRODUCT	1628 60 3599 1308
1481		NZU	COMP5	LOAD CODE	1308 44 1162 1212
1482 1		STL M0010 C		1162 21 9609 1820	
1483		AXC 0001		1820 58 0001 0476	
1484		RAU P0002 A		TEST FOR	0476 60 3600 1358
1485 1		RMI COMP6		CONDENSED	1358 46 1262 1312
1486 1					
1487		RAU T0008 R		CALC PI	1312 60 4667 1571
1488		LDD COMP7 EXP E		FROM LN PI	1571 69 0526 1850
1489	COMP7	STL M0010 C		AND LOAD	0526 21 9609 1583
1490		AXA 0002		1583 50 0002 1702	
1491		AXR 0010		1702 52 0010 1408	
1492		AXC 0001		1408 58 0001 1568	
1493		RMC COMP4	COMP5	1568 49 0628 1212	
1494 1					
1495	COMP8	NZA SPACE		1212 40 1668 1718	
1496		RAL SPEC2 COMP8		1668 65 1775 1379	
1497	SPACE	RAL SPEC3 COMP8		1718 65 1671 1379	
1498	COMP8	LDD PUNCH		PRODUCTS	1379 69 1232 1950
1499		RAU P0001 A		AND CODES	1732 60 3599 1458
1500		NZU COMP2 FROZ		1458 44 1825 1362	
1501	FROZ	LDD UNPAK PCP 1		1362 69 0101 0637	
1502 1					
1503	COMP6	RAU T0008 R COMP7		COND IS NI	1262 60 4667 0526
1504 1					
1505					
1506 1					
1507 1					
1508 1			CONSTANTS FOR PUNCH ROUTINE		
1509 1					
1510	SPEC1	07 M0006	0006		1725 07 9005 0006
1511	SPEC2	00 M0006	0006		1775 00 9005 0006
1512	SPEC3	06 M0006	0006		1671 06 9005 0006
1513 1					
1514 1					
1515	EQU PCR	F0001			
1516	EQU TFF	F0002			
1517	EQU P	F0003			
1518	EQU H	F0004			
1519	EQU I	F0005			
1520	EQU M	F0006			
1521	EQU CF	F0007			
1522	EQU EPSIL	F0008			
1523	EQU MACH	F0009			
1524	EQU T_VAC	F0010			
1525	EQU CP	F0011			
1526	EQU GAMMA	F0012			
1527	EQU LMPT	F0013			
1528	EQU LMTP	F0014			
1529	EQU S	F0015			
1530	EQU NI	F0016			
1531	EQU NT	F0017			
1532	EQU NFRS	F0018			
1533	EQU NCSTR	F0019			
1534	EQU CSTAR	F0020			
1535	EQU AM	F0021			
1536	EQU MAX	F0022			
1537	EQU HSTR	F0023			
1538	EQU AAY	F0024			
1539	EQU HC	F0025			
1540	EQU RECMC	F0026			
1541	EQU NAVT	F0027			
1542	EQU AWT	F0028			
1543	EQU HSTR2	F0029			
1544	EQU PI	F0030			
1545	EQU CONS1	F0031			
1546	EQU CONS2	F0032			
1547	EQU CONS3	F0033			
1548	EQU CONS4	F0034			

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1549      FOU CONSS   F0035
1550      FOU S2     F0036
1551      FOU R     F0037
1552      FOU GC     F0038
1553      FOU IDENT   F0039
1554 1
1555 1
1556 1      SUBROUTINE TO SET ASSIGNED
1557 1      PRESSURE
1558 1
1559  PCP 1      STD LINK
1560  RAL PCPCT    ADVANCE 0637 24 1855 1508
1561  ALO UNITY   PRESSURE 1508 65 0017 1721
1562  STL PCPCT    RATIO 1721 15 0104 1412
1563 1      COUNTER 1412 20 0017 1771
1564  RAA 5001
1565  SLT 0004
1566  STL PROB
1567  RAU R0000 A
1568  STL TESTX
1569  STU PCP
1570  NZU 9999      NEW PC/PE 1768 21 1110 1818
1571 1      TEST FOR 1818 44 1821 9999
1572  RAU PC      LAST PC/PE
1573  FDV PCP
1574  STU P0      CLER1
1575 1
1576  CLFR1 RAB 0018      CLEAR 18 0622 82 0018 1178
1577  RAU WIPE7 8003      PARAMETER 1178 60 1681 8003
1578  8003 STL F0001 P CL 1      STORAGES 8003 20 5110 1072
1579  CL 1      SXB 0001
1580  NZB 8003      LINK 1072 53 0001 1228
1581 1
1582 1      CONSTANTS FOR ASSIGNED
1583 1      PRESSURE SUBROUTINE
1584 1
1585  UNITY 00 0000 0001
1586  WIPE7 STL F0001 P CL 1      0104 00 0000 0001
1587 1
1588 1
1589 1      SUBROUTINE FOR SOLUTION OF
1590 1      N SIMULTANEOUS EQUATIONS
1591 1
1592  SOLVE STD LINK
1593  STU EQUAT
1594  SUP UNITY
1595  NZU OKEH
1596  RAU D0049
1597  FDV D0048
1598  STU D0049      LINK 1758 34 0048 1802
1599  OKEH AUP UNITY      START 1802 21 0049 1855
1600 1
1601 1
1602  BACK STD LINK
1603  STU NOROW
1604  RAU D0049      BACK1 0230 24 1855 1808
1605  START STU NOROW ONLY 1808 21 9049 1322
1606  STD MINEX
1607  STL MINCO
1608  LDD 8000
1609  RD1 AGAIN      STRT1 1322 60 0049 1712
1610  AGAIN STU VARPL MUST EQUA 1662 21 9049 1372
1611  SUP UNITY
1612  PMI SHOVE
1613  MPY 50      INDEX 1778 24 9045 1278
1614  PAR 8002      FOLLOWS 1778 20 9046 0986
1615  EXP NOROW
1616  RAU NOROW
1617  SUP UNITY
1618  NZU BACKS
1619  PAA 8003      INDXB 1762 91 1422 1472
1620  PAC 8003      FOLLOW 1422 21 9048 1479
1621  SET M0001      EQUATIONS 1479 11 0104 1812
1622  LDR D0049 A 012
1623  SET C0001      INDEX THF 1812 46 1522 1572
1624  LDP U0001      C0001 1572 19 0186 1672
1625  U0001 RAU M0001 C0002 0334 88 8003 1822
1626  U0002 NZU C0003 LEAVE BRING EQUA 1822 27 9000 1328
1627  U0003 RAU M0001 A C0004 TO CORE 1328 04 4049 1176
1628  U0004 FDV M0001 C0005 1176 27 9050 1781
1629  U0005 RAM 8003 C0006 1781 09 0050 9050
1630  U0006 STL M0001 A C0007 0055 20 9200 9056
1631  U0007 SXA 0001 C0008 0056 51 0001 9057
1632  U0008 NZA C0003 C0009 0057 40 9052 9058
1633  U0009 STU MAXCO 0058 21 9047 1326
1634  RAA NOROW
1635  SXA 0001
1636  SET C0001
1637  LDR X0001 C0001 1326 30 9049 0384
1638  Y0001 RAU MAXCO C0002 0384 51 0001 1376
1639  Y0002 FSA M0001 A C0003 1376 27 9050 1831
1640  Y0003 PMI C0004 C0006 1831 09 0059 9050
1641  Y0003 PMI C0004 C0006 0059 60 9047 9051
1642  Y0003 PMI C0004 C0006 0060 33 9200 9052
1643  Y0003 PMI C0004 C0006 0061 46 9053 9055

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1641	Y0004	LDD M0001 A C0005		0162	69 9200 9054
1642	Y0005	STD MAXCO C0006		0163	24 9047 9055
1643	Y0006	SXA 0001 C0007		0164	51 0001 9056
1644	Y0007	NZA C0001		0165	40 9050 1426
1645		RSU MINCO	PLACE	1426	61 9046 1683
1646		NZU BOOK	SMALLEST	1683	44 1738 1788
1647		FAD MAXCO	COEFFICIENT	1738	32 9047 1476
1648		RMI POCK	IN MINCO	1476	46 1788 1226
1649	BOOK	LDD MAXCO	AND EQUAT	1788	69 9047 1526
1650		STD MINCO	NUMBER IN	1526	24 9046 1282
1651		LDD VARPL	MINFY	1282	69 9048 1576
1652		STD MINFX	LEAVE	1576	24 9045 1226
1653	LEAVE	RAU VARPL	GO TO NEXT	1226	60 9048 1733
1654		SUP UNITY	EQUATION	1733	11 0104 1422
1655	SHOFE	RAU NOROW		522	60 9049 1579
1656		SUP MINEX		579	11 9045 1676
1657		NZU	STRTO	676	44 1679 0580
1658		RAU NOROW		679	60 9049 1726
1659		SUP UNITY		726	11 0104 1776
1660		MPY 50		776	19 0186 1826
1661		RAA 8002		1826	80 8002 1335
1662		RAU MINEX		1335	60 9045 1378
1663		SUP UNITY		1378	11 0104 1428
1664		MPY 50		1428	19 0186 1478
1665		RAB 8002		1478	82 8002 1528
1666		SFT M0001	SHIFT THE	1528	27 9000 1783
1667		LDR D0037 A	EQUATIONS	1783	09 2037 1578
1668		LDR D0037 P		1578	09 4037 1678
1669		SET M0001		1678	27 9000 0434
1670		STB D0037 R		0434	29 4037 1728
1671		STB D0037 A STRTO		1728	29 2037 0580
1672	STRTO	RAU NOROW STRT1		0580	60 9049 1472
1673	STRT1	SUP UNITY		1472	11 0104 1778
1674		NZE BACKS		1778	45 1332 0526
1675		MPY 50		1332	19 0186 1828
1676		RAB 8002		1828	82 8002 1729
1677		SXB NOROW		1729	53 9049 1779
1678		SET M0001	TRANSFER	1779	27 9000 0484
1679		LDB D0049 R	EQ TO CORE	0484	09 4049 1829
1680		RAA NOROW DIV		1829	80 9049 0630
1681	DIV	SET C0001		0630	27 9050 1385
1682		LBB I0001 C0001	DIVIDE	1385	08 1001 9050
1683	I0001	RAU M0001 A C0002	ELEMENTS	1001	60 9200 9051
1684	I0002	FDV M0001 C0003	OF FIRST	1002	34 9000 9052
1685	I0003	STJ M0001 A C0004	EQUATION	1003	21 9200 9053
1686	I0004	SXA 0001 C0005	BY LEADING	1004	51 0001 9054
1687	I0005	NZA C0001 NEXTR	COEFFIC	1005	40 9050 1030
1688	1				
1689	NEXTR	SET M0002	AND STORE	1030	27 9001 1435
1690		STB D0050 P	BACK ON	1435	29 4050 1180
1691		SET C0001	DRUM	1180	27 9050 1485
1692		LBB J0001	NEW R	1485	08 1006 1230
1693	1				
1694	NEW R	SXB 0050	ANY MORE	1230	53 0050 1036
1695		AXB NOROW	EQUATIONS	1036	52 9049 1280
1696		BOV OFLO1	CHK OVRFL0	1280	47 0534 1535
1697		BMB OUT 1		1535	43 1330 1380
1698		SXB NOROW	YES	1380	53 9049 1430
1699		SET N0001		1430	27 9015 1585
1700		LDB D0049 R		1585	09 4049 1480
1701		RAA NOROW ELMIN		1480	80 9049 9050
1702	OFLO1	HLT 0000 9955		0534	01 0000 9955
1703	OUT 1	RAU NOROW	NO	1330	60 9049 1530
1704		SUP UNITY	START	1530	11 0104 1662
1705	J0001	RSU N0001 C0002	ELIMINATE	1006	61 9015 9051
1706	J0002	FMP M0001 A C0003	A VARIABLE	1007	39 9200 9052
1707	J0003	BOV ZEROU C0004	CHK OVRFL0	1008	47 1580 9053
1708	J0004	FAD N0001 A C0005		1009	32 9215 9054
1709	J0005	STU N0001 A C0006		1010	21 9215 9055
1710	J0006	SXA 0001 C0007		1011	51 0001 9056
1711	J0007	NZA ELMIN		1012	40 9050 1680
1712		SET N0002		1680	27 9016 1685
1713		STB D0050 R NEW R		1685	29 4050 1230
1714	ZEROU	RAU 8002 C0004	OVERFLOW	1580	60 8002 9053
1715	1				
1716	BACKS	RAU N0003 B1	LEAVES THE	0626	60 9017 0584
1717	B1	FDV N0002	LAST	0584	34 9016 1730
1718		LDD EQUAT	VARIABLE	1730	69 1512 1780
1719	1		IN UPPER		
1720		STD NOROW BACK1		1780	24 9049 1712
1721	RACK1	RAB 0000		1712	82 0000 1830
1722		RAC 0001		1830	88 0001 1186
1723		SET C0001		1186	27 9050 1382
1724		LBB K0001 S7		1382	08 1013 1432
1725	1				
1726	S7	SXC 0001		1432	59 0001 1482
1727		STU D0049 C		1482	21 6049 1532
1728		BOV OFLO2	CHK OVRFL0	1532	47 1735 1582
1729		RSL 8007		1582	66 8007 1682
1730		RAA 8002		1682	80 8002 1732
1731		AXA 0001		1732	50 0001 1782

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1732	AXR 0049		1782	52 0049 1832
1733	SXA NOROW		1832	51 0049 0634
1734	BMA	LINK	0634	41 0984 1855
1735	AXA NOROW		0984	50 0049 1034
1736	SET M0001	VARIABLES	1034	27 9000 1184
1737	LDB D0049 C	IN M0001	1184	09 6049 1234
1738	SET N0001	COEFFICNTS	1234	27 9015 1284
1739	LDA D0049 A S1	IN N0001	1284	09 4049 9050
1740 OFLO2	HLT 0000 9966		1735	01 0000 9966
1741 49	49 0000 0000		1334	49 0000 0000
1742 1				
1743 1				
1744 1	CALCULATE AND LEAVE NEXT			
1745 1	VARIABLE IN UPPER			
1746 1				
1747 K0001	SXA 0001 C0002		1013	51 0001 9051
1748 K0002	RSU M0001 A C0003		1014	61 9200 9052
1749 K0003	FMP N0001 A C0004		1015	39 9215 9053
1750 K0004	BOV ZERUP C0005	CHK OVRFLD	1016	47 134 9054
1751 K0005	FAD N0002 A C0006		1017	32 9216 9055
1752 K0006	STU N0001 A C0007		1018	21 9215 9056
1753 K0007	NZA S1 S7		1019	40 9050 1432
1754 ZERUP	RAU 8002 C0005		1384	60 8002 9054
1755 1				
1756 1				
1757 1	SUBROUTINE TO REDUCE MATRIX BY			
1758 1	ONE COLUMN AND ONE ROW			
1759 1				
1760 REDUC	STD LINK	REDUCE	1748	24 1855 1434
1761 RSR 8003		MATRIX	1434	83 8003 1484
1762 RAA 8003		BY	1484	80 8003 1534
1763 SXA 0001 SHIFT	ONE		1534	51 0001 1584
1764 SHIFT AXR 0050	COLUMN		1584	52 0050 1684
1765 SET M0001	AND		1684	27 9000 1734
1766 LDA D0049 R	ONE		1734	09 4049 1784
1767 SET M0001	ROW		1784	27 9000 1785
1768 STB D0000 B			1785	29 4000 1236
1769 SXA 0001			1236	51 0001 1286
1770 NZA SHIFT	LINK		1286	40 1584 1855
1771 1				
1772 1				
1773 1	ROUTINE TO LOAD PACKED VECTORS			
1774 1	AND GENERATE ATOM1 AND SYS THE			
1775 1	PROGRAM DEFINING CONSTANTS			
1776 1				
1777 1	PRECEED PACKED VECTORS WITH			
1778 1	A LOAD HUP TRANSFER CARD WHICH			
1779 1	IS NOP GO TO V0001			
1780 1				
1781 1	FOLLOW PACKED VECTORS WITH A			
1782 1	LOAD HUP CARD WORD1 EQUAL ZERO			
1783 1				
1784 1	THE PROGRAM BYPASSES THE			
1785 1	PROPELLANT IDENTIFICATION CARD			
1786 1				
1787 1	INDEXB TOTALS GASEOUS ATOMS			
1788 1	INDEXC TOTALS CONDENSED PHASES			
1789 1				
1790 1	OASIS SPECIFIES WHICH OF THE			
1791 1	CONDENSED PHASES ARE USED			
1792 1				
1793 REG R1951	1960	READ BAND		
1794 REG V1599	1659	IN PREGION		
1795 RFG C9000	9000			
1796 EQU PCH10	1986	WRD 10 PCH		
1797 EQU ODIN	C0048			
1798 EQU OASIS	C0049			
1799 EQU RELAY	C0050			
1800 1				
1801 8000 RCD R0001	1998	CONSOLE	8000	70 1951 1998
1802 R0001 00 0000	V0001	TRANSFR CD	1951	00 0000 1599
1803 V0001 SFT C0003	V0002		1599	27 9002 1600
1804 V0002 LDB V0003	C0003		1600	09 1601 9002
1805 V0003 PAA 0000	C0004	CLEAR	1601	80 0000 9003
1806 V0004 PAR 0000	C0005	INDEX A B	1602	82 0000 9004
1807 V0005 PAC 0000	C0006	AND C	1603	88 0000 9005
1808 V0006 SUP 8003	C0007		1604	11 8003 9006
1809 V0007 STU RELAY	C0008		1605	21 9049 9007
1810 V0008 RCD PCH10	9977		1606	70 1986 9977
1811 PCH10 NOP 0000	C0009		1986	00 0000 9008
1812 V0009 RAU R0001	C0010	ARE ALL	1607	60 1951 9009
1813 V0010 NZU C0011	C0042	VECTORS IN	1608	44 9010 9041
1814 V0011 RAU R0002	C0012	NO BYPASS	1609	60 1952 9011
1815 V0012 NZU C0013	C0008	NONVECTORS	1610	44 9012 9007
1816 V0013 RAU R0004	C0014		1611	60 1954 9013
1817 V0014 BMI C0025	C0015	IS THIS	1612	46 9024 9014
1818 V0015 SRT C002	C0016	AN ATOM OR	1613	30 0002 9015
1819 V0016 NZU C0025	C0017	MOLECULE	1614	44 9024 9016
1820 V0017 SLT 0001	C0018		1615	35 0001 9017
1821 V0018 SLO ODIN	C0019		1616	16 9047 9018
1822 V0019 PAL R002	C0020		1617	65 8002 9019

1823	V0120	NZE C0025	C0021		1618	45 9024 9020	
1824	V0121	AXP 0001	C0022	GAS ATOM	1619	52 0001 9021	
1825	V0122	RAU RELAY	C0023	ARE ALL	1620	60 9049 9022	
1826	V0123	NZU C0024	C0037	ATMS AHEAD	1621	44 9013 9036	
1827	V0124	HLT 0000	9988		1622	01 0000 9988	
1828	V0125	LDD ODIN	C0026	IT IS A	1623	69 9047 9025	
1829	V0126	STD RELAY	C0027	MOLFCULE	1624	24 9049 9026	
1830	V0127	RAU R0004	C0028	IS PRODUCT	1625	60 1954 9027	
1831	V0128	BMI C0029	C0037	CONDENSED	1626	46 9028 9036	
1832	V0129	RAU OASIS	C0030	YES	1627	60 9048 9029	
1833	V0130	SRT 0001	C0031		1628	30 0001 9030	
1834	V0131	STU OASIS	C0032		1629	21 9048 9031	
1835	V0132	RAL 8002	C0033	IS IT TO /	1630	65 8002 9032	
1836	V0133	NZE C0036	C0034	BE USED	1631	45 9035 9033	
1837	V0134	RAL R0002	C0035	YES	1632	65 1952 9034	
1838	V0135	AXC 0001	C0038		1633	58 0001 9037	
1839	V0136	ALO R0002	C0038	NO	1634	15 1952 9037	
1840	V0137	PAL R0002	C0038		1635	65 1952 9037	
1841	V0138	STL P0001 A	C0039	STORE CODE	1636	20 3599 9038	
1842	V0139	LDD R0004	C0040	AND VECTOR	1637	69 1954 9039	
1843	V0140	STD P0002 A	C0041		1638	24 3600 9040	
1844	V0141	AXA 0002	C0008		1639	50 0002 9007	
1845	V0142	RAU 8007	C0043		1640	60 8007 9042	
1846	V0143	STL P0001 A	C0044		1641	20 3599 9043	
1847	V0144	LDD 8006	C0045		1642	69 8006 9044	
1848	V0145	STD ATOM1	C0046	STORE SYS	1643	24 0642 9045	
1849	V0146	AUP 8001	C0047	AND ATOM1	1644	10 8001 9046	
1850	V0147	STU SYS	CHEK		1645	21 0018 0499	
1851	1	CONSTANTS					
1852	1						
1853	1						
1854	V0048	10 0000	0000	ODIN	1646	10 0000 0000	
1855	V0049	11 1111	1111	OASIS	1647	11 1111 1111	
1856	1	BUILT IN ESTIMATES FOR					
1857	1	ALL THE VARIABLES					
1858	1						
1859	1						
1860	T0008	10 0000	0040	ESTIMATES	0667	10 0000 0040	
1861	T0118	10 0000	0040	FOR LN OF	0677	10 0000 0040	
1862	T0128	10 0000	0040	COMPOSITOR	0687	10 0000 0040	
1863	T0038	10 0000	0040	EQUIVALENT	0697	10 0000 0040	
1864	T0048	10 0000	0040	TO PARTIAL	0707	10 0000 0040	
1865	T0058	10 0000	0040	PRESURES	0717	10 0000 0040	
1866	T0068	10 0000	0040	OF I	0727	10 0000 0040	
1867	T0078	10 0000	0040	ATMOSPHERE	0737	10 0000 0040	
1868	T0088	10 0000	0040	FOR ALL	0747	10 0000 0040	
1869	T0098	10 0000	0040	GASEOUS	0757	10 0000 0040	
1870	T0108	10 0000	0040	PRODUCTS	0767	10 0000 0040	
1871	T0118	10 0000	0040		0777	10 0000 0040	
1872	TC128	10 0000	0040		0787	10 0000 0040	
1873	T0138	10 0000	0040		0797	10 0000 0040	
1874	T0148	10 0000	0040		0807	10 0000 0040	
1875	T0158	10 0000	0040		0817	10 0000 0040	
1876	T0168	10 0000	0040		0827	10 0000 0040	
1877	T0178	10 0000	0040		0837	10 0000 0040	
1878	T0188	10 0000	0040		0847	10 0000 0040	
1879	T0198	10 0000	0040		0857	10 0000 0040	
1880	T0208	10 0000	0040		0867	10 0000 0040	
1881	T0218	10 0000	0040		0877	10 0000 0040	
1882	T0228	10 0000	0040		0887	10 0000 0040	
1883	T0238	10 0000	0040		0897	10 0000 0040	
1884	T0248	10 0000	0040		0907	10 0000 0040	
1885	T0258	10 0000	0040		0917	10 0000 0040	
1886	T0268	10 0000	0040		0927	10 0000 0040	
1887	T0278	10 0000	0040		0937	10 0000 0040	
1888	T0288	10 0000	0040		0947	10 0000 0040	
1889	T0298	10 0000	0040		0957	10 0000 0040	
1890	G0001	50 0000	0051	LNA ESTM T	0001	50 0000 0051	
1891	G0002	82 4300	0051	LNT ESTM T	0002	82 4300 0051	
1892	1						
1893	1	TO RUN AT CONSTANT ENTHALPY					
1894	1	AT VARIOUS PRESSURE RATIOS					
1895	1	LOAD THE FOLLOWING CARD					
1896	1						
1897	1						
1898	FIX H	STL COMFX	H FIX	CONST H	1410	20 0111 1764	
1899	1	TO RUN FROZEN COMPOSITION					
1	CALCULATIONS LOAD THE						
1	FOLLOWING CARD						
1	FPOZ	HLT	9999	9999	1362	01 9999 9999	
1	1900	PAT					
1901							

1902 1  
 1903 1 PUNCH ROUTINE FOR TESTING  
 1904 1 GENERAL ROCKET PERFORMANCE  
 1905 1 CALCULATION  
 1906 1  
 1907 1 PUNCHING IS CONSOLE CONTROLLED  
 1908 1 BY POSITIONS 2 3 4 AND SIGN  
 1909 1 THESE POSITIONS MUST BE EITHER  
 1910 1 EIGHT OR NINE PUNCHING ON 8  
 1911 1  
 1912 1 POSITION 2 PUNCHES ONE MINUS  
 1913 1 P/PO ETC AND NEGATIVE DELTAI  
 1914 1  
 1915 1 POSITION 3 PUNCHES P T AAY  
 1916 1 AND THE COMPOSITIONS NI  
 1917 1  
 1918 1 POSITION 4 PUNCHES THE  
 1919 1 REDUCED MATRIX  
 1920 1  
 1921 1 A MINUS ON CONSOLE PUNCHES  
 1922 1 CORRECTION VARIARLES  
 1923 1  
 1924 1 ANY COMBINATION OF THE FOUR  
 1925 1 PUNCHES MAY BE USED TOGETHER  
 1926 1  
 1927 BLA 1656 1659  
 1928 BLA 0940 0959  
 1929 1  
 1930 1  
 1931 1 PUNCH THE DELS AT THIS TIME  
 1932 1  
 1933 DELS RAL PCH01 PUNCH ONE 1181 65 1336 0941  
 1934 ALO ATOM1 MINUS A 0941 15 0642 0947  
 1935 LDD DELS1 PUNCH OVER AO 0947 69 0950 1950  
 1936 DELS1 RAA 0000 ETC 0950 80 0000 0956  
 1937 RAC 0000 DELS2 0956 88 0000 1386  
 1938 DELS2 RAU P0001 A PUNCH THE 1386 60 3599 0953  
 1939 NZU DELS3 PRODUCT 0953 44 0957 0958  
 1940 STU 9000 A CODES AND 0957 21 9200 1436  
 1941 LDD T0010 C THE DELTAI 1436 69 6669 1486  
 1942 STD 9001 A 1486 24 9201 0942  
 1943 AXA 0002 0942 50 0002 0948  
 1944 AXC 0010 DELS2 0948 58 0010 1386  
 1945 DELS3 RAL 8005 0958 65 8005 1536  
 1946 ALO PCH02 1536 15 0940 0945  
 1947 LDD NEXT1 PUNCH 0945 69 1233 1950  
 1948 1  
 1949 1  
 1950 1 PUNCH THE SOLUTION TO THE  
 1951 1 CURRENT MATRIX  
 1952 1  
 1953 DELX LDD SYS+1 PUNCH THE 1564 69 0079 1586  
 1954 RSA 8001 SOLUTION 1586 81 8001 0943  
 1955 SET 9000 TO THE 0943 27 9000 0949  
 1956 LDB D0049 A CORRECTION 0949 09 2049 0952  
 1957 RAL PCH02 MATRIX 0952 65 0940 0946  
 1958 ALO SYS+2 0946 15 0036 0944  
 1959 LDD UNPAK PUNCH 0944 69 0101 1950  
 1960 1  
 1961 1 CONSTANTS FOR THE PUNCH  
 1962 1 ROUTINE  
 1963 1

1964	PCH01	06	RV000	0002		1336	06	9004	0002
1965	PCH02	06	9000	0000		0940	06	9000	0000
1966	1								
1967			PAT						

1968		BLA	1652	1655						
1969		BLA	0920	0939						
1970	1									
1971	1				PUNCH THE CURRENT VARIABLES					
1972	1									
1973		VARIA	RAU LNT		PUNCH TEMP	1392	60	0002	1657	
1974			LDD VAR01	EXP E	PRESSURE	1657	69	0920	1850	
1975		VAR01	STU 9000		AND AAY	0920	21	9000	0927	
1976			LDD P			0927	69	1112	0921	
1977			STD 9001			0921	24	9001	0928	
1978			LDD AAY			0928	69	1133	0936	
1979			STD 9002			0936	24	9002	0951	
1980			RAL PCH03			0951	65	0954	0959	
1981			LDD VAR02	PUNCH		0959	69	0922	1950	
1982		VAR02	RAA 0000		PUNCH THE	0922	80	0000	0929	
1983			RAC 0000	VAR03	PRODUCT	0929	88	0000	0935	
1984		VAR03	RAU P0001 A		CODE AND	0935	60	3599	1653	
1985			NZU	VAR11	MOLES OF	1653	44	1658	1659	
1986			STD 9000 A		EACH	1658	24	9200	0923	
1987			RAU P0002 A		COMBUSTION	0923	60	3600	0955	
1988			BMI VAR07		PRODUCT	0955	46	0924	0925	
1989			RAU T0008 C			0925	60	6667	0926	
1990			LDD VAR05	EXP E		0926	69	0930	1850	
1991		VAR05	STU 9001 A	VAR09		0930	21	9201	0937	
1992		VAR07	LDD T0008 C			0924	69	6667	0931	
1993			STD 9001 A	VAR09		0931	24	9201	0937	
1994		VAR09	AXA 0002			0937	50	0002	1652	
1995			AXC 0010	VAR03		1652	58	0010	0935	
1996		VAR11	RAL PCH02			1659	65	0940	1654	
1997			ALO 8005			1654	15	8005	0932	
1998			LDD NEXT2	PUNCH		0932	69	1394	1950	
1999	1									
2000	1									
2001	1				PUNCH OUT THE MATRIX					
2002	1									
2003		MTRIX	RAU SYS+1			1503	60	0079	0933	
2004			MPY 50			0933	19	0186	1656	
2005			RAA 8002	MTR01		1656	80	8002	0934	
2006		MTR01	SFT 9000			0934	27	9000	0939	
2007			LDB 0037 A			0939	09	2037	1655	
2008			RAL PCH04			1655	65	1686	1736	
2009			LDD MTR03	PUNCH		1736	69	1786	1950	
2010		MTR03	NZA	LINK1		1786	40	0938	1419	
2011			SXA 0050	MTR01		0938	51	0050	0934	
2012	1									
2013	1									
2014	1				CONSTANTS FOR THE PUNCH					
2015	1				ROUTINE					
2016	1									
2017		PCH03	06	9000	0003		0954	06	9000	0003
2018		PCH04	06	9000	0013		1686	06	9000	0013
2019			PAT							

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2020 1 PROGRAM CHANGE TO CONTROL SIZE  
 2021 1 OF APPLIED CORRECTION  
 2022 1  
 2023 RLA 1652 1655  
 2024 RLA 0920 0939  
 2025 REG C9050 9050  
 2026 1 LOAD AVAILABILITY TABLE GIVEN  
 2027 1 BY CARD NUMBER 1967  
 2028 1  
 2029 NEWOO LDD MAG00 SOLVE 1691 69 0951 1698  
 2030 MAG00 LDD SYS+1 0951 69 0079 0932  
 2031 RSA 8001 0932 81 8001 0938  
 2032 RAB 8001 BRING 0938 82 8001 1652  
 2033 RAC 8001 SOLUTION 1652 88 3001 1658  
 2034 SET M0001 VECTOR TO 1658 27 9000 0920  
 2035 LDB D0049 A MAG01 CORE 0920 09 2049 1653  
 2036 MAG01 RAM M0001 B MAKE ALL 1653 67 9400 0921  
 2037 STL N0001 B COMPONENTS 0921 20 9415 0928  
 2038 NZB MAG03 POSITIVE 0928 42 0931 0933  
 2039 SXR 0001 MAG01 0931 53 0001 1653  
 2040 MAG03 RAU N0001 C MAG05 FIND THE 0933 60 9615 0954  
 2041 MAG05 FSR N0000 C LARGEST 0954 33 9614 0934  
 2042 BMI TOP COMPONENT 0934 46 0937 0939  
 2043 RAU N0000 C MAG07 0937 60 9614 1654  
 2044 TOP FAD N0000 C MAG07 0939 32 9614 1654  
 2045 MAG07 SXC 0001 IF THE 1654 59 0001 0922  
 2046 NZC MAG05 COMPONENT 0922 48 0954 0926  
 2047 FSB MAXMA IS LARGER 0926 33 0929 0955  
 2048 BMI MAG09 THAN MAXMA 0955 46 0959 1659  
 2049 LDD F0040 STORE THE 0959 69 1149 1655  
 2050 STD RATIO NEW01 RATIO OF 1655 24 0923 1444  
 2051 MAG09 FAD MAXMA COMPONENT 1659 32 0929 1656  
 2052 FDV MAXMA TO MAXMA 1656 34 0929 0930  
 2053 STU RATIO NFW01 0930 21 0923 1444  
 2054 MAXMA 50 0000 0051 MAX RATIO 0929 50 0000 0051  
 2055 Q0006 NZC C0001 1025 42 9050 0935  
 2056 FDV RATIO 00007 0935 34 0923 1026  
 2057 NEW21 RAU D0048 B 0512 60 4048 1657  
 2058 FDV RATIO NEW22 1657 34 0923 1753  
 2059 NEW18 RAU D0049 1157 60 0049 0924  
 2060 FDV RATIO NEW19 0924 34 0923 1803  
 2061 NEW60 RSU D0048 1806 61 0048 0925  
 2062 FDV RATIO NEW61 0925 34 0923 1104  
 2063 1  
 2064 1  
 2065 1 PROGRAM MAY BE MODIFIED TO  
 2066 1 CONVERGE FOR ASSIGNED  
 2067 1 TEMPERATURE AND PRESSURE BY  
 2068 1 INCLUDING THE FOLLOWING STEPS  
 2069 1  
 2070 RLA 0910 0919  
 2071 RLA 1650 1651  
 2072 1  
 2073 MC021 RAU HO/R 0570 60 0004 0910  
 2074 STL RV001 MC031 0910 20 9005 0286  
 2075 ITFRA LDD HOLD1 0462 69 0915 0918  
 2076 STD BACKS 0918 24 0626 0936  
 2077 RAU SYS+2 NEWOO 0936 60 0036 1691  
 2078 HOLD1 SUP 8003 B1 0915 11 8003 0584  
 2079 DERIV LDD HOLD2 1755 69 0911 0914  
 2080 STD BACKS 0914 24 0626 1686  
 2081 RAU SYS+2 D1 1686 60 0036 1741  
 2082 HOLD2 RAU N0003 B1 0911 60 9017 0584  
 2083 PAT

INPUT DATA ROUTINE

```

1
8 1
9      RLR 0002  0036
10     RLR 0050  0086
11     RLR 0100  0136
12     RLR 0150  0186
13     RLR 0200  0236
14     RLR 0250  0286
15     RLR 0300  0336
16     RLR 0350  0386
17     RLR 0400  0436
18     RLR 0450  0486
19     RLR 0500  1999
20     RLA 0987  0999
21     RLA 1340  1349
22     REG G0001 0015
23     REG I0040 0045
24     REG F1110 1110
25     REG M9000 9000
26     SYN VFPLS 0598 +FUEL VALV
27     SYN VFMIN 0599 -FUEL VALV
28     SYN VXPLS 0548 +OXID VALV
29     SYN VXMIN 0549 -OXID VALV
30     SYN O/F   0199
31     SYN PCT F 0299
32     SYN EQRAT 0399 EQUIVLENCE
33 1          RATIO
34     SYN CHEK  0499
35     SYN BEGIN 0000
36     SYN PUNCH 1950
37     SYN PC    F0000
38     SYN IDENT F0039
39     SYN R    F0037
40     SYN TEMPO 9011
41     SYN CONS1 1140
42     SYN PROR  1904
43 1          CALCULATE NUMBER OF MOLES OF
44 1          OXIDANT PER MOLE OF FUEL
45 1
46 1
47 1
48     CHEK   RAU O/F           0499  60 0199 0037
49     NZU OXFUL          0037  44 0091 0092
50     RAU PCT F           0092  60 0299 0087
51     NZU PRCNT          0087  44 0141 0142
52     RAU EQRAT          0142  60 0399 0137
53     NZU EQUIV           0137  44 0191 0192
54     HLT 9999  9999  0192  01 9999 9999
55 1
56     OXFUL   RAU O/F           0091  60 0199 0187
57     FAD 10051          0187  32 0090 0237
58     STU TEMPO          0237  21 9011 0095
59     RAU 10053          0095  60 0048 0287
60     FDV TEMPO          0287  34 9011 0140
61     STU PCT F           0140  21 0299 0337
62     EQU     RAU VXPLS        EQU  0337  60 0548 0387
63     FMP O/F             0387  39 0199 0049
64     FAD VFPLS          0049  32 0598 0437
65     STU TEMPO          0437  21 9011 0145
66     RSU VXMIN          0145  61 0549 0487
67     FMP O/F             0487  39 0199 0099
68     FSR VFMIN          0099  33 0599 0987
69     FDV TEMPO          0987  34 9011 0190
70     STU EQRAT          0190  21 0399 0038
71 1
72     PRCNT   RAU 10053        0141  60 0048 0088
73     FSR PCT F           0088  33 0299 0138
74     FDV PCT F           0138  34 0299 0149
75     STU O/F             0149  21 0199 0337
76 1
77     EQUIV   RAU VXPLS        0191  60 0548 0188
78     FMP EQRAT          0188  39 0399 0249
79     FAD VXMIN          0249  32 0549 0238
80     STU TEMPO          0238  21 9011 0195
81     RSU VFPLS          0195  61 0598 0288
82     FMP EQRAT          0288  39 0399 0349
83     FSR VFMIN          0349  33 0599 0338
84     FDV TEMPO          0338  34 9011 0241
85     STU O/F             0241  21 0199 0388
86     FAD 10051          0388  32 0090 0438
87     STU TEMPO          0438  21 9011 0245
88     RAU 10053          0245  60 0048 0488
89     FDV TEMPO          0488  34 9011 0291
90     STU PCT F           0291  21 0299 0038
91 1
92     ATM 1   RAU O/F           0038  60 0199 0988
93     FAD 10051          0988  32 0090 0039
94     STU 1 O/F           1 PLUS C/F 0039  21 0094 0047
95     RAB 0010            0047  82 0010 0089
96     RAA 0000  ATM 2         0089  80 0000 0295
97 1
98     ATM 2   RAU 0537 A       CALCULATE 0295  60 2537 0341
99     FMP O/F             ATOMS PER 0341  39 0199 0449
100    FAD 0587 A           GRAM OF  0449  32 2587 0139
101    FDV 1 O/F            PROPELLANT 0139  34 0094 0144
102    STU G0005 A           0144  21 2005 0189
103    SXB 0001              0189  53 0001 0345

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104	NZB	ATM 3		0345	42 0098 0999
105	AXA 0001	ATM 2		0098	50 0001 0295
106 1					
107	ATM 3	RAU 0547	CALCULATE	0999	60 0547 0239
108	FMP O/F		ENTHALPY	0239	39 0199 1349
109	FAD 0597		OVER R	1349	32 0597 0289
110	FDV 1 O/F		PER GRAM	0289	34 0094 0194
111	FDV R		OF	0194	34 1146 0046
112	STU G0004	DIST2	PROPELLANT	0046	21 0004 0339
113 1					
114 1	AN EIGHT IN POSITION TWO OF				
115 1	CONSOLE CAUSES PUNCHING OF				
116 1	AQ 80 ETC				
117 1					
118	DIST2	RAU 8000		0339	60 8000 0097
119	BD2	IDEN		0097	92 0389 0439
120	RAL SPEC1			0389	65 0242 0147
121	LDD	PUNCH		0147	69 0489 1950
122	RAL SPEC2			0489	65 0292 0197
123	LDD IDEN	PUNCH		0197	69 0439 1950
124 1					
125	IDFN	RAU EQRAT	EQUIV RATO	0439	60 0399 0989
126	STD M0006			0989	24 9005 0395
127	UFA 55 I			0395	02 0148 0240
128	SRT 0002			0240	30 0002 0247
129	SLO 8002			0247	16 8002 0290
130	SLT 0006			0290	35 0006 0340
131	AUP F0039			0340	10 1148 0390
132	STU M0011		IDNTFICATN	0390	21 9010 0297
133	SLT 0008			0297	35 0008 0440
134	NZU	IDEN2		0440	44 0093 0244
135	RAU M0011			0093	60 9010 0490
136	STU F0039	IDEN3		0490	21 1148 0990
137	IDEN2	RAU F0000		0244	60 1109 1340
138	SRT 0001			1340	30 0001 0347
139	SLO 8002			0347	16 8002 0391
140	STD TEMPO			0391	24 9011 0397
141	SRT 0008			0397	30 0008 0441
142	SLO 8002			0441	16 8002 0491
143	ALO TEMPO			0491	15 9011 0991
144	SLT 0001			0991	35 0001 0447
145	AUP M0011			0447	10 9010 1341
146	STU M0011			1341	21 9010 0342
147	STD F0039	IDEN3		0342	24 1148 0990
148	IDEN3	RAU F0000	CONVERT	0990	60 1109 0392
149	STD M0009			0392	24 9008 0198
150	FDV CONS1		CHAM PRESS	0198	34 1140 0442
151	STU F0000		TO ATMOSP	0442	21 1109 0492
152	LDD O/F		OXID/FUEL	0492	69 0199 0992
153	STD M0007		WT RATIO	0992	24 9006 0248
154	LDD PCT F		PERCENT	0248	69 0299 1342
155	STD M0008		FUEL BY WT	1342	24 9007 0193
156	RAU G0004		ENTHALPY	0193	60 0004 0243
157	FMP R			0243	39 1146 0096
158	STU M0010			0096	21 9009 0293
159	RAL SPEC3			0293	65 0146 0343
160	STU PROB		CLEAR PROB	0343	21 1904 0393
161	LDD	PUNCH		0393	69 0196 1950
162	RAA 0050	IDEN1		0196	80 0050 0443
163	SET 9005			0443	27 9005 0348
164	LBB 0537 A			0348	08 2537 0493
165	RAL SPEC3			0493	65 0146 0993
166	LDD	PUNCH		0993	69 0246 1950
167	SET 9005			0246	27 9005 1343
168	LBB 0542 A			1343	08 2542 0445
169	RAL SPEC3			0445	65 0146 0294
170	LDD	PUNCH		0294	69 0497 1950
171	SET 9005			0497	27 9005 0344
172	LBB 0547 A			0344	08 2547 0394
173	RAL SPEC3			0394	65 0146 0444
174	STU M0009		CLEAR	0444	21 9008 0494
175	STD M0010		CLEAR	0494	24 9009 0994
176	LDD	PUNCH		0994	69 0997 1950
177	NZA BEGIN			0997	40 1344 0000
178	RAA 0000	IDEN1		1344	80 0000 0443
179					
180					
181 1		CONSTANTS			
182 1					
183 1					
184	10051	10 0000 0051		0090	10 0000 0051
185	10053	10 0000 0053		0048	10 0000 0053
186	55 I	00 0000 0055		0148	00 0000 0055
187	R	19 8718 0051		1146	19 8718 0051
188	CONS1	14 6960 0652		1140	14 6960 0652
189	SPEC1	00 G0005 0010		0242	00 0005 0010
190	SPEC2	00 G0004 0001		0292	00 0004 0001
191	SPEC3	00 M0006 0006		0146	00 9005 0006
192	SPEC4	00 9005 0006		0495	00 9005 0006
193	PAT				

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1 1          ROCKET PACKAGE EXCERPT FOR
2 1          FOR GENERAL ROCKET PERFORMANCE
3 1
4 1
5 1          SYN PROR    1904
6 1          SYN EXP E  1850
7 1          SYN SORT   1900
8 1          SYN PUNCH  1950
9 1          SYN LINK   1855
10 1         SYN CARDN  1852
11 1         SYN J000N  1961
12 1         REG X1883  1899
13 1         REG C9050  9050
14 1         REG R1951  1960      READ BAND
15 1         REG J1962  1967
16 1         REG K1968  1973
17 1         REG P1977  1986
18 1         REG S1987  1995
19 1         BLR 0000  1832
20 1
21 1
22 1          EXPONENTIAL
23 1
24 1         REG X1883  1899      17 WORDS
25 1
26 1         EXP E     STD LINK
27 1         FMP EX1    EXB1
28 1         EX1 4294  4850
29 1         EXR1 SET 9043
30 1         SET 9043
31 1         LDA X0001
32 1         STU 9040
33 1         FSA 9043
34 1         RMJ FX42
35 1         FAD 9043
36 1         NZU EXB61
37 1         FAD 9043
38 1         BMJ EXB3
39 1         RAU 9040
40 1         RMJ EXB4
41 1         LDD EX2    EXB5
42 1         X0001 40 0000 0052
43 1         EXB2 LDD 8666
44 1         EXB3 RAU 8002
45 1         EXB61 RAU 9040
46 1         FDV EX1
47 1         FAD 9058  LINK
48 1         EXB4 RSU 8003
49 1         STU 9040
50 1         LDD EX3    EXB5
51 1         EXB5 STD 9041
52 1         FAD HALF
53 1         UFA EXP58  9049
54 1         X0007 STU 9042
55 1         FAD 8002  9050
56 1         X0008 FAM 9040
57 1         STU 9040
58 1         LDD 8005
59 1         STD 9043
60 1         RSA 0007
61 1         RAU 8002  9059
62 1         FMP 9040  9044
63 1         X0002 FAD 9258  9045
64 1         X0003 NZA 9046  9047
65 1         X0004 AXA 0001  9059
66 1         X0005 FMP 8003  9048
67 1         X0006 STU 9040  EXB6
68 1         FXR6 RAA 9043
69 1         RSU 9042
70 1         SRT 0002
71 1         RAU 8003
72 1         AUP 9040
73 1         STU 9040  9041
74 1         EX2 RAU 9058
75 1         FDV 9040  LINK
76 1         EX3 RAU 8001  LINK
77 1         HALF 50 0000  0050
78 1         X0009 93 2642  6747
79 1         X0010 25 5491  8048
80 1         X0011 17 5211  2049
81 1         X0012 72 9517  3749
82 1         X0013 25 4393  5750
83 1         X0014 66 2730  8850
84 1         X0015 11 5129  2851
85 1         X0016 10 0000  0051
86 1         EXP58 00 0000  0058
87 1
88 1
89 1          SQUARE ROOT ROUTINE
90 1
91 1         REG C9050  9050
92 1         REG S1987  1995      NINE WORDS
93 1
94 1         SORT STD LINK
95 1         RMJ STOP
96 1         NZE LINK
97 1         STU C0000
98 1         SET C0001
          1900 24 1855 1908
          1908 46 1912 1864
          1864 45 1868 1855
          1868 21 9049 1875
          1875 27 9050 1880

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99	LBB S0001				1880	08 1987 1840
100	SRT 0002		CUTOFF EXP	1840	30 0002 1947	
101	RAU 8002			1947	60 8002 1907	
102	MPY 00050		HALF EXP	1907	19 1914 1834	
103	SUP 8002		SAVE DEC	1834	11 8002 1844	
104	AUP 1ST F			1844	10 1997 1901	
105	ALO 8002	C0001		1901	15 8002 9050	
106	STU C0010	C0002		1987	21 9059 9051	
107	S0002	RAU C0000	C0003	1988	60 9049 9052	
108	S0003	FDV C0010	C0004	1989	34 9059 9053	
109	S0004	FAD C0010	C0005	1990	32 9059 9054	
110	S0005	FMP C0009	C0006	1991	39 9058 9055	
111	S0006	SUP C0010	C0007	1992	11 9059 9056	
112	S0007	NZE C0008		1993	45 9057 1948	
113		RAU C0010	LINK	1948	60 9059 1855	
114	S0008	AUP C0010	C0001	1994	10 9059 9050	
115	S0009	50 0000	0050	1995	50 0000 0050	
116 1						
117	50 00 0000	0050		1914	00 0000 0050	
118	1ST F	70 0000	0025	1997	70 0000 0025	
119	STOP	99 9999	9999	SORT NEG X	1912 99 9999 9999	
120 1						
121 1						
122 1		PUNCH BELL CARDS				
123 1						
124	REG C9050	9050				
125	SYN J000N	1961				
126	REG J1962	1967	SIX WORDS			
127	REG K1968	1973	SIX WORDS			
128	REG P1977	1986	PUNCH BAND			
129 1						
130	PUNCH	STD LINK		START HERE	1950 24 1855 1909	
131	LOD 8003			1909	69 8003 1917	
132	SDA C0005			1917	22 9054 1924	
133	SLT 0004			1924	35 0004 1935	
134	SDA C0006			1935	22 9055 1942	
135	SRT 0002			1942	30 0002 1849	
136	RAU 8003			1849	60 8003 1915	
137	SRT 0002			1915	30 0002 1872	
138	SET C0007			1872	27 9056 1928	
139	LOD WDCT6			1928	69 1881 1934	
140	STD P0009			1934	24 1985 1838	
141	LOD PROR			1838	69 1904 1918	
142	STD P0008			1918	24 1984 1837	
143	LDD C0005	PCH3		1837	69 9054 1944	
144	PCH3	STD P0007		1944	24 1983 1936	
145	ALO CARDN			1936	15 1852 1920	
146	ALO ONE D			1920	15 1923 1879	
147	SDA CARDN			1879	22 1852 1922	
148	STL P0010	NZERO		1922	20 1986 1940	
149	NZERO	RAU C0006		IS NO OF WORDS LESS	1940 60 9055 1998	
150	SUP WDCT6			1998	11 1881 1937	
151	PCH4	PMI LESS6	PCH4		1937 46 1841 1941	
152	STU C0006			1941	21 9055 1949	
153	RAU P0009			1949	60 1985 1946	
154	SRT 0004			1946	30 0004 1974	
155	AUP XM0VE			1974	10 1929 1933	
156	ALO XLOC			1933	15 1938 1996	
157	ALO C0005	MOVEW		1996	15 9054 1853	
158	MOVEW	AUP 09999	8002		1853 10 1925 8002	
159	B002	LOD LOC	8003		8002 69 1999 8003	
160	B003	STD P0007	J000N		8003 24 1983 1961	
161	J0000	RAU C0006	PCH2		1961 60 9055 1975	
162	J0001	RAU C0006	PCH2		1962 60 9055 1975	
163	J0002	ALO ONE D	MOVEW		1963 15 1923 1853	
164	J0003	ALO ONE D	MOVEW		1964 15 1923 1853	
165	J0004	ALO ONE D	MOVEW		1965 15 1923 1853	
166	J0005	ALO ONE D	MOVEW		1966 15 1923 1853	
167	J0006	ALO ONE D	MOVEW		1967 15 1923 1853	
168	PCH?	PCH P0001			1975 71 1977 1930	
169	NZE	LINK			1930 45 1902 1855	
170		RAU P0007			1902 60 1983 1903	
171		AUP P0009			1903 10 1985 1926	
172		STU C0005	PCH3		1926 21 9054 1944	
173 1						
174	LESS6	RAL C0006			1841 65 9055 1976	
175		STD P0009			1976 24 1985 1931	
176		SRT 0004			CLEAR ZFRO	1931 30 0004 1882
177		ALO XCLR	8002		1882 15 1932 8002	
178	8002	00 0000	K0001		8002 00 0000 1968	
179	K0001	STU P0001	K0002		1968 21 1977 1969	
180	K0002	STU P0002	K0003		1969 21 1978 1970	
181	K0003	STU P0003	K0004		1970 21 1979 1971	
182	K0004	STU P0004	K0005		1971 21 1980 1972	
183	K0005	STU P0005	K0006		1972 21 1981 1973	
184	K0006	STU P0006	PCH4		1973 21 1982 1941	
185 1						
186	XCLR	00 0000	K0001		1932 00 0000 1968	
187	WDCT6	00 0006	0000		1881 00 0006 0000	
188	9999	00 0000	9999		1925 00 0000 9999	
189	XLOC	LDD 0000	8003		1938 69 0000 8003	
190	XMOVF	STD P0000	J0001		1929 24 1976 1962	
191	CARDN	00 0000	0000		1852 20 0000 0000	
192	ONE D	00 0001	0000		1923 00 0001 0000	
193	PLA	0000	1832			
194	PAT					

APPENDIX G  
FROZEN-COMPOSITION PROGRAM

```

1 1          GENERAL FROZEN COMPOSITION
2 1          PERFORMANCE PROGRAM
3 1
4 1
5 1
6 1          THIS PROGRAM ASSUMES THAT
7 1          LN OF COMBUSTION COMPOSITION
8 1          TEMPERATURE PRESSURE ENTHALPY
9 1          MOLECULAR WEIGHT FACTOR A AND
10 1         ALL NECESSARY THERMODYNAMIC
11 1         COEFFICIENTS ARE ALREADY IN
12 1         STORAGE
13 1
14 1
15      SYN LNX      1700
16      SYN EXP E    1850
17      SYN SORT     1900
18      SYN PUNCH    1950
19      SYN PCPCT    0017
20      SYN COMEX    0061
21      SYN START    0500
22      SYN TEMP1   1048
23      SYN TEMP2   1049
24      SYN PC      1109
25      SYN RDB     1193
26      SYN LINK    1855
27      SYN CARDN   1852
28      SYN PROB    1904
29      REG A1347   1349
30      REG B1247   1249
31      REG C9050   9050
32      REG F1110   1149
33      REG G0001   0015
34      REG M9000   9000
35      REG P1599   1659
36      REG R1075   1099
37      REG T0660   0959
38      BLR 1832   1999
39      EQU PCP     F0001
40      EQU TEE     F0002
41      EQU P      F0003
42      EQU H      F0004
43      EQU I      F0005
44      EQU M      F0006
45      EQU CF     F0007
46      EQU EPSIL   F0008
47      EQU MACH   F0009
48      EQU I VAC   F0010
49      EQU CP     F0011
50      EQU GAMMA  F0012
51      EQU S      F0015
52      EQU CSTAR  F0020
53      EQU AW     F0021
54      EQU HSTR   F0023
55      EQU AAY    F0024
56      EQU HC     F0025
57      EQU PLNP   F0026
58      EQU SC     F0027
59      EQU AWT    F0028
60      EQU RA     F0029
61      EQU RM     F0030
62      EQU CONS1  F0031
63      EQU CONS2  F0032
64      EQU CONS3  F0033
65      EQU CONS4  F0034
66      EQU CONS5  F0035
67      EQU R      F0037
68      EQU GC     F0038
69      EQU IDENT  F0039
70      EQU ONE    F0040
71      EQU LNT    G0002
72      EQU PO     G0015
73      EQU S CPR  1347
74      EQU S HRT  1348
75      EQU S SR   1349
76      EQU CODE   9000
77      EQU T     9003
78      EQU A     9021
79      EQU B     9022
80      EQU C     9023
81      EQU D     9024
82      EQU E     9025
83      EQU F     9026
84      EQU NI    9027
85      EQU TWO   9028
86      EQU THREE 9029
87      EQU FOUR  9030
88      EQU TEM 1  9049
89      EQU BASIC 9050
90      EQU TEMPO 9059

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E-417

91 1						
92	START	RSM IDENT			0500	68 1148 0053
93		STL IDENT	X1	REVRS SIGN	0053	20 1148 0051
94 1						
95 1		CONVERT LNNI TO NI				
96	X1	RAA 0000			0051	80 0000 0057
97		RAC 0000 X2			0057	88 0000 0063
98	X2	RAL P0001 A			0063	65 3599 0103
99		NZE X5			0103	45 0056 0107
100		RAU P0002 A			0056	60 3600 0055
101		BMI X3 X4			0055	46 0058 0059
102	X4	RAU T0008 C			0059	60 6667 0021
103		LDD EXP E			0021	69 0024 1850
104		STU T0008 C X3			0024	21 6667 0058
105	X3	AXA 0002			0058	50 0002 0064
106		AXC 0010 X2			0064	58 0010 0063
107 1		CLEAR F REGION				
108	X5	SET M0004			0107	27 9003 0062
109		LDB F0004			0062	09 1113 0016
110		RSA 0026			0016	81 0026 0022
111		RAU 8003 X6			0022	60 8003 0029
112	X6	STL F0030 A			0029	20 3139 0042
113		NZA X7			0042	40 0045 0046
114		AXA 0001 X6			0045	50 0001 0029
115 1						
116 1		SAVE TEE HC M AND AAY				
117 1		OF COMBUSTION				
118	X7	LDD M0024	AAY		0046	69 9023 0052
119		STD F0024			0052	24 1133 0036
120		LDD M0025	HC		0036	69 9024 0092
121		STD F0025			0092	24 1134 0037
122		LDD TEE			0037	69 1111 0114
123		STD T			0114	24 9003 0020
124		LDD M0006	M		0020	69 9005 0026
125		STD F0006			0026	24 1115 0018
126 1						
127 1		COMPUTE R/AAY AND STORE IN RA				
128		RAU R			0018	60 1146 0101
129		FDV AAY			0101	34 1133 0033
130		STU RA			0033	21 1138 0041
131 1						
132 1		COMPUTE R/M AND STORE IN RM				
133		RAU R			0041	60 1146 0151
134		FDV M			0151	34 1115 0065
135		STU RM			0065	21 1139 0142
136		RAU 8003			0142	60 8003 0049
137		STL COMEX			0049	20 0061 0164
138 1						
139 1		FOR COMBUSTION OUT IS Z1				
140		LDD Z1			0164	69 0067 0070
141		STD OUT Y1			0070	24 0023 0076
142 1						
143 1		LOOP TO COMPUTE				
144 1		SUM NI CPR				
145 1		SUM NI HRT				
146 1		SUM NI SR				
147 1						
148 1		LOOP IS COMPLETED WHEN ZERO				
149 1		APPEARS IN P REGION				
150 1		THEN GO TO OUT				
151 1		OUT FOR COMB IS Z1				
152 1		OUT FOR THROAT AND EXIT IS				
153 1		FROZN				
154 1						
155	Y1	RAU 8003			0076	60 8003 0083
156		STL S CPR	CLER S CPR		0083	20 1347 0000
157		STL S HRT	CLER S HRT		0000	20 1348 0201
158		STL S SR	CLER S SR		0201	20 1349 0102
159		RAA 0000			0102	80 0000 0108
160		RAC 0000 Y2			0108	88 0000 0214
161	Y2	RAL P0001 A			0214	65 3599 0153
162		NZE OUT			0153	45 0106 0023
163		STL CODE THERM			0106	20 9000 0264
164	THERM	SET 9020			0264	27 9020 0019
165		LBB T0001 C			0019	08 6660 0113
166		RAU 9020			0113	60 9020 0071
167		SUP CODE			0071	11 9000 0079
168		NZU TH009			0079	44 0133 0034
169		HLT 0000 8866			0133	01 0000 8866

170	TH009	SET TWO	0034	27	9028	0039
171		LDB R0001	0039	09	1247	0050
172		RAU D	0050	60	9024	0157
173		FMP T	0157	39	9003	0060
174		FAD C	0060	32	9023	0089
175		FMP T	0089	39	9003	0192
176		FAD B	0192	32	9023	0121
177		FMP T	0121	39	9003	0074
178		FAD A	0074	32	9021	0203
179		FMP NI	0203	39	9027	0156
180		FAD S CPR	0156	32	1347	0073
181		STU S CPR	0073	21	1347	0100
182		RAU D	0100	60	9024	0207
183		FDV FOUR	0207	34	9030	0110
184		FMP T	0110	39	9003	0163
185		STU TEMPO	0163	21	9059	0171
186		RAU C	0171	60	9023	0129
187		FDV THREE	0129	34	9029	0032
188		FAD TEMPO	0032	32	9059	0111
189		FMP T	0111	39	9003	0314
190		STU TEMPO	0314	21	9059	0221
191		RAU B	0221	60	9022	0179
192		FDV TWO	0179	34	9028	0082
193		FAD TEMPO	0082	32	9059	0161
194		FMP T	0161	39	9003	0364
195		STU TEMPO	0364	21	9059	0271
196		RAU E	0271	60	9025	0229
197		FDV T	0229	34	9003	0132
198		FAD TEMPO	0132	32	9059	0211
199		FAD A	0211	32	9021	0091
200		FMP NI	0091	39	9027	0044
201		FAD S HRT	0044	32	1348	0025
202		STU S HRT	0025	21	1348	0251
203		RAU D	0251	60	9024	0109
204		FDV THREE	0109	34	9029	0112
205		FMP T	0112	39	9003	0115
206		STU TEMPO	0115	21	9059	0123
207		RAU C	0123	60	9023	0031
208		FDV TWO	0031	34	9028	0084
209		FAD TEMPO	0084	32	9059	0213
210		FMP T	0213	39	9003	0066
211		FAD B	0066	32	9022	0095
212		FMP T	0095	39	9003	0048
213		STU TEMPO	0048	21	9059	0105
214		RAU A	0105	60	9021	0263
215		FMP LNT	0263	39	0002	0152
216		FAD TEMPO	0152	32	9059	0081
217		FAD F	0081	32	9026	0261
218		FMP NI	0261	39	9027	0414
219		FAD S SR	0414	32	1349	0075
220		STU S SR	0075	21	1349	0202
221		AXA 0002	0202	50	0002	0158
222		AXC 0010	0158	58	0010	0214
223	1	TEST FOR CONVERGENCE				
224	1	IS DEL S ZERO				
225	1					
226	1	YES MEANS CONVERGENCE				
227	1	GO TO BTHER				
228	1					
229	1	NO MEANS NO CONVERGENCE				
230	1	CORRECT T AND THEN GO TO Y1				
231	1					
232	1	FROZN RAU PLNP	0150	60	1135	0139
233		FAD S SR	0139	32	1349	0125
234		STU TEM 1	0125	21	9049	0183
235		FDV SC	0183	34	1136	0086
236		FSB EINSS	0086	33	0189	0165
237		NZU BTHER	0165	44	0069	0120
238		RSU TEM 1	0069	61	9049	0027
239		FAD SC	0027	32	1136	0313
240		FDV S CPR	0313	34	1347	0047
241		FAD LNT	0047	32	0002	0279
242		STU LNT	0279	21	0002	0155
243		LDD EXP E	0155	69	0208	1850
244		STU T	0208	21	9003	0215
245		LDD FROZN	0215	69	0150	0253
246		STD OUT	0253	24	0023	0076
247		Y1				

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248 1
249 1           AFTER CONVERGENCE TEST IF
250 1           CORRECT TDATA IS IN STORAGE
251 1           YES GO TO FIX
252 1           NO GO TO TDATA
253 1
254   BTHER  SET 9050          0120 27 9050 0175
255       LBB TEMP1          0175 08 1048 0301
256       RAU 9051          0301 60 9051 0159
257       FSB T              0159 33 9003 0239
258       BMI TDATA          0239 46 0242 0043
259       RAU T              0043 60 9003 0351
260       FSB 9050          0351 33 9050 0131
261       BMI TDATA  FIX     0131 46 0242 0035
262 1
263 1           READ THERMAL DATA
264 1           WHEN CORRECT TDATA IS FOUND
265 1           GO TO Y1
266   TDATA  RAA 0000          0242 80 0000 0098
267       RAC 0000 TD001      0098 88 0000 0054
268   TD001  RCD BASIC BELL    0054 70 9050 0104
269   BASIC  RAL 9051 RDB      9050 65 9051 1193
270   RDB    SLT 0004          1193 35 0004 0303
271       STU 9051          0303 21 9051 0311
272       SUP P0001 A          0311 11 3599 0353
273       NZU TD005          0353 44 0257 0258
274       LDD T0008 C          0258 69 6667 0170
275       STD 9058          0170 24 9058 0126
276       SET 9051          0126 27 9051 0181
277       SBB T0001 C          0181 28 6460 0363
278       AXA 0002          0363 50 0002 0119
279       AXC 0010 TD001      0119 58 0010 0054
280   TD005  HLT 0000 7766    0257 01 0000 7766
281   BELL   RAU 9051          0104 60 9051 0361
282       FSB T              0361 33 9003 0141
283       BMI TDATA          0141 46 0242 0145
284       RAU T              0145 60 9003 0403
285       FSB 9050          0403 33 9050 0233
286       BMI TDATA          0233 46 0242 0087
287       SET 9050          0087 27 9050 0292
288       SBB TEMP1 Y1        0292 28 1048 0076
289 1
290   FIX    LDD T          0035 69 9003 0191
291       STD TEE          0191 24 1111 0464
292       LDD PO           0464 69 0015 0068
293       STD P            0068 24 1112 0067
294 1
295       EQU PCP M0001
296       EQU TEE M0002
297       EQU P  M0003
298       EQU H  M0004
299       EQU I  M0005
300       EQU M  M0006
301       EQU CF M0007
302       EQU EPSIL M0008
303       EQU MACH M0009
304       EQU I VAC M0010
305       EQU CP  M0011
306       EQU GAMMA M0012
307       EQU S   M0015
308       EQU CSTAR M0020
309       EQU AW  M0021
310       EQU HSTR M0023
311       EQU AAY M0024
312       EQU HC  M0025
313       EQU PLNP M0026
314       EQU SC  M0027
315       EQU AWT M0028
316       EQU RA  M0029
317       EQU RM  M0030
318       EQU CONS1 M0031
319       EQU CONS2 M0032
320       EQU CONS3 M0033
321       EQU CONS4 M0034
322       EQU CONS5 M0035
323       EQU R   M0037
324       EQU GC  M0038
325       EQU IDENT M0039
326       EQU ONE M0040
327 1

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328 1
329 1      CALCULATE ROCKET PERFORMANCE
330 1      PARAMETERS
331 1
332 1      Z1      SET M0001          0067 27 9000 0072
333 1      LDB F0001          0072 09 1110 0413
334 1
335 1      COMPUTE CP
336 1      RAU S CPR          0413 60 1347 0401
337 1      FMP RA             0401 39 9028 0154
338 1      STU CP             0154 21 9010 0411
339 1
340 1      COMPUTE GAMMA
341 1      FSB RM             0411 33 9029 0241
342 1      STU TEM 1          0241 21 9049 0099
343 1      RAU CP             0099 60 9010 0307
344 1      FDV TEM 1          0307 34 9049 0160
345 1      STU GAMMA          0160 21 9011 0117
346 1
347 1      COMPUTE ENTHALPY
348 1      RAU S HRT           0117 60 1348 0453
349 1      FMP TEE             0453 39 9001 0206
350 1      FMP RA             0206 39 9028 0209
351 1      STU H               0209 21 9003 0167
352 1
353 1      TEST COMEX
354 1      ZERO MEANS COMBUSTION
355 1      NONZERO MEANS THROAT OR EXIT
356 1
357 1      RAU COMEX          0167 60 0061 0265
358 1      NZU TOREX          0265 44 0169 0220
359 1
360 1      COMPUTE PSEUDO ENTROPY FOR
361 1      COMBUSTION
362 1      RAU S SR             0220 60 1349 0503
363 1      STU SC             0503 21 9026 0461
364 1      FMP RA             0461 39 9028 0514
365 1      STU S               0514 21 9014 0321
366 1      RSU UNITY           SET COMEX 0321 61 0124 0329
367 1      STU COMEX PNCH       FOR THROAT 0329 21 0061 0564
368 1
369 1      COMPUTE PSEUDO ENTROPY FOR
370 1      THROAT AND EXIT
371 1      TOREX   RAU S SR          0169 60 1349 0553
372 1      FAD PLNP            0553 32 9025 0283
373 1      FMP RA             0283 39 9028 0136
374 1      STU S               0136 21 9014 0093
375 1      RAU COMEX          0093 60 0061 0315
376 1      BMI THROT EXIT       0315 46 0118 0219
377 1      EQU TWO B0001
378 1
379 1      CONVERGENCE TEST FOR THROAT
380 1      IS HC EQUAL TO HSTR
381 1      IF YES GO TO CSTR1
382 1      IF NO THEN CORRECT P AND GO
383 1      TO FROZN
384 1
385 1      THROTT RAU TEE         0118 60 9001 0225
386 1      FDV M               0225 34 9005 0028
387 1      FMP R               0028 39 9036 0231
388 1      FDV TWO             0231 34 1247 0097
389 1      STU RT/2M            0097 21 0252 0205
390 1      FMP GAMMA          0205 39 9011 0308
391 1      FAD H               0308 32 9003 0137
392 1      STU HSTR            0137 21 9022 0195
393 1      FDV HC              0195 34 9024 0148
394 1      FSB EINS            0148 33 0451 0077
395 1      NZU                 CSTR1 0077 44 0281 0182
396 1      RAU GAMMA          0281 60 9011 0289
397 1      FAD ONE             0289 32 9039 0269
398 1      FMP RT/2M            0269 39 0252 0302
399 1      STU TEMPO           0302 21 9059 0259
400 1      RAU HC              0259 60 9024 0217
401 1      FSB HSTR            0217 33 9022 0147
402 1      FDV TEMPO           0147 34 9059 0200
403 1      FAD ONE             0200 32 9039 0379
404 1      FMP P               0379 39 9002 0232
405 1      STU PO              0232 21 0015 0168
406 1      RAU PC              0168 60 1109 0463
407 1      FDV PO              0463 34 0015 0365
408 1      STU R0002           0365 21 1076 0429
409 1      STU F0001           0429 21 1110 0513
410 1      LDD                 LNX   0513 69 0116 1700
411 1      FMP PC              0116 39 1109 0309
412 1      STU F0026           FROZN 0309 21 1135 0150
413 1      CSTR1   LDD CSTR2 SEVRL 0182 69 0085 0038
414 1

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415 1	STORE A/W FOR THROAT				
416	CSTR2	RAU AW			0085 60 9020 0143
417		STD AWT			0143 24 9027 0149
418 1					
419 1	COMPUTE CSTAR				
420	FMP PC				0149 39 1109 0359
421	FMP GC				0359 39 9037 0162
422	FMP CONS1				0162 39 9030 0415
423	STU CSTAR				0415 21 9019 0173
424	LDD UNITY		SET COMEX		0173 69 0124 0127
425	STD COMEX	REMAN	FOR EXIT		0127 24 0061 0614
426 1					
427	EXIT	LDD REMAN	SEVRL		0219 69 0614 0038
428 1					
429 1	COMPUTE THRUST COEFFICIENT CF				
430	REMAN	RAU I			0614 60 9004 0371
431	FMP GC				0371 39 9037 0174
432	FDV CSTAR				0174 34 9019 0177
433	STU CF				0177 21 9006 0135
434 1					
435 1	COMPUTE AREA RATIO				
436	RAU AW				0135 60 9020 0193
437	FDV AWT				0193 34 9027 0096
438	STU EPSIL				0096 21 9007 0603
439 1					
440 1	COMPUTE SP IMP IN VACUUM IVAC				
441	RAU AW				0603 60 9020 0511
442	FMP P				0511 39 9002 0964
443	FMP CONS1				0964 39 9030 0267
444	FAD I				0267 32 9004 0197
445	STU I VAC				0197 21 9009 0255
446 1					
447 1	COMPUTE MACH NUMBER				
448	RAU GAMMA				0255 60 9011 0563
449	FMP TEE				0563 39 9001 0166
450	FMP CONS2				0166 39 9031 0319
451	FDV M				0319 34 9005 0122
452	LDD MACH1	SORT			0122 69 0275 1900
453	MACH1	STU TEMPO			0275 21 9059 0333
454	RAU I				0333 60 9004 0291
455	FDV TEMPO				0291 34 9059 0094
456	STU MACH	PNCH			0094 21 9008 0564
457	SEVRL	STD LINK1			0038 24 0341 0144
458 1					
459 1	COMPUTE SPECIFIC IMPULSE I				
460	RAU HC				0144 60 9024 0501
461	FSB H				0501 33 9003 0331
462	FDV CONS3				0331 34 9032 0134
463	LDD IMPUL	SORT			0134 69 0187 1900
464	IMPUL	FMP CONS4			0187 39 9033 0040
465	STU I				0040 21 9004 0247
466 1					
467 1	COMPUTE A/W				
468	RAU TEE				0247 60 9001 0305
469	FDV P				0305 34 9002 0358
470	FDV M				0358 34 9005 0561
471	FDV I				0561 34 9004 1014
472	FMP CONS2				1014 39 9031 0317
473	FDV CONS1				0317 34 9030 0270
474	STU AW	LINK1			0270 21 9020 0341
475 1					
476 1	PUNCH RESULTS THEN GO TO PCP 1				
477	PNCH	RAU 8003			0564 60 8003 0421
478		STL CARDN			0421 20 1852 0355
479		SET M0001			0355 27 9000 0210
480		STB F0001			0210 29 1110 0613
481		RSA 0005			0613 81 0005 0369
482		RAB 0004			0369 82 0004 0325
483		LDD IDENT			0325 69 9038 0381
484		STD M0011	PNCH1		0381 24 9010 0237
485	PNCH1	NZB	PCP 1		0237 42 0090 0391
486		SXB 0001			0090 53 0001 0146
487		AXA 0005			0146 50 0005 0352
488		SET M0006			0352 27 9005 0357
489		LBB F0001	A		0357 08 3110 0963
490		NZA SPEC			0963 40 0216 0367
491		RAL SPEC1	PNCH2		0367 65 0320 0375
492	PNCH2	LDD PNCH1	PUNCH		0375 69 0237 1950
493	SPEC	RAL SPEC2	PNCH2		0216 65 0419 0375
494	COMP1	LDD FROZN	PCP 1		0250 69 0150 0391
495 1					

496	1				
497		EQU PCP	F0001		
498		EQU TEE	F0002		
499		EQU P	F0003		
500		EQU H	F0004		
501		EQU I	F0005		
502		EQU M	F0006		
503		EQU CF	F0007		
504		EQU EPSIL	F0008		
505		EQU MACH	F0009		
506		EQU I VAC	F0010		
507		EQU CP	F0011		
508		EQU GAMMA	F0012		
509		EQU S	F0015		
510		EQU CSTAR	F0020		
511		EQU AW	F0021		
512		EQU HSTR	F0023		
513		EQU AAY	F0024		
514		EQU HC	F0025		
515		EQU PLNP	F0026		
516		EQU SC	F0027		
517		EQU AWT	F0028		
518		EQU RA	F0029		
519		EQU RM	F0030		
520		EQU CONS1	F0031		
521		EQU CONS2	F0032		
522		EQU CONS3	F0033		
523		EQU CONS4	F0034		
524		EQU CONS5	F0035		
525		EQU R	F0037		
526		EQU GC	F0038		
527		EQU IDENT	F0039		
528		EQU ONE	F0040		
529	1				
530	1	ADVANCE PRESSURE RATIO PCP			
531	1	COMPUTE PC LN PC/PE			
532	1	AND STORE IN PLNP			
533	1				
534	PCP	1	RAL PCPCT	0391	65 0017 0471
535			ALO UNITY	0471	15 0124 0479
536			STL PCPCT	0479	20 0017 0370
537			RAA 8001	0370	80 8001 0176
538			SLT 0004	0176	35 0004 0287
539			STL PROB	0287	20 1904 0407
540			RAU R0000 A	0407	60 3074 0529
541			STU PCP	0529	21 1110 1013
542			NZU 9999	1013	44 0417 9999
543			LDD LNX	0417	69 0420 1700
544			FMP PC	0420	39 1109 0409
545			STU PLNP	0409	21 1135 0088
546			RAU PC	0088	60 1109 1063
547			FDV PCP	1063	34 1110 0260
548			STU PO	0260	21 0015 0150
549	1				
550	1	CONSTANTS FOR PROGRAM			
551	ONE	10 0000	0051	1149	10 0000 0051
552	B0001	20 0000	0051	1247	20 0000 0051
553	B0002	30 0000	0051	1248	30 0000 0051
554	B0003	40 0000	0051	1249	40 0000 0051
555	CONS1	14 6960	0652	1140	14 6960 0652
556	CONS2	86 4554	0052	1141	86 4554 0052
557	CONS3	10 0000	0054	1142	10 0000 0054
558	CONS4	29 4980	0053	1143	29 4980 0053
559	CONS5	57 0000	0050	1144	57 0000 0050
560	R	19 8718	0051	1146	19 8718 0051
561	GC	32 1740	0052	1147	32 1740 0052
562	EINS	00 1000	0053	0451	00 1000 0053
563	EINSS	01 0000	0052	0189	01 0000 0052
564	UNITY	00 0000	0001	0124	00 0000 0001
565	SPEC1	07 M0006	0006	0320	07 9005 0006
566	SPEC2	00 M0006	0006	0419	00 9005 0006
567	1				

568 1  
 569 1 LNX ROUTINE EXCERPT FROM  
 570 1 THE ROCKET PACKAGE  
 571 1  
 572 1  
 573 REG C9050 9050  
 574 1  
 575 LNX STD LINK 1700 24 1355 0408  
 576 LDD OP1 0408 69 0611 1064  
 577 STD C0005 1064 24 9054 0470  
 578 NZU HLT 0470 44 0223 0224  
 579 BMI HLT 0223 46 0224 0227  
 580 SRT 0002 EXPON IN 0227 30 0002 0383  
 581 ALO EXP52 LO PUT IN 0383 15 0186 0441  
 582 STL C0001 FLT NOTATN 0441 20 9050 0198  
 583 SLO 8001 CLEAR LO 0198 16 8001 0405  
 584 ALO 51EXP NUM IN UPR 0405 15 0458 1163  
 585 SLT 0002 ADD 51 EXP 1163 35 0002 0469  
 586 STU C0002 0469 21 9051 0277  
 587 RAU C0001 SUB 51 FRM 0277 60 9050 0185  
 588 FSB 51LNK EXPONENT 0185 33 0138 0465  
 589 FMP LN10 MUL LN 10 0465 39 0218 0268  
 590 FAD LN3 ADD LN 3 0268 32 0521 0297  
 591 STU C0001 0297 21 9050 0455  
 592 RAU C0002 0455 60 9051 1213  
 593 FAD K X MINUS 3 1213 32 0266 0243  
 594 STU C0003 OVER 0243 21 9052 0551  
 595 RAU C0002 X PLUS 3 0551 60 9051 0459  
 596 FSB K 0459 33 0266 0293  
 597 FDV C0003 EQUALS Y 0293 34 9052 0196  
 598 FAD 8003 FORM 2Y 0196 32 8003 0425  
 599 ALO 8001 Y IN LOWER 0425 15 8001 0433  
 600 STU C0003 2Y IN 9003 0433 21 9052 0491  
 601 RSU 8002 MINUS Y IN 0491 61 8002 0199  
 602 FMP 8001 Y SQUARED 0199 39 8001 0402  
 603 STU C0002 0402 21 9051 0509  
 604 FMP K1 0509 39 0212 0262  
 605 FAD K2 0262 32 0515 0541  
 606 FMP C0002 0541 39 9051 0194  
 607 FAD K3 FORM 0194 32 0347 0273  
 608 FMP C0002 NUMERATOR 0273 39 9051 0226  
 609 FAD K4 0226 32 0579 0505  
 610 STU C0004 0505 21 9053 1263  
 611 RAU C0002 1263 60 9051 0571  
 612 FMP K5 0571 39 0274 0324  
 613 FAD K6 0324 32 0327 0653  
 614 FMP C0002 0653 39 9051 0256  
 615 FAD K7 FORM 0256 32 0559 0235  
 616 FMP C0002 DENOMINATOR 0235 39 9051 0188  
 617 FAD K4 0188 32 0579 0555  
 618 FDV C0004 QUOTIENT 0555 34 9053 0508  
 619 FMP C0003 MULT BY 2Y 0508 39 9052 0961  
 620 FAD C0001 0961 32 9050 0591  
 621 FMP C0005 LINK 0591 39 9054 1855  
 622 HLT HLT 1111 1111 0224 01 1111 1111  
 623 1  
 624 1 LN X ROUTINE CONSTANTS  
 625 EXP52 00 0000 0052 0186 00 0000 0052  
 626 51EXP 51 0000 0000 0458 51 0000 0000  
 627 51LNK 51 0000 0052 0138 51 0000 0052  
 628 K 30 0000 0051 0266 30 0000 0051  
 629 LN10 23 0258 5151 0218 23 0258 5151  
 630 LN3 10 9861 2351 0521 10 9861 2351  
 631 OP1 10 0000 0051 0611 10 0000 0051  
 632 K1 81 5850 8249 DENOM 4 0212 81 5850 8249  
 633 K2 73 4265 7350 DENOM 3 0515 73 4265 7350  
 634 K3 16 1538 4651 DENOM 2 0347 16 1538 4651  
 635 K4 99 9999 9950 0579 99 9999 9950  
 636 K5 17 0496 1749 NUM 4 0274 17 0496 1749  
 637 K6 39 5804 2050 NUM 3 0327 39 5804 2050  
 638 K7 12 8205 1351 NUM 2 0559 12 8205 1351

PAT												
1	000	000	0450	050	1110000000	950	1000	1111111111	1450	1500	1100011000	1950
2	000	001	0451	0501	110000000	951	1001	1111111111	1451	1501	1100111000	1951
3	000	000	0452	0502	1111000000	952	1002	1111111111	1452	1502	1100111000	1952
4*	000	000	0453	0503	1111000000	953	1003	1111111111	1453	1503	1100111000	1953
5	000	000	0454	0504	1111000000	954	1004	0011111111	1454	1504	1100111000	1954
6	000	111	0455	0505	110000000	955	1005	1111111111	1455	1505	1100111000	1955
7	000	001	0456	0506	1111000000	956	1006	1111111111	1456	1506	1100111000	1956
8	000	000	0457	0507	1111000000	957	1007	1111111111	1457	1507	1100111000	1957
9	000	000	0458	0508	1110000000	958	1008	1111111111	1458	1508	1100111000	1958
10	000	000	0459	0509	110000000	959	1009	1101111111	1459	1509	1100111000	1959
11	000	111	0460	051	1110000001	960	1010	1101111111	1460	1510	1101111000	1960
12	000	000	0461	0511	1101111111	961	1011	1101111111	1461	1511	1101111000	1961
13	000	111	0462	0512	1110000001	962	1012	1101111111	1462	1512	1101111000	1962
14	000	000	0463	0513	1110000001	963	1013	000000011111	1463	1513	1101111000	1963
15	000	000	0464	0514	1100000001	964	1014	0011111111	1464	1514	1101111000	1964
16	000	111	0465	0515	1100000001	965	1015	1101111111	1465	1515	1101111000	1965
17	000	001	0466	0516	1110000001	966	1016	1101111111	1466	1516	1101111000	1966
18	000	111	0467	0517	1110000001	967	1017	1101111111	1467	1517	1101111000	1967
19	000	000	0468	0518	1110000001	968	1018	1101111111	1468	1518	1101111000	1968
20	000	111	0469	0519	1110000001	969	1019	1101111111	1469	1519	1101111000	1969
21	000	000	0470	052	1110000001	970	1020	1101111111	1470	1520	1101111000	1970
22*	0001111111	0471	0521	10000001	971	1021	1101111111	1471	1521	1101111000	1971	
23	000	111	0472	0522	1110000001	972	1022	1101111111	1472	1522	1101111000	1972
24	000	000	0473	0523	1110000001	973	1023	1101111111	1473	1523	1101111000	1973
25	000	001	0474	0524	1110000001	974	1024	1101111111	1474	1524	1101111000	1974
26	000	111	0475	0525	1110000001	975	1025	1001111111	1475	1525	1101111000	1975
27	000	000	0476	0526	1110000001	976	1026	1001111111	1476	1526	1101111000	1976
28*	1111111111	0477	0527	1110000001	977	1027	1001111111	1477	1527	1101111000	1977	
29	000	000	0478	0528	1110000001	978	1028	1001111111	1478	1528	1101111000	1978
30*	1111111111	0479	0529	10000001	979	1029	1001111111	1479	1529	1101111000	1979	
31	000	011	0480	053	1110000001	980	1030	1001111111	1480	1530	1101111000	1980
32	000	'1111	0481	0531	1110000001	981	1031	1001111111	1481	1531	1101111000	1981
33	000	001	0482	0532	1110000001	982	1032	1001111111	1482	1532	1101111000	1982
34*	0001111111	0483	0533	1110000001	983	1033	1001111111	1483	1533	1101111000	1983	
35	000	1111	0484	0534	1110000001	984	1034	1001111111	1484	1534	1101111000	1984
36*	000	111111	0485	0535	1110000001	985	1035	1001111111	1485	1535	1101111000	1985
37	000	1111	0486	0536	1110000001	986	1036	1001111111	1486	1536	1101111000	1986
38*	000	111111	0487	0537	1110000001	987	1037	1001111111	1487	1537	1101111000	1987
39	000	1111	0488	0538	1110000001	988	1038	1001111111	1488	1538	1101111000	1988
40*	1111111111	0489	0539	1110000001	989	1039	1001111111	1489	1539	1101111000	1989	
41	000	000	0490	054	1110000001	990	1040	1001111111	1490	1540	1101111000	1990
42	000	111	0491	0541	10000001	991	1041	1001111111	1491	1541	1101111000	1991
43	000	1111	0492	0542	1110000001	992	1042	1001111111	1492	1542	1101111000	1992
44*	000	111111	0493	0543	1110000001	993	1043	1000111111	1493	1543	1101111000	1993
45*	000	111111	0494	0544	1110000001	994	1044	1001111111	1494	1544	1101111000	1994
46*	000	111111	0495	0545	1110000001	995	1045	1001111111	1495	1545	1101111000	1995
47	000	111	0496	0546	1110000001	996	1046	1001111111	1496	1546	1101111000	1996
48*	000	111111	0497	0547	1110000001	997	1047	1001110111	1497	1547	1101111000	1997
49*	000	111111	0498	0548	1110000001	998	1048	0001110111	1498	1548	1101111000	1998
			0499	0549	1110000001	999	1049	0001110111	1499	1549	1001111000	1999

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APPENDIX H  
VECTOR AND PROPELLANT PROGRAM

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1 1      PROGRAM FOR ASSEMBLING
2 1      COMBUSTION PRODUCT PACKED
3 1      VECTORS AND FUEL AND OXIDANT
4 1      GRAM ATOM RATIOS ENTHALPIES
5 1      AND OXIDATION NUMBERS
6 1
7      REG A0001    0011    ATOM TABLE
8      REG F0100    0199    FUELS
9      REG X0200    0299    OXIDANTS
10     REG L0300   0309    PCTS FUEL
11     REG D0310   0319    PCTS OXID
12     REG H0320   0329    FUEL ENTH
13     REG E0330   0339    OXID ENTH
14     REG W0340   0349    ATOMIC WTS
15     REG S0350   0359    OXID NUMBR
16     REG N0360   0379    MOLES
17     REG G0380   0399    GRAM ATOMS
18 1      PER GRAM
19      REG M0400   0510    ATOMIC WTS
20      REG V0600   0710    SYMBOL AND
21 1      OXID TABLE
22      REG U0800   0809
23      REG R1951   1960    READ BAND
24      REG P1977   1986    PUNCH BAND
25      REG C9000   9000
26      BLR 0000    0000
27      BLR 0090    0099    ZEROS
28      BLR 0360    0379    SPARE
29      BLR 0537    0549    OXIDANT
30      BLR 0587    0599    FUEL
31      BLR 0900    0909
32      BLR 1500    1999
33      SYN PUNCH   1930
34      SYN RMPCH   1940
35      EQU TEMPO   C0001    TEMPORARY
36      EQU TEMP1   C0002    TEMPORARY
37      EQU TEMP2   C0003    TEMPORARY
38      EQU R000X   R0001
39 1
40      EQU U01XX   U0101
41      EQU V00XX   V0001
42      EQU M00XX   M0001
43      EQU XXXXX   0000
44 1
45 1      TABLE OF ATOMIC WEIGHTS
46      M0001    39 9440  0052    ARGON      0400    39 9440  0052
47      M0002    22 7000  0053    ACTINIUM   0401    22 7000  0053
48      M0003    10 7880  0053    SILVER     0402    10 7880  0053
49      M0004    26 9800  0052    ALUMINUM   0403    26 9800  0052
50      M0005    24 3000  0053    AMERICIUM  0404    24 3000  0053
51      M0006    74 9100  0052    ARSENIC   0405    74 9100  0052
52      M0007    21 1000  0053    ASTATINE   0406    21 1000  0053
53      M0008    19 7000  0053    GOLD      0407    19 7000  0053
54      M0009    10 8200  0052    BORON     0408    10 8200  0052
55      M0010    90 1300  0051    BERYLLIUM 0410    90 1300  0051
56      M0011    20 9000  0053    BISMUTH   0411    20 9000  0053
57      M0012    24 5000  0053    BERKELIUM 0412    24 5000  0053
58      M0013    13 7360  0053    BARIUM    0409    13 7360  0053
59      M0014    79 9160  0052    BROMINE   0413    79 9160  0052
60      M0015    12 0110  0052    CARBON    0414    12 0110  0052
61      M0016    40 0800  0052    CALCIUM   0415    40 0800  0052
62      M0017    11 2410  0053    CADMIUM   0416    11 2410  0053
63      M0018    14 0130  0053    CERIUM    0417    14 0130  0053
64      M0019    24 8000  0053    CALIFORNUM 0418    24 8000  0053
65      M0020    35 4570  0052    CHLORINE  0419    35 4570  0052
66      M0021    24 5000  0053    CURIUM    0420    24 5000  0053
67      M0022    58 9400  0052    COBALT    0421    58 9400  0052
68      M0023    52 0100  0052    CHROMIUM  0422    52 0100  0052
69      M0024    13 2910  0053    CESIUM    0423    13 2910  0053
70      M0025    63 5400  0052    COPPER    0424    63 5400  0052
71      M0026    16 2510  0053    DYSPROSIUM 0425    16 2510  0053
72      M0027    25 5000  0053    EINSTEINUM 0426    25 5000  0053
73      M0028    16 7270  0053    ERBIUM    0427    16 7270  0053
74      M0029    15 2000  0053    EUROPIUM  0428    15 2000  0053
75      M0030    19 0000  0052    FLUORINE  0429    19 0000  0052
76      M0031    55 8500  0052    IRON      0430    55 8500  0052
77      M0032    25 2000  0053    FERMIUM   0431    25 2000  0053
78      M0033    22 3000  0053    FRANCIUM  0432    22 3000  0053
79      M0034    69 7200  0052    GALLIUM   0433    69 7200  0052
80      M0035    15 7260  0053    GADOLINIUM 0434    15 7260  0053
81      M0036    72 6000  0052    GERMANIUM 0435    72 6000  0052
82      M0037    10 0800  0051    HYDROGEN  0436    10 0800  0051

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83	M0038	40	0300	0051	HELlUM	0437	40	0300	0051
84	M0039	17	8580	0053	HAFNIUM	0438	17	8580	0053
85	M0040	20	0610	0053	MERCURY	0439	20	0610	0053
86	M0041	16	4940	0053	HOLMIUM	0440	16	4940	0053
87	M0042	12	6910	0053	IODINE	0441	12	6910	0053
88	M0043	11	4820	0053	INDIUM	0442	11	4820	0053
89	M0044	19	2200	0053	IRIDIUM	0443	19	2200	0053
90	M0045	39	1000	0052	POTASSIUM	0444	39	1000	0052
91	M0046	83	8000	0052	KRYPTON	0445	83	8000	0052
92	M0047	13	8920	0053	LANTHANUM	0446	13	8920	0053
93	M0048	69	4000	0051	LITHIUM	0447	69	4000	0051
94	M0051	17	4990	0053	LUTETIUM	0450	17	4990	0053
95	M0052	24	3200	0052	MAGNESIUM	0451	24	3200	0052
96	M0053	54	9400	0052	MANGANESE	0452	54	9400	0052
97	M0054	95	9500	0052	MOLYBDENUM	0453	95	9500	0052
98	M0055	25	6000	0053	MENDELEVUM	0454	25	6000	0053
99	M0056	14	0080	0052	NITROGEN	0455	14	0080	0052
100	M0057	22	9910	0052	SODIUM	0456	22	9910	0052
101	M0058	92	9100	0052	NIOBIUM	0457	92	9100	0052
102	M0059	14	4270	0053	NEODYMIUM	0458	14	4270	0053
103	M0060	20	1830	0052	NEON	0459	20	1830	0052
104	M0061	58	7100	0052	NICKEL	0460	58	7100	0052
105	M0062	23	7000	0053	NEPTUNIUM	0461	23	7000	0053
106	M0063	16	0000	0052	OXYGEN	0462	16	0000	0052
107	M0064	19	0200	0053	OSMIUM	0463	19	0200	0053
108	M0065	30	9750	0052	PHOSPHORUS	0464	30	9750	0052
109	M0066	23	1000	0053	PROTACTINIUM	0465	23	1000	0053
110	M0067	20	7210	0053	LEAD	0466	20	7210	0053
111	M0068	10	6700	0053	PALLADIUM	0467	10	6700	0053
112	M0069	14	5000	0053	PROMETHIUM	0468	14	5000	0053
113	M0070	21	0000	0053	POLONIUM	0469	21	0000	0053
114	M0071	14	0920	0053	PRASEODYMM	0470	14	0920	0053
115	M0072	19	5090	0053	PLATINUM	0471	19	5090	0053
116	M0073	24	2000	0053	PLUTONIUM	0472	24	2000	0053
117	M0074	22	6050	0053	RADIUM	0473	22	6050	0053
118	M0075	85	4800	0052	RUBIDIUM	0474	85	4800	0052
119	M0076	18	6220	0053	RHENIUM	0475	18	6220	0053
120	M0077	10	2910	0053	RHODIUM	0476	10	2910	0053
121	M0078	22	2000	0053	RADON	0477	22	2000	0053
122	M0079	10	1100	0053	RUTHENIUM	0478	10	1100	0053
123	M0080	32	0660	0052	SULFUR	0479	32	0660	0052
124	M0081	12	1760	0053	ANTIMONY	0480	12	1760	0053
125	M0082	44	9600	0052	SCANDIUM	0481	44	9600	0052
126	M0083	78	9600	0052	SELENIUM	0482	78	9600	0052
127	M0084	28	0900	0052	SILICON	0483	28	0900	0052
128	M0085	15	0350	0053	SAMARIUM	0484	15	0350	0053
129	M0086	11	8700	0053	TIN	0485	11	8700	0053
130	M0087	87	6300	0052	STRONTIUM	0486	87	6300	0052
131	M0088	18	0950	0053	TANTALUM	0487	18	0950	0053
132	M0089	15	8930	0053	TERBIUM	0488	15	8930	0053
133	M0090	99	0000	0052	TECHNETIUM	0489	99	0000	0052
134	M0091	12	7610	0053	TELLURIUM	0490	12	7610	0053
135	M0092	23	2050	0053	THORIUM	0491	23	2050	0053
136	M0093	47	9000	0052	TITANIUM	0492	47	9000	0052
137	M0094	20	4390	0053	THALLIUM	0493	20	4390	0053
138	M0095	16	8940	0053	THULIUM	0494	16	8940	0053
139	M0096	23	8070	0053	URANIUM	0495	23	8070	0053
140	M0097	50	9500	0052	VANADIUM	0496	50	9500	0052
141	M0098	18	3860	0053	TUNGSTEN	0497	18	3860	0053
142	M0101	13	1300	0053	XENON	0500	13	1300	0053
143	M0102	88	9200	0052	YTTRIUM	0501	88	9200	0052
144	M0103	17	3040	0053	YTTERBIUM	0502	17	3040	0053
145	M0104	65	3800	0052	ZINC	0503	65	3800	0052
146	M0105	91	2200	0052	ZIRCONIUM	0504	91	2200	0052
147	1				TABLE OF VALENCES				
148	1								
149	V0001	61	0000	0000	ARGON	0.00	61	0000	0000
150	V0002	61	6300	0000	ACTINIUM	0.01	61	6300	0000
151	V0003	61	6700	0000	SILVER	0.02	61	6700	0000
152	V0004	61	7300	0003	ALUMINUM	0.03	61	7300	0003
153	V0005	61	7400	0000	AMERICIUM	0.04	61	7400	0000
154	V0006	61	8200	0000	ARSENIC	0.05	61	8200	0000
155	V0007	61	8300	0000	ASTATINE	0.06	61	8300	0000
156	V0008	61	8400	0000	GOLD	0.07	61	8400	0000
157	V0009	62	0000	0003	BORON	0.08	62	0000	0003
158	V0010	62	6100	0000	BARIUM	0.09	62	6100	0000
159	V0011	62	6500	0002	BERYLliUM	0.10	62	6500	0002
160	V0012	62	6900	0000	BISMUTH	0.11	62	6900	0000
161	V0013	62	7200	0000	BERKELIUM	0.12	62	7200	0000
162	V0014	62	7900	0001	BROMINE	0.13	-62	7900	0001
163	V0015	63	0000	0004	CARBON	0.14	63	0000	0004
164	V0016	63	6100	0002	CALCIUM	0.15	63	6100	0002
165	V0017	63	6400	0000	CADMiUM	0.16	63	6400	0000
166	V0018	63	6500	0000	CERIUM	0.17	63	6500	0000

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167	V0019	63	6600	0000	CALIFORNUM	0618	63	6600	0000	
168	V0020	-	63	7300	0001	CHLORINE	0619	-63	7300	0001
169	V0021	63	7400	0000	CURIUM	0620	63	7400	0000	
170	V0022	63	7600	0000	COBALT	0621	63	7600	0000	
171	V0023	63	7900	0000	CHROMIUM	0622	63	7900	0000	
172	V0024	63	8200	0000	CESIUM	0623	63	8200	0000	
173	V0025	63	8400	0000	COPPER	0624	63	8400	0000	
174	V0026	64	8800	0000	DYSPROSIUM	0625	64	8800	0000	
175	V0027	65	0000	0000	EINSTEINUM	0626	65	0000	0000	
176	V0028	65	7900	0000	ERBIUM	0627	65	7900	0000	
177	V0029	65	8400	0000	EUROPIUM	0628	65	8400	0000	
178	V0030	-	66	0000	FLUORINE	0629	-66	0000	0001	
179	V0031	66	6500	0000	IRON	0630	66	6500	0000	
180	V0032	66	7400	0000	FERMIUM	0631	66	7400	0000	
181	V0033	66	7900	0000	FRANCIUM	0632	66	7900	0000	
182	V0034	67	6100	0000	GALLIUM	0633	67	6100	0000	
183	V0035	67	6400	0000	GADOLINIUM	0634	67	6400	0000	
184	V0036	67	6500	0000	GERMANIUM	0635	67	6500	0000	
185	V0037	68	0000	0001	HYDROGEN	0636	68	0000	0001	
186	V0038	68	6500	0000	HELIUM	0637	68	6500	0000	
187	V0039	68	6600	0000	HAFNIUM	0638	68	6600	0000	
188	V0040	68	6700	0000	MERCURY	0639	68	6700	0000	
189	V0041	68	7600	0000	HOLMIUM	0640	68	7600	0000	
190	V0042	-	69	0000	IODINE	0641	-69	0000	0001	
191	V0043	69	7500	0000	INDIUM	0642	69	7500	0000	
192	V0044	69	7900	0000	IRIDIUM	0643	69	7900	0000	
193	V0045	72	0000	0001	POTASSIUM	0644	72	0000	0001	
194	V0046	72	7900	0000	KRYPTON	0645	72	7900	0000	
195	V0047	73	6100	0000	LANTHANUM	0646	73	6100	0000	
196	V0048	73	6900	0001	LITHIUM	0647	73	6900	0001	
197	V0051	73	8400	0000	LUTETIUM	0650	73	8400	0000	
198	V0052	74	6700	0002	MAGNESIUM	0651	74	6700	0002	
199	V0053	74	7500	0000	MANGANESE	0652	74	7500	0000	
200	V0054	74	7600	0000	MOLYBDENUM	0653	74	7600	0000	
201	V0055	74	8500	0000	MENDELEVUM	0654	74	8500	0000	
202	V0056	75	0000	0000	NITROGEN	0655	75	0000	0000	
203	V0057	75	6100	0001	SODIUM	0656	75	6100	0001	
204	V0058	75	6200	0000	NIOBIUM	0657	75	6200	0000	
205	V0059	75	6400	0000	NEODYMIUM	0658	75	6400	0000	
206	V0060	75	6500	0000	NEON	0659	75	6500	0000	
207	V0061	75	6900	0000	NICKEL	0660	75	6900	0000	
208	V0062	75	7700	0000	NEPTUNIUM	0661	75	7700	0000	
209	V0063	-	76	0000	OXYGEN	0662	-76	0000	0002	
210	V0064	76	8200	0000	OSMIUM	0663	76	8200	0000	
211	V0065	77	0000	0000	PHOSPHORUS	0664	77	0000	0000	
212	V0066	77	6100	0000	PROTACTIUM	0665	77	6100	0000	
213	V0067	77	6200	0000	LEAD	0666	77	6200	0000	
214	V0068	77	6400	0000	PALLADIUM	0667	77	6400	0000	
215	V0069	77	7400	0000	PROMETHIUM	0668	77	7400	0000	
216	V0070	77	7600	0000	POLONIUM	0669	77	7600	0000	
217	V0071	77	7900	0000	PRASEODYMM	0670	77	7900	0000	
218	V0072	77	8300	0000	PLATINUM	0671	77	8300	0000	
219	V0073	77	8400	0000	PLUTONIUM	0672	77	8400	0000	
220	V0074	79	6100	0000	RADIUM	0673	79	6100	0000	
221	V0075	79	6200	0000	RUBIDIUM	0674	79	6200	0000	
222	V0076	79	6500	0000	RHENIUM	0675	79	6500	0000	
223	V0077	79	6800	0000	RHODIUM	0676	79	6800	0000	
224	V0078	79	7500	0000	RADON	0677	79	7500	0000	
225	V0079	79	8400	0000	RUTHENIUM	0678	79	8400	0000	
226	V0080	82	0000	0004	SULFUR	0679	82	0000	0004	
227	V0081	82	6200	0000	ANTIMONY	0680	82	6200	0000	
228	V0082	82	6300	0000	SCANDIUM	0681	82	6300	0000	
229	V0083	82	6500	0000	SELENIUM	0682	82	6500	0000	
230	V0084	82	6900	0004	SILICON	0683	82	6900	0004	
231	V0085	82	7400	0000	SAMARIUM	0684	82	7400	0000	
232	V0086	82	7500	0000	TIN	0685	82	7500	0000	
233	V0087	82	7900	0000	STRONTIUM	0686	82	7900	0000	
234	V0088	83	6100	0000	TANTALUM	0687	83	6100	0000	
235	V0089	83	6200	0000	TERBIUM	0688	83	6200	0000	
236	V0090	83	6300	0000	TECHNETIUM	0689	83	6300	0000	
237	V0091	83	6500	0000	TELLURIUM	0690	83	6500	0000	
238	V0092	83	6800	0000	THORIUM	0691	83	6800	0000	
239	V0093	83	6900	0000	TITANIUM	0692	83	6900	0000	
240	V0094	83	7300	0000	THALLIUM	0693	83	7300	0000	
241	V0095	83	7400	0000	THULIUM	0694	83	7400	0000	
242	V0096	84	0000	0000	URANIUM	0695	84	0000	0000	
243	V0097	85	0000	0000	VANADIUM	0696	85	0000	0000	
244	V0098	86	0000	0000	TUNGSTEN	0697	86	0000	0000	
245	V0101	87	6500	0000	XENON	0700	87	6500	0000	
246	V0102	88	0000	0000	YTTRIUM	0701	88	0000	0000	
247	V0103	88	6100	0000	YTTERBIUM	0702	88	6100	0000	
248	V0104	89	7500	0000	ZINC	0703	89	7500	0000	
249	V0105	89	7900	0000	ZIRCONIUM	0704	89	7900	0000	

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251 1      CLEAR ROUTINE
252 1
253   CLEAR    RAA 0010          0050  80 0010 0056
254     RAM 8002 CLR 1          0056  67 8002 0015
255   CLR 1    STU 9049 A       0015  21 9749 0023
256     NZA      CLR 2          0023  40 0026 0027
257   CLR 2    SXA 0001 CLR 1  0026  51 0001 0015
258     SET 9049          0027  27 9049 0032
259     STB A0001          0032  29 0001 0054
260   CLR 3    RAA 0300 CLR 3   0054  80 0300 0060
261     SET 9050          0060  27 9050 0065
262     SBB 0090 A          0065  28 2090 0043
263     NZA      SET01          0043  40 0046 0047
264     SXA 0010 CLR 3       0046  51 0010 0060
265   SET01   RSU UNITY          SET ATOM 0047  61 0550 0055
266     STU ATMCT          COUNTER 0055  21 0560 0013
267     STD RELAY READ        SET SWITCH 0013  24 0016 0019
268 1
269 1
270 1      READ ROUTINE
271   READ    RCD R0001          READ CARD 0019  70 1951 0051
272     LDD R0001          TRANSFER 0051  69 1951 0554
273     STD P0001          INPUT FROM 0554  24 1977 0030
274     LDD R0002          READ BAND 0030  69 1952 0555
275     STD P0002          TO PUNCH 0555  24 1978 0031
276     LDD R0003          BAND    0031  69 1953 0556
277     STD P0003          0556  24 1979 0082
278     LDD R0004          0082  69 1954 0057
279     STD P0004          0057  24 1980 0033
280     LDD R0005          0033  69 1955 0058
281     STD P0005          0058  24 1981 0034
282     LDD R0006          0034  69 1956 0059
283     STD P0006          0059  24 1982 0035
284     RAU R0010          0035  60 1960 0515
285     STL P0007          CLER P000 0515  20 1983 0036
286     STD P0009          CLER P000C 0036  24 1985 0038
287     SRT 0002          0038  30 0002 0045
288     STU P0008          0045  21 1984 0037
289     NZU      PV007          SET P0010 0037  44 0041 0042
290     ALO 823RD          TO PUNCH 0041  15 0044 0049
291     STL P0010          PNCH    TYPE1 CARD 0049  20 1986 0039
292   PV007   RAU R0004          REARRANGE 0042  60 1954 0559
293     SRT 0004          VECTOR IN 0559  30 0004 0069
294     SLO 8002          WORDS 2 3 0069  16 8002 0077
295     STD R0004          4 5 AND 6 0077  24 1954 0557
296     SLT 0004          0557  35 0004 0017
297     STU SYMBL          SAVE SYMBL 0017  21 0022 0025
298     RAL R0004          0025  65 1954 0759
299     SLT 0002          0759  35 0002 0565
300     SLO 8002          0565  16 8002 0073
301     STD TEMPO          0073  24 9000 0029
302     ALO R0003          0029  15 1953 0757
303     SLT 0008          0757  35 0008 0075
304     STU R0003          0075  21 1953 0756
305     STL TEMP1          0756  20 9001 0014
306     RAU R0006          0014  60 1956 0061
307     SRT 0004          0061  30 0004 0021
308     STL R0006          0021  20 1956 0859
309     RAL 8003          0859  65 8003 0067
310     SLT 0004          0067  35 0004 0527
311     AUP R0005          0527  10 1955 0959
312     SRT 0004          0959  30 0004 0519
313     STL R0005          0519  20 1955 0558
314     AUP TEMP1          0558  10 9001 0715
315     STU R0004          0715  21 1954 0857
316     RAU TEMPO          0857  60 9000 0765
317     SRT 0002          0765  30 0002 0071
318     AUP R0004          0071  10 1954 1009
319     STU R0004 LOOK          1009  21 1954 0957
320 1      CONSTANTS FOR READ ROUTINE
321   823RD  00 0000 0880          0044  00 0000 0880
322 1
323 1      TABLE LOOKUP ROUTINE TO FIND
324 1      CORRECT ROUTINE FOR SYMBOL
325 1      BEING PROCESSED
326 1
327   LOOK    LDD SYMBL          0957  69 0022 0525
328     TLU U0001          0525  84 0800 0755
329     SUP 8003          0755  11 8003 0063
330     SRT 0004          0063  30 0004 0523
331     ALO 100 I 8002          0523  15 0076 8002
332   8002  00 0000 U01XX          8002  00 0000 0900
333 1

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334	U0101	RAU SYMBL	ATM PROGRM	0900	60 0022 0577
335		SUP ATM		0577	11 0080 0085
336		NZU	PV009	0085	44 0089 0040
337		HLT 9999	1111	WRONG SMLB	0089 01 9999 1111
338 1					
339	U0102	RAU SYMBL	BOP PROGRM	0901	60 0022 0727
340		SUP BOP		0727	11 0530 0535
341		NZU	CLEAR	0535	44 0739 0050
342		HLT 9999	2222	WRONG SMLB	0739 01 9999 2222
343 1					
344	U0103	RAU SYMBL	FUEL	0902	60 0022 0777
345		SRT 0006	ENTHALPY	0777	30 0006 0741
346		SLO 8002	PROGRAM	0741	16 8002 0749
347		STD CODE		0749	24 0052 0855
348		SLT 0006		0855	35 0006 0569
349		SUP EF		0569	11 0072 0827
350		NZU	OK 3	0827	44 0081 0532
351		HLT 9999	3333	WRONG SMLB	0081 01 9999 3333
352	OK 3	RAA 0319	PAR 1		0532 80 0319 0088
353 1					
354 1					
355 1			CONSOLE POSITION 2 IS SET TO 8		
356 1			IF IT IS DESIRED TO PUNCH OUT		
357 1			FUELS OXIDANTS PERCENTS AND		
358 1			ENTHALPIES		
359 1					
360 1					
361	U0104	RAU SYMBL	PROPELLANT	0903	60 0022 0877
362		SUP END	READY TO	0877	11 0580 0585
363		NZU	PROCESS	0585	44 0789 0740
364		HLT 9999	DIST2 4444	WRONG SMLB	0789 01 9999 4444
365	DIST2	LDD 8000		0740	69 8000 0746
366		B02	END 1	0746	92 0799 0551
367		RAL SPEC5		0799	65 0552 1007
368		LDD END 1	PUNCH	1007	69 0551 1930
369		SPEC5 00 0100	0240		0552 00 0100 0240
370 1					
371	U0105	RAU SYMBL	OXIDANT	0904	60 0022 0927
372		SRT 0006	ENTHALPY	0927	30 0006 0791
373		SLO 8002	PROGRAM	0791	16 8002 0849
374		STD CODE		0849	24 0052 0955
375		SLT 0006		0955	35 0006 0719
376		SUP EX		0719	11 0522 0977
377		NZU	OK 5	0977	44 0531 0582
378		HLT 9999	5555	WRONG SMLB	0531 01 9999 5555
379	OK 5	RAA 0329	PAR 1		0582 80 0329 0088
380 1					
381	U0106	RAU SYMBL	FUEL	0905	60 0022 1027
382		SRT 0008	PROGRAM	1027	30 0008 0745
383		SLO 8002		0745	16 8002 0053
384		STD CODE		0053	24 0052 1005
385		SLT 0008		1005	35 0008 0573
386		SUP F		0573	11 0526 0581
387		NZU	OK 6	0581	44 0735 0086
388		HLT 9999	6666	WRONG SMLB	0735 01 9999 6666
389	OK 6	RAA 0099		0086	80 0099 0742
390		STL R0007	PV180	CLER R0007	0742 20 1957 0760
391 1					
392	U0107	RAU SYMBL	MOLECULE	0906	60 0022 1077
393		SUP MOL	PROGRAM	1077	11 0730 C785
394		NZU	PV015	0785	44 0839 0790
395		HLT 9999	7777	WRONG SMLB	0839 01 9999 7777
396 1					
397	U0108	RAU SYMBL	PERCENT	0907	60 0022 1127
398		SRT 0006	FUEL	1127	30 0006 0841
399		SLO 8002	PROGRAM	0841	16 8002 0899
400		STD CODE		0899	24 0052 1055
401		SLT 0006		1055	35 0006 0769
402		SUP PF		0769	11 0572 1177
403		NZU	OK 8	1177	44 0731 0732
404		HLT 9999	8888	0731	01 9999 8888
405	OK 8	RAA 0299	PAR 1		0732 80 0299 0088
406 1					
407	U0109	RAU SYMBL	PERCENT	0908	60 0022 1227
408		SRT 0006	OXIDANT	1227	30 0006 0891
409		SLO 8002	PROGRAM	0891	16 8002 0949
410		STD CODE		0949	24 0052 1105
411		SLT 0006		1105	35 0006 0819
412		SUP PX		0819	11 0722 1277
413		NZU	OK 9	1277	44 0781 0782
414		HLT 9999	9999	0781	01 9999 9999
415	OK 9	RAA 0309	PAR 1		0782 80 0309 0088
416 1					

417	U0110	RAU SYMBL		OXIDANT PROGRAM	0909	60 0022 1327
418		SRT 0008			1327	30 0008 0795
419		SLO 8002			0795	16 8002 0553
420		STD CODE			0553	24 0052 1155
421		SLT 0008			1155	35 0008 0723
422		SUP X			0723	11 0576 0831
423		NZU OK 10			0831	44 0835 0536
424		HLT 9999 0000		WRONG SML	0835	01 9999 0000
425	OK 10	RAA 0199			0536	80 0199 0792
426		STL R0007	PV180	CLER R0007	0792	20 1957 0760
427	1	CONSTANTS FOR TABLE LOOKUP				
428	1	ROUTINE				
429	1				0080	61 8374 0000
430	ATM	61 8374 0000			0530	62 7677 0000
431	BOP	62 7677 0000			0072	65 6600 0000
432	EF	65 6600 0000			0580	65 7564 0000
433	END	65 7564 0000			0522	65 8700 0000
434	EX	65 8700 0000			0526	66 0000 0000
435	F	66 0000 0000			0730	74 7673 0000
436	MOL	74 7673 0000			0572	77 6600 0000
437	PF	77 6600 0000			0722	77 8700 0000
438	PX	77 8700 0000			0576	87 0000 0000
439	X	87 0000 0000			0800	61 8374 0000
440	U0001	61 8374 0000	ATM		0801	62 7677 0000
441	U0002	62 7677 0000	BOP		0802	65 6699 0000
442	U0003	65 6699 0000	EF9		0803	65 7564 0000
443	U0004	65 7564 0000	END		0804	65 8799 0000
444	U0005	65 8799 0000	EX9		0805	66 9900 0000
445	U0006	66 9900 0000	F9		0806	74 7673 0000
446	U0007	74 7673 0000	MOL		0807	77 6699 0000
447	U0008	77 6699 0000	PF9		0808	77 8799 0000
448	U0009	77 8799 0000	PX9		0809	87 9900 0000
449	U0010	87 9900 0000	X9		0076	00 0000 0100
450	100 1	00 0000 0100				
451	1	ROUTINE FOR PACKED VECTORS				
452	1	ATOMS START AT PV009 AND				
453	1	MOLECULES START AT PV015				
454	1					
455	1					
456	PV009	LDD R0007	PLACE CODE	0040	69 1957 0810	
457		STD P0009	IN OUTPUT	0810	24 1985 0738	
458		RAU RELAY	ITS ATOM	0738	60 0016 0521	
459		NZU PV011		0521	44 0575 0726	
460		HLT 2222	8888	0726	01 2222 8888	
461	1					
462	PV011	RAL R0002	SWITCH NOT	0575	65 1952 1057	
463		SLT 0004	INITIALIZE	1057	35 0004 0517	
464		SUP 8003	IS ATOM	0517	11 8003 0725	
465		NZE PV013	MORE THAN	0725	45 0028 0079	
466		HLT 3333	7777	0028	01 3333 7777	
467	PV013	RAL ATMCT	YES STOP	0079	65 0560 0815	
468		ALO UNITY	NO	0815	15 0550 1205	
469		STL ATMCT	ADVANCE	1205	20 0560 0513	
470		ALO R0002	ATOM COUNT	0513	15 1952 1107	
471		AUP ATMCT	STORE ATOM	1107	10 0560 0865	
472		SLO 8002	COLUMN	0865	16 8002 0773	
473		SLT 0004	EQUIVALENT	0773	35 0004 0083	
474		ALO 8001	IN TABLE	0083	15 8001 0941	
475		AUP STORE 8003		0941	10 0744 8003	
476	8003	STL A0001	PACKA	8003	20 0001 0754	
477		RAU ATMC	FORM ATOM	0754	60 0560 0915	
478		SLT 0001	VECTOR	0915	35 0001 0571	
479		AUP UNITY	STORE IN	0571	10 0550 1255	
480		STU P0007	PUNCH BAND	1255	21 1983 0586	
481	PV015	LDD R0007	PLACE CODE	0790	69 1957 0860	
482		STD P0009	IN OUTPUT	0860	24 1985 0788	
483		RAU RELAY	IS THIS	0788	60 0016 0721	
484		NZU PV019	FIRST MO-	0721	44 0775 0776	
485		STL RELAY	YES	0775	20 0016 0869	
486		RAU UNITY	DID WE	0869	60 0550 1305	
487		SLT 0001	PROCESS	1305	35 0001 0511	
488		SUP 8001	MORE THAN	0511	11 8001 0919	
489		SUP ATMCT	TEN ATOMS	0919	11 0560 0965	
490		BMI PV017		0965	46 0018 0969	
491		HLT 4444 6666	TOO MANY	0018	01 4444 6666	
492	PV017	STU COUNT	SET SOLIDS	0969	21 0024 0776	
493	1		COUNTER			
494	PV019	RAU R0010	NO IS THIS	0776	60 1960 1015	
495		SRT 0001	MOLECULE	1015	30 0001 0771	
496		RAL 8002	CONDENSID	0771	65 8002 0529	
497		NZE PV023		0529	45 0832 0533	
498		RAU COUNT	YES MAY WE	0832	60 0024 0579	
499		NZU PV024	PROCESS IT	0579	44 0583 0084	
500		HLT 5555	NO	0084	01 5555 5555	

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501	PV024	SUP UNITY			YES	0583	11 0550 1355
502		STU COUNT	PV023			1355	21 0024 0533
503	PV023	RAU R0005			IS MOLECULE	0533	60 1955 1059
504		NZU	PV025		MORE THAN	1059	44 0563 0064
505 1					15 PLACES		
506		HLT 6666	4444		YES	0563	01 6666 4444
507	PV025	RAL R0002				0064	65 1952 1157
508		NZE PV031				1157	45 0910 0561
509		HLT 7777	3333		NO MOLECULE	0561	01 7777 3333
510	PV031	RAU CNTR1			CLEAR DATA	0910	60 0713 0567
511		STU CNTRX			ADDRESS	0567	21 0772 0825
512		STL TEMP1	PV032		SET ZERO	0825	20 9001 0882
513	PV032	RAL R0002			IS PRODUCT	0882	65 1952 1207
514		NZE	PV115		FINISHED	1207	45 0960 0711
515		SLT 0001			NO	0960	35 0001 0717
516		SUP NINE1				0717	11 0020 0875
517		NZU LETTR	NUMBR			0875	44 0729 0780
518	LETTR	LDL PV032	PV033			0729	69 0882 0885
519	PV033	STD LINK				0885	24 0838 0991
520		RAL R0002				0991	65 1952 1257
521		AUP TEMP1				1257	10 9001 1065
522		SLT 0002				1065	35 0002 0821
523		STU TEMP1				0821	21 9001 0779
524		STL R0002				0779	20 1952 1405
525		RAU CNTRX				1405	60 0772 1377
526		AUP TWO D				1377	10 0830 0935
527		STU CNTRX	LINK			0935	21 0772 0838
528 1							
529	NUMBR	LDD PV034	PV033			0780	69 0733 0885
530	PV034	RAU TEMP1				0733	60 9001 1041
531		SRT 0002	PV087			1041	30 0002 0747
532	PV087	SLO NINE			STORE	0747	16 0750 1455
533		SLO 8002			MAGNITUDE	1455	16 8002 0763
534		STD MAGNI			OF THE	0763	24 0066 1019
535		SCT 0000			COMPONENT	1019	36 0000 1091
536		STU COMPO	PV089			1091	21 0796 0999
537	PV089	RAL A000X			SEARCH	0999	65 1550 0856
538		LDD PV091			SYMBOL	0856	69 1109 0012
539		SDA PV091	8001		TABLE FOR	0012	22 1109 8001
540 1					COMPONENT		
541	PV091	RAL A0001	PV093			1109	65 0001 0956
542	PV093	NZE	PV095			0956	45 1010 0761
543		SRT 0001				1010	30 0001 0767
544		SLT 0001				0767	35 0001 0823
545		SLO COMPO				0823	16 0796 0751
546		NZE	PV097			0751	45 0354 1006
547		RAL PV091			ADVANCE	0854	65 1109 0813
548		ALO ONE D			ONE PLACE	0813	15 0516 0871
549		STL PV091	8001		ALONG	0871	20 1109 8001
550 1					TABLE		
551	PV095	HLT 8888	2222		NOT IN	0761	01 8888 2222
552 1					TABLE		
553	PV097	RAL PV091			GOT THE	1006	65 1109 0863
554		LDD PV099			RIGHT ONE	0863	69 0566 1069
555		SDA PV099	8001			1069	22 0566 8001
556	PV099	RAU A0001	PV100		ADD IT TO	0566	60 0001 1056
557	PV100	SRT 0001			REST OF	1056	30 0001 0913
558		ALO MAGNI			PACKED	0913	15 0066 0921
559		SUP 8003			VECTOR IN	0921	11 8003 0829
560		AUP P0007			P0007	0829	10 1983 0087
561		SLT 0002				0087	35 0002 0743
562		STU P0007				0743	21 1983 0736
563		RAL R0003	CNTRX		SHIFT	0736	65 1953 0772
564	CNTRX	SLT XXXXX	PV101		WORD 3	0772	35 0000 0845
565 1							
566	PV101	AUP R0002				0845	10 1952 1307
567		STU R0002				1307	21 1952 1106
568		STL R0003				1106	20 1953 1156
569 1							
570		RAL CNTRX			CNTRY DATA	1156	65 0772 1427
571		LDD CNTR2			ADRES SAME	1427	69 0880 0789
572		SDA CNTRY			AS CNTRX	0783	22 0737 0840
573 1							
574		RAL R0004	CNTRY		SHIFT	0840	65 1954 0737
575	CNTRY	SLT XXXXX	PV102		WORD 4	0737	35 0000 1159
576	PV102	AUP R0003				1159	10 1953 1357
577		STU R0003				1357	21 1953 1206
578		STL R0004	PV031			1206	20 1954 0910
579	PV115	RAU R0010				0711	60 1960 1115
580		SRT 0001				1115	30 0001 0971
581		RAU R002				0971	60 8002 0979
582		NZU	PV116		A SIGN FOR	0879	44 0833 0586
583		RSU P0007			THE PACKED	0833	61 1983 0787
584		STU P0007	PV116		VECTOR	0787	21 1983 0586
585	PV116	LDD B3RD				0586	69 0389 0842
586		STD P0010	PNCH			0842	24 1986 0039
587	PNCH	PCH P0001	READ			0039	71 1977 0019

588 1  
 589 1           CONSTANTS FOR PACKED VECTOR  
 590 1           ROUTINE  
 591 1  
 592   UNITY    00 0000 0001                   0550 00 0700 0001  
 593   ONE D    00 0001 0000                   0516 00 0001 0000  
 594   TWO D    00 0002 0000                   0830 00 0002 0000  
 595   NINEI    00 0000 0009                   0020 00 0000 0009  
 596   NINE     90 0000 0000                   0750 90 0000 0000  
 597   STORE    STL A0001 PACKA               0744 20 0001 0754  
 598   A000X    00 A0001 0000                1550 00 0001 0000  
 599   CNTR1    SLT 0000 PV101                0713 35 0000 0845  
 600   CNTR2    SLT 0000 PV102                0880 35 0000 1159  
 601   83RD     00 0000 0800                0889 00 0000 0800  
 602 1  
 603 1  
 604 1           ROUTINE FOR STORINGS FUELS AND  
 605 1           OXIDANTS  
 606 1  
 607   PV180    RAU RELAY                   IF NO    0760 60 0016 1021  
 608            NZU                           MOLECULES  
 609 1           PV198                        1021 44 0925 0826  
 610 1           IS THIS  
 611 1           FIRST FUEL  
 612   STL RELAY                           OR OXIDANT  
 613   RAU NINEI                           YES     0925 20 0016 1119  
 614   SUP ATMCT                          ARE THERE  
 615   BMI                                   1119 60 0020 0975  
 616   HLT 9988                           MORE THAN  
 617   PV198    RAU R0002                   0975 11 0560 1165  
 618            NZU PV200                   TEN ATOMS  
 619            HLT 9876                   1165 46 0068 0826  
 620   PV200    STL TEMP1                9988           0068 01 9988 9988  
 621            STD TEMP2                YES     0826 60 1952 1407  
 622            STU RELA1                NO LETTE'S  
 623            RAB 0000                   OR NUMBE'S  
 624 1           PV201    RAL R0002           1407 44 0811 0062  
 625            NZE                           0062 01 9876 9876  
 626            SLT 0001                   IS SYMBOL  
 627            SUP NINEI                0817 11 0020 1025  
 628            BMI LETR                LET OR NUM  
 629            NUMR                       1025 46 0528 0929  
 630   LETR     RAU RELA1                DO WE STOR  
 631            NZU                           0528 60 0078 0883  
 632            PV221                       PREV COEFF  
 633            RAL R0002                0883 44 0887 0888  
 634            AUP TEMP1                NO     0887 65 1952 0758  
 635            SLT 0002                0758 10 9001 1215  
 636 1           STU TEMP1                1215 35 0002 1071  
 637            PV209    STL R0002           1071 21 9001 0979  
 638            RSC 0003                   0979 20 1952 1256  
 639   PV210    RAL R0006 C               PV210    SHIFT  
 640            SLT 0002                   WORDS 2 3  
 641            AUP R0005 C                4 5 AND 6  
 642            STU R0005 C                0512 65 7956 0911  
 643            STL R0006 C                0911 35 0002 0867  
 644            NZC                           0867 10 7955 1209  
 645            AXC 0001                   1209 21 7955 0858  
 646   NUMR     STU RELA1                0858 20 7956 1259  
 647            STU RELA1                1259 48 0562 0837  
 648            AXC 0001                   0562 58 0001 0512  
 649            AUP TEMP2                0929 21 0078 0931  
 650            SLT 0001                   CLER RELA1  
 651   PV220    STU TEMP2                ADD TO CNT  
 652            LDD PAR 6                0931 52 0001 0937  
 653   PV221    LDD PV200                0937 10 9002 0895  
 654            STD LINK                0895 35 0001 0851  
 655            RSC 0009                0851 21 9002 0979  
 656            RAU TEMP1                0861 69 0514 C917  
 657            SCT 0000                0888 69 0811 0917  
 658   PV223    STU TEMP2                0917 24 0838 1141  
 659            PV222                   1141 89 0009 0797  
 660            SRT 0001                0797 60 9001 1306  
 661            SLT 0001                1306 36 0000 1029  
 662            SLO TEMP1                1029 21 9001 0987  
 663            NZE                           1029 65 6010 1265  
 664            NZC                        0987 30 0001 1121  
 665   PV224    AXC 0001                1121 35 0001 1477  
 666 1           PV225    HLT 4321           FIND  
 667            RAU CODE                SYMBOL N  
 668            SLT 0001                TABLE  
 669            SRT 0008                1477 16 9001 0985  
 670            NZU PV227                0985 45 0938 0939  
 671            PV226    RAU 100 I        0938 48 1191 0892  
 672            PV227                   1191 58 0001 0987  
 673            PV226                   0892 01 4321 4321  
 674            NOT IN  
 675            TABLE  
 676            GENERATE  
 677            STORAGE  
 678            LOCATION

672 PV227 AUP 8005 1037 10 8005 0945  
 673 AUP 8007 0945 10 8007 0753  
 674 SLT 0004 0753 35 0004 0963  
 675 AUP MASK1 0963 10 0716 1171  
 676 STU PV233 1171 21 0876 1079  
 677 RAU TEN I IS NUMBER 1079 60 0932 1087  
 678 SUP 8006 OVER TEN 1087 11 8006 0995  
 679 BMI PV230 DIGITS 0995 46 0048 1049  
 680 HLT 2233 4455 YES ERROR 0048 01 2233 4455  
 681 PV230 NZU PV231 IS IT TEN 1049 44 0853 0954  
 682 SUP ONE I NO 0853 11 1356 0961  
 683 NZU PV232 IS IT NINE 0961 44 1365 0766  
 684 HLT 5544 3322 YES ERROR 0766 01 5544 3322  
 685 PV231 RAU TEMP2 PV233 0954 60 9002 0876  
 686 PV232 RAU TEMP2 1365 60 9002 0873  
 687 SCT 0000 0873 36 0000 1045  
 688 AUP 8006 1045 10 8006 0953  
 689 RAB 0050 0953 82 0050 1309  
 690 AUP 8006 1309 10 8006 0967  
 691 SLO 8002 PV233 0967 16 8002 0876  
 692 PV233 STU XXXXX LINK 0876 21 0000 0838  
 693 1  
 694 1  
 695 1       CONSTANTS FOR FUELS AND  
 696 1       OXIDANTS ROUTINE  
 697 1  
 698 ONE I 00 0000 0001 1356 00 0000 0001  
 699 NINEI 00 0000 0009 0020 00 0000 0009  
 700 TEN I 00 0000 0010 0932 00 0000 0010  
 701 100 I 00 0000 0100 0076 00 0000 0100  
 702 MASK1 STU 0000 LINK 0716 21 0000 0838  
 703 1  
 704 1  
 705 1  
 706 1       ROUTINE FOR STORING ENTHALPIES  
 707 1       AND PERCENTS FOR FUELS AND  
 708 1       OXIDANTS  
 709 1  
 710 PAR 1 RAU R0004 0088 60 1954 1359  
 711 STL TEMPO 1359 20 9000 0816  
 712 NZU ERR 1 0816 44 1169 0070  
 713 ERR 1 HLT 8888 1111 PARAMETER 1169 01 8888 1111  
 714 1  
 715 1 MORE THAN  
 10 FIGURES 0070 83 0001 0926  
 716 RSB 0001 COLAP 0926 88 0005 0982  
 717 COLAP RAC 0005 0982 65 5953 1008  
 718 RAL R0003 B 0982 NUMBER BY 1008 16 1011 1415  
 719 SLO 90909 PAR 2 REMOVING 1415 35 0001 1221  
 720 PAR 2 SLT 0001 NINES 1221 10 9000 1129  
 721 AUP TEMPO 1129 35 0001 1035  
 722 SLT 0001 1035 21 9000 0793  
 723 STU TEMPO 0793 11 8003 0951  
 724 SUP 8003 0951 59 0001 1058  
 725 SXC 0001 1058 48 1415 0712  
 726 NZC PAR 2 0712 42 1465 0866  
 727 NZB PAR 3 1465 52 0001 0926  
 728 AXB 0001 COLAP 0866 60 0052 1108  
 729 PAR 3 RAU CODE GENERATE 1108 35 0001 0916  
 730 SLT 0001 STORAGE 0916 30 0009 1137  
 731 SRT 0009 LOCATION 1137 44 1241 0942  
 732 NZU PAR 5 PAR 4 0942 60 0932 1241  
 733 PAR 4 RAU TEN I PAR 5 1241 10 8005 1099  
 734 PAR 5 AUP 8005 1099 35 0004 1409  
 735 SLT 0004 1409 10 0762 1017  
 736 AUP MASK5 1017 15 9000 8003  
 737 ALO TEMPO 8003 8003 20 0000 0514  
 738 8003 STL XXXXX PAR 6 0514 71 1977 0019  
 739 PAR 6 PCH P0001 READ  
 740 1  
 741 1  
 742 1       CONSTANTS FOR ENTHALPIES AND  
 743 1       PERCENTS ROUTINE  
 744 1  
 745 TEN I 00 0000 0010 0932 00 0000 0010  
 746 90909 90 9090 9090 1011 90 9090 9090  
 747 MASK5 STL 0000 PAR 6 0762 20 0000 0514  
 748 1  
 749 1

750 1  
 751 1 ROUTINE TO CALCULATE THE GRAM  
 752 1 ATOMS AND ENTHALPIES AND THE  
 753 1 OXIDATION NUMBERS PER GRAM OF  
 754 1 COMBINED FUEL OR PER GRAM OF  
 755 1 COMBINED OXIDANT  
 756 1  
 757 END 1 RAA 0010 0551 80 0010 1158  
 758 RAC 0010 1158 88 0010 0564  
 759 RAB 0001 END 2 0564 82 0001 0520  
 760 END 2 RAU 8003 0520 60 8003 0578  
 761 STL TEMPO END 3 CLER TEMP: 0578 20 9000 0786  
 762 END 3 RAU L0000 C ADD ALL 0786 60 6299 1003  
 763 FAD TEMPO THE FUEL 1003 32 9000 0983  
 764 STU TEMPO OR OXIDANT 0983 21 9000 1291  
 765 RAU L0000 C PERCENTS 1291 60 6299 1053  
 766 FDV 10053 AND CONVR: 1053 34 1406 1456  
 767 STU C0010 C TO FRACTN'S 1456 21 9609 1013  
 768 SXA 0001 1013 51 0001 1219  
 769 NZA END 4 1219 40 0822 0923  
 770 SXC 0001 END 3 0822 59 0001 0786  
 771 END 4 RAU TEMPO ARE PERCNT 0923 60 9000 0981  
 772 FSB 11051 REALLY 0981 33 0534 1061  
 773 BMI FRACT PRCNT FRACTIONS 1061 46 0714 0966  
 774 FRACT RAU TEMPO END 5 0714 60 9000 1271  
 775 PRCNT SET C0010 C 0966 27 9609 1321  
 776 SBB L0000 C 1321 28 6299 0752  
 777 RAU TEMPO 0752 60 9000 1459  
 778 FDV 10053 END 5 1459 34 1406 1271  
 779 END 5 FSB 10051 1271 33 0524 1001  
 780 RAM 8003 1001 67 8003 1110  
 781 AUP 47 I 1110 10 1063 1067  
 782 SUP 8002 1067 11 8002 1075  
 783 BMI END 6 1075 46 0728 1179  
 784 HLT 1111 1111 PERCENTS 0728 01 1111 1111  
 785 1 OUT OF LIMITS  
 786 1  
 787 END 6 NZB MW 1 1179 42 1032 1033  
 788 SXB 0001 1032 53 0001 1038  
 789 RAA 0010 1038 80 0010 0794  
 790 RAC 0020 END 2 0794 88 0020 0520  
 791 1  
 792 1  
 793 1 LOCATE AND STORE THE REQUIRED  
 794 1 OXIDATION NUMBERS AND ATOMIC  
 795 1 WEIGHTS  
 796 1  
 797 1 CONSOLE POSITION 3 IS SET TO 8  
 798 1 IF IT IS DESIRED TO PUNCH OUT  
 799 1 ATOMIC WEIGHTS AND OXIDATION  
 800 1 NUMBERS  
 801 1  
 802 1  
 803 MW 1 RAA 0000 MW 2 FIND ATOM 1033 80 0000 0989  
 804 MW 2 RAU A0001 A WEIGHT AND 0989 60 2001 1208  
 805 NZU DIST3 OXID NO 1208 44 1111 0812  
 806 SRT 0001 OF COLUMN 1111 30 0001 1117  
 807 SLO 8002 ONE 1117 16 8002 1125  
 808 SLT 0001 ELEMENT 1125 35 0001 1031  
 809 ALO MASK6 1031 15 0584 1039  
 810 LDD 8003 1039 69 8003 0846  
 811 TLU V0001 MW 3 0846 84 0600 1258  
 812 MW 3 STL TEMPO 8001 1258 20 9000 8001  
 813 8001 RAL V00XX MW 4 8001 65 0600 1308  
 814 MW 4 SLT 0009 1308 35 0009 1229  
 815 SUP 8003 1229 11 8003 1187  
 816 BMI MW 5 1187 46 0890 1341  
 817 SLO 51 I MW 6 0890 16 0843 0847  
 818 MW 5 ALO 51 I MW 6 1341 15 0843 0847  
 819 MW 6 STL S0001 A MW 7 OXID NO 0847 20 2350 1103  
 820 MW 7 RAL TEMPO 1103 65 9000 1161  
 821 SLO 200 D 1161 16 0764 1269  
 822 LDD MASK7 1269 69 0872 1175  
 823 SDA TEMPO 8001 1175 22 9000 8001  
 824 8001 LDD M00XX MW 8 8001 69 0400 1153  
 825 MW 8 STD W0001 A ATOMIC W 1153 24 2340 0893  
 826 AXA 0001 MW 2 NEXT ELM 0893 50 0001 0989  
 827 1  
 828 DIST3 LDD 8000 0812 69 8000 0568  
 829 BD3 AR 1 0568 93 1371 0973  
 830 RAL SPEC6 1371 65 0574 1279  
 831 LDD AR 1 PUNCH 1279 69 0973 1930  
 832 SPEC6 00 W0001 0020 0574 00 0340 0020  
 833 1

834	AR 1	RAA 0000			0973	80 0000 1329
835		RAB 0190			1329	82 0190 1085
836		RAC 0020	AR 2		1085	88 0020 1391
837	AR 2	SUP 8003			1391	11 8003 1149
838		STU TEMPO	AR 3	CLER TEMPO	1149	21 9000 1358
839	AR 3	RAU W0001 A		ATOMIC WT	1358	60 2340 1095
840		NZU	AR 4		1095	44 1199 0850
841		FMP F0001 B		ATOM COEFF	1199	39 4100 0950
842		FAD TEMPO		TEMPO HAS	0950	32 9000 1379
843		STU TEMPO		MOL WT	1379	21 9000 1237
844		AXA 0001			1237	50 0001 0943
845		AXB 0001			0943	52 0001 1249
846		SXA 0010			1249	51 0010 1408
847		NZA	AR 29		1408	40 1211 0862
848		AXA 0010	AR 3		1211	50 0010 1358
849	AR 29	AXA 0010	AR 4		0862	50 0010 0850
850	AR 4	RAU L0000 C		CALCULATE	0850	60 6299 1203
851		NZU	AR 30	NUMBER OF	1203	44 1458 1160
852		FDV TEMPO	AR 30	MOLES OF	1458	34 9000 1160
853	AR 30	STU N0000 C		EACH FUEL	1160	21 6359 0912
854		SXB 2010		OR OXIDANT	0912	53 2010 1319
855		BMB AR 5		WHICH GIVE	1319	43 0922 1023
856		RAA 0000		1 GRAM OF	1023	80 0000 1429
857		SXC 0001	AR 2	COMBINED	1429	59 0001 1391
858 1				FUEL AND 1 GRAM OF		
859 1				COMBINED OXIDANT		
860	AR 5	RAU 10051			0922	60 0524 1479
861		STU RELAY			1479	21 0016 1369
862		SET 9030			1369	27 9030 0724
863		LBB H0001		FUEL ENTH	0724	08 0320 1073
864		SET 9050			1073	27 9050 0778
865		LDR N0001		FUEL MOLES	0778	09 0360 1113
866		SET 9040		CLEAR 904	1113	27 9040 0718
867		LBB 0090		BAND	0718	08 0090 0993
868		RSA 0009			0993	81 0009 1299
869		RAB 0000			1299	82 0000 1210
870		RAC 0000	AR 6		1210	88 0000 1016
871	AR 6	SUP 8003			1016	11 8003 1123
872		STU TEMPO	AR 7	CLER TEMPO	1123	21 9000 1081
873	AR 7	RAU 9059 A		MOLES	1081	60 9259 1089
874		FMP F0001 B		ATOM COEFF	1089	39 4100 1000
875		FAD TEMPO			1000	32 9000 0930
876		STU TEMPO			0930	21 9000 1287
877		RMA	AR 8		1287	41 0940 1441
878		AXA 0001			0940	50 0001 0896
879		AXB 0010	AR 7		0896	52 0010 1081
880	AR 8	STU 9040 C		9040 TO	1441	21 9640 1349
881		RAU A0002 C		9049	1349	60 6002 1260
882		NZU	AR 9	CONTAIN	1260	44 1163 0814
883		RSA 0009		ATOMS PER	1163	81 0009 1419
884		SXB 0089		GRAM OF	1419	53 0089 1225
885		AXC 0001	AR 6	FUEL OR	1225	58 0001 1016
886 1				OXIDANT		
887	AR 9	SUP 8003			0814	11 8003 1421
888		STU TEMPO		CLER TEMPO	1421	21 9000 0980
889		STD TEMP1		CLER TEMP1	0980	24 9001 0836
890		STD TEMP2		CLER TEMP2	0836	24 9002 0992
891		RSA 0009	AR 10		0992	81 0009 0748
892	AR 10	RAU S0010 A			0748	60 2359 1213
893		FMP 9049 A		PLUS AND	1213	39 9249 1066
894		BMI	AR 11	MINUS	1066	46 1469 0570
895		FAD TEMP1		VALENCES	1469	32 9001 1399
896		STU TEMP1	AR 12	PER GRAM	1399	21 9001 1310
897	AR 11	FAD TEMPO		OF FUEL	0570	32 9000 1449
898		STU TEMPO	AR 12	OR OXIDANT	1449	21 9000 1310
899	AR 12	BMA	AR 13		1310	41 1263 0864
900		AXA 0001	AR 10		1263	50 0001 0748
901	AR 13	RSA 0009	AR 14		0864	81 0009 0720
902	AR 14	RAU 9059 A		ENTHALPY	0720	60 9259 0828
903		FMP 9039 A		PER GRAM	0828	39 9239 1131
904		FAD TEMP2		OF FUEL	1131	32 9002 1261
905		STU TEMP2		OR OXIDANT	1261	21 9002 0770
906		BMA	AR 15		0770	41 1173 0774
907		AXA 0001	AR 14		1173	50 0001 0720
908	AR 15	RAU RELAY			0774	60 0016 1471
909		NZU	PCH O		1471	44 1275 0976
910		STL RELAY	PCH F		1275	20 0016 0820
911	PCH F	SET 9040		PUNCH	0820	27 9040 1325
912		SBB 0587		ATOMS AND	1325	28 0587 0990
913		RAL SPEC1		ENTHALPY	0990	65 1049 0897
914		LDD	RMPCH	AND VALENCE	0897	69 1050 1940
915		SET 9000		PER GRAM	1050	27 9000 1360
916		STB 0598		OF FUEL	1360	29 0598 1051
917		LDD TEMP2			1051	69 9002 1410
918		STD 0597			1410	24 0597 1100
919		RAL SPEC2			1100	65 1253 1460
920		LDD	RMPCH		1460	69 1313 1940

921	SET 9030	OXIDANT	1313	27 9030 0768
922	LBB E0001	ENTHALPIES	0768	08 0330 1083
923	SET 9050	OXIDANT	1083	27 9050 1088
924	LDB N0011	MOLES	1088	09 0370 1223
925	SET 9040	CLEAR 904	1223	27 9040 0878
926	LBB 0090	BAND	0878	08 0090 1093
927	RSA 0009		1093	81 0009 1499
928	RAB 0100		1499	82 0100 1311
929	RAC 0000	AR 6	1311	88 0000 1016
930	PCH O SET 9040	PUNCH	0976	27 9040 1181
931	SBB 0537	ATOMS AND	1181	28 0537 1040
932	RAL SPEC3	ENTHALPY	1040	65 1143 0947
933	LDD RMPCH	AND VALENCE	0947	69 1150 1940
934	SET 9000	PER GRAM	1150	27 9000 1361
935	STB 0548	OF OXIDANT	1361	29 0548 1101
936	LDD TEMP2		1101	69 9002 1411
937	STD 0547		1411	24 0547 1200
938	RAL SPEC4		1200	65 1303 1461
939	LDD FINIS RMPCH		1461	69 0914 1940
940	1	CONSTANTS FOR CALCULATING		
941	1	ROUTINE		
942	1			
943	MASK6 RAL 0000 MW 4		0584	65 0000 1308
944	MASK7 LDD 0000 MW 8		0872	69 0000 1153
945	47 I 00 0000 0047		1063	00 0000 0047
946	51 I 00 0000 0051		0843	00 0000 0051
947	200 D 00 0200 0000		0764	00 0200 0000
948	10053 10 0000 0053		1406	10 0000 0053
949	11051 11 0000 0051		0534	11 0000 0051
950	10051 10 0000 0051		0524	10 0000 0051
951	FINIS HLT 9999 9999	END PROGRAM	0914	01 9999 9999
952	SPEC1 00 0587 0010		1043	00 0587 0010
953	SPEC2 00 0597 0003		1253	00 0597 0003
954	SPEC3 00 0537 0010		1143	00 0537 0010
955	SPEC4 00 0547 0003		1303	00 0547 0003
956	1	ROCKET PACKAGE EXCERPT FOR		
957	1	VECTOR AND PROPELLANTS PROGRAM		
958	1			
959	1			
960	BLA 1500 1999			
961	BLR 0000 1499			
962	1	OUTPUT ROUTINE		
963	1	PUNCH BELL CARDS		
964	1			
965	1			
966	REG C9050 9050			
967	REG J1991 1996			
968	REG K1965 1970			
969	REG P1977 1986			
970	SYN J000N 1990			
971	SYN PROB 1864			
972	EQU LOC 0000			
973	1			
974	PUNCH STD LINK	START HERE	1930	24 0838 1541
975	LDD 8003		1541	69 8003 1548
976	SDA C0005	1ST WORD	1548	22 9054 1504
977	SLT 0004		1504	35 0004 1515
978	SDA C0006	NUMBER WDS	1515	22 9055 1522
979	SRT 0002		1522	30 0002 1529
980	RAU 8003		1529	60 8003 1537
981	SRT 0002		1537	30 0002 1543
982	SET C0007		1543	27 9056 1598
983	LDD WDCT6		1598	69 1501 1554
984	STD P0009		1554	24 1985 1538
985	LDD PROB		1538	69 1864 1517
986	STD P0008		1517	24 1984 1587
987	LDD C0005 PCH3		1587	69 9054 1593
988	PCH3 STD P0007		1593	24 1983 1536
989	ALO CARDN		1536	15 1539 1643
990	ALO ONE D		1643	15 0516 1521
991	SDA CARDN		1521	22 1539 1542
992	STL P0010 NZERO		1542	20 1986 1589
993	NZERO RAU C0006	IS NO OF	1589	60 9055 1547
994	SUP WDCT6	WORDS LESS	1547	11 1501 1505
995	BMI LESS6 PCH4		1505	46 1508 1509
996	PCH4 STU C0006		1509	21 9055 1567
997	RAU P0009		1567	60 1985 1639
998	SRT 0004		1639	30 0004 1549
999	AUP XMOVE	SET TO MOV	1549	10 1502 1507
1000	ALO XLOC	N WORDS	1507	15 1510 1565
1001	ALO C0005 MOVEW		1565	15 9054 1523

1002	MOVEW	AUP 09999	8002		1523	10 1526 8002
1003	8002	LDL LOC	8003		8002	69 0000 8003
1004	8003	STD P0007	J000N		8003	24 1983 1990
1005	J0000	RAU C0006	PCH2		1990	60 9055 1597
1006	J0001	RAU C0006	PCH2		1991	60 9055 1597
1007	J0002	ALO ONE D	MOVEW		1992	15 0516 1523
1008	J0003	ALO ONE D	MOVEW		1993	15 0516 1523
1009	J0004	ALO ONE D	MOVEW		1994	15 0516 1523
1010	J0005	ALO ONE D	MOVEW		1995	15 0516 1523
1011	J0006	ALO ONE D	MOVEW		1996	15 0516 1523
1012	PCH2	PCH P0001			1597	71 1977 1527
1013	NZE		LINK	IS IT DONE	1527	45 1530 0838
1014		RAU P0007			1530	60 1983 1637
1015		AUP P0009			1637	10 1985 1689
1016		STU C0005	PCH3		1689	21 9054 1593
1017 1						
1018	LESS6	RAL C0006			1508	65 9055 1615
1019		STD P0009			1615	24 1985 1588
1020		SRT 0004		CLEAR ZERO	1588	30 0004 1599
1021		ALO XCLER	8002		1599	15 1552 8002
1022	8002	00 0000	K0001		8002	00 0000 1965
1023	K0001	STU P0001	K0002		1965	21 1977 1966
1024	K0002	STU P0002	K0003		1966	21 1978 1967
1025	K0003	STU P0003	K0004		1967	21 1979 1968
1026	K0004	STU P0004	K0005		1968	21 1980 1969
1027	K0005	STU P0005	K0006		1969	21 1981 1970
1028	K0006	STU P0006	PCH4		1970	21 1982 1509
1029 1						
1030	XCLER	00 0000	K0001		1552	00 0000 1965
1031	WDCT6	00 0006	0000		1501	00 0006 0000
1032	9999	00 0000	9999		1526	00 0000 9999
1033	XLOC	LDL 0000	8003		1510	69 0000 8003
1034	XMOVE	STD P0000	J0001		1502	24 1976 1991
1035	CARDN	00 0000	0000		1539	00 0000 0000
1036	ONE D	00 0001	0000		0516	00 0001 0000
1037 1						
1038 1		OUTPUT ROUTINE				
1039 1		RANDOM LOCATION CARDS WITH				
1040 1		ZERO VALUES OMITTED				
1041 1						
1042	REG C9050	9050				
1043	REG L1841	1844				
1044	REG P1977	1986				
1045	REG O1845	1845				
1046	SYN LOC	0000				
1047 1						
1048	RMPCH	STD LINK			1940	24 0838 1591
1049		LDL 8006		SAVE INDEX	1591	69 8006 1647
1050		STD C0003		ACC B AND	1647	24 9052 1503
1051		LDL 8007		C	1503	69 8007 1559
1052		STD C0004			1559	24 9053 1665
1053		RAC 8002		NO OF WDS	1665	88 8002 1573
1054 1						
1055		LDL 8003			1573	69 8003 1580
1056		SDA C0005		1ST WORD	1580	22 9054 1586
1057		SLT 0004			1586	35 0004 1697
1058		SDA C0006		NUMBER WDS	1697	22 9055 1604
1059		SRT 0002			1604	30 0002 1511
1060		RAU 8003			1511	60 8003 1519
1061		SRT 0002			1519	30 0002 1525
1062		SET C0007			1525	27 9056 1630
1063		LBB L0001		C0004 IS	1630	08 1841 1544
1064		STL C0006		COL 80	1544	20 9055 1602
1065		RSB 0004		LOCATION	1602	83 0004 1558
1066		RAL C0005			1558	65 9054 1715
1067		ALO PCHX	ENT1	C0003 IS	1715	15 1518 1623
1068	ENT1	STL C0005		CURRENT	1623	20 9054 1680
1069 1				LOCATION		
1070		ALO XRAU	8002		1680	15 1533 8002
1071	8002	RAU LOC	00001		8002	60 0000 1845
1072	00001	NZU MOVER	C0007	C0007 HAS	1845	44 1649 9056
1073 1				L0001		
1074	L0001	SXC 0001			1841	59 0001 1747
1075		NZC	FINS		1747	48 1500 1551
1076		RAL C0005			1500	65 9054 1557
1077		ALO ONE D	ENT1		1557	15 0516 1623
1078 1						

1079	MOVER	STD P0005 R		MOVE WD	1649	24	5981	1534
1080		RAL C0005			1534	65	9054	1641
1081		STD P0010 R			1641	24	5986	1739
1082		NZB PCH5		IS CARD	1739	42	1592	1693
1083		AXB 0001 C0007		FULL YET	1592	52	0001	9056
1084	PCH5	BMI PLUS			1693	46	1546	1797
1085		SLO C0006 BOTH		FIX COL 8	1546	16	9055	1553
1086	PLUS	ALO C0006 BOTH			1797	15	9055	1553
1087	BOTH	STL P0010			1553	20	1986	1789
1088		RAL RMCDN		NUMBER CDS	1789	65	1642	1847
1089		ALO ONE I			1847	15	1356	1561
1090		STL RMCDN			1561	20	1642	1545
1091		LDD P0009			1545	69	1985	1638
1092		SIA P0009			1638	23	1985	1688
1093		PCH P0001		PUNCH CARD	1688	71	1977	1577
1094		RSB 0004 C0008		C0008 HAS	1577	83	0004	9057
1095	L0002	STU C0006 C0007		L0002	1842	21	9055	9056
1096	1							
1097	ONE D	00 0001 0000			0516	00	0001	0000
1098	ONE I	00 0000 0001		ONE INSTR	1356	00	0000	0001
1099	XRAU	59 9999 02001			1533	59	9999	3845
1100	PCHX	00 0000 8000			1518	00	0000	8000
1101	RMCDN	00 0000 0000		RANDOM CD	1642	00	0000	0000
1102	1			NUMBER				
1103	FINS	SET C0007		CHANGE	1551	27	9056	1506
1104		LBB L0003		ORDERS	1506	08	1843	1596
1105		RSL PCHX		FOR FINS	1596	66	1518	1673
1106		STL C0005 C0007			1673	20	9054	9056
1107	L0003	LDD 8003 MOVER			1843	69	8003	1649
1108	L0004	RAB C0001		RESTOR	1844	82	9050	1652
1109		RAC C0002 LINK		INDX ACC	1652	88	9051	0838
1110		PAT						

## APPENDIX I

## 533 CONTROL PANEL ("ROCKET BOARD") WIRING INSTRUCTIONS

I. Read card C is used for reading Bell format cards. The word positions are numbered from the right (see 650 Manual of Operation, p. 10):

Read card C (card column)	Storage entry C	Word size entry C
11	Sign of word 1	
12-21	Word 1, positions 10 to 1	10
22	Sign of word 2	
23-32	Word 2, positions 10 to 1	10
33	Sign of word 3	
34-43	Word 3, positions 10 to 1	10
44	Sign of word 4	
45-54	Word 4, positions 10 to 1	10
55	Sign of word 5	
56-65	Word 5, positions 10 to 1	10
66	Sign of word 6	
67-76	Word 6, positions 10 to 1	10
6-9	Word 7, positions 8 to 5, emit sign +	8
5, 77-79	Word 8, positions 8 to 5, emit sign +	8
80, 1-4	Word 9, positions 9 to 5, emit sign +	9
10	Word 10, position 5, emit sign +; positions 4 to 1 of words 7, 8, 9, and 10 wired to emit zero	5

II. Read card B is used for reading Random location format cards:

Read card B (card column)	Storage entry B	Word size entry B
5-15	Word 1, positions 10 to 1, col. 15 is sign	10
20-30	Word 2, positions 10 to 1, col. 30 is sign	10
35-45	Word 3, positions 10 to 1, col. 45 is sign	10
50-60	Word 4, positions 10 to 1, col. 60 is sign	10
65-75	Word 5, positions 10 to 1, col. 75 is sign	10
1-4	Word 6, positions 8 to 5, emit sign +	8
16-19	Word 7, positions 8 to 5, emit sign +	8
31-34	Word 8, positions 8 to 5, emit sign +	8
46-49	Word 9, positions 8 to 5, emit sign +	8
61-64	Co-selector 1 transferred points (U, 1 to 4) (make col. 61 a split wire. p. 119)	
76-80	Not wired Words 6 to 9 emit zero into positions 4 to 1	

Selector wiring for determining and entering the word count in word 10 and ensuring that word 10 is a legitimate word is as follows:

Co-selector 1 common (W, 1 to 4) to word 10, positions 8 to 5  
storage entry B

Word size of word 10. entry B is 8

Co-selector 1 normal (V, 1 to 4), to (V, 32). (This guarantees a nonzero value on word 10 to preserve the negative sign for a branch on minus test.)

Emit zeros to word 10, positions 4 to 2, storage entry B

Emit sign of word 10 minus (V, 28)

Pilot selector 1 common (K, 23) to word 10, position 1, storage entry B

Pilot selector 1 normal (J, 23) to emit zero

Pilot selector 1 transferred (H, 23) to pilot selector 2 common (K, 24)

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Pilot selector 2 transferred (H, 24) to pilot selector 3 common (K, 25)  
 Pilot selector 3 normal (J, 25) to emit 2 (W, 21)  
 Pilot selector 3 transferred (H, 25) to pilot selector 4 common (K, 26)  
 Pilot selector 4 normal (J, 26) to emit 3 (X, 21)  
 Pilot selector 4 transferred (H, 26) to pilot selector 5 common (K, 27)  
 Pilot selector 5 normal (J, 27) to emit 4 (Y, 21)  
 Pilot selector 5 transferred (H, 27) to emit 5 (Z, 21)  
 Pilot selector 2 normal (J, 24) to emit 1 (V, 21)  
 First reading col. 1 (A, 23) to load (B, 21)  
 First reading col. 1 (A, 23) to common of col. split } split wire (Z, 34)  
 Col. split 0-9 (Y, 34) to D pick pilot selector 1 (F, 23)

Co-selector 3 pick (R, 25) to col. split 12-X (X, 34)  
 Co-selector 3 common (W, 11) to emit 9 (W, 34)  
 Co-selector 3 transfer (U, 11) to entry B (D, 21)

First reading col. 16 (A, 38) to D pick pilot selector 2 (F, 24)  
 First reading col. 31 (C, 33) to D pick pilot selector 3 (F, 25)  
 First reading col. 46 (C, 28) to D pick pilot selector 4 (F, 26) (Split wire, p. 120)  
 First reading col. 61 (D, 23) to D pick pilot selector 5 (F, 27)  
 Couple pilot selector 5 (G, 27) to co-selector pickup 1 (S, 23)

Digit impulse (Q, 21) to digit selector common (R, 21)  
 First reading col. 15 (A, 37) to col. split 12-X (X, 33)  
 Col. split common (Z, 33) to entry B (D, 22)

Hold for pilot selectors 1 to 5 (P, 23 to 27) and co-selectors 1 and 3 (U, 23 and 25) are wired to read hold (T, 39).

III. Read card A is used to read input cards (SOAP II format) for Vector and Propellant Program (requires the alphabetic attachment and pilot selectors 11, 12, 13):

First reading col. 3 (A, 25) to col. split common (Z, 35)  
 Col. split 12-X (X, 35) to entry A (C, 22)  
 Entry A (C, 23) to pilot selector 12-X pick (E, 34)  
 Pilot selector 12 couple exit (G, 34) to alphabetic control WI (AL, 12) and also to W2 to W6.

Storage entry A, word 10, position 3 (J, 19) to pilot selector 13  
 common (K, 35)  
 Pilot selector 13 normal (J, 35) to zero read impulse (AN, 20)  
 Pilot selector 13 transfer (H, 35) to read card A, col. 41 (C, 1)  
 Pilot selector 13 D pick (F, 35) to first reading col. 41 (C, 23)  
 Storage entry A, word 10, position 2 (J, 20) to pilot selector 13  
 common (N, 35)  
 Pilot selector 13 normal (M, 35) to zero read impulse (AP, 20)  
 Pilot selector 13 transfer (L, 35) to read impulse 9 (V, 34)  
 Storage entry A, word 10, position 1 (J, 21) to pilot selector 11  
 common (N, 33)  
 Pilot selector 11 normal (M, 33) to zero read impulse (AP, 21)  
 Pilot selector 11 transfer (L, 33) to read impulse 8 (V, 33)  
 Pilot selector 11 D pick (F, 33) to first reading, col. 42 (C, 24)  
 Read card A, col. 43 (C, 3) to storage entry A, word 1, position 5  
 (E, 6)  
 Read card A, col. 44 to 47 (C, 4 to 7) split wire to word 1, positions  
 4 to 1 (E, 7 to 10) and to word 7, positions 4 to 1 (H,  
 7 to 10)  
 Read card A, col. 48 to 50 (C, 8 to 10) to word 4, positions 5 to 3  
 (F, 17 to 19)  
 Read card A, col. 51 (C, 11) to word 2, position 5 (E, 17)  
 Read card A, col. 52 to 55 (C, 12 to 15) split wire to word 2,  
 positions 4 to 1 (E, 18 to 21) and to word 8, positions 4 to 1  
 (H, 18 to 21)  
 Read card A, col. 56 (C, 16) to word 4, position 2 (F, 20)  
 Read card A, col. 57 (C, 17) to word 3, position 5 (F, 6)  
 Read card A, col. 58 to 61 (C, 18 to D, 1) split wire to word 3,  
 positions 4 to 1 (F, 7 to 10) and to word 9, positions 4 to 1  
 (J, 7 to 10)  
 Read card A, col. 62 (D, 2) to word 4, position 1 (F, 21)  
 Read card A, col. 63 to 67 (D, 3 to 7) to word 5, positions 5 to 1  
 (G, 6 to 10)  
 Read card A, col. 68 to 72 (D, 8 to 12) to word 6, positions 5 to 1  
 (G, 17 to 21)  
 First reading, col. 43 to 47 (C, 25 to 29) to alphabetic first read,  
 word 1, positions 5 to 1 (AK, 13 to 17)  
 Col. 48 to 50 (C, 30 to 32) to alphabetic first read, word 4,  
 positions 5 to 3 (AL, 18 to 20)  
 Col. 51 to 55 (C, 33 to 37) to alphabetic first read, word 2,  
 positions 5 to 1 (AK, 18 to 22)  
 Col. 56 (C, 38) to alphabetic first read, word 4, position 2 (AL,  
 21)  
 Col. 57 to 61 (C, 39 to D, 23) to alphabetic first read, word 3,  
 positions 5 to 1 (AL, 13 to 17)  
 Col. 62 (D, 24) to alphabetic first read, word 4, position 1 (AL, 22)  
 Col. 63 to 67 (D, 25 to 29) to alphabetic first read, word 5,  
 positions 5 to 1 (AM, 13 to 17)  
 Col. 68 to 72 (D, 30 to 34) to alphabetic first read, word 6, posi-  
 tions 5 to 1 (AM, 18 to 22)

Read validity check wire off (AR, 43) to (AR, 44)  
 Chain wire pilot selector hold of pilot selectors 11, 12, and 13  
 (P, 33 to 35) to read hold (T, 39)  
 Word size entry A, words 7 to 9 (AL, 7 to 9) to word size emitter 4  
 (AK, 5)  
 Word size entry A, word 10 (AL, 10) to word size emitter 3 (AK, 4)

IV. Punch card C is used to punch Bell format cards and Trace format cards:

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Punch card C (card column)	Storage exit C
11	Sign of word 1
12-21	Word 1, positions 10 to 1
22	Sign of word 2
23-32	Word 2, positions 10 to 1
33	Sign of word 3
34-43	Word 3, positions 10 to 1
44	Sign of word 4
45-54	Word 4, positions 10 to 1
55	Sign of word 5
56-65	Word 5, positions 10 to 1
66	Co-selector 7 common (W, 59) Co-selector 7 normal (V, 59) to word 6 sign (AG, 64)(Split wire, see Trace cards)
67	Word 6, position 10
68-72	Co-selectors 6 and 7 common (W, 54 to 58) Co-selectors 6 and 7 normal (W, 54 to 58) to word 6, positions 9 to 5
73-76	Word 6, positions 4 to 1
6-9	Co-selector 6 common (W, 50 to 53) Co-selector 6 normal (V, 50 to 53) to word 7, positions 8 to 5
5, 77-79	Word 8, positions 8 to 5
10	Word 9, position 5
80, 1-4	Word 10, positions 9 to 5

For Trace cards:

Co-selector 6 transfer (U, 50 to 53) to word 7, positions 4 to 1

Co-selectors 6 and 7 transfer (U, 54 to 57) to word 8, positions

4 to 1

Co-selector 7 transfer (U, 58) to word 6, sign position

Co-selector 7 transfer (U, 59) to word 8, sign position

An 8 in position 9 of word 10 causes Trace cards to be punched by  
means of control information:

Control information (AM, 56) to co-selectors 6 and 7 pick (R, 28,  
29)

Co-selectors 6 and 7 hold (T, 28, 29) to punch hold (R, 39)

Jack plug "P+" (V, 42) to (W, 42)

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## V. Punch card B is used to punch Random location cards:

Punch card B (card column)	Storage exit B
5-15	Word 1, positions 10 to 1, col. 15 is sign
20-30	Word 2, positions 10 to 1, col. 30 is sign
35-45	Word 3, positions 10 to 1, col. 45 is sign
50-60	Word 4, positions 10 to 1, col. 60 is sign
65-75	Word 5, positions 10 to 1, col. 75 is sign
1	Pilot selector 6 common (K, 28) Pilot selector 6 normal (J, 28) to word 6, position 8
2-4	Word 6, positions 7 to 5
16	Pilot selector 7 common (K, 29) Pilot selector 7 normal (J, 29) to word 7, position 8
17-19	Word 7, positions 7 to 5
31	Pilot selector 8 common (K, 30) Pilot selector 8 normal (J, 30) to word 8, position 8
32-34	Word 8, positions 7 to 5
46	Pilot selector 9 common (K, 31) Pilot selector 9 normal (J, 31) to word 9, position 8
47-49	Word 9, positions 7 to 5
61	Pilot selector 10 common (K, 32) Pilot selector 10 normal (J, 32) to word 10, position 8
62-64	Word 10, positions 7 to 5
76-79	Word 9, positions 4 to 1
80	Word 10, position 9

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CA-16 back

Pilot selector 6 I pick (G, 28) to sign word 6  
Pilot selector 7 I pick (G, 29) to sign word 7  
Pilot selector 8 I pick (G, 30) to sign word 8  
Pilot selector 9 I pick (G, 31) to sign word 9  
Pilot selector 10 I pick (G, 32) to sign word 10  
Co-selector 2 pick (R, 24) to punch X impulse (A, 43)  
Co-selector 2 common (W, 6) to punch hold (R, 39)  
Co-selector 2 transferred (U, 6) split wire to transfer of pilot  
selectors 6 to 10 inclusive (L, 28 to 32)  
Pilot selectors 6 to 10 common (N, 28 to 32) to pilot selector  
hold 6 to 10 (Q, 28 to 32)  
Co-selector 2 hold (T, 24) to punch hold (S, 39)  
Control information 4 (AK, 61) to punch E (D, 43)

VI. Punch card A is used to punch SOAP II format cards:

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Punch card A (card column)	Storage exit A
1	Col. split common (AM, 52) Col. split 0-9 (AL, 52) to emit 6 (AA, 43) Col. split 12-X (AK, 52) to emit 12 (S, 43); Wire DI (Q, 43) to common (R, 43)
2-6	Emit 9,1,9,5,4, respectively, from punch emitter
7-10	Co-selector 5 common positions 4 to 1 (W, 46 to 49) Co-selector 5 normal positions 4 to 2 (V, 46 to 48) to emit 1,9,5, respectively, from punch emitter Co-selector 5 normal position 1 (V, 49) to col. split common (AM, 45) Col. split 0-9 (AL, 45) to emit 3 Col. split 12-X (AK, 45) to emit 12 (S, 43) Co-selector 5 transfer positions 4 to 2 (U, 46 to 48) to emit 8,0,0, respectively Co-selector 5 transfer position 1 (U, 49) to col. split common (AM, 46) Col. split 0-9 (AL, 46) to emit 3 Col. split 12-X (AK, 46) to emit 12 (S, 43)
11-20	Word 9, positions 10 to 1, wire sign of word 9 to col. 20 with col. split (AM, 47)
21	Emit 2
22	Emit 4
23-26	Word 8, positions 8 to 5
27-29	Emit 8,0,0, respectively
30	Col. split common (AM, 48) Col. split 0-9 (AM, 48) to emit 0 Col. split 12-X (AM, 48) to emit 12
31-40	Word 7, positions 10 to 1, wire sign through col. split to col. 40 and 42
41	Word 8, position 1
42	Sign of word 7
43-47	Word 1, positions 5 to 1
48-50	Word 4, positions 5 to 3
51-55	Word 2, positions 5 to 1
56	Word 4, position 2
57-61	Word 3, positions 5 to 1
62	Word 4, position 1
63-67	Word 5, positions 5 to 1
68-72	Word 6, positions 5 to 1

Control information 2 (AK, 63) to co-selector 5 pick (R, 27)  
 Control information 3 (AK, 62) to Alpha cut W1 and also chain wire  
     to W2, W3, W4, W5, and W6  
         3 (AL, 62) to Punch A (C, 43)  
 Co-selector 5 hold (T, 27) to punch hold (R, 40)

## REFERENCES

1. Traustel, S.: Berechnung von Vergasungsgleichgewichten durch Losung von Zwei Gleichungen mit Zwei Unbekannten. Z.V.D.I., Bd. 88, Dec. 1944, pp. 688-690.
2. Brinkley, Stuart R., Jr.: Note on the Conditions of Equilibrium for Systems of Many Constituents. Jour. Chem. Phys., vol. 14, no. 9, Sept. 1946, pp. 563-564.
3. Brinkley, Stuart R., Jr.: Calculation of the Equilibrium Composition of Systems of Many Constituents. Jour. Chem. Phys., vol. 15, no. 2, Feb. 1947, pp. 107-110.
4. Krieger, F. J., and White, W. B.: A Simplified Method for Computing the Equilibrium Composition of Gaseous Systems. Jour. Chem. Phys., vol. 16, no. 4, Apr. 1948, pp. 358-360.
5. Wenner, Ralph R.: Prediction of Reaction Equilibria. Chem. Eng. Prog., vol. 45, no. 3, Mar. 1949, pp. 194-207.
6. Sachsel, G. F., Mantis, M. E., and Bell, J. C.: A Note on the Calculation of Multicomponent Propellant Gas Compositions. Third Symposium on Combustion and Flame and Explosion Phenomena, The Williams & Wilkins Co. (Baltimore), 1949, pp. 620-623.
7. Winternitz, Paul F.: A Method for Calculating Simultaneous, Homogeneous Gas Equilibria and Flame Temperatures. Third Symposium on Combustion and Flame and Explosion Phenomena, The Williams & Wilkins Co. (Baltimore), 1949, pp. 623-633.
8. Kandiner, Harold J., and Brinkley, Stuart R., Jr.: Calculation of Complex Equilibrium Relations. Ind. and Eng. Chem., vol. 42, no. 5, May 1950, pp. 850-855.
9. Huff, Vearl N., Gordon, Sanford, and Morrell, Virginia E.: General Method and Thermodynamic Tables for Computation of Equilibrium Composition and Temperature of Chemical Reactions. NACA Rep. 1037, 1951. (Supersedes NACA TN's 2113 and 261.)

- 4 -
10. Martin, Frederick J., and Yachter, Morris: Calculation of Equilibrium Gas Compositions. Ind. and Eng. Chem., vol. 43, no. 11, Nov. 1951, pp. 2446-2449.
  11. Kobe, Kenneth A., and Leland, Thomas W.: Calculation of Chemical Equilibrium in Complex Systems. Bur. Eng. Res. Spec. Pub. no. 26, Univ. of Texas, 1954.
  12. Martinez, J. S., and Elverum, G. W., Jr.: A Method of Calculating the Performance of Liquid-Propellant Systems Containing the Species C, H, O, N, F, and One Other Halogen - with Tables of Required Thermochemical Properties to 6000° K. Memo. No. 20-121, Jet Prop. Lab, C.I.T., Dec. 6, 1955. (Contract DA-04-495-ORD-18.)
  13. Donegan, A. J., and Farber, M.: Solution of Thermochemical Propellant Calculations on a High-Speed Computer. Jet Prop., vol. 26, no. 3, Mar. 1956, pp. 164-171.
  14. Brinkley, Stuart R., Jr.: Computational Methods in Combustion Calculations. Vol. II of Combustion Processes - High Speed Aerodynamics and Jet Propulsion, B. Lewis, R. N. Pease, and H. S. Taylor, eds., Princeton Univ. Press, 1956, pp. 64-98.
  15. Weinberg, F. J.: Explicit Equations for the Calculation, by Successive Approximations, of Equilibrium Gas Compositions at High Temperatures: the Hydrogen + Carbon + Oxygen and the Hydrogen + Carbon + Oxygen + Nitrogen Systems Without Solid Carbon Formation. Proc. Roy. Soc. (London), ser. A, vol. 241, no. 1224, July 23, 1957, pp. 132-140.
  16. McIntire, R. L.: Computers and Thermodynamics. Automatic Control, vol. 8, no. 2, Feb. 1958, pp. 51-55.
  17. Chu, S. T.: An Iterative Method of Determining Equilibrium Compositions of Reacting Gases. Jet Prop., vol. 28, no. 4, Apr. 1958, pp. 252-254.
  18. White, W. B., Johnson, S. M., and Dantzig, G. B.: Chemical Equilibrium in Complex Mixtures. Jour. Chem. Phys., vol. 28, no. 5, May 1958, pp. 751-755.
  19. Hilsenrath, J., Klein, M., and Sumida, D. Y.: Mechanized Computation of Thermodynamic Tables at the National Bureau of Standards: The Calculation of the Equilibrium Composition and Thermodynamic Properties of Dissociated and Ionized Gaseous Systems. Thermodynamic and Transport Properties of Gases, Liquids, and Solids - Symposium on Thermal Properties, ASME and McGraw-Hill Book Co., Inc., 1959, pp. 416-437.

- 1 T#-1
20. Wilkins, Roger L., and Payne, William H.: High Speed Machine Calculation of the Performance of Rocket Propellants Containing N-Elements. Res. Rep. 59-15, Rocketdyne, North Am. Aviation, Inc., Feb. 24, 1959.
  21. Fiegenbutz, L. V.: Combustion Charts for High Energy Fuels. II - A Description of General Methods for Calculating Equilibrium Concentrations of Combustion Products. Rep. No. ZR-658-031, Convair, Mar. 2, 1959.
  22. Villars, D. S.: A Method of Successive Approximations for Computing Combustion Equilibria on a High Speed Digital Computer. Jour. Phys. Chem., vol. 63, no. 4, Apr. 1959, pp. 521-525.
  23. Scarborough, James B.: Numerical Mathematical Analysis. Johns Hopkins Press (Baltimore), 1930, pp. 187-190.
  24. Bridgman, P. W.: Condensed Collection of Thermodynamic Formulas. Harvard Univ. Press, Cambridge (Mass.), 1926.
  25. Gordon, Sanford, and Huff, Vearl N.: Theoretical Performance of Liquid Hydrazine and Liquid Fluorine as a Rocket Propellant. NACA RM E53E12, 1953.
  26. Huff, Vearl N., Turner, Don N., and Reese, Oliver W.: General-Purpose Subroutines for the IBM 650 Magnetic Drum Data-Processing Machine with Attachments. NASA TN D-68, 1959.

TABLE I. - COEFFICIENTS FOR OBTAINING THERMODYNAMIC DATA FOR SEVERAL SUBSTANCES  
[Coefficients for use in equations (105) to (107).]

Substance (a)	Temperature interval, °K	Coefficients					
		A	B	C	D	E	F
C	150 - 300	+2527 8238 51	+1867 6400 47	-2011 9997 45	+3832 8460 42	+1318 3612 56	+4598 3693 51
	300 - 500	+2511 0513 51	+2241 3464 46	-2064 1813 44	+2504 6361 41	+1318 3951 56	+4694 0319 51
	500 - 700	+2505 9144 51	+1127 5624 46	-6304 0443 43	+5333 3425 40	+1318 4070 56	+4722 3131 51
	700 - 1000	+2503 4230 51	+5325 3290 45	-2160 0382 43	+1354 8725 40	+1318 4156 56	+4737 1984 51
	1000 - 1300	+2503 2775 51	+5521 0150 45	+585 14748 43	+1385 6245 39	+1318 4123 56	+4737 2493 51
	1300 - 1700	+2504 6546 51	+9314 5910 45	+2465 5200 43	+1190 5484 43	+1318 3969 56	+4726 7149 51
	1700 - 2100	+2501 5285 51	+5907 5500 45	-1820 8474 43	+949 17040 43	+1318 3700 56	+4749 6818 51
	2100 - 2600	+2484 4570 51	-1345 7700 46	+8780 3410 42	+2879 3740 39	+1318 4349 56	+4852 5918 51
	2600 - 3200	+2472 3652 51	-6335 7912 46	+3975 0497 43	-3693 6212 39	+1319 6460 56	+4990 5948 51
	3200 - 3800	+2476 2539 51	-6493 0882 46	+3155 2588 43	+5893 3109 39	+1319 0115 56	+4990 7555 51
	3800 - 4400	+2504 1340 51	-7041 0160 46	+5063 4142 43	+5359 6037 39	+1318 6229 56	+4783 1816 51
	4400 - 5000	+2566 5888 51	-6519 6370 46	+155 2568 46	+4063 3061 39	+1317 6142 56	+4455 1751 51
	5000 - 6000	+2610 4540 51	-4741 7690 46	+2664 8172 43	+2304 3960 39	+1315 6607 56	+3935 3511 51
Graphite	300 - 500	+5673 0710 50	-2106 2241 48	+1744 0045 46	-1691 9439 43	+4619 0744 55	-2545 1750 51
	500 - 700	+1058 3269 51	-2064 1842 48	+1091 7536 46	-7970 7376 42	+4607 1927 55	+5175 2399 51
	700 - 1000	+1628 3807 51	-1307 2653 48	+5023 1415 46	-2756 8704 42	+4584 8409 55	-8591 5430 51
	1000 - 1300	+2289 3860 51	-3947 4982 47	+9829 2657 45	-2901 7265 41	+4546 1211 55	-1287 2346 52
	1300 - 1700	+2407 1476 51	-6784 1780 47	+1008 1106 45	-3136 4202 41	+4537 7132 55	-1361 1991 52
	1700 - 2100	+2709 5422 51	-2313 1973 47	+3670 0610 45	-8357 2671 40	+4507 5530 55	-1573 1714 52
	2100 - 2600	+2841 4329 51	-1619 7368 47	+2059 3854 45	-3684 0068 40	+4491 5653 55	-1667 5373 52
	2600 - 3200	+2958 2033 51	-1146 5505 47	+1154 2930 45	-1567 2361 40	+4474 0549 55	-1753 4601 52
	3200 - 3800	+3040 3247 51	-9509 5628 46	+7614 5316 43	-7812 3581 39	+4460 0657 55	-1814 4793 52
	3800 - 4400	+3097 3807 51	-9187 9709 46	+1814 4345 43	-5311 3595 39	+4449 1831 55	-1856 9802 52
	4400 - 5000	+3152 7766 51	-8885 2831 46	+1518 2079 43	-3740 3256 39	+4436 8642 55	-1899 1194 52
CC1	150 - 300	+3820 2364 51	+6255 4820 47	-7410 0490 45	+2285 0707 43	+1092 3347 56	+5349 2058 51
	300 - 500	+3693 1871 51	-6286 6910 47	+7775 5823 45	-8061 1528 45	+1092 5828 56	+6074 2136 51
	500 - 700	+3912 5704 51	-5230 0920 47	+4222 7425 45	-3279 9984 43	+1092 0413 56	+4884 6073 51
	700 - 1000	+4115 6696 51	-4342 0808 47	+1693 0922 45	-9680 7575 41	+1091 2721 56	+3666 0743 51
	1000 - 1300	+4271 6614 51	-2203 0847 47	+1118 7616 44	-2567 8704 42	+1090 4684 56	+2678 1140 51
	1300 - 1700	+4378 2291 51	-9382 1810 46	+2108 6630 44	-6167 2272 40	+1089 6529 56	+1956 5236 51
	1700 - 2100	+4428 6744 51	-5606 4340 46	+9128 2970 43	-8479 8548 39	+1088 7729 56	+1368 9058 51
	2100 - 2600	+4461 6643 51	-3393 9946 46	+4442 3777 43	-5571 2362 39	+1088 4376 56	+1199 9462 51
	2600 - 3200	+4484 6128 51	-2289 1842 46	+2381 3945 43	-5771 2305 39	+1088 1620 56	+1079 4739 51
	3200 - 3800	+4500 7379 51	-1781 1586 46	+1497 8228 43	-5752 0030 38	+1087 8935 56	+9798 5788 50
	3800 - 4400	+4513 7299 51	-1439 6338 46	+1005 6037 43	-6609 4573 38	+1087 6927 56	+9117 3280 50
	4400 - 5000	+4522 5949 51	-1319 2912 46	+7941 9120 42	-5808 8556 42	+1087 4110 56	+8309 5849 50
CC1 <sub>4</sub>	150 - 300	+6883 4230 51	-2183 6856 49	+2209 0207 47	-3765 2673 44	+4132 9670 55	-2005 0830 51
	300 - 500	+6534 3172 51	-7160 8000 48	+6201 5460 45	-7111 6167 43	+4098 5503 55	+1142 3036 52
	500 - 700	+1008 7133 52	-5270 2740 48	+2629 9117 46	-2170 8108 43	+4052 5210 55	+1988 7565 52
	700 - 1000	+1120 9988 52	-2287 4085 48	+9077 1820 45	+5423 6390 42	+4023 5045 55	+2659 6737 52
	1000 - 1300	+1195 6348 52	-1043 2162 48	+2943 6828 45	-1282 6918 42	+3986 5351 55	+1130 0846 52
	1300 - 1700	+1248 4721 52	-3391 1184 47	+7258 7051 44	-2336 0965 41	+3945 8748 55	+320 8744 52
	1700 - 2100	+1268 0666 52	-1729 2303 47	+2873 9710 44	-7327 1794 40	+3926 8367 55	+3677 0046 52
	2100 - 2600	+1279 3339 52	-8857 1920 46	+1192 5272 44	+2449 6562 40	+3912 7677 55	+3709 6992 52
	2600 - 3200	+1286 1578 52	-4880 6790 46	+5345 6302 43	-8955 1435 39	+3902 3779 55	+3760 5577 52
	3200 - 3800	+1290 2043 52	-3013 4232 46	+2724 8863 43	-3823 5766 39	+3895 0427 55	+3791 3780 52
	3800 - 4400	+1292 8751 52	-1886 0004 46	+1451 7234 43	-1740 7449 39	+3889 1827 55	+3812 2942 52
	4400 - 5000	+1294 5807 52	-1253 5153 46	+8422 0090 42	-8823 9152 38	+3884 8198 55	+3825 9243 52
	5000 - 6000	+1296 2205 52	-6498 6420 45	+3820 8266 42	-3347 9564 38	+3879 6914 55	+3839 4390 52
CF	150 - 300	+3640 0400 51	+8085 8640 47	-1026 9011 46	+2428 4900 43	+1140 5783 56	+4867 6076 51
	300 - 500	+3498 5413 51	-4528 6370 47	+3399 6376 45	-1921 1982 43	+1140 9729 56	+5674 6721 51
	500 - 700	+3577 7497 51	-8040 8130 47	+4156 7731 45	-2824 2658 42	+1140 7415 56	+5176 7255 51
	700 - 1000	+3810 1072 51	-6265 2490 47	+2385 5286 45	-1274 7825 42	+1140 9158 55	+3918 2736 51
	1000 - 1300	+4048 2657 51	-3385 1238 47	+1061 8631 45	-2475 8782 41	+1140 6368 56	+2414 2551 51
	1300 - 1700	+4225 0270 51	-5209 1787 47	+4574 3037 44	-1339 8215 41	+1140 2978 56	+1226 0050 51
	1700 - 2100	+4334 2200 51	-1335 8603 47	+2161 7485 44	-5212 2758 40	+1140 2672 56	+4713 8170 50
	2100 - 2600	+4411 7942 51	-8377 6910 46	+3466 3361 44	-2048 7978 40	+1140 3778 56	+8671 8950 49
	2600 - 3200	+4467 8185 51	-5822 8670 46	+4020 6162 44	-8903 5200 39	+1140 5100 56	+4985 2010 50
	3200 - 3800	+4508 2460 51	-4630 6640 46	+3870 6033 43	-4884 6039 39	+1140 8215 56	+8008 8070 50
	3800 - 4400	+4541 0295 51	-3813 2796 46	+2644 8087 43	-2541 3761 39	+1140 1526 56	+1050 5867 51
	4400 - 5000	+4569 6116 51	-3184 7846 46	+1851 2604 43	-1379 0052 39	+1140 4685 56	+1273 6745 51
	5000 - 6000	+4608 1204 51	-2076 7807 46	+9178 6561 42	-2634 8774 38	+1140 3042 56	+1586 8660 51
CF <sub>2</sub>	150 - 300	+4048 5275 51	-2616 5412 48	+2155 9333 46	-2058 6114 43	+6584 7865 55	+5829 4252 51
	300 - 500	+4074 4857 51	-5299 6320 48	+2064 5751 46	-1981 1983 43	+6584 1442 55	+5860 2914 51
	500 - 700	+4691 9175 51	-2394 9638 48	+1263 9499 46	-9151 6968 42	+6568 6792 55	+2344 8275 51
	700 - 1000	+5409 6786 51	-1408 4350 48	+5348 7413 45	-2842 5180 42	+6559 7513 55	+5019 9885 51
	1000 - 1300	+6025 9535 51	-7504 6540 47	+2030 6869 45	-7987 0809 41	+6504 7319 55	+2079 2299 51
	1300 - 1700	+6398 7799 51	-3929 7130 47	+8155 2021 44	-2451 9736 41	+6475 5249 55	+8433 7600 51
	1700 - 2100	+6642 6054 51	-2224 2190 47	+3545 7494 44	-8257 7665 40	+6450 9950 55	+1013 7338 52
	2100 - 2600	+6788 3007 51	-1372 2127 47	+1756 5186 44	-3252 4740 40	+6432 4476 55	+1119 1218 52
	2600 - 3200	+6891 2452 51	-9243 3170 47	+1943 4160 43	-1396 0756 40	+6416 6267 55	+1195 3073 52
	3200 - 3800	+6967 1014 51	-5796 6480 46	+5630 0653 45	-6591 8731 39	+6402 7074 55	+1252 6276 52
	3800 - 4400	+7021 0652 51	-5466 6732 46	+3777 3931 43	-3621 0579 39	+6390 9978 55	+1294 2206 52
	4400 - 5000	+7058 0449 51	-4920 3790 46	+2933 2725 43	-2428 1894 39	+6382 1426 55	+1322 8904 52
	5000 - 6000	+7097 4438 51	-3117 6367 46	+2148 5733 43	-1461 5182 39	+6370 9039 55	+1354 3379 52
CF <sub>3</sub>	150 - 300	+4415 9046 51	-1079 2001 49	+1028 9803 47	-1547 4411 44	+3294 5442 55	+6322 6310 51
	300 - 500	+6929 4769 51	+6869 2840 48	-6064 6133 46	+8848 4060 43	+3233 5181 55	+8614 0405 51
	500 - 700	+1344 2602 51	-5167 3100 48	+2151 1245 46	-1307 2694 43	+3257 6653 55	+4378 9560 51
	700 - 1000	+6412 2022 51	-5167 3100 48	+2151 1245 46	-1307 2694 43	+3209 7765 55	+1238 8123 52
	1000 - 1300	+7725 6912 51	-5167 3100 48	+2151 1245 46	-1307 2694 43	+3209 7765 55	+2139 6277 52
	1300 - 1700	+9068 6613 51	-1109 2747 48	+2576 9457 45	-8070 0746 41	+3114 9770 55	+2559 1310 52
	1700 - 2100	+9682 7034 51	-6585 8810 47	+1229 5950 45	-2863 4956 40	+3061 1725 55	+2883 3685 52
	2100 - 2600	+1013 8660 52	-4418 4184 47	+7821 4418 47	-1094 2288 40	+3001 1267 55	+3127 2861 52
	2600 - 3200	+1047 7649 52	-5066 9283 47	+4132 9340 44	-5398 9138 40	+2961 3366 55	+3137 2861 52
	3200 - 3800	+1076 8882 52	-3381 4409 47	+3076 1815 44	-3205 5453 40	+2914 5240 55	+3339 4045 52
	3800 - 4400	+1102 5318 52	-3277 2624 47	+2461 8412 44	-2128 3409 40	+2865 7705 55	+3330 0856 52
	4400 - 5000	+1125 0822 52	-3285 332				

TABLE I. - Continued. COEFFICIENTS FOR OBTAINING THERMODYNAMIC DATA FOR SEVERAL SUBSTANCES  
Coefficients for use in equations (105) to (107)

Substance (a)	Temperature Interval, °K	Coefficients						
		A	B	C	D	E	F	
CH	150 - 300	+3512 7827 51	+4436 0810 46	-5378 9030 44	+1146 7347 42	+1344 6458 56	+1985 4362 51	
	300 - 500	+3518 9332 51	+8459 1000 46	-1000 7610 44	+1731 4444 42	+1344 6317 56	+1950 3265 51	
	500 - 700	+3488 5121 51	-1451 9700 46	-1474 4120 44	+9635 7727 41	+1344 7464 56	+2140 1459 51	
	700 - 1000	+3400 5554 51	-5633 2939 47	+1934 0930 45	-6925 5161 41	+1345 2502 56	+2759 7067 51	
	1000 - 1300	+3354 5554 51	-8189 6840 47	+2173 4717 45	-8003 0517 41	+1344 7547 56	+2069 0007 51	
	1300 - 1700	+3387 6747 51	-6520 0620 47	+1371 1096 45	-4245 5.02 41	+1342 4710 56	+1544 3006 49	
	1700 - 2100	+4192 6268 51	-4067 2700 47	+6710 9154 41	-1698 9.91 41	+1339 0392 56	+2447 1172 51	
	2100 - 2600	+4465 9529 51	-2009 4469 47	+2655 2706 46	-5298 6.84 40	+1335 5994 56	+4436 8745 51	
	2600 - 3200	+4432 7107 51	-9757 7450 46	+9834 5740 43	-1542 4.02 40	+1333 0493 56	-5686 5605 51	
	3200 - 3800	+4698 1775 51	-7731 9646 46	+5967 1047 43	-5318 9447 39	+1332 0116 56	-6167 2269 51	
CH <sub>4</sub>	3800 - 4400	+4702 1190 51	-1030 5653 43	+7078 2557 43	-6550 3692 39	+1332 3200 56	-6159 9416 51	
	4400 - 5000	+4683 7437 51	-1461 5449 47	+9345 2300 43	-9239 1945 35	+1333 4036 56	-5958 5943 51	
	5000 - 6000	+4705 6474 51	-1610 6331 47	+9697 5105 39	-9522 1471 36	+1333 1471 56	-6102 7716 51	
	150 - 300	+4041 7634 51	-2256 4400 47	-8630 3440 43	+2562 920 43	+1060 6422 56	-6347 7250 50	
	300 - 500	+3771 6119 51	-1914 0720 47	+1365 0700 44	-5564 2687 42	+1061 2254 56	+9066 3870 50	
	500 - 700	+4137 3746 51	-3826 2485 46	+1000 8230 44	-1134 4742 43	+1060 5115 56	-8222 6700 50	
	700 - 1000	+4950 9077 51	-3992 5555 46	+1469 0695 46	-7032 1539 42	+1057 6295 56	-5511 1720 51	
	1000 - 1300	+6265 1238 51	-3552 4016 46	+9493 8230 43	-3578 7489 42	+1051 0805 56	-1351 2928 52	
	1300 - 1700	+7669 1443 51	-239 0212 46	+5320 7298 43	-1596 8105 42	+1040 0233 56	-2280 0662 52	
	1700 - 2100	+1000 9984 51	-1821 1247 46	+2963 0253 45	-7240 6212 41	+1028 9329 56	-3153 5615 52	
	2100 - 2600	+9999 5267 51	-1151 4294 47	+1522 5193 45	-3042 6540 41	+1015 9947 56	-3919 9002 52	
	2600 - 3000	+1082 7726 52	-7167 4950 47	+7708 7057 44	-1264 4178 41	+1003 5136 56	-4530 1437 52	
	3000 - 3400	+1139 5575 52	-6744 1100 47	+4200 8572 44	-5793 1231 40	+9932 4942 55	-4961 4187 52	
CO	3400 - 4000	+1178 8522 52	-5183 3398 47	+2393 0379 44	-2833 4861 40	+9846 8256 55	-5268 2486 52	
	4000 - 5000	+1205 5418 52	-2229 3658 44	+1456 2454 44	-1510 8845 40	+9779 0778 55	-5881 0165 52	
	5000 - 6000	+1232 4498 52	-1249 1856 47	+7039 3966 43	-6132 8844 39	+9695 2767 35	-3702 5529 52	
	150 - 300	+3501 4842 51	+1087 8922 46	-2132 6547 44	+7176 7187 41	+3308 6242 55	+3809 0776 51	
	300 - 500	+3504 8282 51	+5717 3880 46	-7717 9140 44	+1944 3969 41	+3308 3690 55	+3790 2032 51	
	500 - 700	+4557 2625 51	-2833 5849 46	+1252 0380 43	-3568 1188 41	+3310 1729 55	+4099 1393 51	
	700 - 1000	+3478 1473 51	-5369 0403 47	+9537 7791 43	-5091 6461 41	+3310 1638 55	+4029 9306 51	
	1000 - 1300	+3651 5854 51	-5144 8902 47	+1100 4670 43	-5272 3366 41	+3301 4098 55	+2971 0270 51	
	1300 - 1700	+3860 8374 51	-3546 9347 46	+7406 0246 44	-2247 5935 41	+3285 9734 55	+1582 1786 51	
	1700 - 2100	+3840 9774 51	-3244 4447 46	+3930 0538 44	-9628 6663 40	+3269 0418 55	+3411 6830 50	
	2100 - 2600	+1812 5464 51	-1491 5448 47	+1963 8756 44	-3860 7574 40	+3251 7557 55	-6791 5710 50	
	2600 - 3200	+3646 4008 31	-1019 4119 41	+9428 1210 40	+1001 4612 44	-1599 3818 40	+3235 9292 55	-1463 2026 51
	3200 - 3800	+3436 4008 31	-1419 2221 51	+5453 3767 43	-7027 3322 39	+3222 2132 55	-2039 2716 51	
CO <sub>2</sub>	3800 - 4400	+4419 6250 51	-3153 4215 43	+3308 2674 39	+3210 1502 55	-2466 3384 51		
	4400 - 5000	+4655 6250 51	-3418 0326 46	+2087 5301 43	-1818 9818 39	+3200 9544 55	-2753 9920 51	
	5000 - 6000	+4689 0699 51	-2554 6512 46	+1923 6630 43	-9051 5936 38	+3190 9734 55	-3024 6520 51	
	150 - 300	+3563 7140 51	-4925 8570 47	+4560 0397 46	-6280 3430 43	+5747 4400 51	-5400 7202 51	
	300 - 500	+3816 8846 51	-2963 9146 46	+2490 7914 44	-2567 1204 43	+4925 1570 52	+5954 0791 51	
	500 - 700	+4442 4313 51	-2694 4402 46	+1430 5622 46	-1054 0891 42	+4926 1823 55	+6296 7070 50	
	700 - 1000	+5077 4390 51	-1862 6330 48	+7097 4891 45	-3794 5406 43	+4927 1910 55	-3119 0925 51	
	1000 - 1300	+5616 2514 51	-1466 4518 45	+3992 8769 45	-1616 5220 42	-6690 3300 53	-6421 4910 51	
	1300 - 1700	+6233 4300 51	-7697 8340 47	+1624 9078 45	-1707 1747 45	-1122 1388 54	-1054 0477 52	
	1700 - 2100	+6653 7149 51	-4526 7290 47	+7387 7457 44	-1790 7679 41	-1524 1600 54	-1347 7832 52	
	2100 - 2600	+6946 1749 51	-2588 8846 47	+3782 6632 44	-6523 5648 40	-1891 5354 54	-1559 6591 52	
	2600 - 3200	+7139 6491 51	-1012 4495 47	+8494 4890 43	-1007 5545 40	-2485 6878 54	-1823 3039 52	
COF <sub>2</sub>	3200 - 3800	+7296 9855 51	-1012 4495 47	+8494 4890 43	-1007 5545 40	-2485 6878 54	-1867 0777 52	
	3800 - 4400	+7355 3181 51	-9492 3200 46	+6828 6345 43	-7193 5879 39	-2598 7416 54	-1931 4164 52	
	4400 - 5000	+7412 2505 51	-8253 2950 46	+5117 7600 43	-4618 8168 39	-2726 6119 54	-1931 4164 52	
	5000 - 6000	+7482 8204 51	-4081 2490 46	+2673 6624 39	-2799 4552 39	-1087 2569 54	-2802 5647 52	
	150 - 300	+4131 1379 51	-8226 1920 48	+7478 2778 46	-9970 6473 43	+2401 0874 54	+7645 5412 51	
	300 - 500	+4500 8690 51	+4581 6857 46	+4789 2357 43	+2320 2046 54	+5555 4412 51		
	500 - 700	+5678 2507 51	-4772 8324 48	+2562 2417 44	-1955 9689 43	+2047 8396 54	-1676 0000 50	
	700 - 1000	+6831 6009 51	-2985 4402 46	+1430 5622 46	-1054 0891 42	+1675 3595 54	-1624 2150 51	
	1000 - 1300	+7879 7798 51	-1693 2846 45	+4684 2722 45	-1945 3137 42	+1089 3110 54	-1429 1012 52	
	1300 - 1700	+8678 4190 51	-7908 5084 47	+1673 8397 45	-5273 3118 41	-6047 53 53	-1962 5655 52	
	1700 - 2100	+9108 8118 51	-4627 0084 47	+7630 4546 44	-1928 3389 41	+6145 8280 52	-2261 6387 52	
	2100 - 2600	+9396 9763 51	-2546 8965 46	+3401 2225 46	-5657 7252 40	-7892 8137 53	-2470 5039 52	
	2600 - 3200	+9587 0253 51	-1454 6465 47	+1576 5313 44	-6262 8817 40	-5779 4560 53	-2612 2675 52	
	3200 - 3800	+9704 5646 51	-9199 5550 46	+8210 4640 43	-1147 7945 40	-7497 7630 52	-2701 4363 52	
Cl	3800 - 4400	+9781 4824 51	-5987 9330 46	+4458 2054 46	-8439 1950 39	-9565 4820 53	-2761 5713 52	
	4400 - 5000	+9832 8204 51	-4081 2490 46	+2673 6624 39	-2799 4552 39	-1087 2569 54	-2802 5647 52	
	5000 - 6000	+9883 3737 51	-2174 6468 46	+1235 8455 43	-1028 8883 39	-1244 9725 54	-2844 2947 52	
	150 - 300	+2499 7173 51	-5624 1480 47	+4632 7003 45	+1141 2433 42	+1653 2049 55	+5612 5486 51	
	300 - 500	+2506 4788 51	-5929 6416 47	+5200 7614 45	-6222 5033 42	+1632 9938 55	+5573 8263 51	
	500 - 700	+2656 4730 51	-2859 9690 47	+1686 3535 46	-6122 5100 42	+1629 1113 55	+5735 7792 51	
	700 - 1000	+2743 3927 51	-4672 4505 45	+3294 7080 43	-1111 0739 41	+1625 6851 55	+4193 6441 51	
	1000 - 1300	+2761 6558 51	+9775 6604 46	-2503 7621 44	+824 8597 40	+1625 9067 55	+4191 7613 51	
	1300 - 1700	+2762 2371 51	-7245 6250 46	-1178 8354 44	+2808 4541 40	+1633 5555 55	+4191 7613 51	
	1700 - 2100	+2620 4236 51	+4588 0250 46	-6064 0607 43	+1211 7404 40	+1617 6549 55	+5022 9170 51	
	2100 - 2600	+2587 6175 51	+2858 2904 46	-3064 8118 41	+503 4422 40	+1642 4883 55	+5266 1807 51	
	2600 - 3200	+2565 1467 51	+1900 4820 46	-1679 7858 43	+231 8560 39	+1646 6403 53	+5434 7772 51	
	3200 - 3800	+2549 4787 51	+1200 0393 46	-9597 3450 42	+421 1857 39	+1650 0529 55	+5559 0897 51	
Cl <sub>2</sub>	3800 - 4400	+2539 0046 51	+9115 8820 45	-5941 3944 39	+615 1819 38	+1652 6975 55	+5642 4806 51	
	4400 - 5000	+2528 1946 51	+3179 6460 46	-7130 3870 43	+2735 3050 40	+3467 1976 54	+1942 1692 50	
	5000 - 6000	+2506 7680 51	+1734 0760 47	-2492 1302 40	+668 4165 40	+3199 1353 54	-9806 3395 50	
	150 - 300	+3448 0294 51	-1638 5656 48	+2692 6483 46	-478 5249 43	+3934 6532 54	+6890 4000 51	
	300 - 500	+3535 3409 51	-1132 5256 48	+1031 7245 46	-119 1520 43	+3873 9265 54	+4963 9378 51	
	500 - 700	+3579 0533 51	-1771 5547 46	+4259 4980 45	-351 7128 42	+3815 0122 54	+3572 8781 51	
	700 - 1000	+3649 2029 51	-3765 4088 47	+4145 0640 45	-873 1259 41	+3752 5719 54	+2509 1450 51	
	1000 - 1300	+3688 1534 51	-1874 1948 47	+5195 4893 44	-215 2894 41	+3696 4574 54	+1760 9050 51	
	1300 - 1700	+3678 1904 51	-7895 4060 46	+1610 2315 44	-1523 1719 40	+3628		

TABLE I. - Continued. COEFFICIENTS FOR OBTAINING THERMODYNAMIC DATA FOR SEVERAL SUBSTANCES

[Coefficients for use in equations (105) to (107).]

Substance (a)	Temperature Interval, °K	Coefficients					
		A	B	C	D	E	F
ClF <sub>3</sub>	150 - 300	+5127 0429 51	-1749 4520 49	+1761 6464 47	-2976 1208 44	+2856 0159 55	+4659 5420 51
	300 - 500	+6457 5624 51	-5893 7083 48	+5115 6181 46	-5909 3643 43	+2828 1043 55	+2930 9810 51
	500 - 700	+7730 3861 51	-3819 8758 48	+2115 3958 46	-1756 7111 43	+2798 6643 55	+9857 9920 51
	700 - 1000	+8622 9749 51	-1802 3217 48	+7167 0960 45	+4305 6373 42	+2767 0675 55	+1520 7148 52
	1000 - 1300	+9203 6441 51	-8107 5540 47	+2291 6450 45	-1002 4218 42	+2739 3569 55	+1887 3181 52
	1300 - 1700	+9616 4442 51	-2539 0922 47	+5440 6701 44	-1755 2752 41	+2707 5754 55	+2168 5910 52
	1700 - 2100	+9764 0535 51	-1278 0686 47	+2126 0319 44	+5422 3408 40	+2693 2176 55	+2271 7800 52
	2100 - 2600	+9847 6403 51	-6517 8960 46	+8787 1110 43	+1805 4192 40	+2682 7742 55	+2332 5352 52
	2600 - 3200	+9897 9694 51	-3586 5496 46	+3936 3035 43	+6597 0677 39	+2675 1109 55	+2370 0484 52
	3200 - 3800	+9927 8564 51	-2207 8365 46	+2001 7247 43	+2809 9884 39	+2669 6912 55	+2392 8132 52
F	3800 - 4400	+9946 9377 51	-1412 0292 46	+1092 2948 43	-1315 6062 39	+2665 5387 55	+2407 7328 52
	4400 - 5000	+9959 2224 51	-9559 0740 45	+6462 9910 42	-6817 9250 38	+2662 4430 55	+2417 5282 52
	5000 - 6000	+9971 6836 51	-4900 9530 45	+2907 6060 42	-2567 3024 38	+2658 5622 55	+2427 7976 52
	300 - 500	+2774 1677 51	+1569 7918 47	-1219 8418 45	+8817 6073 41	+2448 1175 55	+3274 3817 51
	500 - 700	+2741 1306 51	+2447 1894 47	-1290 5400 45	+9364 9496 41	+2448 8816 55	+3442 3810 51
P <sub>2</sub>	700 - 1000	+2668 2300 51	+1435 7079 47	+5466 0762 44	+2926 9741 41	+2451 8215 55	+3882 1075 51
	1000 - 1300	+2606 1647 51	+7594 5950 46	+2066 6151 44	+8244 1470 40	+2455 3341 55	+4278 5777 51
	1300 - 1700	+2568 8565 51	+3901 3852 46	+8171 2274 43	+2516 1409 45	+2458 2444 55	+4530 4593 51
	1700 - 2100	+2543 7180 51	+1989 4083 46	+3203 1108 43	+7669 7618 39	+2460 7969 55	+4706 8085 51
	2100 - 2600	+2530 2137 51	+1158 2342 46	+1516 1332 43	+2979 4828 39	+2462 5383 55	+4804 8492 51
	2600 - 3200	+2520 8123 51	+6763 1070 45	+7187 4217 42	+1160 3995 39	+2464 0181 55	+4875 0108 51
	3200 - 3800	+2514 3282 51	+3904 6228 45	+3373 8858 42	+4456 9788 38	+2465 2647 55	+4924 7717 51
	3800 - 4400	+2510 0138 51	+2262 4946 45	+1637 1748 42	+1810 1580 38	+2466 2929 55	+4958 8764 51
	4400 - 5000	+2507 8249 51	+1625 4622 45	+1023 3196 42	+1001 0333 38	+2466 8878 55	+4976 3975 51
	5000 - 6000	+2529 8070 46	+2658 8548 43	+1685 9673 39	+2978 4168 55	+3341 3410 51	
H	150 - 300	+3474 8807 51	-2479 3670 47	+2808 0384 45	+4516 8609 42	+3067 9524 55	+4488 2780 51
	300 - 500	+3499 3010 51	-1230 4361 48	+1038 5229 46	-1091 0390 43	+3067 9438 55	+4441 2399 51
	500 - 700	+3781 3514 51	-1031 1322 48	+5565 7851 45	+4317 1200 42	+3061 1457 55	+4916 9669 51
	700 - 1000	+4041 7357 51	+5868 2000 47	+2277 7137 45	+1285 7726 42	+3051 4311 55	+1359 1435 51
	1000 - 1300	+4247 3596 51	-3180 6992 47	+8736 8100 45	+3561 1383 41	+3040 9909 55	+6212 3900 49
	1300 - 1700	+4395 0680 51	+1548 4066 47	+3196 9833 42	+9363 6692 40	+3029 8390 55	+9330 9680 50
	1700 - 2100	+4473 0713 51	-1083 0146 47	+1705 8185 45	+3801 9221 40	+3022 6281 55	+1468 3319 51
	2100 - 2600	+4530 1221 51	+8004 6210 46	+1001 6324 46	+1705 3955 40	+3015 9621 55	+1873 5356 51
	2600 - 3200	+4577 2369 51	+6669 1418 46	+6657 6164 43	+8791 4462 39	+3009 4373 55	+2213 6134 51
	3200 - 3800	+4617 9447 51	+6168 3545 46	+4992 5151 43	+5319 2178 39	+3002 9324 55	+2510 8582 51
H <sub>2</sub>	3800 - 4400	+4656 6023 51	+5845 5975 46	+3970 3472 43	+3521 4000 39	+2995 9930 55	+2784 3785 51
	4400 - 5000	+4686 8046 51	+5734 8144 46	+3364 9472 43	+2580 7455 39	+2989 1276 55	+3027 5170 51
	5000 - 6000	+4726 7301 51	+5239 8070 46	+2658 8548 43	+1685 9673 39	+2978 4168 55	+3341 3410 51
	150 - 300	+2500 3116 51	+4852 8250 45	+6211 4920 43	+1415 8863 41	+4294 5264 55	+4609 6828 50
	300 - 500	+2499 6710 51	+2385 2015 45	+2047 2396 43	+2955 4273 40	+4294 5386 55	+4573 1922 50
HCl	500 - 700	+2499 0717 51	+3432 3430 45	+1896 0083 43	+1754 6524 40	+4294 5892 55	+4533 8129 50
	700 - 1000	+2499 5645 51	+1261 8040 45	+4772 2317 42	+3092 1566 39	+4294 5582 55	+4561 8786 50
	1000 - 1300	+2498 9933 51	+2095 0920 45	+6015 1655 42	+2948 5802 39	+4294 6101 55	+4522 0179 50
	1300 - 1700	+2499 5803 51	+1102 0773 44	+6488 9065 40	+4834 1707 36	+4294 5389 55	+4589 9392 50
	1700 - 2100	+2499 2764 51	+1021 2900 45	+1742 6965 42	+5235 9488 38	+4294 6258 55	+4537 6904 50
	2100 - 2600	+2499 9862 51	+4814 9770 43	+2852 3330 39	+7596 2533 36	+4294 5410 55	+4590 4575 50
	2600 - 3200	+2500 3308 51	+1682 7689 44	+2310 5728 41	+4594 2012 37	+4294 4715 55	+4617 5197 50
	3200 - 3800	+2500 2231 51	+6871 4240 43	+8940 1590 40	+1468 3878 37	+4294 4842 55	+4609 4814 50
	3800 - 4400	+2499 6156 51	+2770 3100 44	+2094 2038 41	+2893 9034 37	+4294 6455 55	+4559 8696 50
	4400 - 5000	+2498 9665 51	+5593 0800 44	+3785 6331 41	+4517 9884 37	+4294 8763 55	+4504 7409 50
HF	150 - 300	+2989 2484 51	+4103 4770 48	+4407 7218 46	+8356 1287 43	+3401 1138 55	+1324 4021 51
	300 - 500	+3383 2407 51	+4324 5254 47	+3912 7278 45	+5061 2747 42	+3393 0261 55	+3572 0562 51
	500 - 700	+3459 0074 51	+1656 0656 47	+9153 4690 44	+7399 4236 41	+3391 6394 55	+3981 7170 51
	700 - 1000	+3480 7949 51	+8057 9160 46	+2316 5882 45	+2880 5124 38	+3391 4081 55	+4101 0320 51
	1000 - 1300	+3497 5983 51	+1102 0773 44	+6488 9065 40	+4834 1707 36	+4294 5389 55	+4589 9392 50
	1300 - 1700	+3498 2764 51	+1021 2900 45	+1742 6965 42	+5235 9488 38	+4294 6258 55	+4537 6904 50
	1700 - 2100	+3554 3280 51	+2214 0298 47	+2252 3788 47	+3163 7688 40	+4337 4923 55	+7304 4520 51
	2100 - 2600	+3550 3308 51	+2473 1652 47	+2122 3369 44	+2701 7443 40	+3392 1516 55	+7227 5210 51
	2600 - 3200	+3550 2231 51	+1542 7069 47	+1065 7981 40	+1000 6309 39	+3278 8324 55	+9597 2790 51
	3200 - 3800	+3516 8247 51	+1611 9098 47	+9808 8242 43	+8461 6973 39	+3267 4437 55	+1005 6383 52
H <sub>2</sub> O	3800 - 4400	+4316 5332 51	+4983 7368 46	+2766 7672 43	+1976 9074 39	+6599 3656 38	+3168 4849 55
	4400 - 5000	+4613 8860 51	+6368 8580 46	+2766 2305 43	+6509 3656 38	+3168 4849 55	+1251 6853 52
	5000 - 6000	+3507 7834 51	+3434 8560 46	+3783 9075 45	+7488 3407 41	+7840 0952 54	+2478 6303 51
	150 - 300	+3496 6325 51	+8772 1500 45	+1483 8166 44	+5505 0572 41	+7844 5758 54	+2549 0010 51
	300 - 500	+3455 5431 51	+2524 1094 47	+8256 9265 45	+2240 1276 41	+7868 1516 54	+2838 6335 51
	500 - 700	+3497 7739 51	+4336 2524 47	+1120 6186 45	+3799 5512 41	+7857 2051 54	+2632 6456 51
	700 - 1000	+3637 7472 51	+4092 2196 47	+8387 1455 45	+2412 5676 41	+7762 0326 54	+1733 9321 51
	1000 - 1300	+3756 5869 51	+3262 2034 47	+5240 1857 44	+1237 0559 45	+7587 5851 54	+4355 1680 50
	1300 - 1700	+3748 9902 51	+3159 4679 47	+6167 8857 44	+1505 2076 41	+3394 2702 55	+3995 7133 51
	1700 - 2100	+3584 4555 51	+3452 5690 47	+5352 7626 44	+1178 9801 41	+3386 2783 55	+4672 5704 51
H <sub>2</sub> O	2100 - 2600	+3759 4391 51	+2880 8338 47	+3644 3990 44	+6459 7047 40	+3365 5684 55	+5907 5856 51
	2600 - 3200	+3950 4861 51	+2214 0298 47	+2252 3788 47	+3163 7688 40	+3337 4923 55	+7304 4520 51
	3200 - 3800	+4015 1762 51	+2473 1652 47	+2122 3369 44	+2701 7443 40	+3392 1516 55	+7227 5210 51
	3800 - 4400	+4259 9189 51	+1542 7069 47	+1065 7981 40	+1000 6309 39	+3278 8324 55	+9597 2790 51
	4400 - 5000	+4316 8247 51	+1611 9098 47	+9808 8242 43	+8461 6973 39	+3267 4437 55	+1005 6383 52
H <sub>2</sub> O	5000 - 6000	+4402 7997 51	+4449 8300 46	+3783 6208 45	+1184 3407 41	+7488 3407 41	+1658 1832 50
	300 - 500	+3984 3281 51	+1560 3100 47	+8521 9880 46	+9334 5693 41	+5702 9188 54	+2361 4200 48
	500 - 700	+3995 7858 51	+5866 2548 47	+2777 9813 45	+1277 3920 42	+5705 5261 54	+7248 4000 48
	700 - 1000	+4103 2581 51	+7272 2748 47	+2513 6379 45	+932 8919 41	+5673 7398 54	+5886 8940 50
	1000 - 1300	+4273 7895 51	+9457 9644 47	+2418 4150 45	+7900 2882 41	+5608 4188 54	+1548 2509 51
	1300 - 1700	+4561 3587 51	+9361 2130 47	+1893 3559 45	+5227 3842 41	+5420 0843 54	+3374 7881 51
	1700 - 2100	+4985 3551 51	+8042 8280 47	+1277 9848 45	+2926 8695 41	+5036 1704 54	+6240 3270 51
	2100 - 2600	+5419 7867 51	+5975 1330 47	+7745 7137 44	+1467 6260 41	+4512 4857 54	+9338 7540 51
	2600 - 3200						

TABLE I. - Concluded. COEFFICIENTS FOR OBTAINING THERMOCHEMICAL DATA FOR SEVERAL SUBSTANCES

[Coefficients for use in equations (15) to (107).]

Substance (a)	Temperature Interval, °K	Coefficients					
		A	B	C	D	E	F
N	300 - 500	+2499 6710 51	-2385 2015 45	+2047 2396 43	-2955 4273 40	+5707 9313 55	+4183 1808 51
	500 - 700	+2499 1148 51	-3267 4440 45	+1798 0743 43	-1659 2209 40	+5707 9603 55	+4186 8511 51
	700 - 1000	+2499 6036 51	-1131 0429 45	+4232 2090 42	-2736 5544 39	+5707 9478 55	+4183 9375 51
	1000 - 1300	+2499 0940 51	-1901 1726 45	+5442 2129 42	-2666 8173 39	+5707 9952 55	+4187 5999 51
	1300 - 1700	+2500 2204 51	+3451 2550 44	-9655 6710 41	+4200 6645 38	+5707 9078 55	+4179 7565 51
	1700 - 2100	+2501 6390 51	+2522 5800 45	-4789 7317 42	+1627 5565 39	+5707 7262 55	+4169 0522 51
	2100 - 2600	+2508 6192 51	+1107 6049 46	-1756 3073 43	+5016 8252 39	+5706 6696 55	+4115 3955 51
	2600 - 3200	+2517 3414 51	+2174 0230 46	-1034 2712 43	+7858 2646 39	+5705 0383 55	+4045 6309 51
	3200 - 3800	+2512 6194 51	+1967 0040 46	-2871 0071 43	+7694 4866 39	+5706 2395 55	+4063 2194 51
	3800 - 4400	+2482 1655 51	-6399 2200 45	-8909 3904 42	+4843 1658 39	+5715 2935 55	+4343 0639 51
	4400 - 5000	+2434 1623 51	-5054 2730 46	+1913 3373 43	+1308 3373 39	+5732 4433 55	+4765 1025 51
	5000 - 6000	+2351 2887 51	-1171 7309 47	+5608 4591 43	-2764 8502 39	+5766 8718 55	+5513 9770 51
N <sub>2</sub>	150 - 300	+3501 6234 51	+1419 9930 46	-2221 4814 44	+6337 0257 41	+5739 5697 53	+3078 0353 51
	300 - 500	+3507 3207 51	+6478 8790 46	-7700 5600 44	+1686 9531 42	+5827 6963 52	+3045 5391 51
	500 - 700	+3468 1570 51	-1742 8035 47	+6732 6921 44	+6988 8312 40	+8673 6314 52	+3295 4226 51
	700 - 1000	+3462 1286 51	+24539 6402 47	+1622 1534 42	+4933 2511 41	+8776 6703 52	+3385 9335 51
	1000 - 1300	+3600 4480 51	+24986 5174 47	+3221 7619 45	+4933 4174 41	+8094 8196 53	+2555 2204 51
	1300 - 1700	+3793 9348 51	-1715 9601 47	+7751 5395 46	+2578 2167 41	+6865 5239 53	+1278 3599 51
	1700 - 2100	+3979 4425 51	-2618 0593 47	+4257 4284 46	+1039 0909 41	+4949 4356 53	+3226 6000 48
	2100 - 2600	+4142 6524 51	-1649 2670 47	+2167 6242 44	+4284 4626 40	+3093 6592 53	+1092 8453 51
	2600 - 3200	+4249 0571 51	-1349 9359 47	+1106 6286 46	+1770 7380 40	+1332 3675 53	+1962 7879 51
	3200 - 3800	+4327 1936 51	-7332 7190 46	+6383 0855 43	+8465 0756 39	+4394 6700 51	+2551 1939 51
	3800 - 4400	+4382 7162 51	-5322 6420 46	+3896 3172 43	+4232 2187 39	-1248 3259 53	+2990 7052 51
	4400 - 5000	+4426 8870 51	-3934 9468 46	+2455 1316 43	+2274 3750 39	-2321 5622 53	+3332 6930 51
	5000 - 6000	+4882 3937 51	+1235 5686 47	-7763 4410 43	+8482 4648 39	-1669 0365 54	+6686 7119 51
NH <sub>3</sub>	150 - 300	+3501 4877 51	-1135 4880 46	+3492 4950 43	+1605 9661 41	+5707 5674 55	+1837 3594 51
	300 - 500	+3506 9044 51	+1658 8050 46	+1893 7787 44	+3971 7660 41	+5707 4332 55	+1806 0451 51
	500 - 700	+3507 6770 51	+2796 6700 46	-3019 6472 44	+5706 5528 41	+5707 4505 55	+1802 3397 51
	700 - 1000	+3467 4923 51	-1587 8517 47	+4682 2623 44	-3133 4757 40	+5709 6465 55	+2076 5108 51
	1000 - 1300	+3476 0496 51	-3595 9897 47	+8992 4746 44	-2700 9943 41	+5710 4331 55	+2082 2903 51
	1300 - 1700	+3578 3151 51	-3917 3724 47	+7834 3879 44	-2085 4695 41	+5703 9404 55	+1443 5951 51
	1700 - 2100	+3753 2238 51	-3437 2875 47	+5329 0472 44	-1133 8710 41	+5688 4282 55	+2671 2430 50
	2100 - 2600	+3924 7695 51	-2774 1647 47	+3440 1817 44	+5700 1390 40	+5668 6761 55	+9419 7230 50
	2600 - 3200	+4082 2543 51	-2416 9060 47	+2402 2699 44	+3132 6809 40	+5647 1309 55	+2072 8080 51
	3200 - 3800	+4226 3537 51	-2291 3941 47	+1856 8495 44	+1990 5685 40	+5624 2276 55	+3121 4787 51
	3800 - 4400	+5768 5140 52	-6242 7160 49	+5044 9155 46	+7082 5339 42	+3413 8686 56	+8395 4054 53
	4400 - 5000	+1813 5084 53	-8906 1750 49	+6213 1583 46	+7379 7011 42	+6834 6534 56	+1553 9865 54
	5000 - 6000	+2323 8668 52	-1115 6880 49	+6734 9310 45	+6814 6304 41	+1606 8773 56	+2311 5519 53
NH <sub>3</sub>	150 - 300	+0016 0739 51	-5921 7280 47	+2172 9700 45	+8870 2067 42	+4660 2050 55	+2676 3530 50
	300 - 500	+3929 2082 51	-1358 1227 48	+1045 1508 46	+6997 1157 42	+4662 0202 55	+7631 5510 50
	500 - 700	+2742 7432 51	-2082 9945 48	+1039 4443 46	+6171 7799 42	+4656 2775 55	+6133 4010 50
	700 - 1000	+4643 7799 51	-2103 0382 48	+7635 1643 45	+3465 0380 42	+4641 3606 55	+3108 4650 51
	1000 - 1300	+5267 2607 51	-2084 8879 47	+5491 9755 44	+1988 4803 42	+4612 0057 55	+6662 3930 51
	1300 - 1700	+6020 3398 51	-1698 3392 48	+3497 6990 45	+1020 9245 42	+4558 7608 55	+1178 4321 52
	1700 - 2100	+6822 7393 51	-1316 2876 47	+4216 6664 45	+5097 7779 41	+4484 9963 55	+1725 3776 52
	2100 - 2600	+7558 4148 51	-8904 3840 47	+1171 7555 45	+2312 0365 41	+4395 8496 55	+2253 4893 52
	2600 - 3200	+8185 0643 51	-5794 8770 47	+6205 9477 46	+1099 0955 41	+4301 8145 55	+2717 1443 52
	3200 - 3800	+8640 1560 51	-3931 9340 47	+3470 3306 46	+4747 1369 40	+4219 6290 55	+5062 3326 52
	3800 - 4400	+8964 9398 51	-2692 3282 47	+2017 9453 46	+2711 7716 40	+4149 2986 55	+5314 0852 52
	4400 - 5000	+9187 2759 51	-1912 4119 47	+1245 5081 44	+1282 4365 40	+4609 3525 55	+3429 7616 52
	5000 - 6000	+9414 7085 51	-1099 4602 47	+6180 2898 43	+6046 0492 39	+4021 6185 55	+3679 8456 52
NO	300 - 500	+3629 9214 51	+2657 5880 47	-2717 2093 45	+4670 8630 42	+1177 3583 55	+4650 8256 51
	500 - 700	+3526 2159 51	-3237 2407 47	+1496 6665 45	+5017 5322 41	+1180 6009 55	+5281 0742 51
	700 - 1000	+3761 2043 51	+5723 3784 47	+2111 8083 45	+1023 0275 42	+1179 4145 55	+5064 8751 51
	1000 - 1300	+3769 9172 51	-6894 8460 47	+1322 3357 44	+5147 2119 41	+1169 0270 55	+3897 0127 51
	1300 - 1700	+3976 2131 51	-3140 6382 47	+6572 2561 44	+2009 1463 41	+1153 6702 55	+2461 7464 51
	1700 - 2100	+4137 1746 51	-2076 7231 47	+3380 3593 44	+8273 2029 40	+1138 5290 55	+1351 2723 51
	2100 - 2600	+4255 7731 51	-1265 1294 47	+1656 3960 44	+3228 0166 40	+1123 5766 55	+4673 8600 50
	2600 - 3200	+4344 0587 51	-8120 9610 46	+8518 4400 43	+1311 7501 40	+1110 2937 55	+1928 0800 50
	3200 - 3800	+4413 5660 51	-5677 9250 46	+4786 5005 43	+5809 5741 39	+1098 7485 55	+6803 6460 50
	3800 - 4400	+4455 4771 51	-4305 6534 46	+2995 3452 43	+8283 0271 39	+1088 9003 55	+1035 1524 51
	4400 - 5000	+4489 7869 51	-3762 9946 46	+2235 0024 43	+1791 0895 39	+1081 6691 55	+1270 7127 51
	5000 - 6000	+4509 2548 51	-3723 3052 46	+1802 9307 43	+1226 2702 39	+1072 4569 55	+1546 9048 51
O	150 - 300	+2832 8173 51	+1431 7687 48	-1468 4834 46	+2566 9894 43	+3017 4976 55	+3217 0845 51
	300 - 500	+2718 6413 51	+3870 4329 47	-3379 2646 45	+3969 6103 42	+3019 9635 55	+3891 1039 51
	500 - 700	+2629 9259 51	+2286 8597 47	-1271 4552 42	+1065 1442 42	+3021 9345 55	+4354 2996 51
	700 - 1000	+2576 2890 51	+1028 8519 47	-4106 0040 44	+2484 6390 41	+3023 8309 55	+4676 2053 51
	1000 - 1300	+2547 0979 51	+5221 5330 46	-1496 6858 44	+6739 3053 40	+3025 1125 55	+4858 4101 51
	1300 - 1700	+2519 3465 51	+1151 2610 46	-2514 3283 43	+8031 2904 39	+3027 2774 55	+5048 5617 51
	1700 - 2100	+2514 1793 51	+9680 0900 45	-1678 4195 43	+4800 0132 39	+3027 7264 55	+5083 3051 51
	2100 - 2600	+2508 6997 51	+6151 5400 45	-9959 5160 43	+2961 9744 39	+3028 4518 55	+5123 9201 51
	2600 - 3200	+2508 8516 51	+6191 4220 45	-1014 7413 43	+3113 4905 39	+3028 8330 55	+5137 3787 51
	3200 - 3800	+2496 0645 51	-4318 7665 46	+1785 1200 41	+1353 7926 39	+3031 3904 55	+5222 2555 51
	3800 - 4400	+2484 1660 51	-1828 7300 46	+9952 7176 42	+1281 2973 39	+3035 1914 55	+5331 3668 51
	4400 - 5000	+2461 6602 51	-3966 3519 46	+2327 9192 43	+1788 5282 39	+3043 5044 55	+5332 3795 51
O <sub>2</sub>	150 - 300	+3507 8622 51	+5736 8300 46	-1566 0917 47	+3507 9823 42	+1022 7365 54	+6768 3884 51
	300 - 500	+3468 1122 51	-2094 4310 47	+1311 3020 42	+6112 4133 41	+1031 5694 54	+6905 2651 51
	500 - 700	+3491 8904 51	-6759 0190 47	+3398 6627 44	+8078 8706 42	+1030 0629 54	+6853 9311 51
	700 - 1000	+3655 2327 51	-6543 3148 47	+2462 0346 42	+1270 0679 42	+6864 3794 53	+5884 3554 51
	1000 - 1300	+3504 0901 51	-4442 4074 47	+1199 2093 42	+6611 9082 41	+6845 0760 53	+3119 0523 51
	1300 - 1700	+4108 9900 51	-2517 0318 47	+5093 9020 42	+1049 3115 41	+6835 7753 53	+917 6760 50
	1700 - 2100	+4222 7020 51	-1953 0831 47	+2975 1070 42	+5972 9259 40	+4789 9642 53	+3765 2250 50
	2100 - 2600	+4302 7917 51	-1791 1603 47	+2194 9064 42	+3693 6626 40	+4957 1490 53	+8280 3550 51
	2600 - 3200	+4378 2138 51	-1859 5901 47	+1888 4518 42	+2642 8824 40	+4957 0489 53	+8280 3550 51
	3200 - 3800	+4481 6232 51	-1804 0341 47	+1535 7064 42	+1904 1376 40	+4295 5642 53	+1649 5016 51
	3800 - 4400	+4595 4599 51	-1604 0929 47	+1175 2869 44	+1306 8516 40	+4835 3000 51	+1514 2771 51
	4400 - 5000	+4700 9554 51	-1392 3351 47	+90			

TABLE II. - INPUT TO VECTOR  
AND PROPELLANT DECK\*

E-417

Product code	Card column		
	44-47	48-50	51-60
0037	BOP		
0054	ATM	H	
0061	ATM	N	
0450	MOL	O	
0451	MOL	H2	
0650	MOL	H2O1	
0651	MOL	N2	
0750	MOL	N1O1	
0751	MOL	O2	
	F1	O1H1	
		N2H4	
EF1		1547029756	
PF1		1000000053	
X1		H2O2	
EX1		2868162655	
PX1		1000000053	

\*The symbol  $\overline{O}$  is used to indicate the alphabetic letter; the symbol O is used for zero.

TABLE III. - OUTPUT OF VECTOR AND PROPELLANT DECK

Type of card	Product code	Packed vector	Product code	
	Card column			
	17-20	31-40	44-47	48-50
Packed vectors	0037	0000000001	0037	ATM
	0054	0000000011	0054	ATM
	0061	0000000021	0061	ATM
	0450	0000000002	0450	MOL
	0451	00000000221	0451	MOL
	0650	0000000012	0650	MOL
	0651	0000001121	0651	MOL
	0750	0000000022	0750	MOL
	0751	0000002101	0751	MOL
				H N O H2 H2O1 N2 N1O1 O2 O1H1
Cards for listing only to check input				F1 EF1 PFI X1 EX1 PX1 N2H4 1547029756 1000000053 H2O2 2868162655 1000000053

Type of card	Drum loca- tion	Contents	Drum loca- tion	Contents	Drum loca- tion	Contents
	Card column					
	1-4	5-15	16-19	20-30	31-34	35-45
$a_f$ (hydrogen) $b_f$ (nitrogen)	0587	1248127850+	0588	6240639049+		
Fuel enthalpy, $h_f$ Fuel valence, $v_f^+$	0597	4827226954+	0598	1248127850+		
$a_x$ (hydrogen) $c_x$ (oxygen)	0537	5879586049+	0539	5879586049+		
Oxidant enthalpy, $h_x$ Oxidant valence, $v_x^+$ Oxidant valence, $v_x^-$	0547	8431804353+	0548	5879586049+	0549	1175917250-

TABLE IV. - INPUT TO MAIN OPERATING DECIDE

TABLE V. - OUTPUT OF MAIN OPERATING IECK

9005	6	EQUIV RATO R +8571 4286 50	O/F +1592 1118 51	PRCNT FUEL +3857 8583 52	PC PSIA +6000 0000 53	ENTH CAL/ GM +2380 1691 54	IDENT FICA TN +0857 0208 63		1
9005	6	A SUB F +1248 1278 50	B SUB F +6240 6390 49	C SUB F	D SUB F	E SUB F	+0857 0208 63		2
9005	b	F SUB F	G SUB F	H SUB F	I SUB F	J SUB F	+0857 0208 63		3
9005	6	FUEL ENTH HF +4827 2269 54	FUEL +VAL VF <sup>+</sup> +1248 1278 50	FUEL -VAL VF <sup>-</sup>			+0857 0208 63		4
9005	6	A SUB X +5879 5860 49	B SUB X	C SUB X +5879 5860 49	D SUB X	E SUB X	+0857 0208 63		5
9005	6	F SUB X	G SUB X	H SUB X	I SUB X	J SUB X	+0857 0208 63		6
9005	6	OXID ENTH HX +8431 8043 53	OXID +VAL VX <sup>+</sup> +5879 5860 49	OXID -VAL VX <sup>-</sup> -1175 9172 50			+0857 0208 63		7
IDENT FICA TN									
CARD NO.									
PRESS RATO MOLEC WT CP CAL/ GM PI SUB I	TEMP K THRST COEF CF GAMMA PI SUB T	PRESS ATM AREA RATO DLNM/ DLNP T PI SUB EP	ENTH CAL/ GM MACH NO. DLNM/ DLNT P PISUB CSTR	SPEC IMP I VAC ENTRO PY C STAR	RRRR CASE PC				
CODE 0 37	H	CODE 0 54	N						1
CODE 0 61	O	CODE 4 50	H2						2
CODE 4 51	H2O	CODE 6 50	N2						3
CODE 6 51	NO	CODE 7 50	O2						4
CODE 7 51	OH								5
9005	6	+1000 0000 51	+2E20 0975 54	+4082 7418 52	+2380 1693 54		+0857 0208 63	1	7 0001
9005	6	+1832 4978 52					+0857 0208 63	1	0 0002
9005	6	+8600 2537 50	+1170 6861 51	+3918 7000 48	-9967 4585 49	+3202 5166 51	+0857 0208 63	1	0 0003
9005	6		+1130 7117 49				+0857 0208 63	1	0 0004
9005	6	+0000 0000 37	+1884 9336 50	+0000 0000 54	+1198 2934 46		+0857 0208 63	1	0 0005
9005	6	+0000 0000 61	+7941 1497 48	+0000 0004 50	+4652 5476 51		+0857 0208 63	1	0 0006
9005	6	+0000 0004 51	+2661 5805 52	+0000 0006 50	+8986 4247 51		+0857 0208 63	1	0 0007
9005	6	+0000 0006 51	+3950 4512 49	+0000 0007 50	+1860 7803 49		+0857 0208 63	1	0 0008
9005	6	+0000 0007 51	+3180 8095 50				+0857 0208 63	1	0 0009
*									
9005	6	+1763 0118 51	+2599 0325 54	+2315 7770 52	+2213 8880 54	+1202 8578 53	+0857 0208 63	2	7 0001
9005	6	+1839 4694 52	+6718 3421 50	+1000 0000 51	+9999 9900 50	+2218 3977 53	+0857 0208 63	2	0 0002
9005	6	+7500 1172 50	+1184 4539 51	+1866 4000 48	+6000 4567 49	+3202 5172 51	+0857 0208 63	2	0 0003
9005	6	+3211 9738 48	+6C78 4200 48		+1279 7000 48	+5760 4609 54	+0857 0208 63	2	0 0004
9005	6	+0000 0000 37	+6129 6978 49	+0000 0000 54	+1574 5346 45		+0857 0208 63	2	0 0005
9005	6	+0000 0000 61	+1289 9700 48	+0000 0004 50	+2592 6825 51		+0857 0208 63	2	0 0006
9005	6	+0000 0004 51	+1528 1160 52	+0000 0006 50	+5123 4150 51		+0857 0208 63	2	0 0007
9005	6	+0000 0006 51	+8852 1215 48	+0000 0007 50	+3154 4989 48		+0857 0208 63	2	0 0008
9005	6	+0000 0007 51	+8591 8027 49				+0857 0208 63	2	0 0009
*									
9005	6	+2041 3710 52	+1703 3560 54	+2000 0000 51	+1650 2977 54	+2520 0886 53	+0857 0208 63	3	7 0001
9005	6	+1846 0004 52	+1407 5494 51	+3609 2728 51	+2542 3479 51	+2836 6442 53	+0857 0208 63	3	0 0002
9005	6	+5727 2366 50	+1231 6744 51	+1190 0000 46	+4021 9322 47	+3202 5170 51	+0857 0208 63	3	0 0003
9005	6	+9255 6857 47	+1309 3700 48	-3527 1000 48		+5760 4609 54	+0857 0208 63	3	0 0004
9005	6	+0000 0000 37	+7135 4999 46	+0000 0000 54	+3884 2841 39		+0857 0208 63	3	0 0005
9005	6	+0000 0000 61	+5726 6914 42	+0000 0004 50	+2221 9334 50		+0857 0208 63	3	0 0006
9005	6	+0000 0004 51	+1333 2781 51	+0000 0006 50	+4444 3360 50		+0857 0208 63	3	0 0007
9005	6	+0000 0006 51	+6396 0183 44	+0000 0007 50	+1556 5795 43		+0857 0208 63	3	0 0008
9005	6	+0000 0007 51	+2297 8421 46				+0857 0208 63	3	0 0009
*									
9005	6	+4082 7420 52	+1491 6308 54	+1000 0000 51	+1531 2268 54	+2717 8889 53	+0857 0208 63	4	7 0001
9005	6	+1846 0388 52	+1518 0271 51	+5861 1205 51	+2917 3866 51	+2974 9172 53	+0857 0208 63	4	0 0002
9005	6	+5517 8364 50	+1242 4039 51	+1500 0000 45	-6049 8219 51	+3202 5166 51	+0857 0208 63	4	0 0003
9005	6	+6988 0686 47	+1429 7700 48	-3409 9000 48		+5760 4609 54	+0857 0208 63	4	0 0004
9005	6	+0000 0000 37	+5278 4766 45	+0000 0000 54	+2759 3682 37		+0857 0208 63	4	0 0005
9005	6	+0000 0000 61	+3627 2626 40	+0000 0004 50	+1111 0859 50		+0857 0208 63	4	0 0006
9005	6	+0000 0004 51	+6666 6369 50	+0000 0006 50	+2222 2154 50		+0857 0208 63	4	0 0007
9005	6	+0000 0006 51	+1479 0822 43	+0000 0007 50	+1023 7844 41		+0857 0208 63	4	0 0008
9005	6	+0000 0007 51	+9075 8745 44				+0857 0208 63	4	0 0009
*									
9005	6	+6804 5699 52	+1348 1969 54	+6000 0001 50	+1453 1962 54	+2840 0511 53	+0857 0208 63	5	7 0001
9005	6	+1846 0433 52	+1586 2586 51	+8449 4012 51	+3195 2580 51	+3062 3705 53	+0857 0208 63	5	0 0002
9005	6	+5381 3067 50	+1251 2292 51	+3000 0004 46	-1082 3945 46	+3202 5168 51	+0857 0208 63	5	0 0003
9005	6	+5786 3330 47	+1481 9800 46	-3340 6000 48		+5760 4609 54	+0857 0208 63	5	0 0004
9005	6	+0000 0000 37	+5962 6786 44	+0000 0000 54	+2889 5353 35		+0857 0208 63	5	0 0005
9005	6	+0000 0007 51	+4003 4378 35	+0000 0004 50	+6666 6369 49		+0857 0208 63	5	0 0006
9005	6	+0000 0004 51	+3299 9971 50	+0000 0006 50	+1333 3227 50		+0857 0208 63	5	0 0007
9005	6	+0000 0006 51	+6167 0896 41	+0000 0007 50	+1403 8250 39		+0857 0208 63	5	0 0008
9005	6	+0000 0007 51	+5969 0563 43				+0857 0208 63	5	0 0009

Type of equation	Equation number in text	Gaseous molecules						Gaseous atoms						Condensed phases					
		$\Delta \ln n_1$	$\Delta \ln n_2$	$\Delta \ln n_3$	---	$\Delta \ln n_Z$	$\Delta \ln n_Y$	$\Delta \ln n_X$	---	---	$\Delta \ln n_{\text{H}_2}$	$\Delta \ln n_{\text{N}_2}$	$\Delta \ln n_{\text{O}_2}$	---	$\Delta \ln n_{\text{H}}$	$\Delta \ln n_{\text{N}}$	$\Delta \ln n_{\text{O}}$	$\Delta \ln A$	$\Delta \ln T$
Gaseous equilibria	(29)	1	0	0	0	-a <sub>1</sub>	-b <sub>1</sub>	-c <sub>1</sub>	---	0	0	0	0	0	0	0	0	-q <sub>1</sub>	-q <sub>1</sub>
		0	1	0	0	-a <sub>2</sub>	-b <sub>2</sub>	-c <sub>2</sub>	---	0	0	0	0	0	0	0	0	-q <sub>2</sub>	-q <sub>2</sub>
		0	0	1	0	-a <sub>3</sub>	-b <sub>3</sub>	-c <sub>3</sub>	---	0	0	0	0	0	0	0	0	-q <sub>3</sub>	-q <sub>3</sub>
		0	0	0	0	---	---	---	---	0	0	0	0	0	0	0	0	---	---
Mass balance	(28)	a <sub>1</sub> n <sub>1</sub>	a <sub>2</sub> n <sub>2</sub>	a <sub>3</sub> n <sub>3</sub>	---	r <sub>2</sub>	0	0	---	a <sub>X</sub> n <sub>X</sub>	a <sub>N</sub> n <sub>N</sub>	---	a <sub>T</sub> n <sub>T</sub>	0	0	0	0	AΔα	AΔα
		b <sub>1</sub> n <sub>1</sub>	b <sub>2</sub> n <sub>2</sub>	b <sub>3</sub> n <sub>3</sub>	---	0	n <sub>Y</sub>	0	0	---	b <sub>M</sub> n <sub>M</sub>	b <sub>N</sub> n <sub>N</sub>	---	b <sub>T</sub> n <sub>T</sub>	0	0	0	AΔc	AΔc
		c <sub>1</sub> n <sub>1</sub>	c <sub>2</sub> n <sub>2</sub>	c <sub>3</sub> n <sub>3</sub>	---	0	0	n <sub>X</sub>	0	---	c <sub>X</sub> n <sub>X</sub>	c <sub>N</sub> n <sub>N</sub>	---	c <sub>T</sub> n <sub>T</sub>	0	0	0	AΔc	AΔc
		---	---	---	0	0	0	0	0	---	---	---	---	---	0	0	0	0	---
Condensed-phase equilibria	(30)	0	0	0	0	---	---	---	---	0	0	0	0	0	0	0	0	0	0
		0	0	0	0	0	a <sub>M</sub>	b <sub>M</sub>	c <sub>M</sub>	---	0	0	0	0	0	0	0	0	0
		0	0	0	0	a <sub>N</sub>	b <sub>N</sub>	c <sub>N</sub>	---	0	0	0	0	0	0	0	0	0	0
Pressure	(31)	p <sub>1</sub>	p <sub>2</sub>	p <sub>3</sub>	---	p <sub>Z</sub>	p <sub>Y</sub>	p <sub>X</sub>	---	0	0	0	0	0	0	0	0	0	0
		(H <sub>T</sub> <sup>0</sup> ) <sub>1</sub> n <sub>1</sub>	(H <sub>T</sub> <sup>0</sup> ) <sub>2</sub> n <sub>2</sub>	(H <sub>T</sub> <sup>0</sup> ) <sub>3</sub> n <sub>3</sub>	---	(H <sub>T</sub> <sup>0</sup> ) <sub>Z</sub> n <sub>Z</sub>	(H <sub>T</sub> <sup>0</sup> ) <sub>Y</sub> n <sub>Y</sub>	(H <sub>T</sub> <sup>0</sup> ) <sub>X</sub> n <sub>X</sub>	---	(H <sub>T</sub> <sup>0</sup> ) <sub>N</sub> n <sub>N</sub>	(H <sub>T</sub> <sup>0</sup> ) <sub>O</sub> n <sub>O</sub>	---	(H <sub>T</sub> <sup>0</sup> ) <sub>H</sub> n <sub>H</sub>	---	(H <sub>T</sub> <sup>0</sup> ) <sub>T</sub> n <sub>T</sub>	0	0	0	
Enthalpy*	(32)	(H <sub>T</sub> <sup>0</sup> ) <sub>1</sub> n <sub>1</sub>	(H <sub>T</sub> <sup>0</sup> ) <sub>2</sub> n <sub>2</sub>	(H <sub>T</sub> <sup>0</sup> ) <sub>3</sub> n <sub>3</sub>	---	(S <sub>T</sub> <sup>0</sup> ) <sub>Z</sub> n <sub>Z</sub>	(S <sub>T</sub> <sup>0</sup> ) <sub>Y</sub> n <sub>Y</sub>	(S <sub>T</sub> <sup>0</sup> ) <sub>X</sub> n <sub>X</sub>	---	(S <sub>T</sub> <sup>0</sup> ) <sub>N</sub> n <sub>N</sub>	(S <sub>T</sub> <sup>0</sup> ) <sub>O</sub> n <sub>O</sub>	---	(S <sub>T</sub> <sup>0</sup> ) <sub>H</sub> n <sub>H</sub>	---	(S <sub>T</sub> <sup>0</sup> ) <sub>T</sub> n <sub>T</sub>	0	0	0	

\* Row vector to be substituted in place of enthalpy row for isentropic expansion to assigned pressure:

Entropy	(33)	(S <sub>T</sub> ) <sub>1</sub> <sup>n<sub>1</sub></sup>	(S <sub>T</sub> ) <sub>2</sub> <sup>n<sub>2</sub></sup>	(S <sub>T</sub> ) <sub>3</sub> <sup>n<sub>3</sub></sup>	---	(S <sub>T</sub> ) <sub>Z</sub> <sup>n<sub>Z</sub></sup>	(S <sub>T</sub> ) <sub>Y</sub> <sup>n<sub>Y</sub></sup>	(S <sub>T</sub> ) <sub>X</sub> <sup>n<sub>X</sub></sup>	---	(S <sub>T</sub> ) <sub>N</sub> <sup>n<sub>N</sub></sup>	(S <sub>T</sub> ) <sub>O</sub> <sup>n<sub>O</sub></sup>	---	(S <sub>T</sub> ) <sub>H</sub> <sup>n<sub>H</sub></sup>	(S <sub>T</sub> ) <sub>T</sub> <sup>n<sub>T</sub></sup>	0	0	AΔS
---------	------	---	---	---	-----	---	---	---	-----	---	---	-----	---	---	---	---	-----

Figure 1. - General matrix of correction equations for adiabatic combustion at assigned pressure.

Type of equation	Gaseous atoms				Condensed phases				Constant
	$\Delta \ln p_Z$	$\Delta \ln p_Y$	$\Delta \ln p_X$	$\Delta \ln p_1$	$\Delta n_M$	$\Delta n_N$	$\Delta n_A$	$\Delta \ln T$	
Mass balance	$\sum a_1^2 p_1$	$\sum a_1 b_1 p_1$	$\sum a_1 c_1 p_1$	$\sum a_1 c_1 p_1$	$a_M$	$a_N$	$\sum a_1 n_1$	$\sum a_1 q_1 p_1$	$A\Delta a + \sum a_1 \delta_1 p_1$
	$\sum a_1 b_1 p_1$	$\sum b_1^2 p_1$	$\sum b_1 c_1 p_1$	$\sum b_1 c_1 p_1$	$b_M$	$b_N$	$\sum b_1 n_1$	$\sum b_1 q_1 p_1$	$A\Delta b + \sum b_1 \delta_1 p_1$
	$\sum a_1 c_1 p_1$	$\sum b_1 c_1 p_1$	$\sum c_1^2 p_1$	$\sum c_1^2 p_1$	$c_M$	$c_N$	$\sum c_1 n_1$	$\sum c_1 q_1 p_1$	$A\Delta c + \sum c_1 \delta_1 p_1$
	---	---	---	---	---	---	---	---	---
Condensed-phase equilibria	---	---	---	---	0	0	0	0	---
	$a_M$	$b_M$	$c_M$	$c_M$	0	0	0	0	$\delta_M$
	$a_N$	$b_N$	$c_N$	$c_N$	0	0	0	0	$\delta_N$
	Pressure	$\sum a_1 p_1$	$\sum b_1 p_1$	$\sum c_1 p_1$	---	0	0	0	$\sum q_1 p_1$
Enthalpy*	$\sum (H_T^o) a p_1$	$\sum (H_T^o) b p_1$	$\sum (H_T^o) c p_1$	$\sum (H_T^o) c p_1$	$(H_T^o)_M$	$(H_T^o)_N$	$\sum (H_T^o)_{1,1}^{n_1}$	$\sum (H_T^o)_{1,1}^{n_1}$	$\sum q_1 p_1$
	---	---	---	---	---	---	$\sum (H_T^o)_{1,1}^{n_1}$	$\sum (H_T^o)_{1,1}^{n_1}$	$\sum (H_T^o)_{1,1}^{n_1}$

\* Row vector to be substituted in place of enthalpy row for isentropic expansion to assigned pressure:

Entropy	$\sum (S_T)_1^i a p_1$	$\sum (S_T)_1^i b p_1$	$\sum (S_T)_1^i c p_1$	$(S_T)_M^i$	$(S_T)_N^i$	$\sum (S_T)_1^i r_1$	$\sum (S_T)_1^i p_1$	$\sum (S_T)_1^i \delta_1 p_1$	$A\Delta S +$
---------	------------------------	------------------------	------------------------	-------------	-------------	----------------------	----------------------	-------------------------------	---------------

Figure 2. - General reduced augmented matrix for adiabatic combustion at assigned pressure. (Summations in terms of  $p_1$  for gaseous products only. Summations in terms of  $n_1$  for all products.)

Type of equation	Gaseous atoms			Condensed phases		
	$\left(\frac{\partial \ln p_Z}{\partial \ln T}\right)_P$	$\left(\frac{\partial \ln p_Y}{\partial \ln T}\right)_P$	$\left(\frac{\partial \ln p_X}{\partial \ln T}\right)_P$	$\left(\frac{\partial n_M}{\partial \ln T}\right)_P$	$\left(\frac{\partial n_N}{\partial \ln T}\right)_P$	$-\left(\frac{\partial \ln A}{\partial \ln T}\right)_P$
Mass balance	$\sum a_1^2 p_1$	$\sum a_1 b_1 p_1$	$\sum a_1 c_1 p_1$	---	---	Constant
	$\sum a_1 b_1 p_1$	$\sum b_1^2 p_1$	$\sum b_1 c_1 p_1$	---	$a_N$	$\sum a_1 q_1 p_1$
	$\sum a_1 c_1 p_1$	$\sum b_1 c_1 p_1$	$\sum c_1^2 p_1$	---	$b_N$	$\sum b_1 n_1$
	---	---	---	---	$c_N$	$\sum c_1 n_1$
Condensed-phase equilibria	---	---	---	---	---	$\sum c_1 q_1 p_1$
	$a_M$	$b_M$	$c_M$	---	---	---
	$a_N$	$b_N$	$c_N$	---	---	---
Pressure	$\sum a_1 p_1$	$\sum b_1 p_1$	$\sum c_1 p_1$	---	0	0
					0	$\sum q_1 p_1$

Figure 3. - General reduced augmented matrix for partial derivatives at constant pressure. (Summations in terms of  $p_i$  for gaseous products only. Summations in terms of  $n_i$  for all products.)

Type of equation	Gaseous atoms			Condensed phases	
	$\left(\frac{\partial \ln p_Z}{\partial \ln A}\right)_T$	$\left(\frac{\partial \ln p_Y}{\partial \ln A}\right)_T$	$\left(\frac{\partial \ln p_X}{\partial \ln A}\right)_T$	$\left(\frac{\partial \ln M}{\partial \ln A}\right)_T$	$\left(\frac{\partial \ln N}{\partial \ln A}\right)_T$
Mass balance	$\sum a_1^2 p_1$	$\sum a_1 b_1 p_1$	$\sum a_1 c_1 p_1$	---	$a_N$
	$\sum a_1 b_1 p_1$	$\sum b_1^2 p_1$	$\sum b_1 c_1 p_1$	---	$b_N$
	$\sum a_1 c_1 p_1$	$\sum b_1 c_1 p_1$	$\sum c_1^2 p_1$	---	$c_N$
	---	---	---	---	---
Condensed-phase equilibria	--	--	--	0	0
	$a_M$	$b_M$	$c_M$	0	0
	$a_N$	$b_N$	$c_N$	0	0

Figure 4. General reduced augmented matrix for partial derivatives at constant temperature. (Summations in terms of  $p_1$  for gaseous products only. Summations in terms of  $n_1$  for all products.)

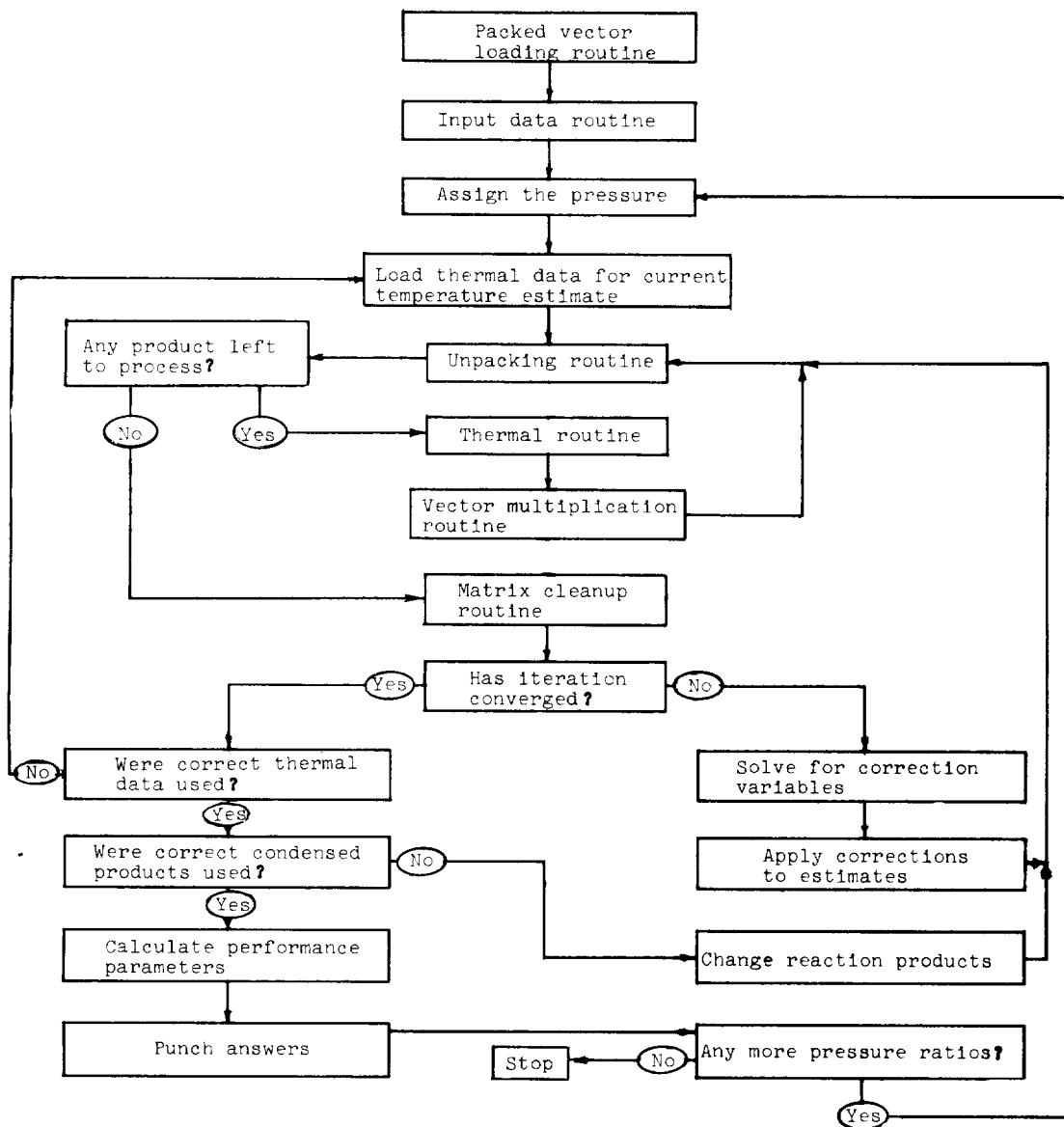


Figure 5. - Flow chart for Main Calculating Program.

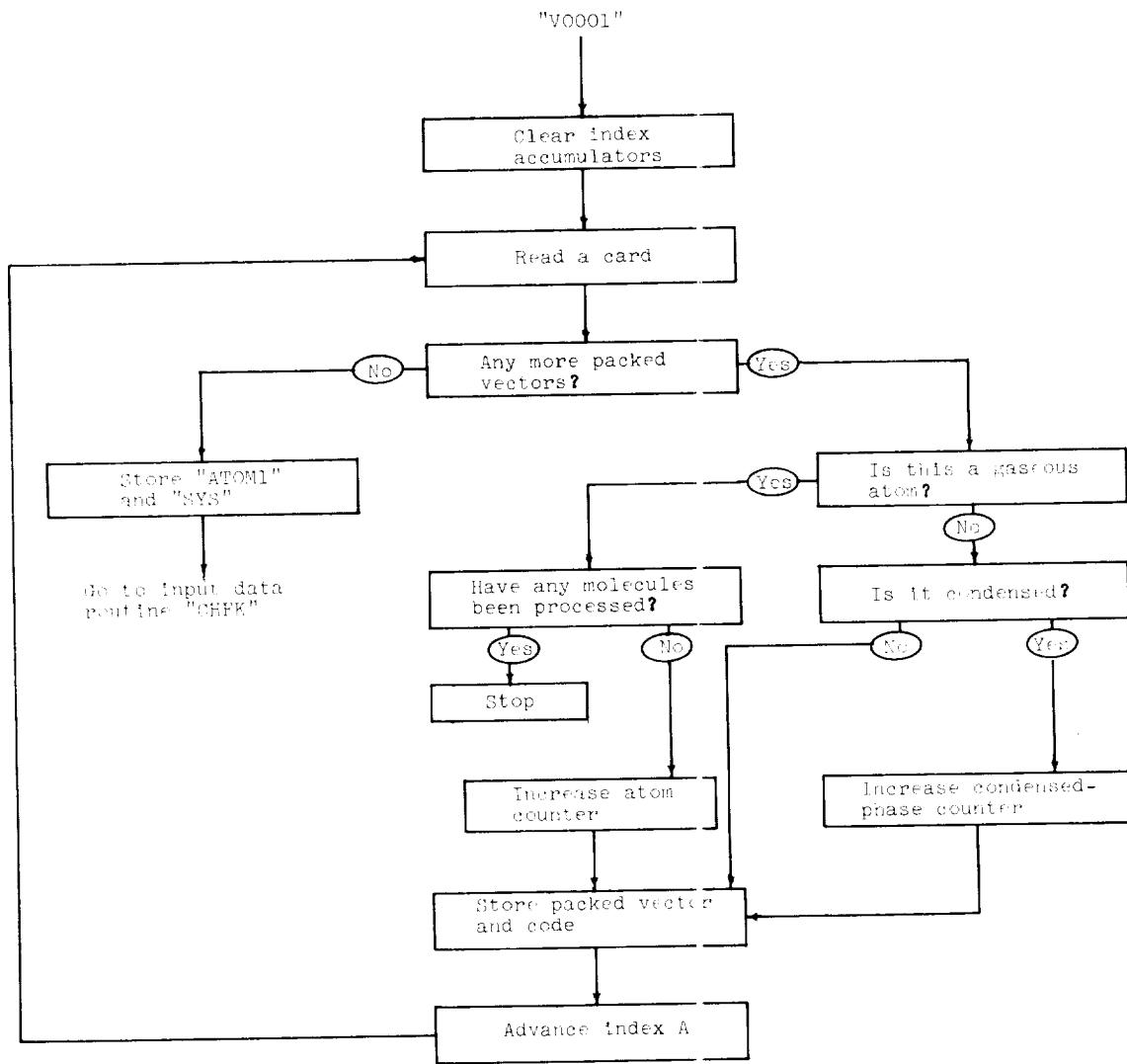


Figure 6. - Flow chart for packed vector loading.

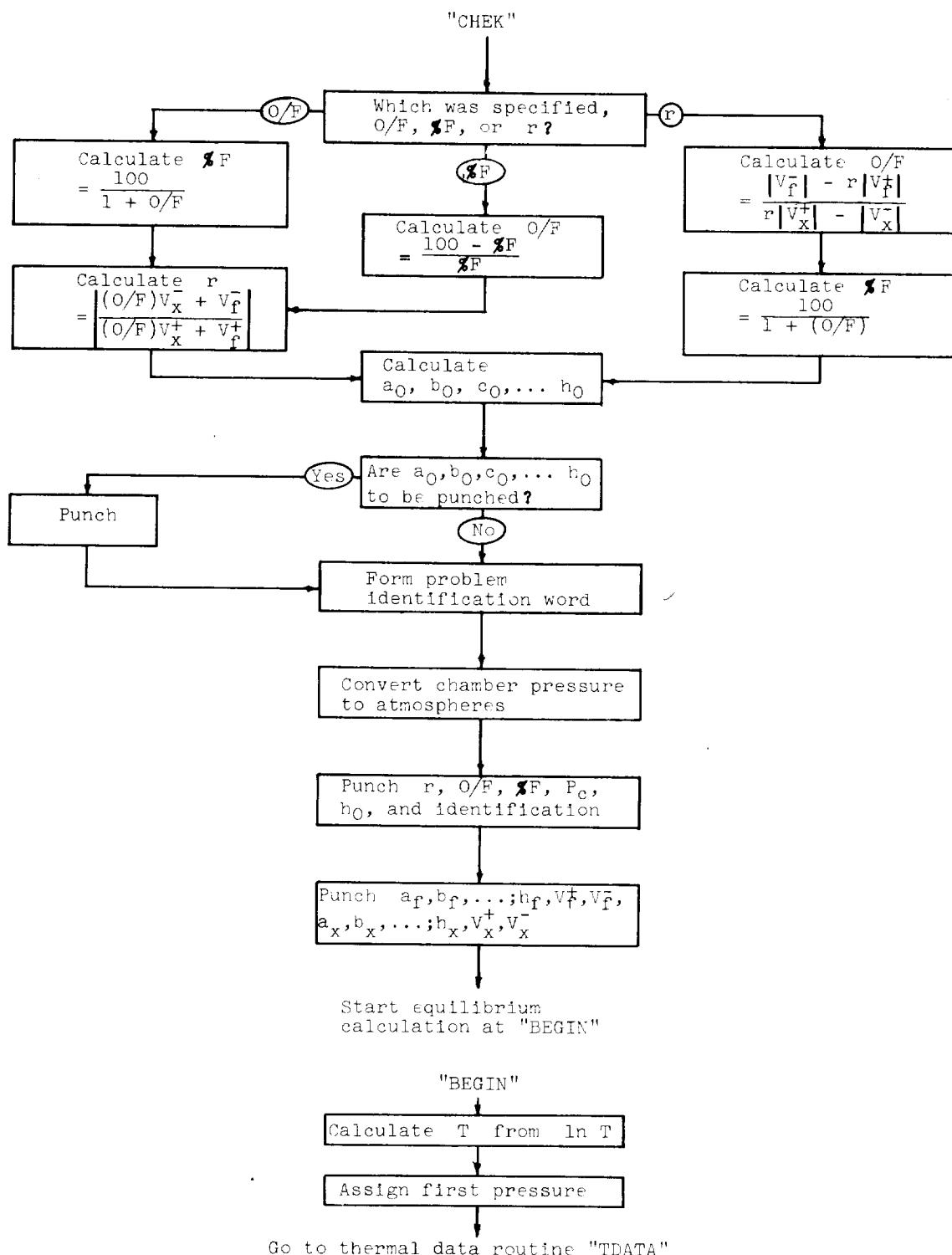


Figure 7. - Flow chart for input data routine.

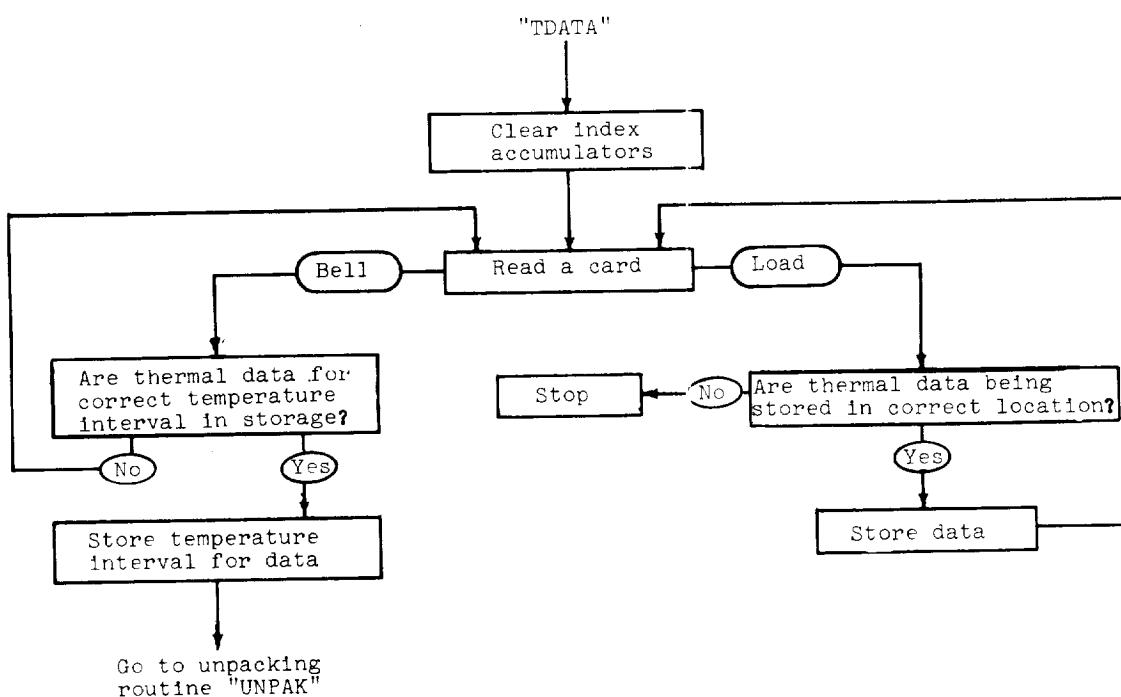


Figure 8. - Flow chart for load thermal data.

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CA-19

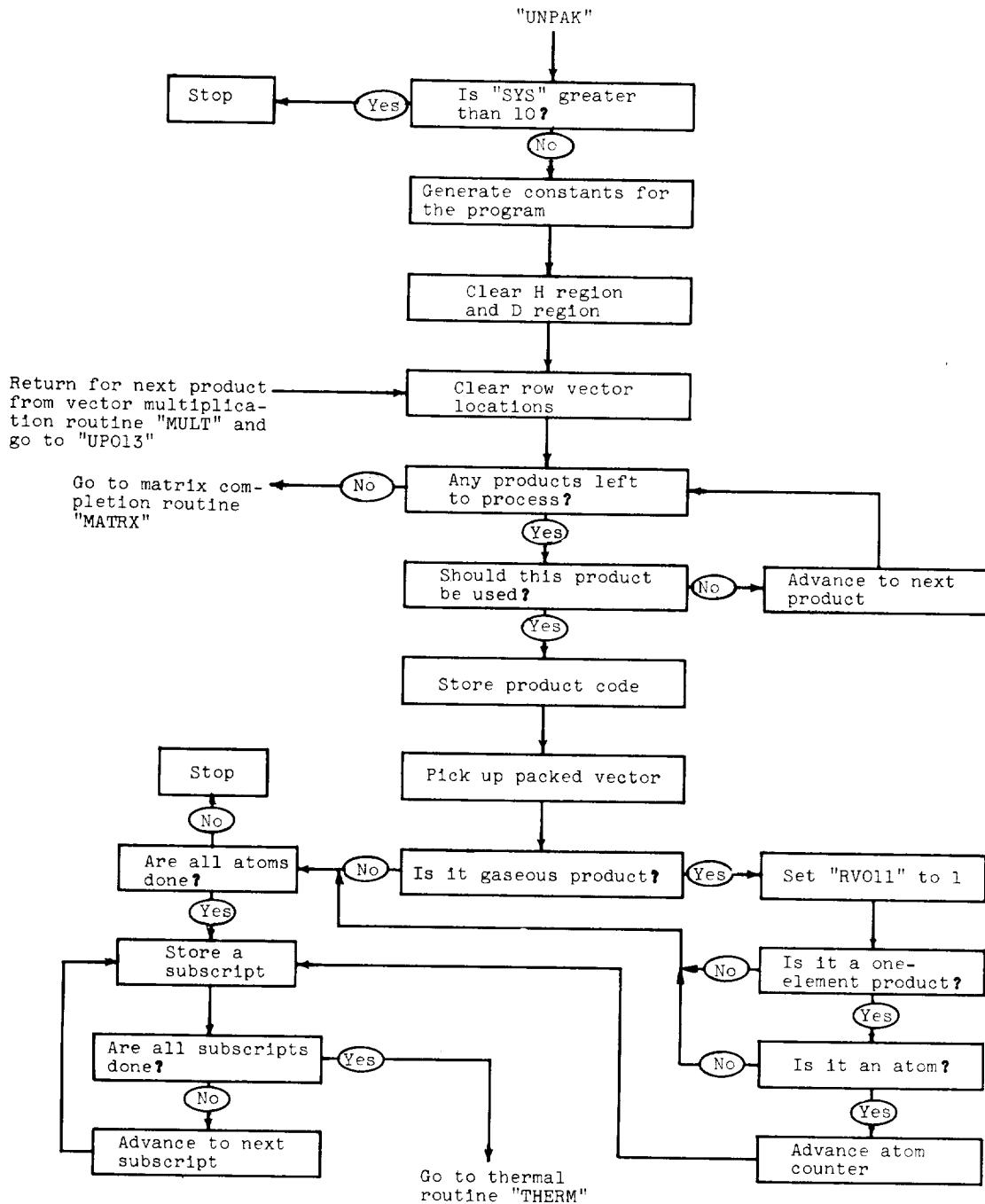


Figure 9. - Flow chart for unpacking routine.

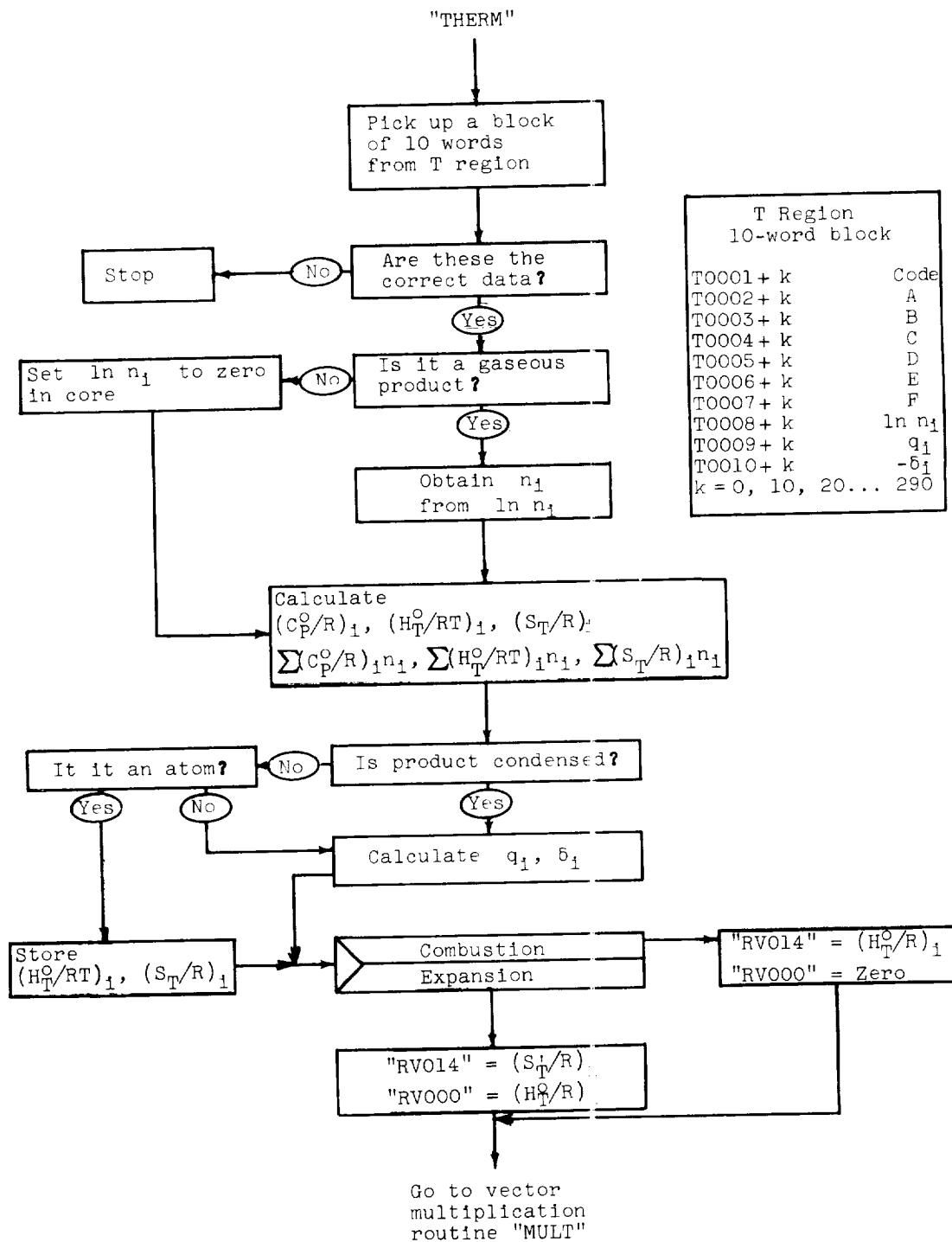


Figure 10. - Flow chart for thermal routine.

E-417

CA-19 back

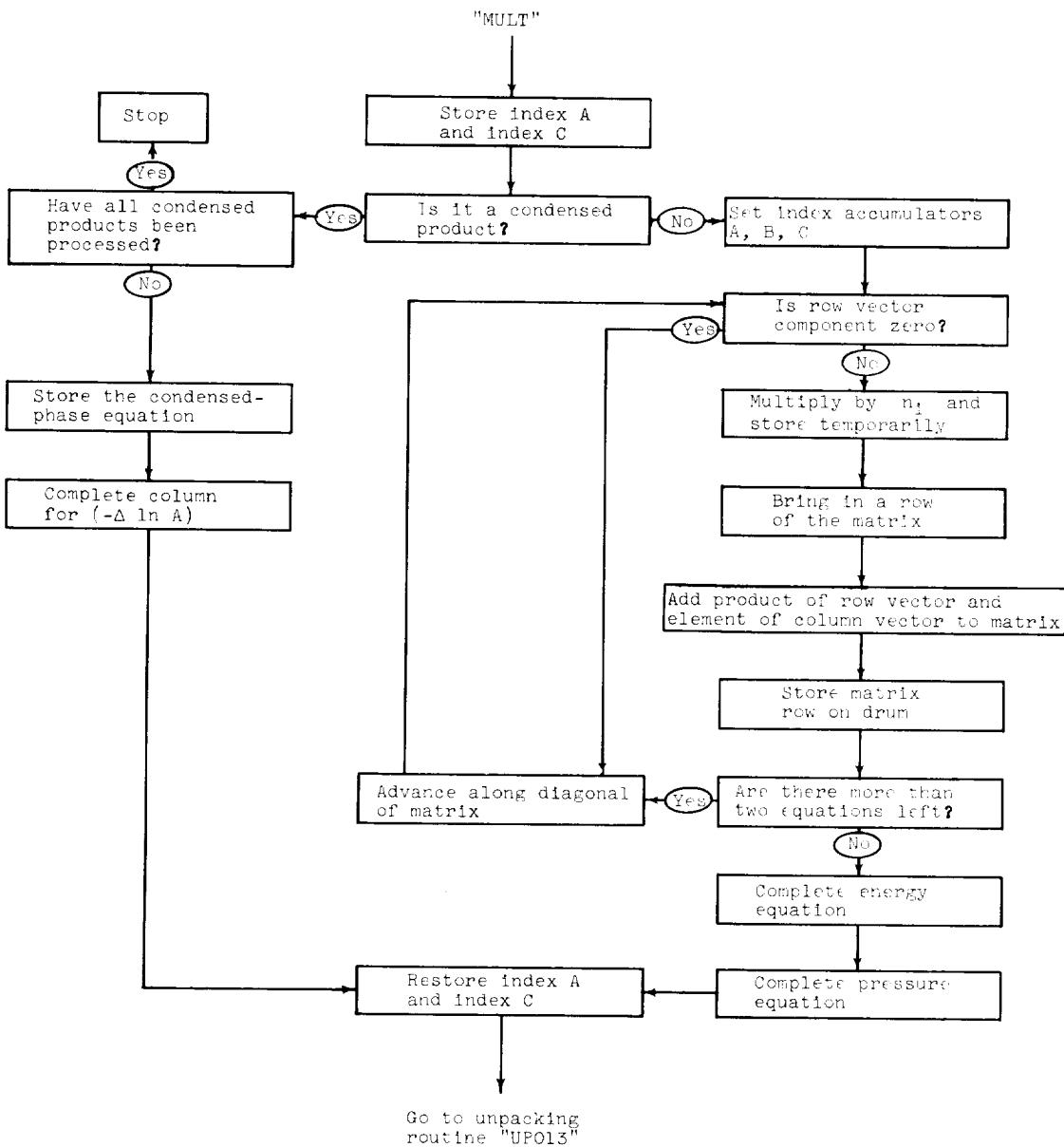


Figure 11. - Flow chart for vector multiplication routine.

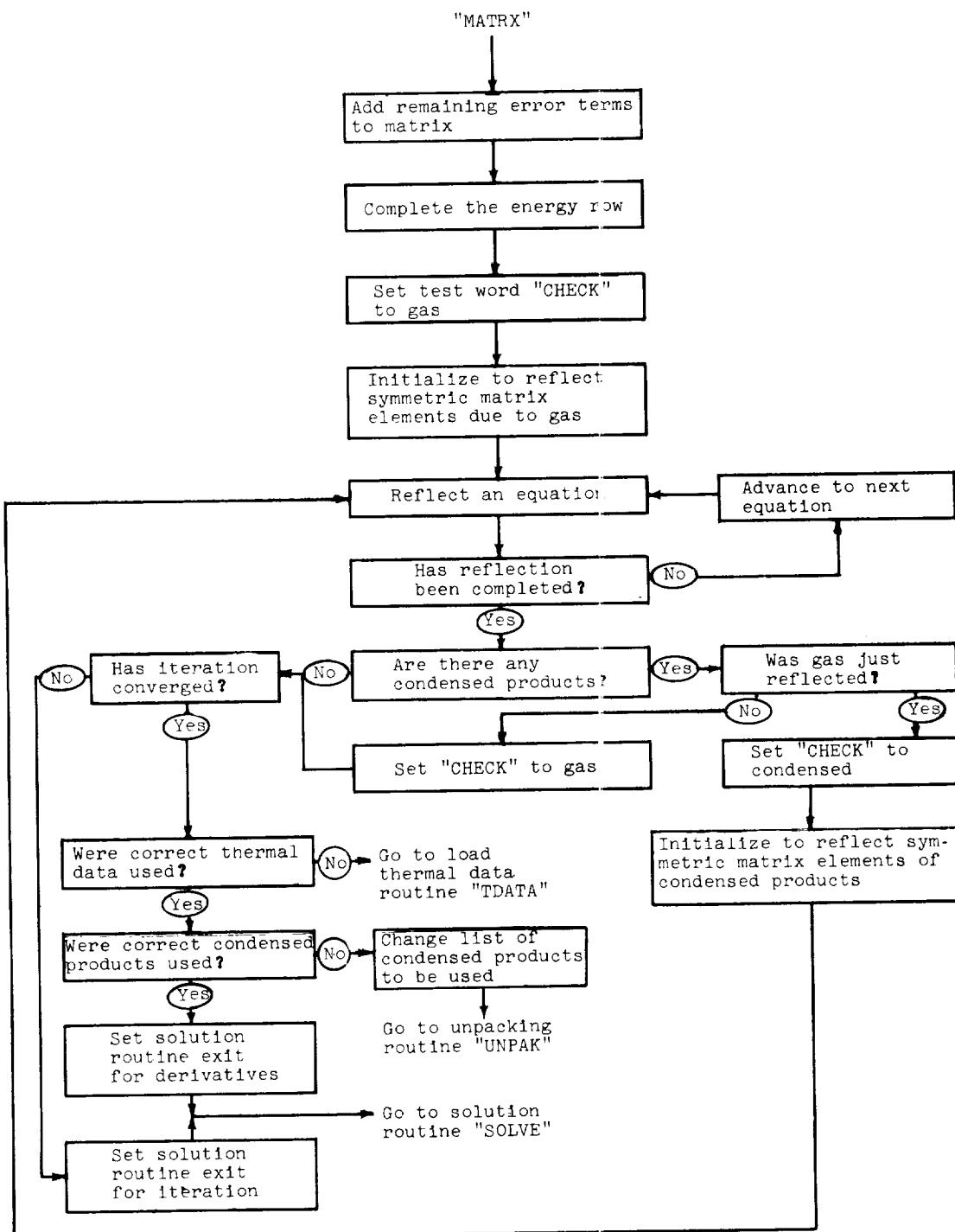


Figure 12. - Flow chart for matrix completion routine.

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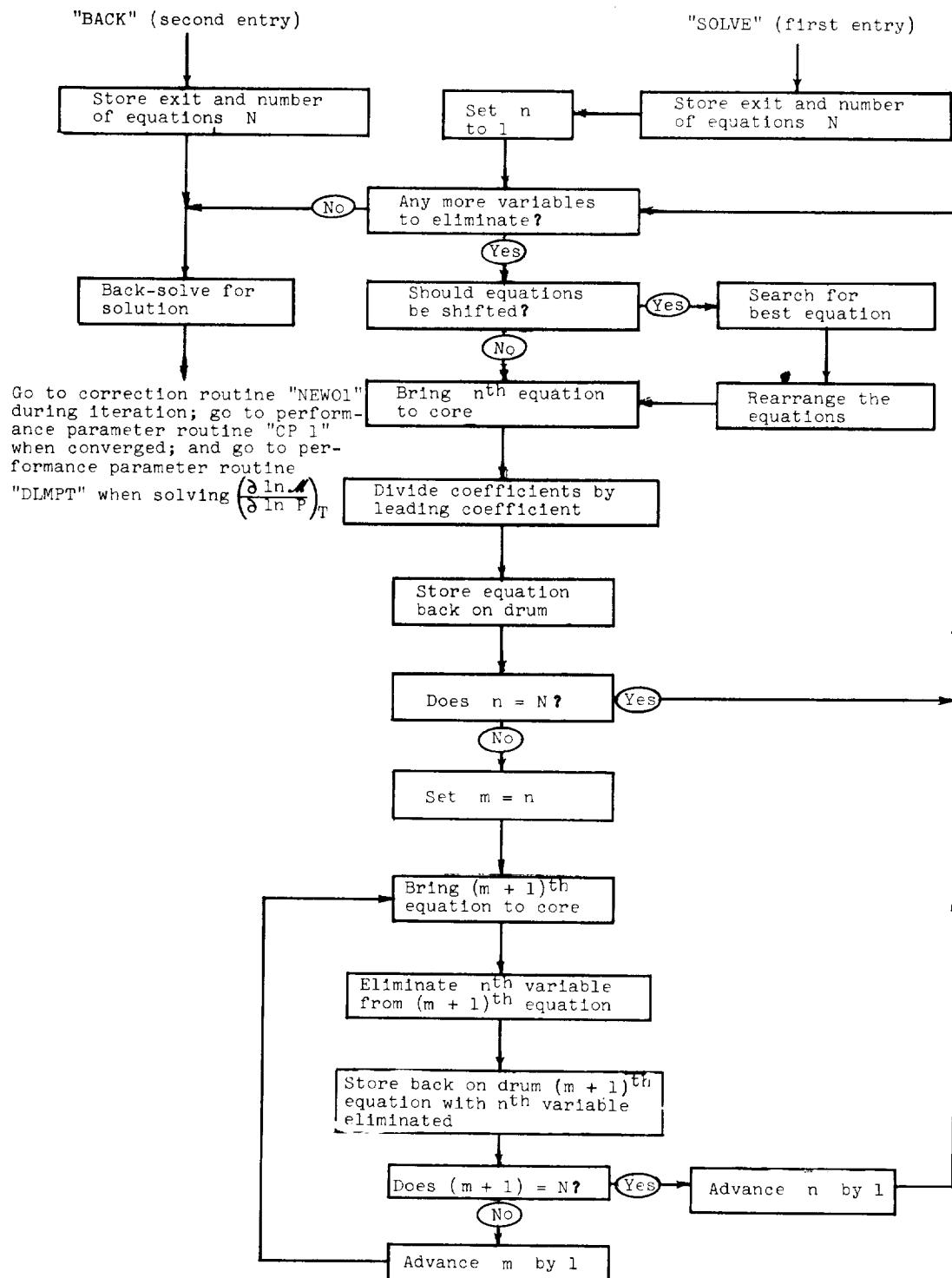


Figure 13. - Flow chart for matrix solution routine.

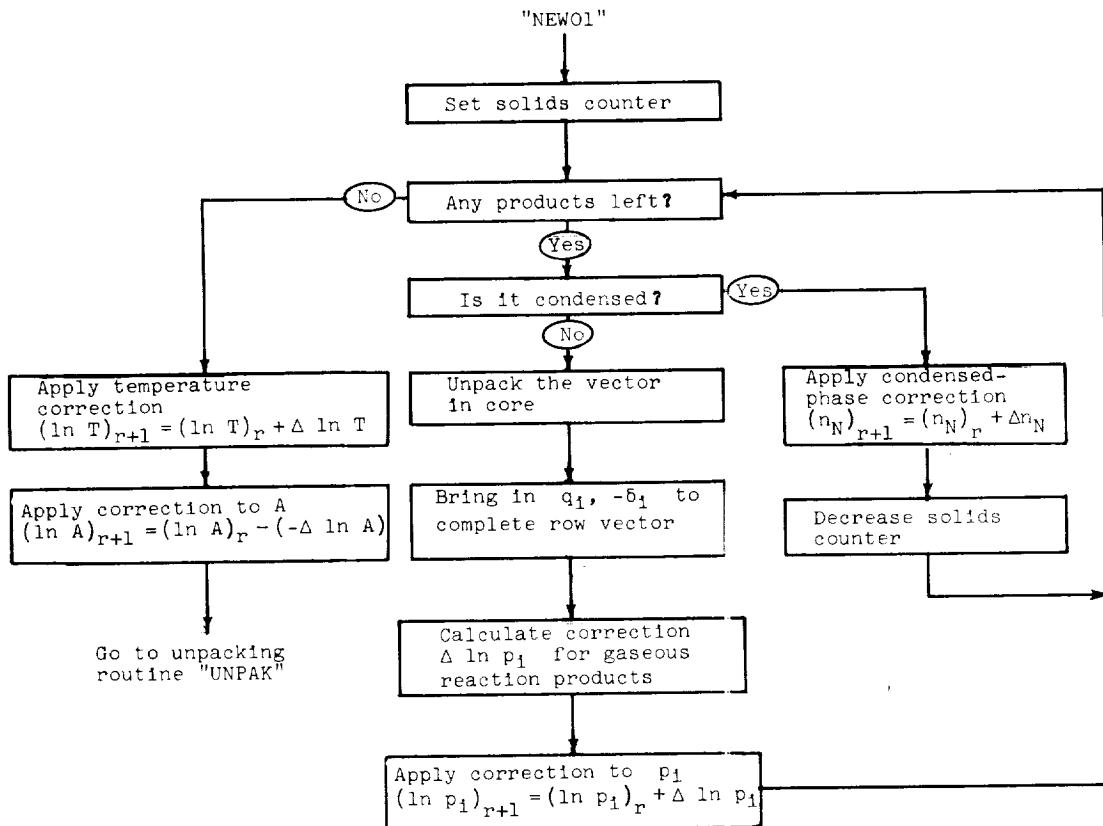


Figure 14. - Flow chart for correction routine.

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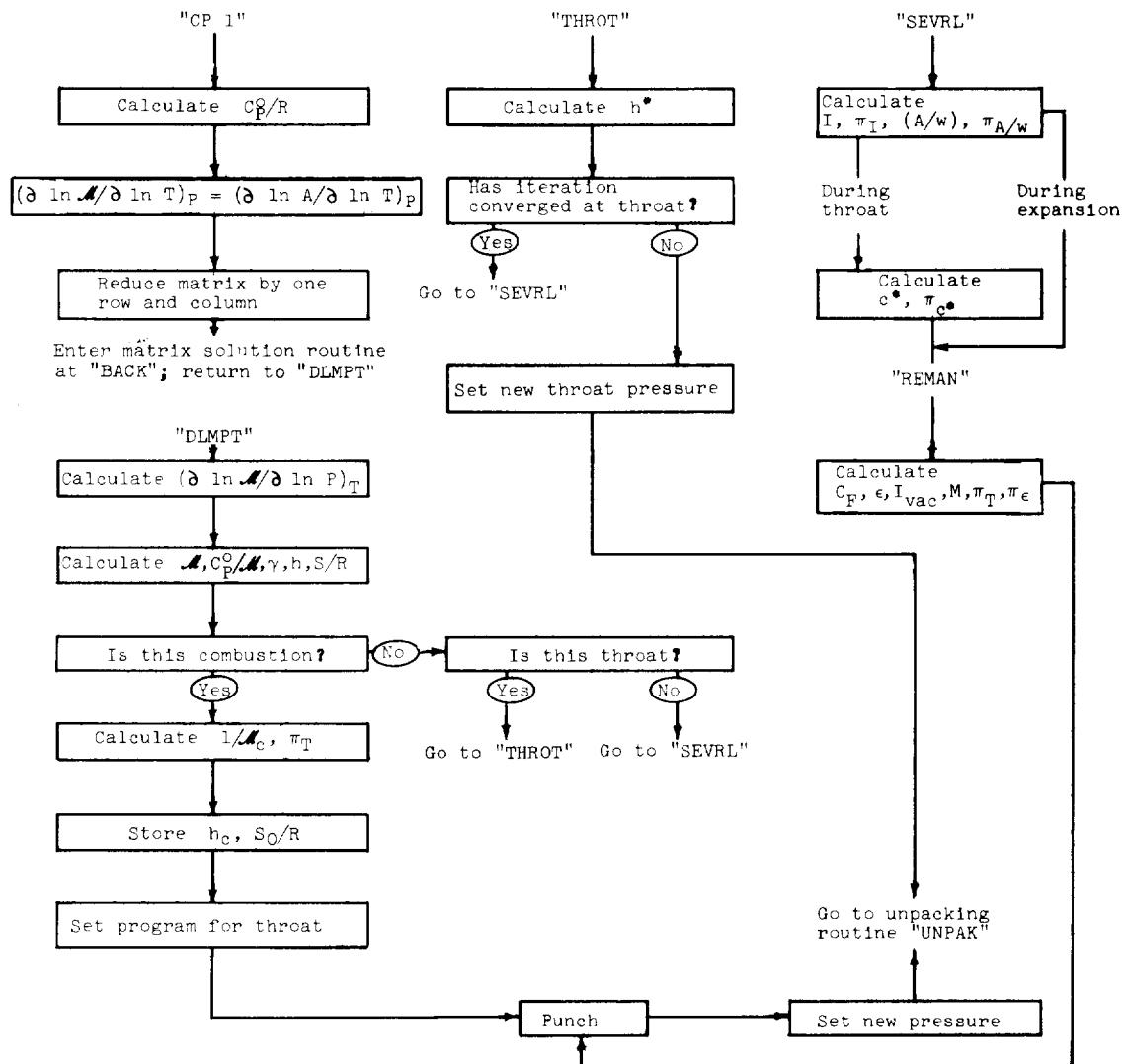


Figure 15. - Flow chart for performance-parameter routine.

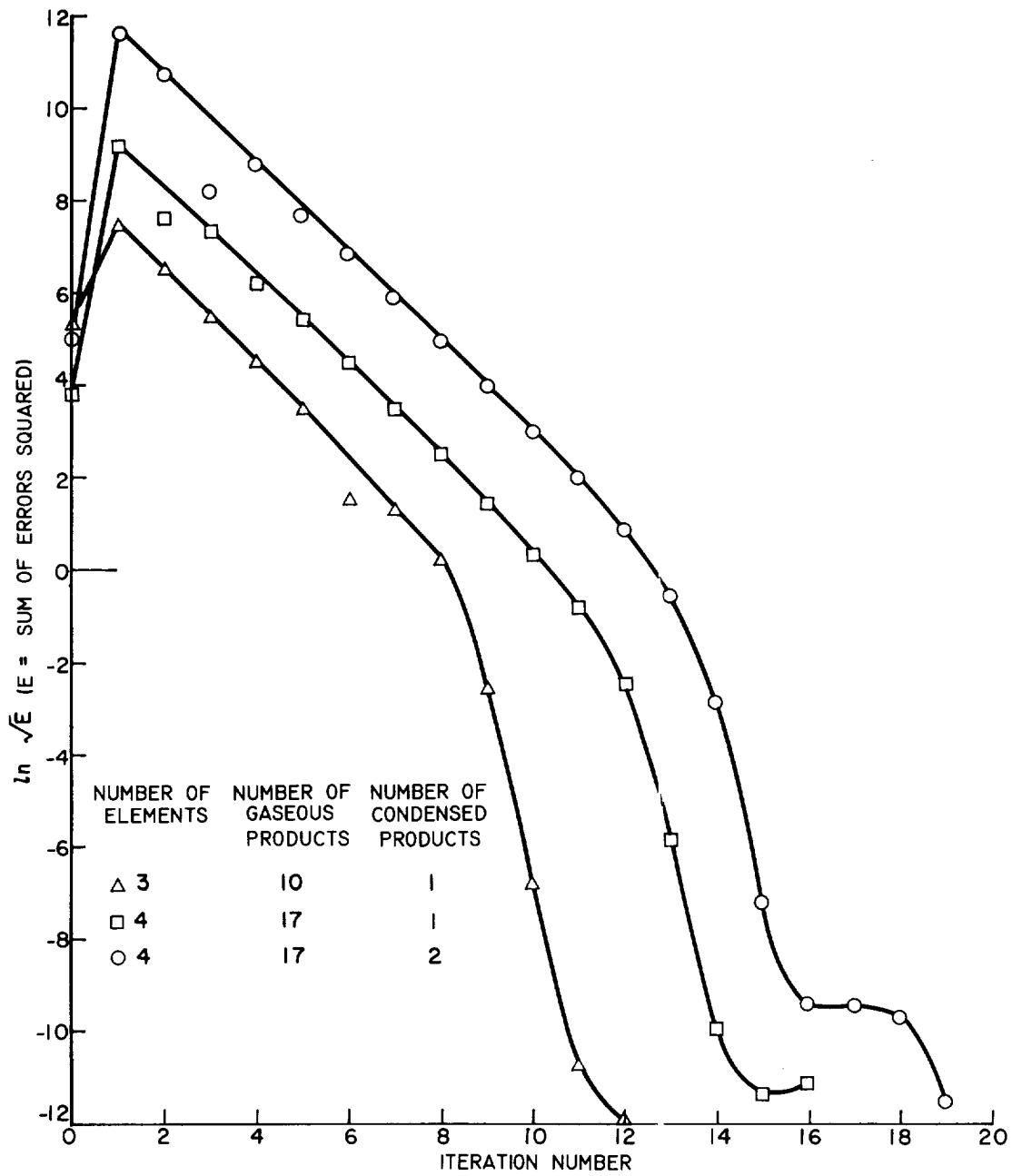
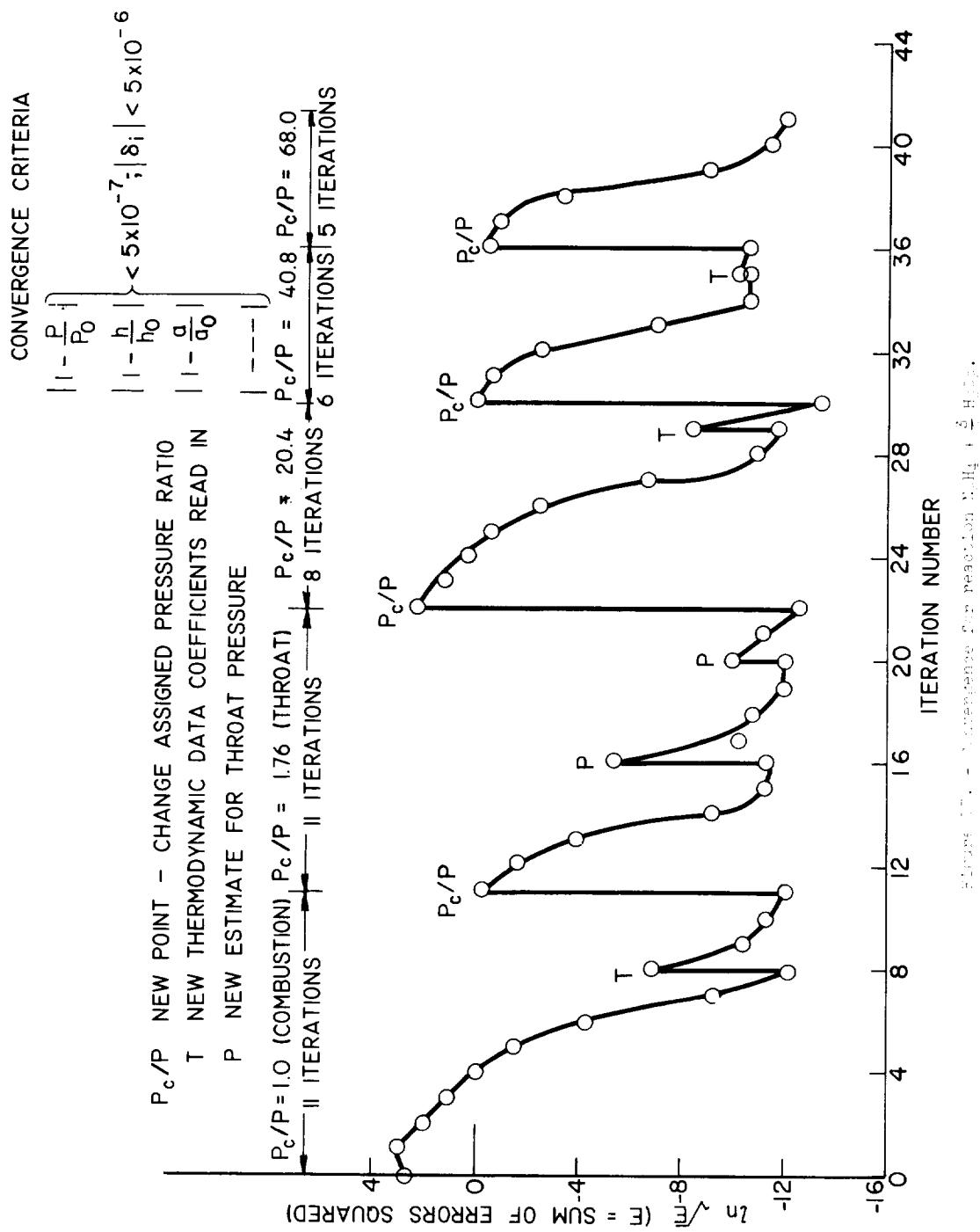


Figure 16. - Rate of convergence for several propellants.



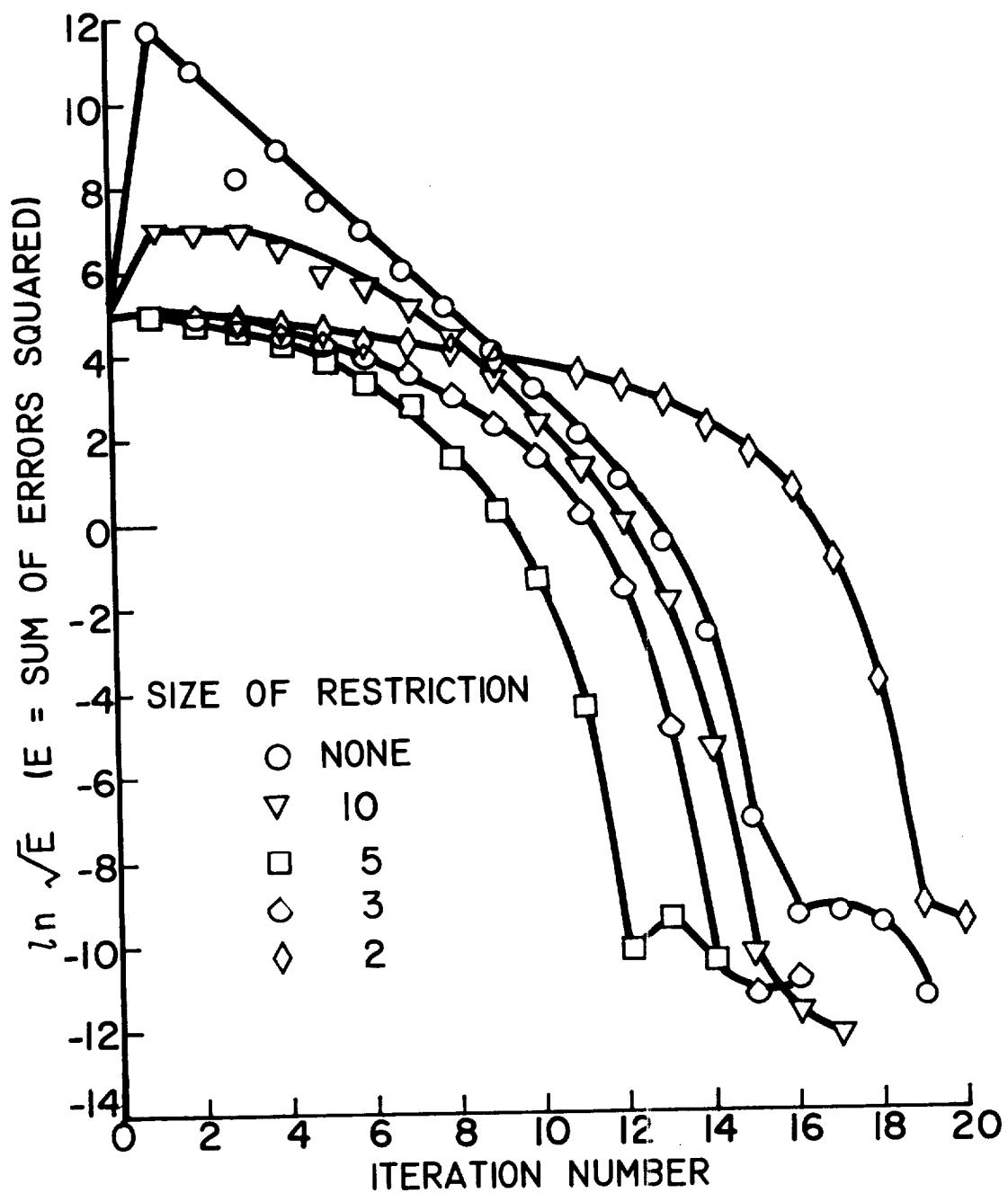


Figure 18. - Solution vector control and convergence;  
4 elements, 17 gaseous products, 2 condensed products.

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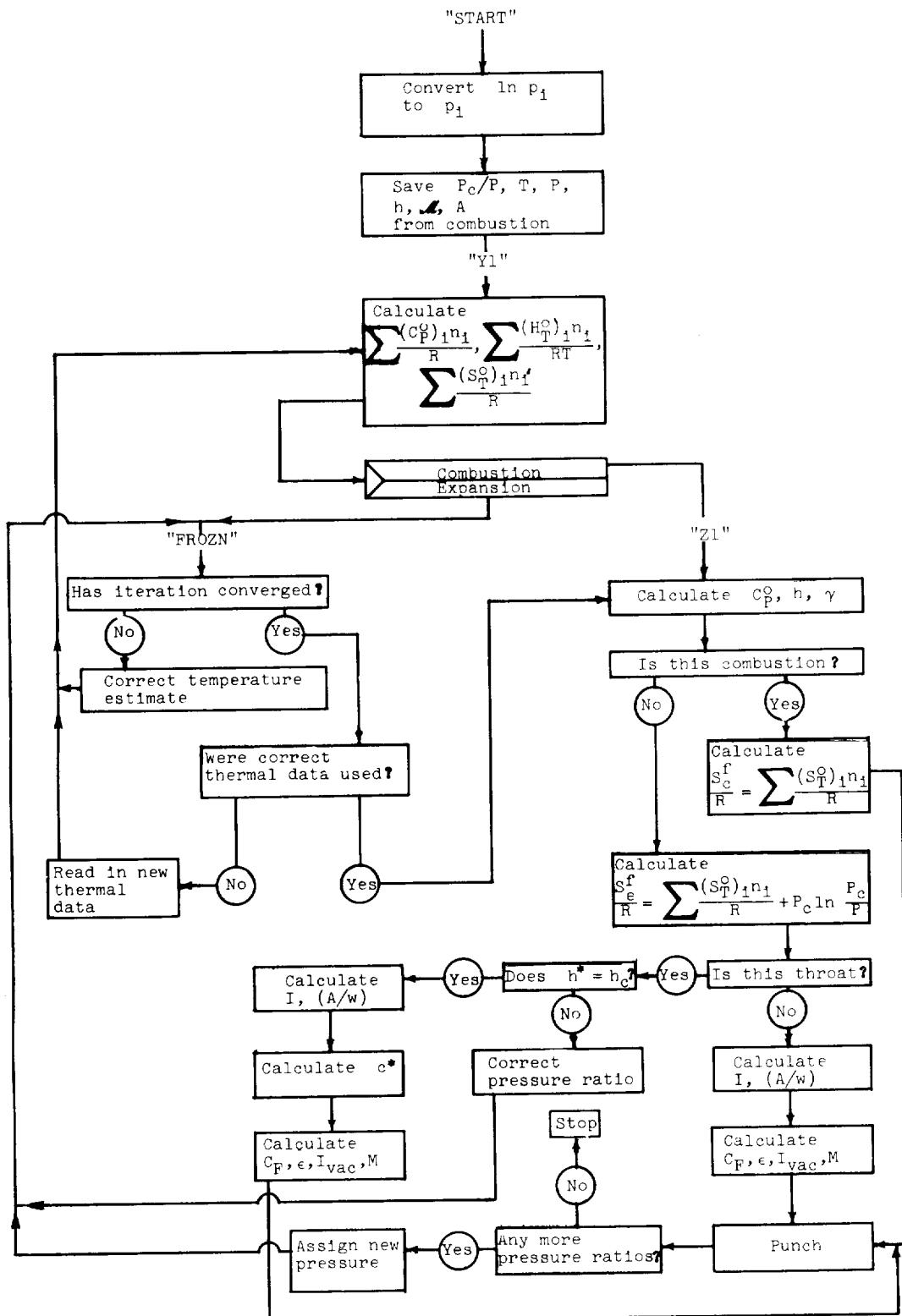


Figure 19. - Flow chart for frozen-composition routine.

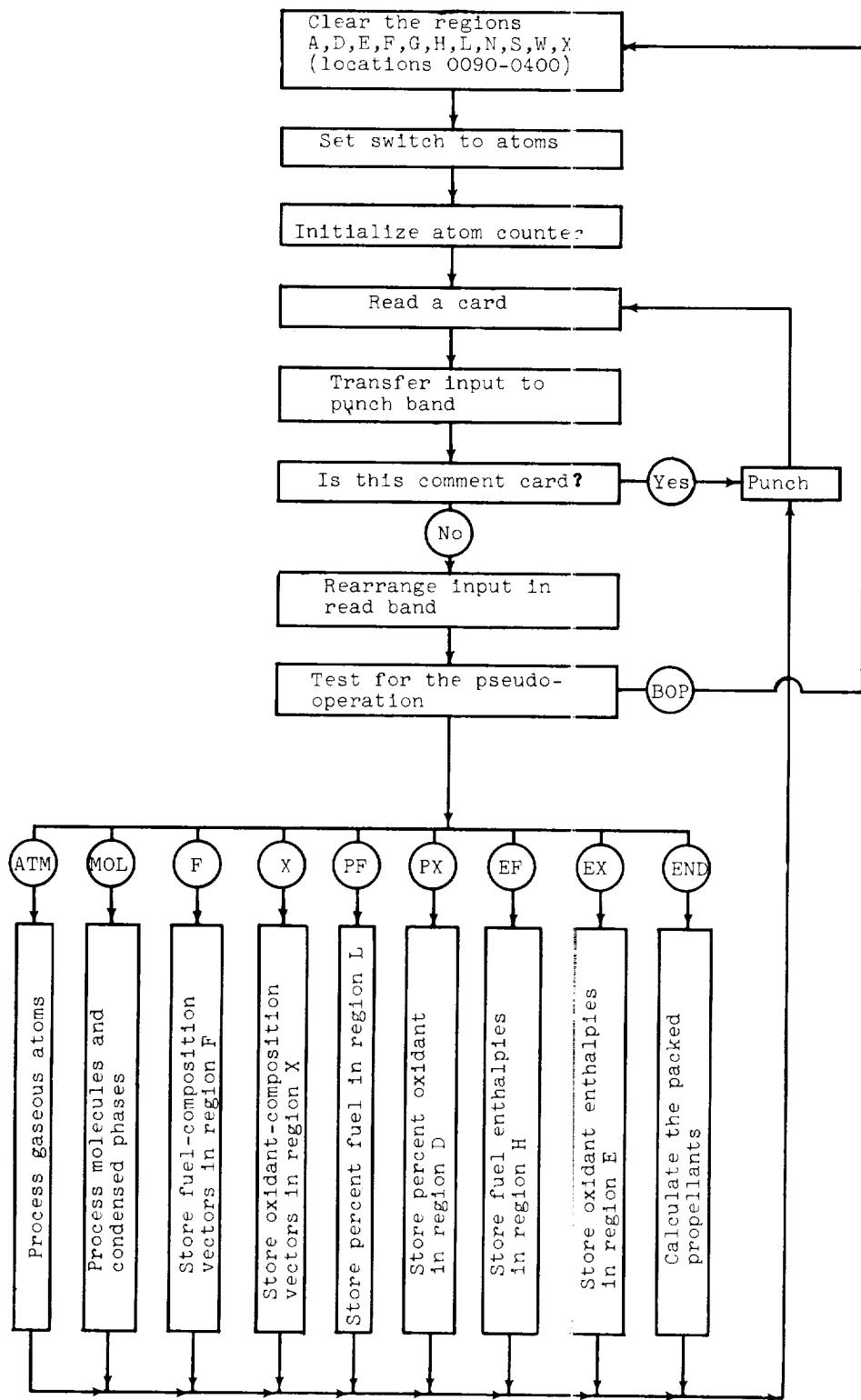


Figure 20. - Flow chart for Vector and Propellant Program.

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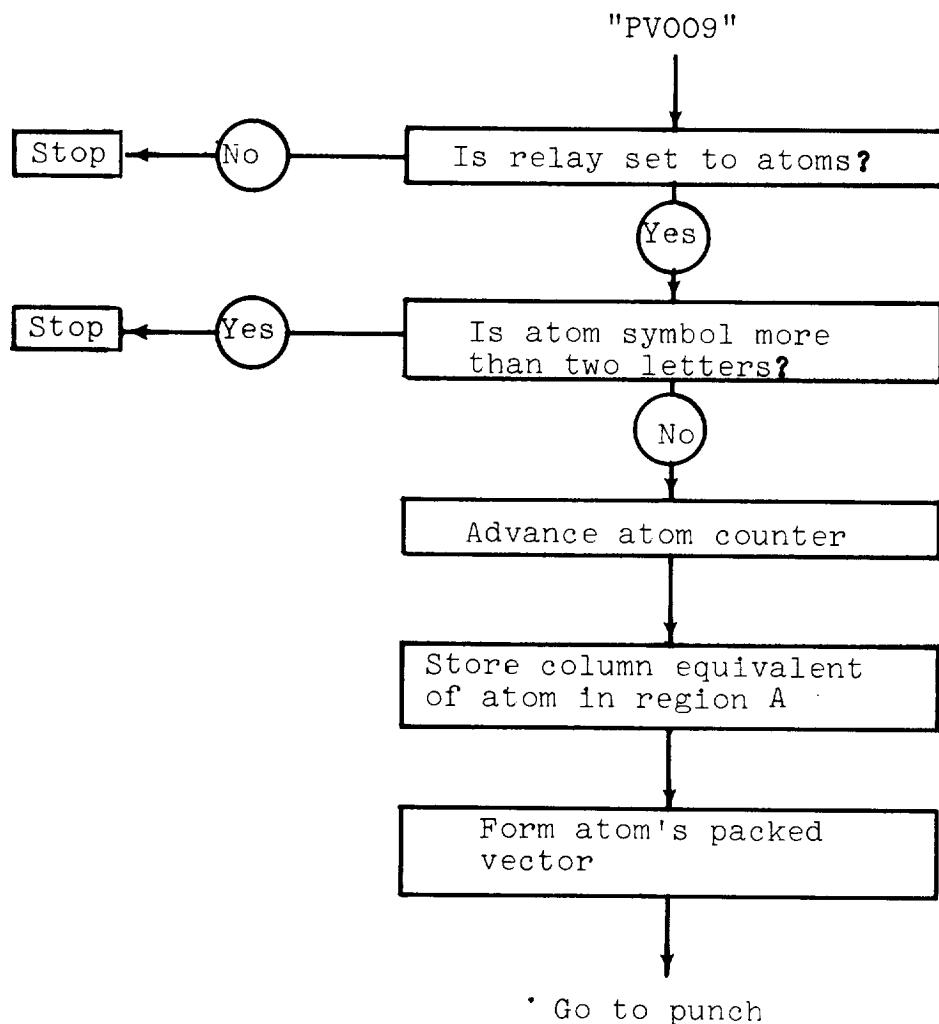


Figure 21. - Flow chart for ATM (pseudo-operation).

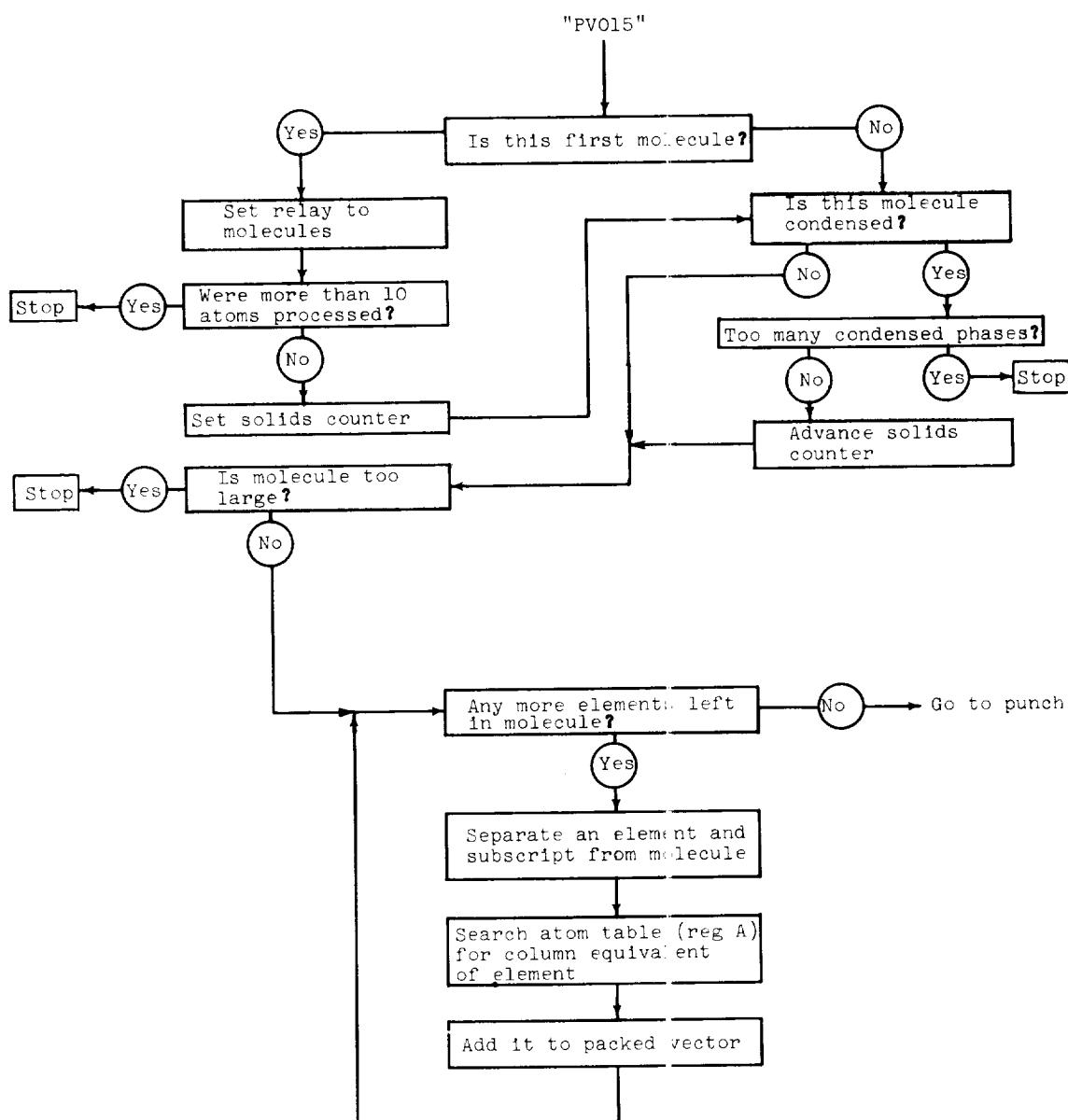


Figure 22. - Flow chart for MOL (pseudo-operation).

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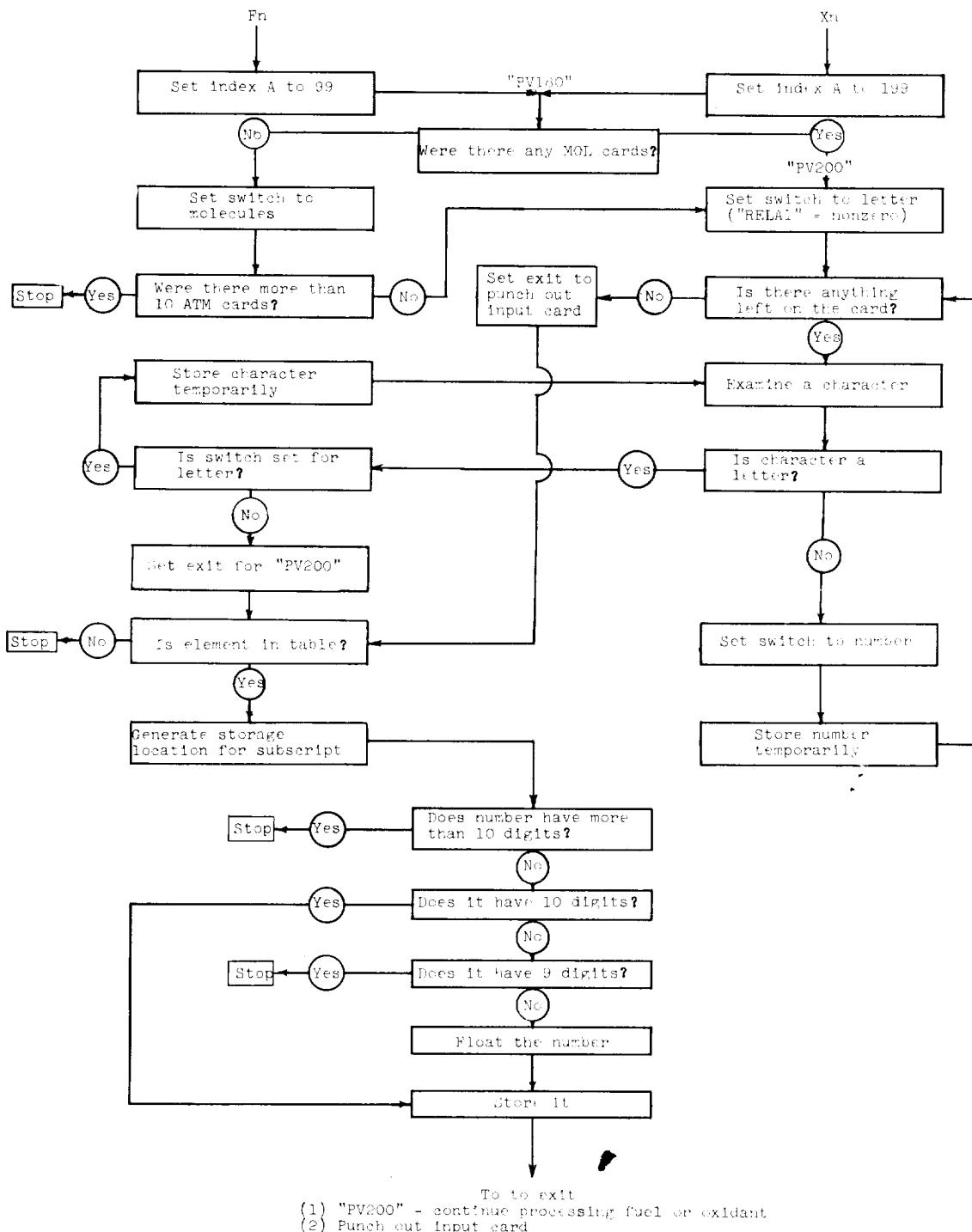


Figure 23. - Flow chart for F and X (pseudo-operations).

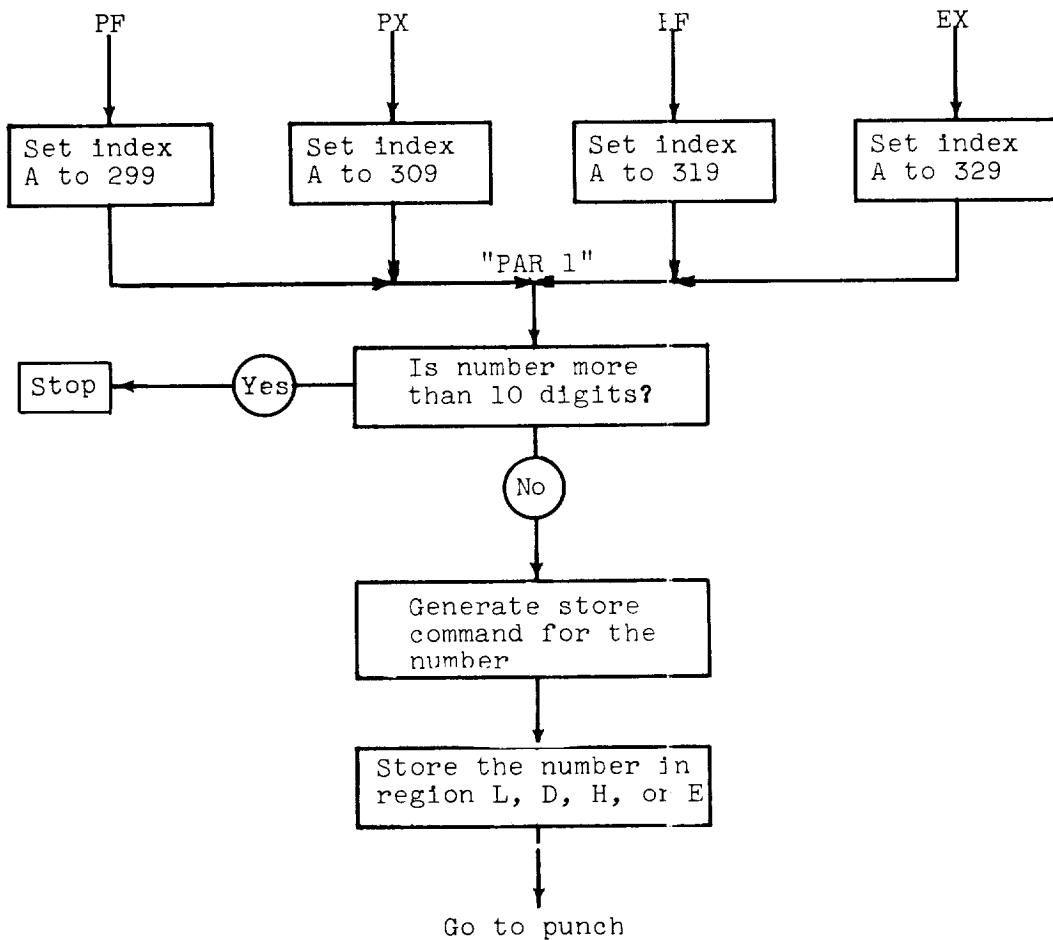


Figure 24. - Flow chart for percent fuel or oxidant and enthalpy of fuel or oxidant (pseudo-operations).

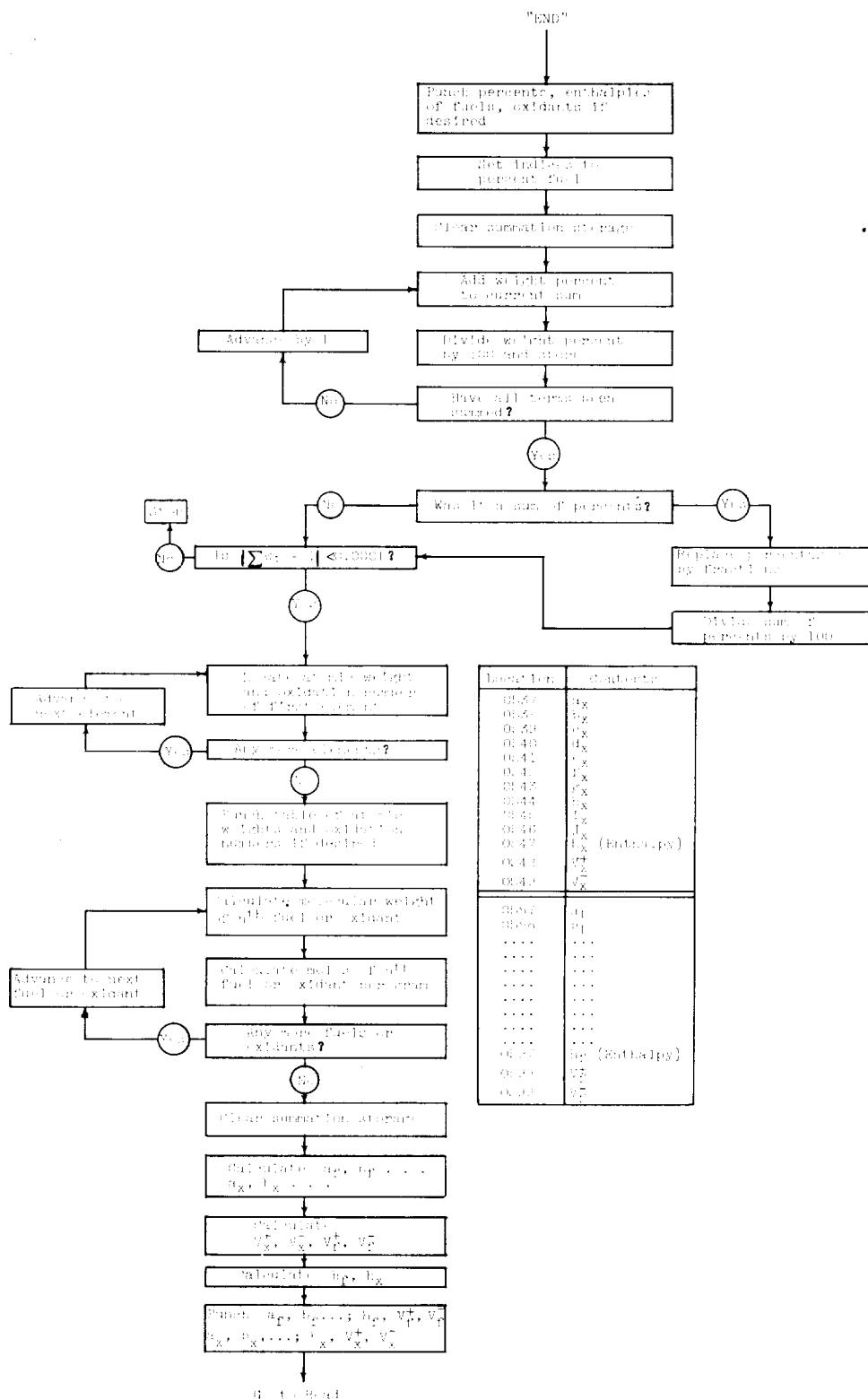


Figure 10c - Flow chart for propellant propellant mixture.



<p>NASA TN D-132 National Aeronautics and Space Administration. <b>A GENERAL METHOD FOR AUTOMATIC COMPUTATION OF EQUILIBRIUM COMPOSITIONS AND THEORETICAL ROCKET PERFORMANCE OF PROPELLANTS.</b> Sanford Gordon, Frank J. Zeleznik, and Vearl N. Huff. October 1959. 161p. diagrs., tabs. OTS price, \$3.00. (NASA TECHNICAL NOTE D-132)</p> <p>A general computer program for chemical equilibrium and rocket performance calculations was written for the IBM 650 computer with 2000 words of drum storage, 60 words of high-speed core storage, indexing registers, and floating point attachments. The program can carry out combustion and isentropic-expansion calculations on a chemical system that may include as many as 10 different chemical elements, 30 reaction products, and 25 pressure ratios. It calculates composition, temperature, pressure, specific impulse, specific impulse in vacuum, characteristic velocity, thrust coefficient, area ratio, molecular weight, Mach (over) Copies obtainable from NASA, Washington</p>	<p>1. Engines, Rocket (3.1.8) 2. Fuels - Rockets (Includes Fuel and Oxidant) (3.4.3.3) 3. Combustion - Rocket Engines (3.5.2.5) I. Gordon, Sanford II. Zeleznik, Frank J. III. Huff, Vearl N. IV. NASA TN D-132</p> <p>A general computer program for chemical equilibrium and rocket performance calculations was written for the IBM 650 computer with 2000 words of drum storage, 60 words of high-speed core storage, indexing registers, and floating point attachments. The program can carry out combustion and isentropic-expansion calculations on a chemical system that may include as many as 10 different chemical elements, 30 reaction products, and 25 pressure ratios. It calculates composition, temperature, pressure, specific impulse, specific impulse in vacuum, characteristic velocity, thrust coefficient, area ratio, molecular weight, Mach (over) Copies obtainable from NASA, Washington</p>
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number, specific heat, isentropic exponent, enthalpy,  
entropy, and several thermodynamic first derivatives.

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entropy, and several thermodynamic first derivatives.

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